

Citation for published version:

Raikova, S, Chuck, C, McManus, M, Allen, M, Yallop, M & Baena, S 2016, 'Exploring a range of UK seaweed species for the production of fuels and fertiliser'.

Publication date:
2016

Document Version
Publisher's PDF, also known as Version of record

[Link to publication](#)

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Exploring a range of UK seaweed species for the production of fuels and fertiliser



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1. Macroalgae

- Marine biomass has a higher photosynthetic efficiency (ca. 6–8 %) than terrestrial crops (ca. 1–2 %)¹
- Macroalgae are an abundant natural resource, and a promising feedstock for third-generation biofuels
- Promising source of novel fuel crops—no competition with agriculture and less areal constraint
- Numerous methods of processing to fuels: chemical, biological, thermochemical



Fig. 1: Common UK macroalga *Ascophyllum nodosum*

2. Hydrothermal liquefaction

- Hydrothermal liquefaction (HTL) is an inexpensive and energy-efficient thermochemical route to whole biomass conversion
- HTL is carried out using subcritical water (310–360 °C, 100–180 bar) as both a solvent and a reactant for the conversion of biomass to a range of products

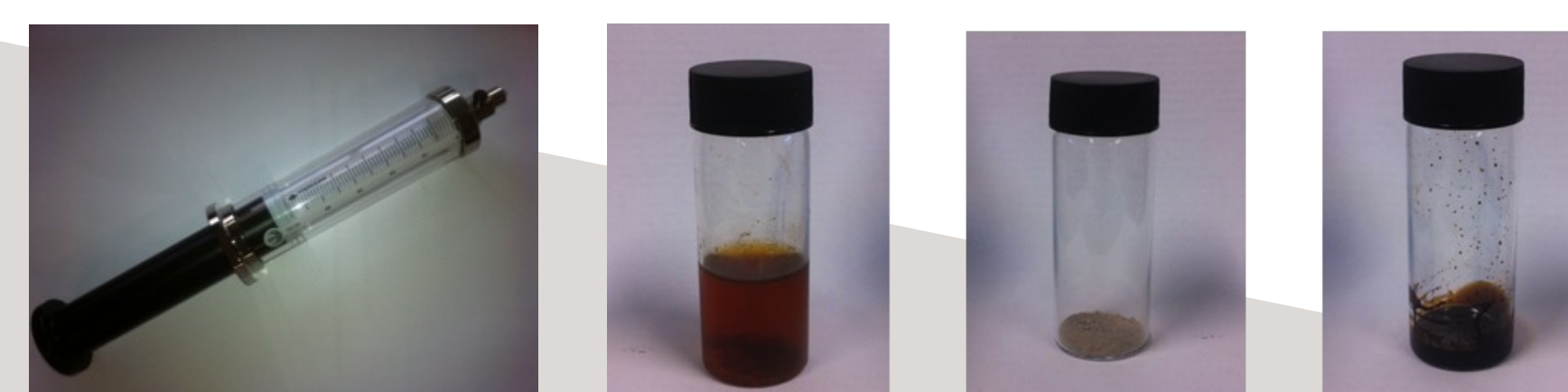


Fig. 2: HTL products. L to R: bio-gas, aqueous phase, bio-char and bio-crude oil

3. Biorefinery concept

All products generated via HTL can be used within a biorefinery to create value

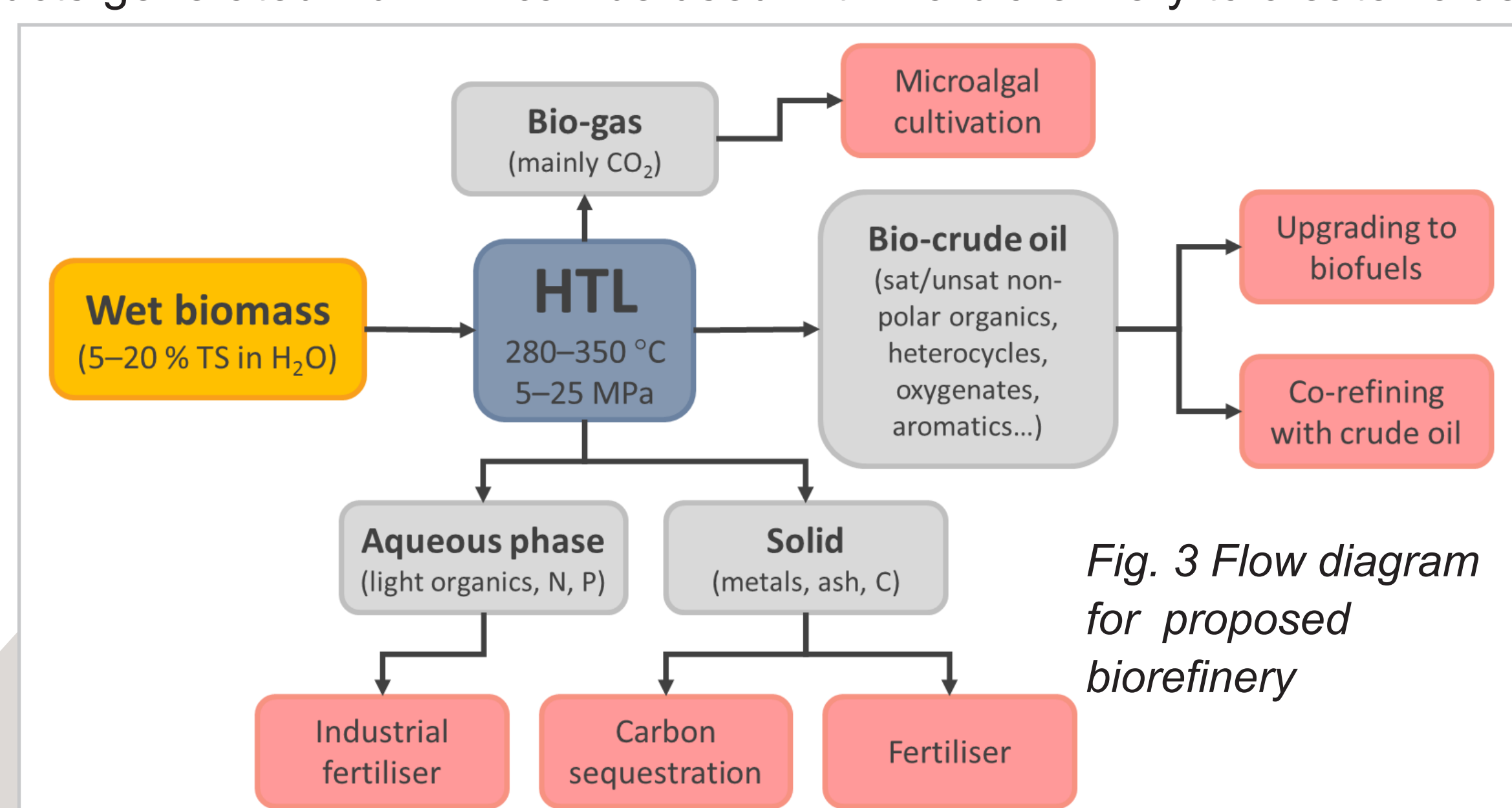


Fig. 3 Flow diagram for proposed biorefinery

Project aims

- Pinpoint HTL conditions for optimal energy and nutrient recovery using brown macroalga *Ascophyllum nodosum*
- Focus on maximising conversion to bio-crude oil and increasing ammonia and phosphate in aqueous products
- Screen a range of South West UK macroalgae for fuel production to build up a UK fuel and fertiliser production biorefinery design

4. System optimisation

- HTL was used to process the macroalga *Ascophyllum nodosum* in a batch system
- A range of temperatures between 300–350 °C was used, as well as a range of heating rates 5–60 °C min⁻¹
- The composition and properties of each product phase were examined



Fig. 4: Batch reactor set-up

5. Optimisation of HTL conditions

- Higher heating rates give higher bio-crude oil yields (literature precedent)²
- Higher processing temperatures give higher bio-crude yields
- No notable correlation between temperature and elemental composition or energy recovery in bio-crude oil
- Increasing temperatures improves ammonia recovery in aqueous product, but depletes phosphate

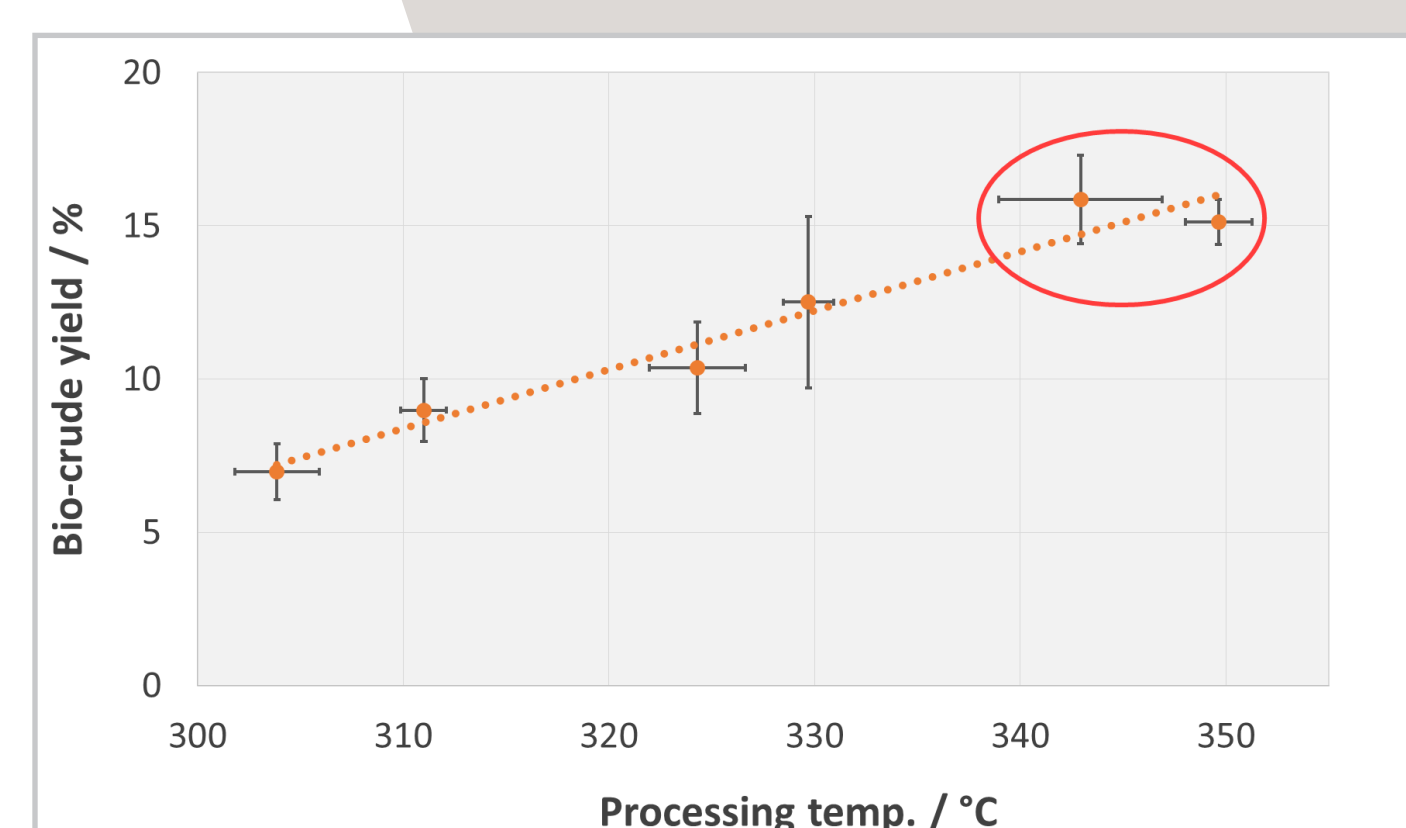


Fig. 5: Effect of temperature on bio-crude oil production

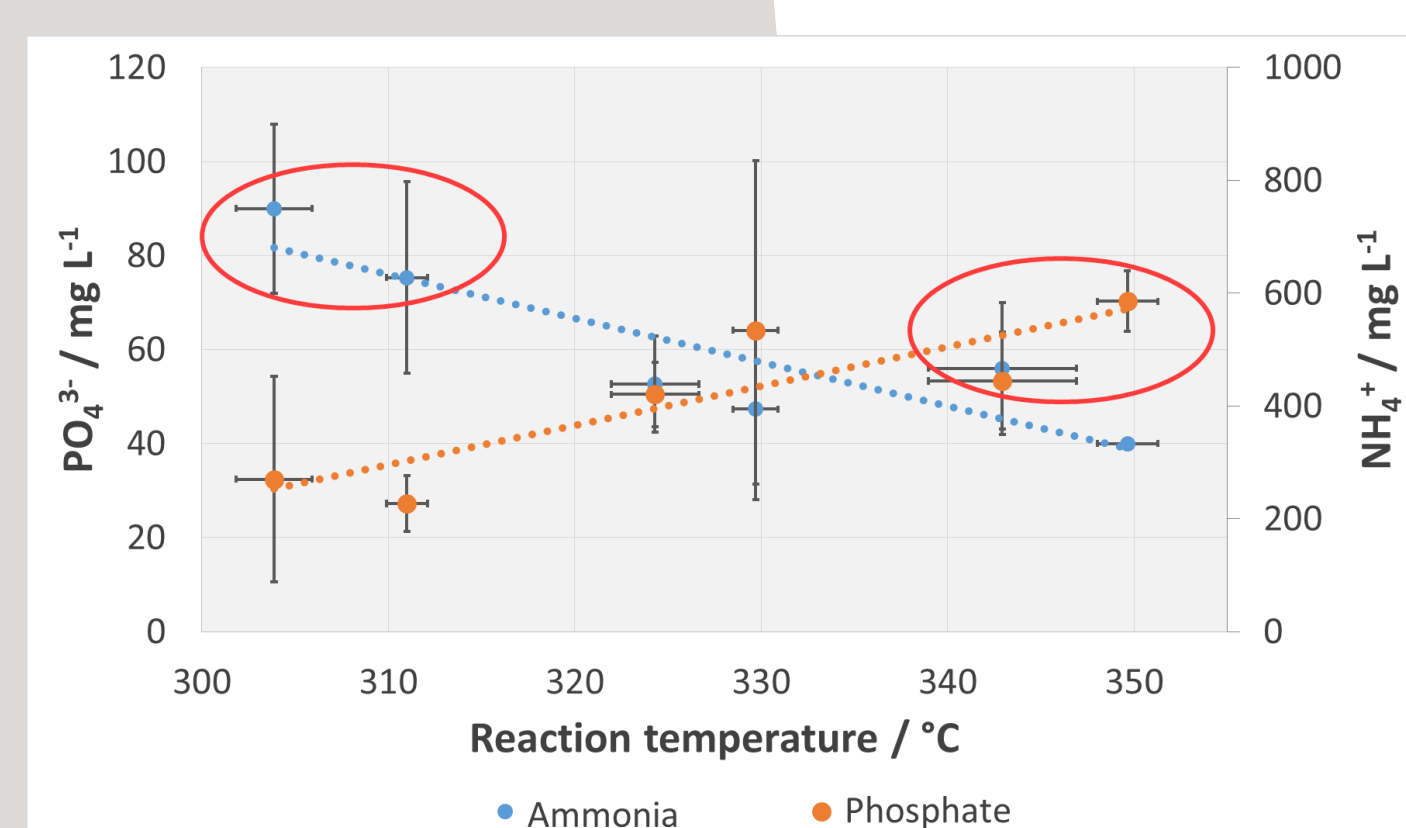


Fig. 6: Effect of temperature on ammonia and phosphate recovery in aqueous products

- From an economic standpoint, maximising bio-crude yields is more favourable – nutrient recovery will be a secondary valorisation route

Temperature	Heating rate
345 °C	ca. 30 °C min ⁻¹

Table 1: Final optimised HTL conditions

6. Species screening—early findings

- Optimised HTL conditions were used to process a range of South West UK seaweeds

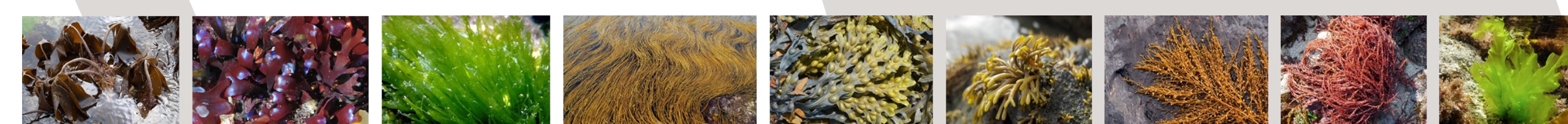


Fig. 7: Several of the macroalgae species used in HTL screening. (L to R: *L. hyperborea*, *C. crispus*, *U. intestinalis*, *H. elongata*, *F. vesiculosus*, *S. muticum*, *S. chordalis*, *U. lactuca*)

- Trends relating initial biomass composition to product distribution and properties were analysed

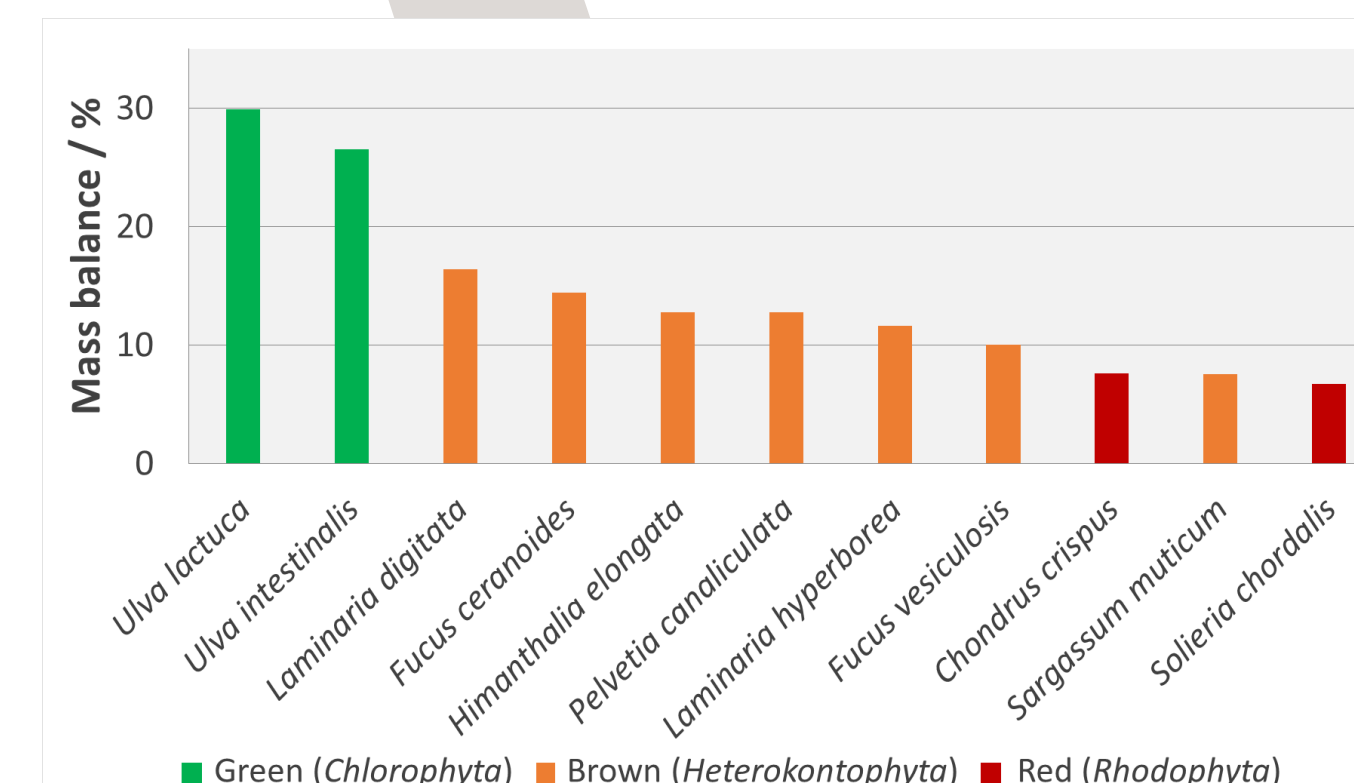


Fig. 8: Species effect on bio-crude recovery

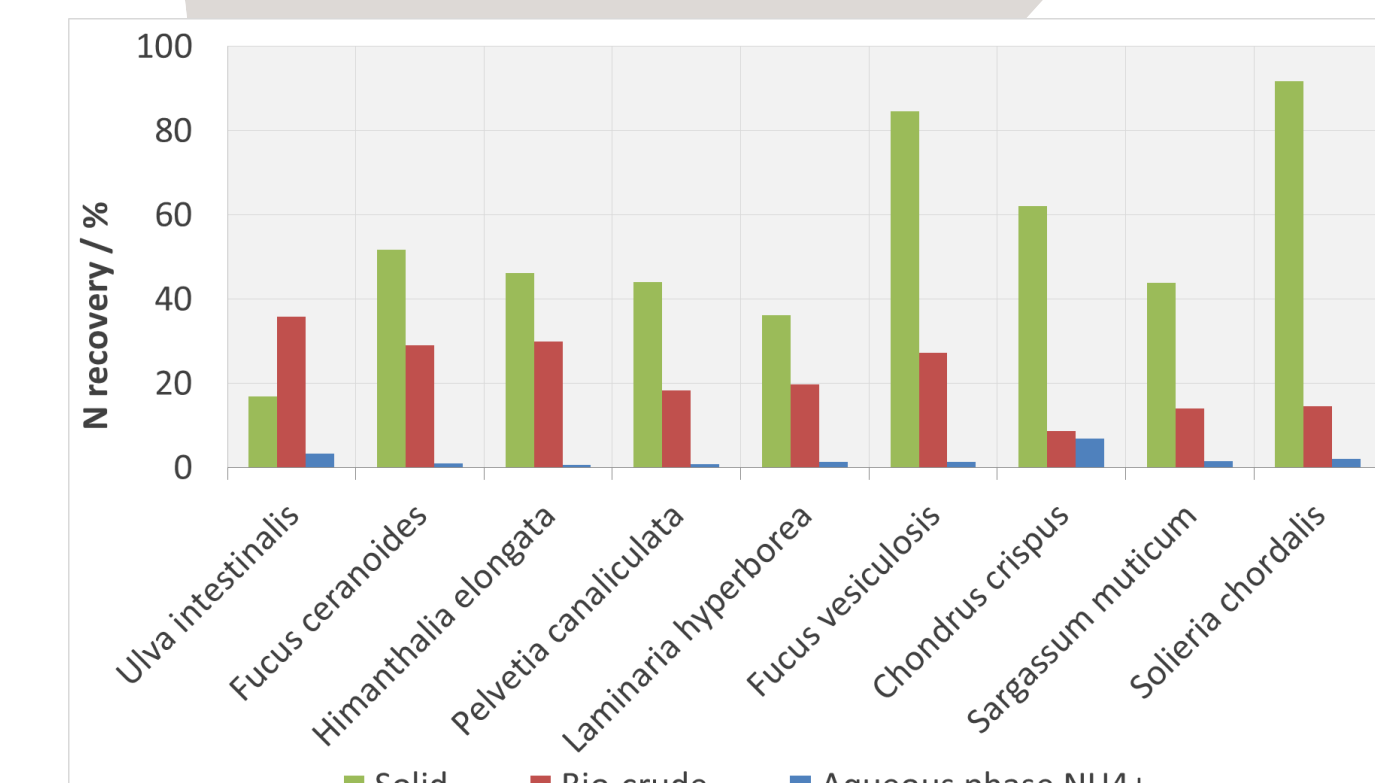


Fig. 9: Nitrogen recovery in product phases

- Green seaweeds (*Chlorophyta*) gave the highest yields of bio-crude oil (Fig. 8)
- Nitrogen from biomass proteins was found to accumulate preferentially in the solid residue, but high biomass protein content also resulted in some additional N partitioning to aqueous phase and bio-crude oil (Fig. 9)

7. Further work

- Further investigation of the complex relationship between biomass and product composition to rationalise reactivity
- Based on this, a set of specifications for an ideal biomass for the proposed biorefinery model will be laid out
- A theoretical biorefinery model will be built up, and a Life Cycle Assessment (LCA) carried out

References

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