

Wet Air Oxidation Treatment of Spent Caustic in Ethylene Plants and Petroleum Refineries

SAWEA

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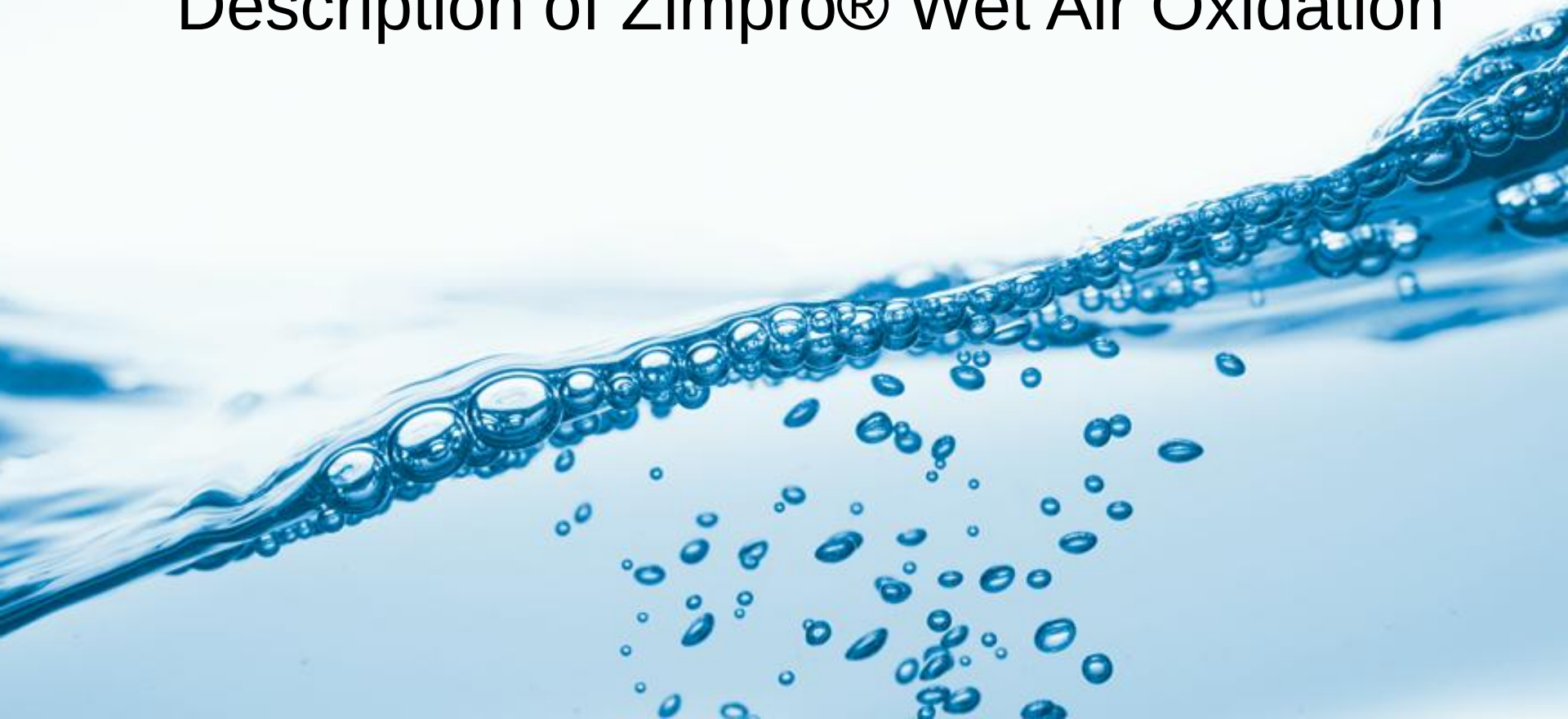
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Steven Olsen

Overview

- **Description of the Zimpro® WAO process**
- **Spent Caustic Chemistry**
- **Autoclave and Full Scale Data**
 - **Ethylene Spent Caustic**
 - **Refinery Spent Caustic**
- **Conclusions**

Description of Zimpro® Wet Air Oxidation



What is Wet Air Oxidation?

- Oxidation of Soluble or Suspended Components in an Aqueous Matrix
- Oxygen (Air) is the Oxidizing Species
- Oxidation Reactions Occur at Elevated Temperatures and Pressures



BASF, Port Arthur, Texas

Wet Air Oxidation For High Strength Industrial Wastewaters

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Repsol, Tarragona, Spain

Common Uses

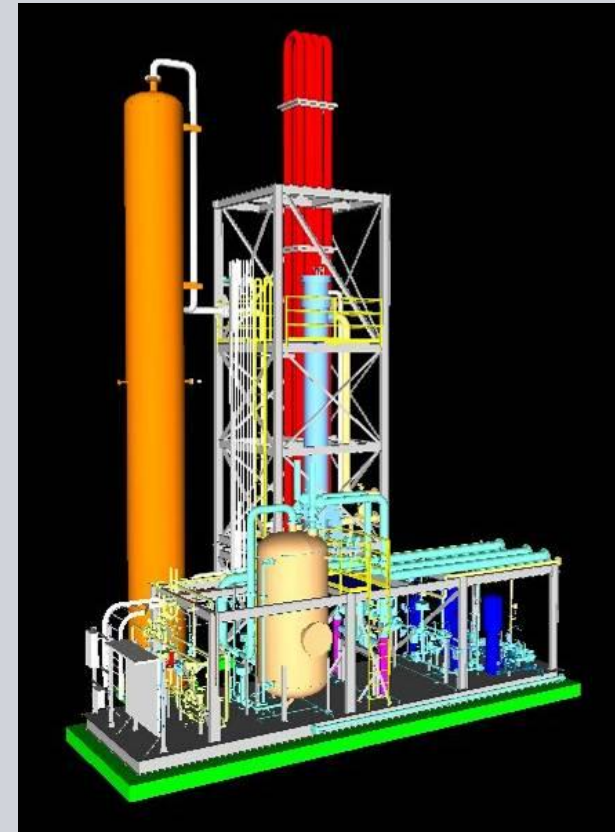
- Destruction of Specific Constituents
- Pretreatment for Biological Polishing
- Gross Reduction in COD Loading

Wet Air Oxidation For High Strength Industrial Wastewaters

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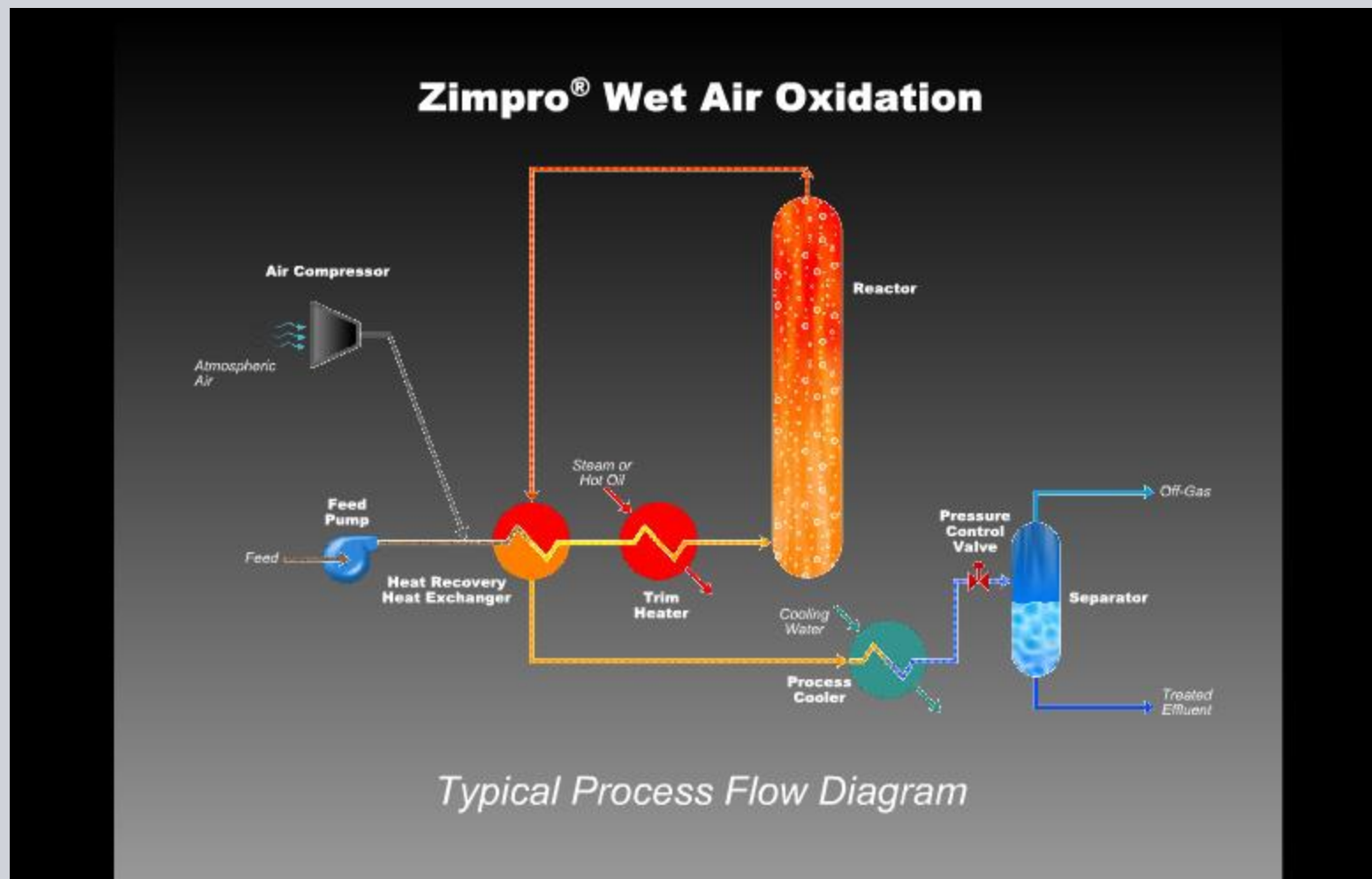
Typical Industrial Wet Air Oxidation Feed Characteristics

Flow Range:	1 to 50 m ³ /h
COD Range:	10,000 to 100,000 mg/L
Temperature Range:	150 to 320°C
Pressure Range:	5 to 225 barg



Wet Air Oxidation –Typical Process Flow Diagram

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Wet Air Oxidation

Process Variables

- Oxidation Temperature and Pressure
- Hydraulic Detention Time
- Oxidant – Typically Air or Oxygen
- Flow Configuration
- Oxidation Enhancer



Atofina, Rho Italy

Spent Caustic Chemistry



Classification of Spent Caustics

Type	Principle COD Source	Source	Operating Conditions
Sulfidic	Sulfides and/or mercaptans	Ethylene or LPG	130°C / 7 barg to 200°C / 27.5 barg
Cresylic	Phenolic compounds and reduced sulfur	FCC Gasoline Washes	200°C / 27.5 barg to 260°C / 86 barg
Naphthenic	Naphthenic compounds and reduced sulfur	Kerosene, Diesel, and Jet Fuel	240°C / 55 barg to 260°C / 86 barg

Issues With Spent Caustic Produced in the Petrochemical Industry

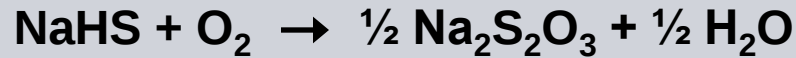


Spent Caustic
Before and After
WAO Treatment

- Odors caused by sulfides, mercaptans and volatile organics
- Potential inhibitory or toxic effects in biological treatment
- Hazards associated with toxicity
- High chemical oxygen demand
- Tendency to foam
- Corrosive

Sulfidic Reactions During WAO of Spent Caustics

Sulfide - NaHS



Thiosulfate - $\text{Na}_2\text{S}_2\text{O}_3$



Mercaptan - NaSR



Organic Reactions During WAO of Spent Caustics

Cresylic Acids - $\text{C}_6\text{H}_5\text{O-Na}$

- $\text{C}_6\text{H}_5\text{O-Na} + \text{O}_2 + \text{NaOH} \rightarrow \text{Na}_2\text{CO}_3 + \text{H}_2\text{O}$
- $\text{C}_6\text{H}_5\text{O-Na} + \text{O}_2 + \text{NaOH} \rightarrow \text{Na}_2\text{CO}_3 + \text{CH}_3\text{COO-Na} + \text{H}_2\text{O}$

Naphthenic Acids - $\text{Na-C}_{12}\text{H}_{22}\text{O}_2$

- $\text{Na-C}_{12}\text{H}_{22}\text{O}_2 + \text{O}_2 + \text{NaOH} \rightarrow \text{Na}_2\text{CO}_3 + \text{H}_2\text{O}$
- $\text{Na-C}_{12}\text{H}_{22}\text{O}_2 + \text{O}_2 + \text{NaOH} \rightarrow \text{Na}_2\text{CO}_3 + \text{CH}_3\text{COO-Na} + \text{H}_2\text{O}$

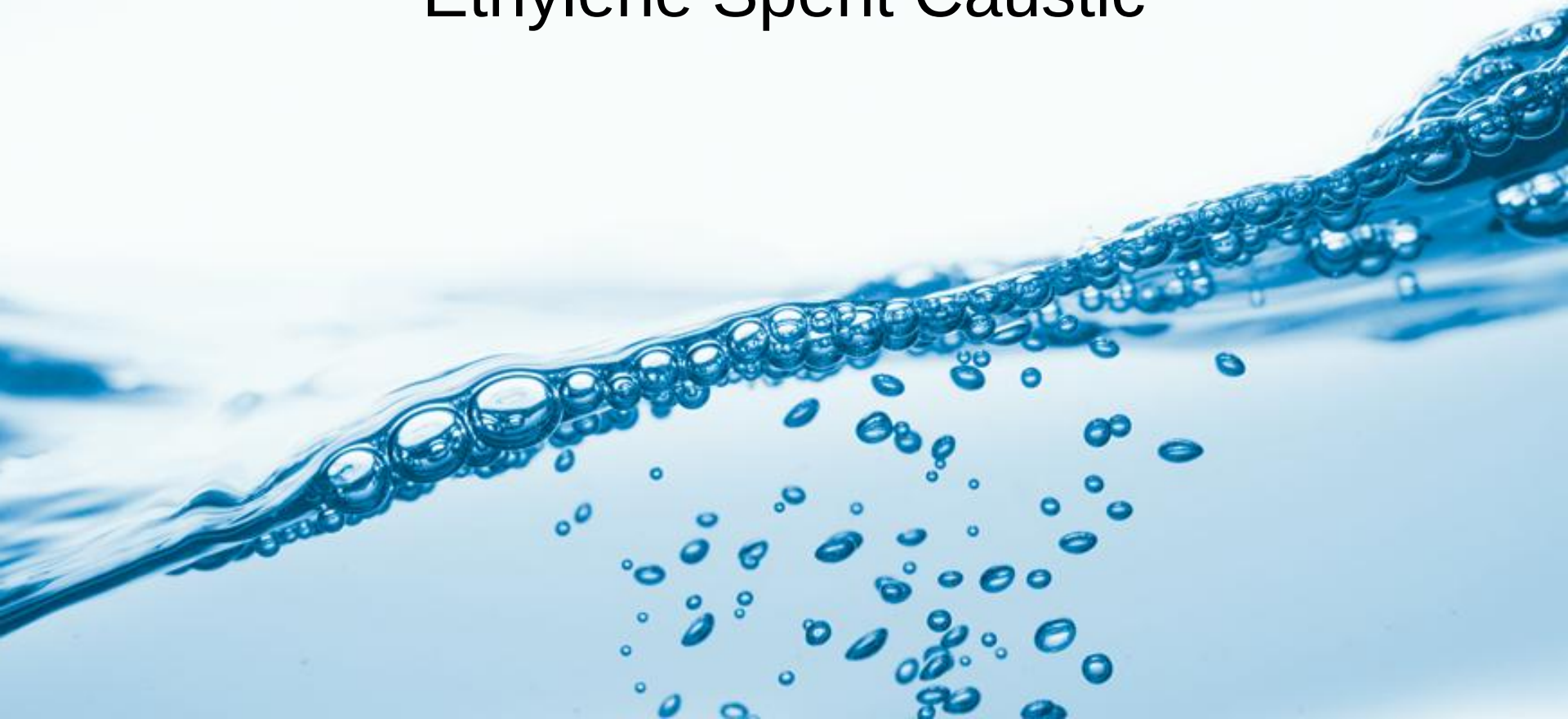
Autoclave and Full Scale Results



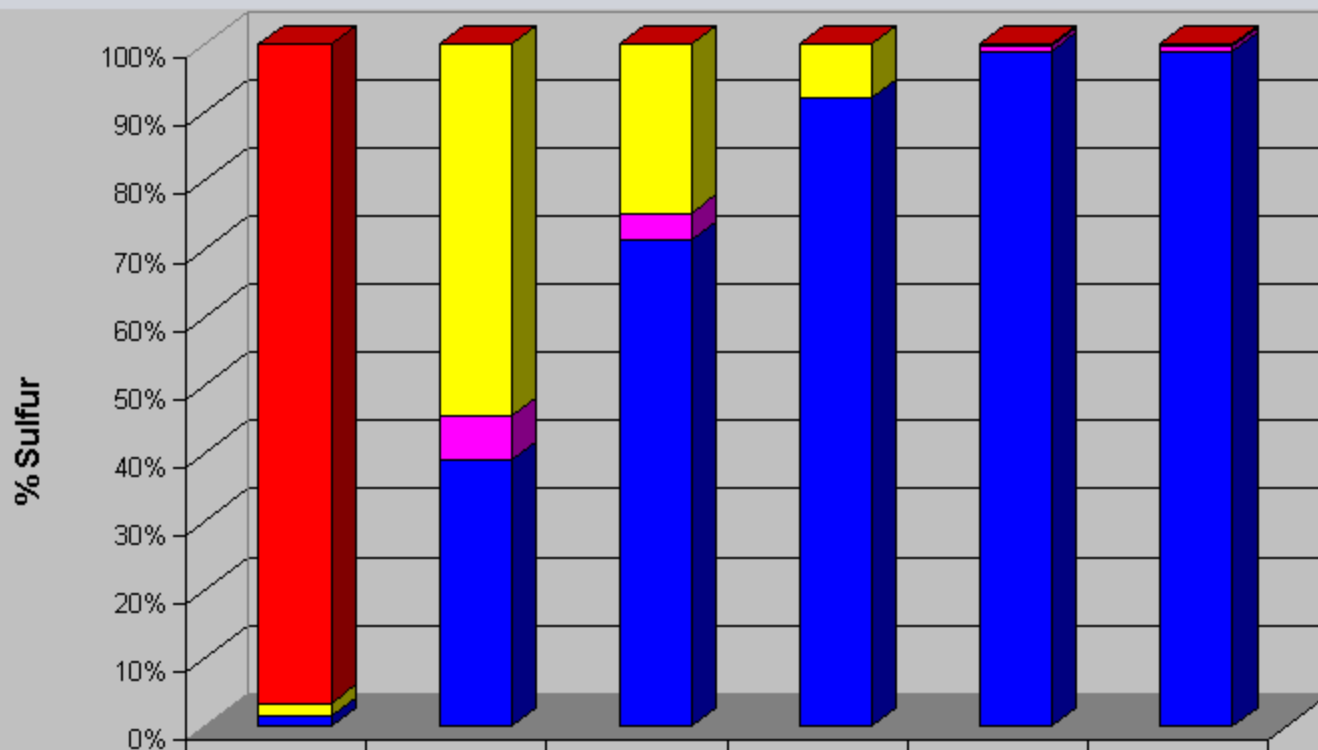
Autoclave and Full Scale Results

- **Oxidation of Sulfidic Components**
- **Biotreatability of WAO Effluent**
- **Overall COD Destruction**

Ethylene Spent Caustic



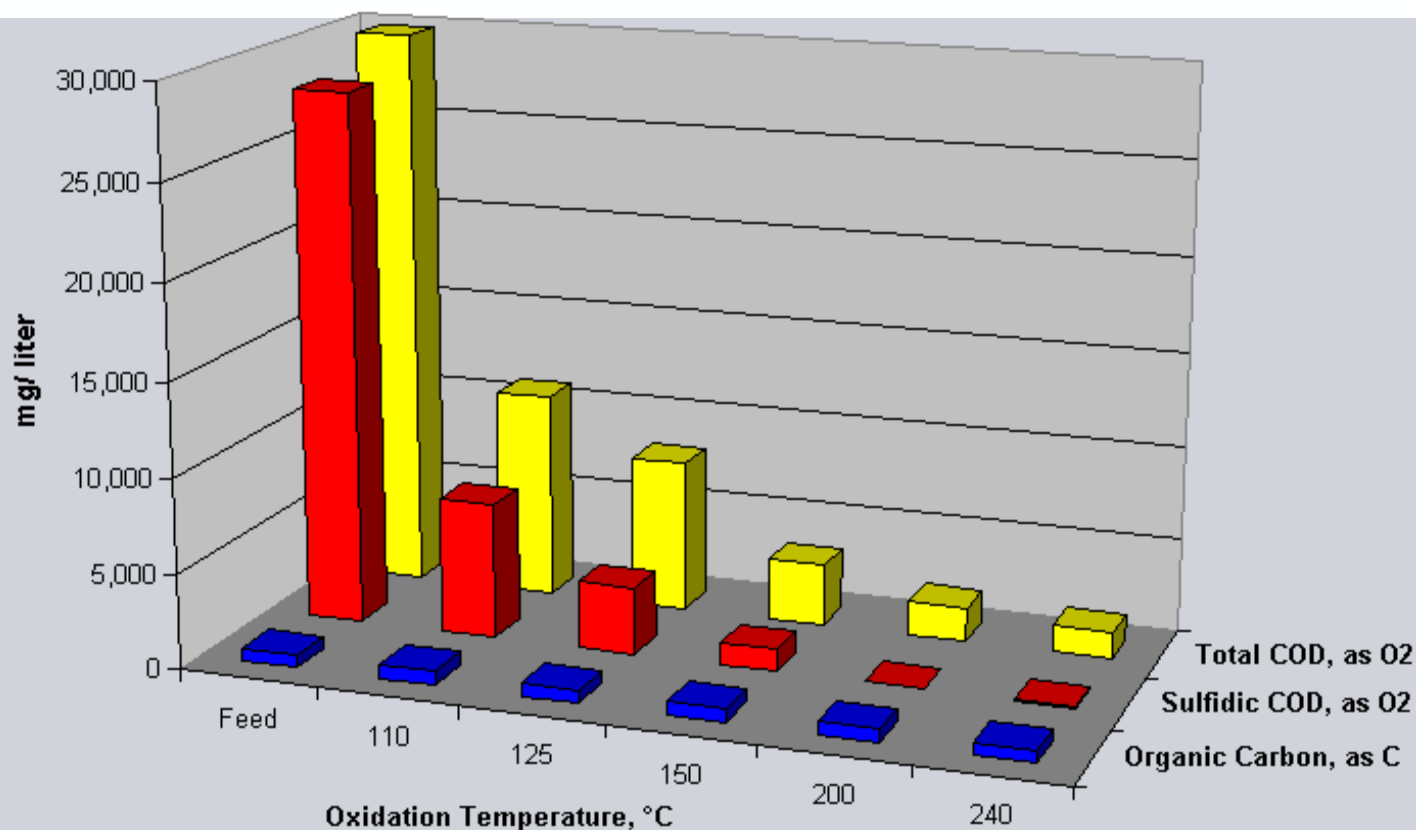
Wet Air Oxidation Ethylene Spent Caustic – Sulfidic Components



Oxidation Temperature, °C	Feed	110	125	150	200	240
■ Sulfide (NaHS/Na ₂ S as S)	13900	<10	<10	<10	<1	<1
■ Thiosulfate (Na ₂ S ₂ O ₃ as S)	275	5,503	2,686	949	40	31
■ Sulfite (NaSO ₃ as S)	5	643	435	4	81	85
■ Sulfate (Na ₂ SO ₄ as S)	200	3,940	7,740	11,200	12,500	11,100

Wet Air Oxidation

Ethylene Spent Caustic – Sulfidic / Organic COD



	Feed	110	125	150	200	240
■ Organic Carbon, as C	648	747	708	710	641	537
■ Sulfidic COD, as O2	28,085	7,184	3,567	1,185	90	80
■ Total COD, as O2	29,800	10,900	8,040	3,260	1,830	1,410

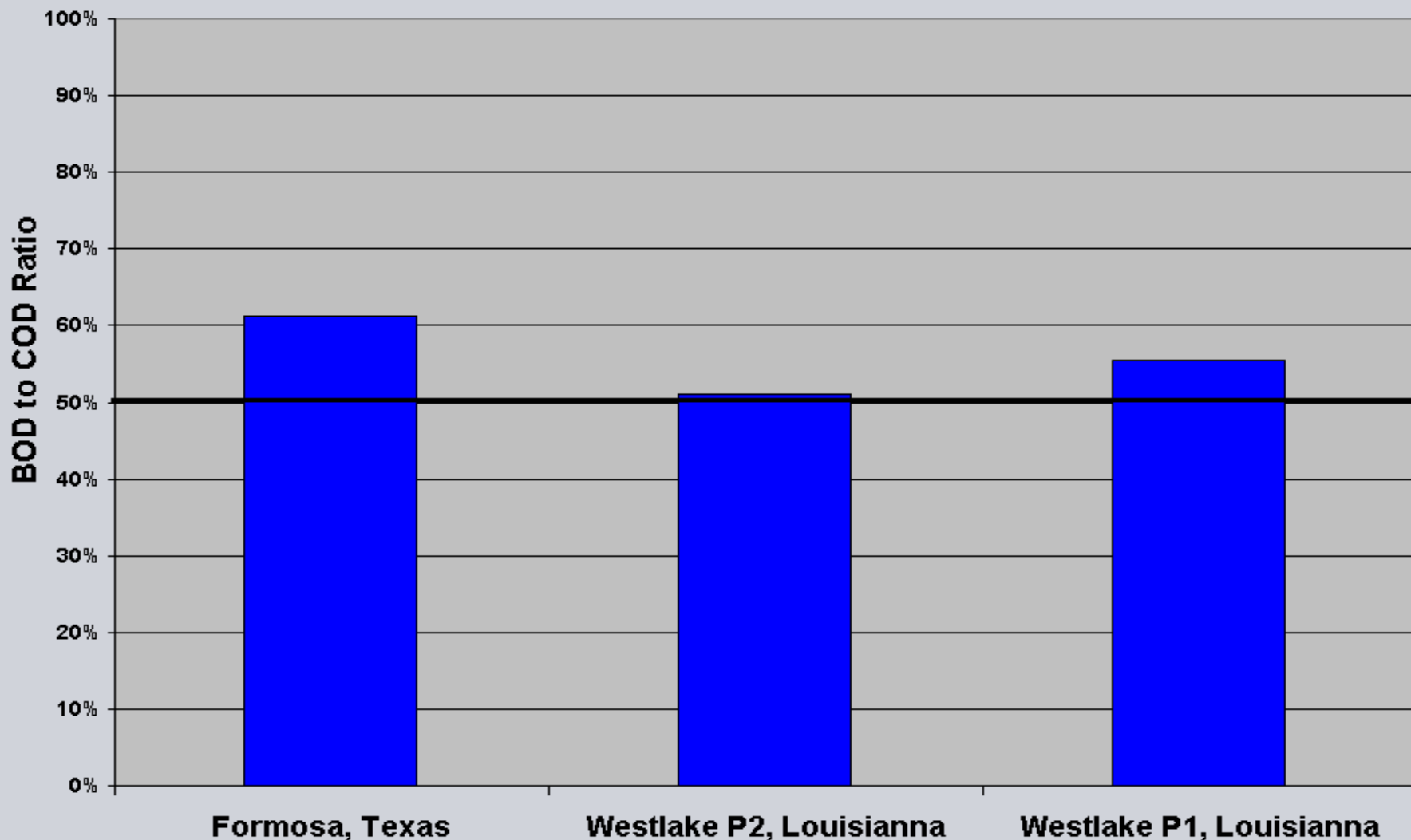
Full Scale WAO Case Studies

Ethylene Spent Caustic

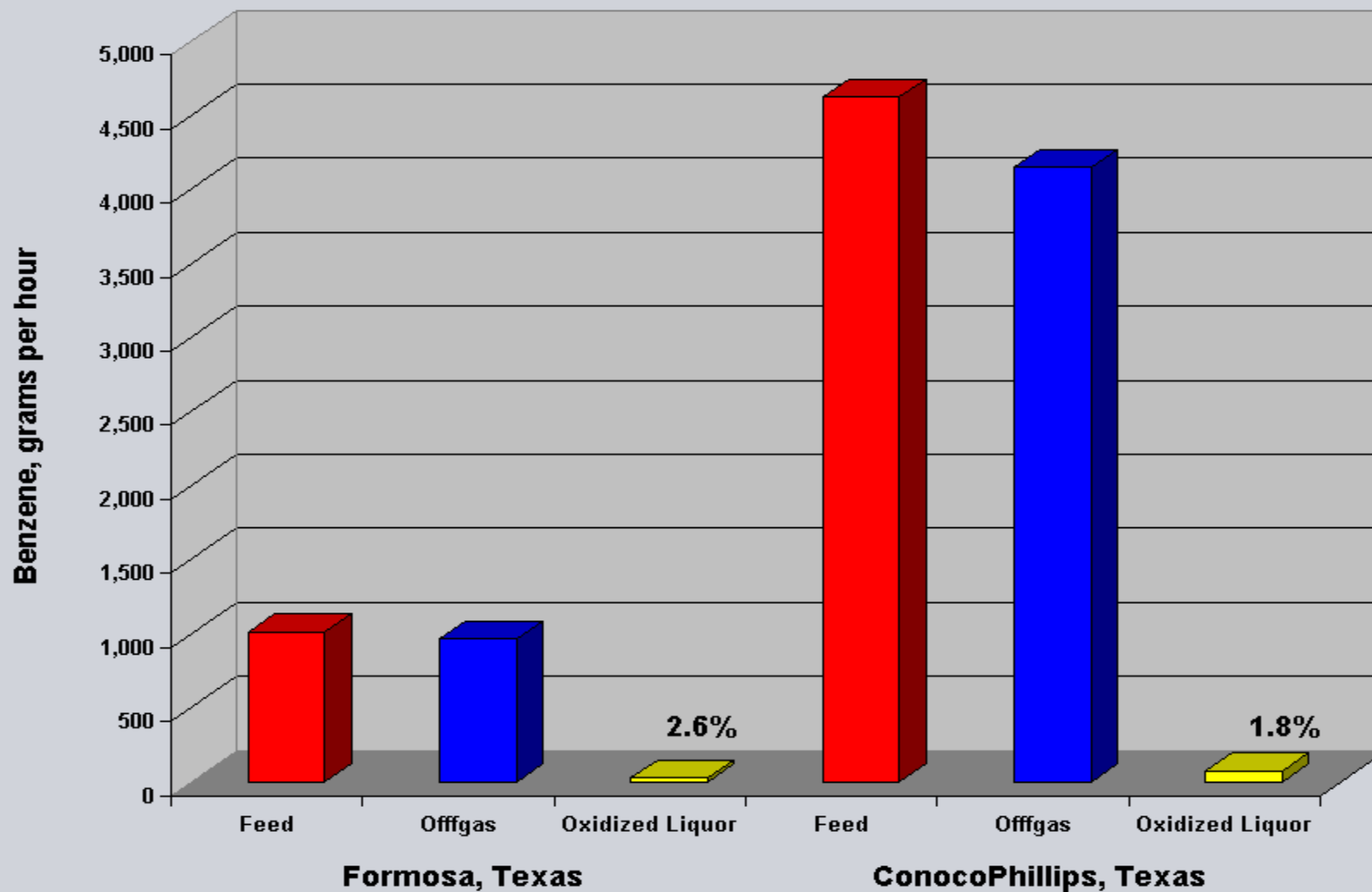


		ConocoPhillips, Texas		BASF, Texas	
		Feed	Effluent	Feed	Effluent
Temperature, °C			135		200
Residence Time, minutes			60		60
Analysis	Units				
COD	mg/L	10,500	2,300	11,700	2,870
Sulfide-S	mg/L	4,031	<1	4,990	<1
Thiosulfate-S	mg/L	<224	959	49	<16
Sulfite-S	mg/L	<64	204	28	10
Sulfate-S	mg/L	<55	2,940	507	5,190
Mercaptan-CH ₃ SH	mg/L	---	---	298	---
Methyl Mercaptan	mg/L	---	---	---	<0.4
Ethyl Mercaptan	mg/L	--	---	---	<0.4
Calculated Sulfidic COD	mg/L	8,060	1,300	10,500	<50
% Sulfidic COD Destruction	%	---	84	---	>99.5

WAO Ethylene Spent Caustic Biodegradability



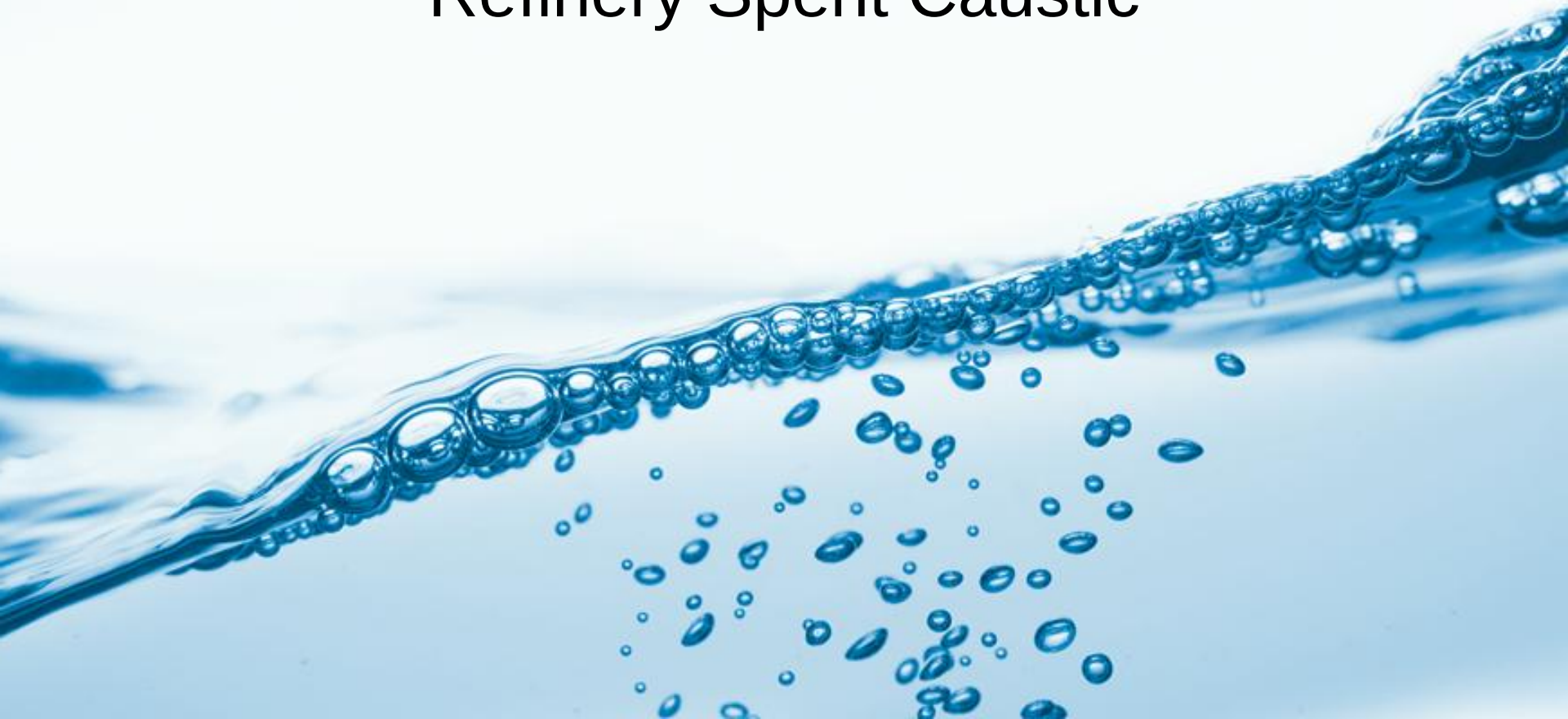
Benzene Stripping



WAO Ethylene Spent Caustic

- **Operation at 200°C**
 - **Sulfide < 1 mg/l as S**
 - **Mercaptan < 1 mg/l as Methyl / Ethyl**
 - **Thiosulfate < 100 mg/l as S**
- **Remaining Organic COD is Biodegradable**
 - **BOD to COD Ratio > 0.5**

Refinery Spent Caustic

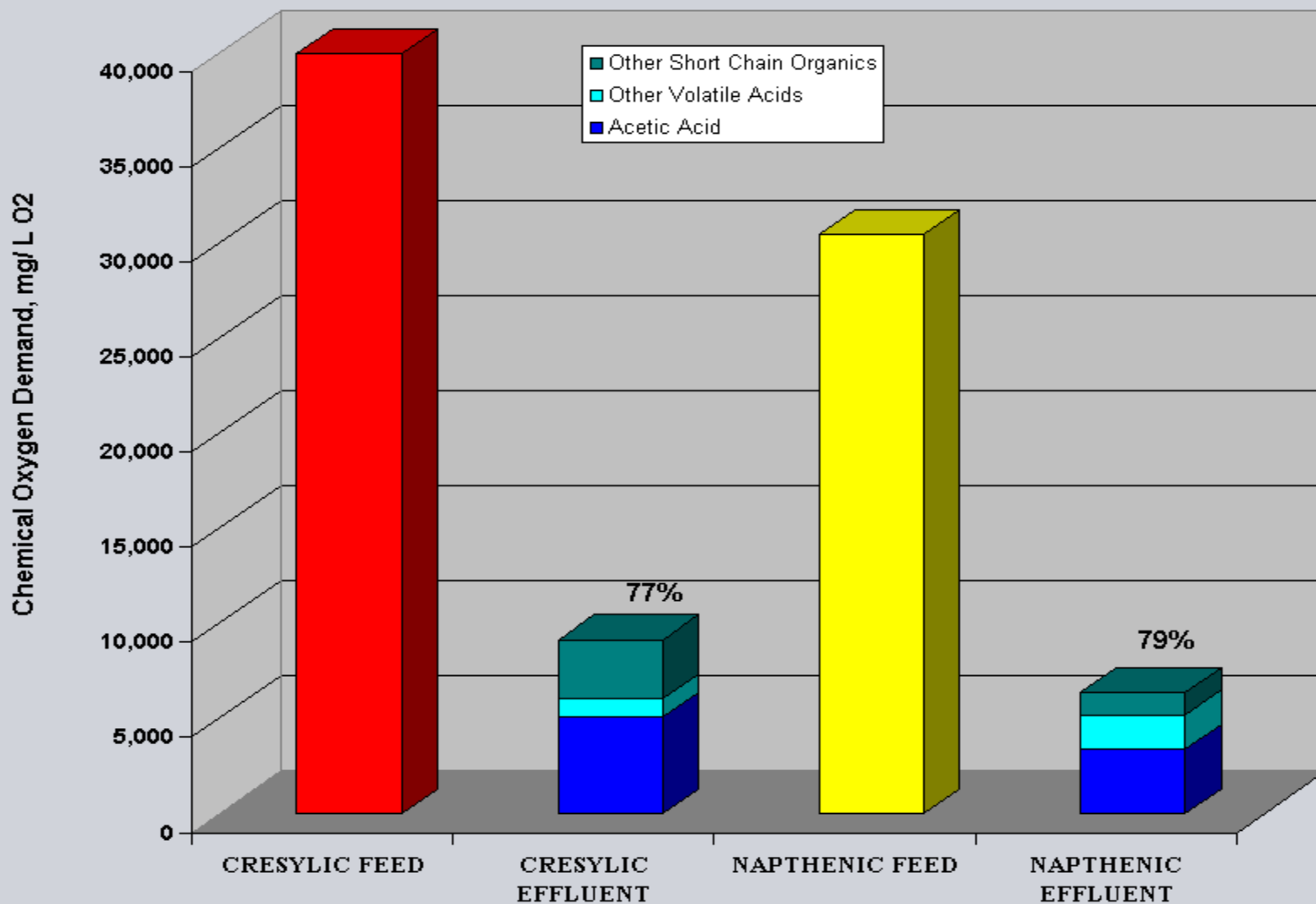


Wet Air Oxidation Refinery Spent Caustic

- Operating Conditions Dependent on Mixture Composition
- Assure Biological Treatability
- Sulfidic (LPG, etc) - 200°C / 27.5 barg
 - **Higher Mercaptan Content**
- Cresylic – 200°C / 27.5 barg to 260°C / 86 barg
 - **COD Reduction**
- Napthenic – 240°C / 55 barg to 260°C / 85 barg
 - **Prevent Foaming**

Wet Air Oxidation Organic Refinery Spent Caustic – 260°C

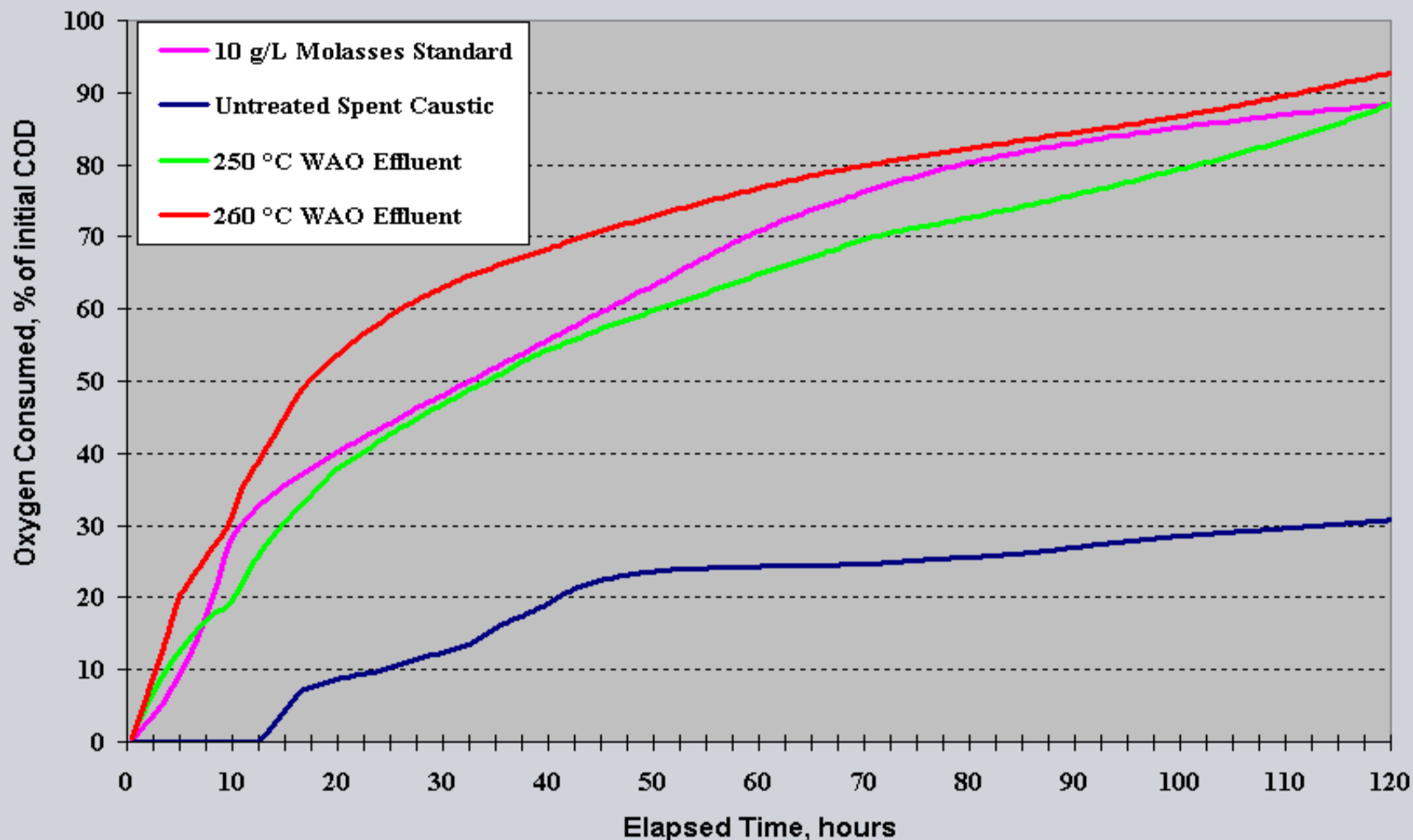
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Water Technologies

WAO of Napthenic Spent Caustic – Respirometer Trendplot



Full Scale WAO Study – Refinery Spent Caustic Mixture

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Repsol-YPF, La Pampilla, Peru

Repsol YPF Refinery

Spent Caustic Composition



	Sulfidic spent caustics	Naphthenic spent caustics	Cresylic spent caustics
COD as g/l	7 - 110	50 – 100	165 - 230
TOC, g/l as C	0.02 – 4	11 – 25	23 - 60
DIC, g/l as C	0.15 – 5	0 – 0.16	0.33 – 0.35
Sulfide, g/l as S⁼	2 – 53	< 0.001	0 - 64
Mercaptans, g/l as S⁼	0 – 28	< 0.03	0 – 5.4
Thiosulfate, g/l as S⁼	0 – 3.7	0.07 – 0.13	10 - 12
Total Phenols, g/l	0.003 – 0.02	2 – 10	14 - 20

Repsol YPF Refinery

Zimpro® WAO Performance



	Destruction	Feed	Effluent (measured, after dilution)
COD, mg/l as O ₂	85%	73,000	6,300
TOC, mg/l as C	73%	15,000	2,400
Sodium, mg/l as Na	-	41,000	24,000
pH	-	13.2	8.9
Sulfide, mg/l as S ⁼	> 99.9	8,500	< 1
Sulfite, mg/l as S ⁼	> 99.9	100	< 2
Mercaptans, mg/l as CH ₃ SH	> 98.8	1,500	< 30
Thiosulfate, mg/l as S ₂ O ₃	> 98.8	1,500	< 30
Total phenols, mg/l as C ₆ H ₆ O	> 99.6	6,500	36
Flow rate, m ³ /h		0.67	1.14

- **Biological Treatability**
 - **Effluent BOD/COD Ratio : 0.58**
 - **Volatile Acid COD: 4,150 mg/L**
 - **66% of Effluent COD**
- **Sulfidic Components Non-Detectable**
 - **Including Mercaptans**



Conclusions

- **Reasons For Treatment**
 - **Biotreatable Effluent**
 - **No Sulfide Odors**
 - **No H₂S emissions**
 - **Minimize Downstream Corrosion**
 - **Eliminate Foaming Problems**



Conclusions

- **Ethylene Spent Caustic (Sulfidic)**
 - **Sulfide <1 mg/l as S**
 - **Mercaptans <1 mg/l**
 - **Thiosulfate <100 mg/l as S**

Conclusions

- **Refinery Spent Caustic (Higher Temperature for Organics)**
 - **Elimination of Sulfides and Mercaptans**
 - **High Conversion of Complex Organics to Short Chain Compounds**
 - **Both Sulfidic and Organic COD Reduction**

Thank You!

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