# HYDROCARBON ENGINEERING

December 2022



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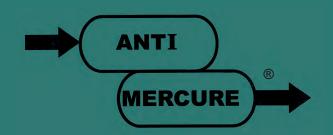
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**December 2022 Volume 27 Number 12 ISSN 1468-9340** 

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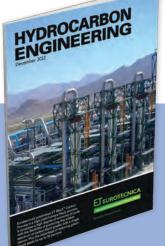
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# HYDROCARBON ENGINEERING



# **CALLUM O'REILLY SENIOR EDITOR**

his winter, the eyes of the world will be on Qatar; the hosts of the 2022 FIFA World Cup. The spotlight on this year's tournament has been a little more intense than usual, with a wide range of issues dominating the headlines. Allegations of corruption in the awarding of the tournament to Qatar back in 2010

have long dogged FIFA, and a number of other off-the-field controversies have cast a shadow over the competition, including human rights issues and concerns surrounding the tournament's sustainability pledges.

As the goals start to fly in, the column inches will swiftly move towards the football itself, but the sociopolitical issues surrounding this year's World Cup are likely to live on longer than the sporting achievements of the teams taking part.

Aside from the numerous controversies surrounding the tournament, the circumstances surrounding Qatar's rise to prominence are quite extraordinary, and the country's energy sector is at the heart of why it is capable of hosting one of the world's premier sporting festivals. A recent article in the *Financial Times (FT)* explored how Qatar's state-owned oil and gas group's bold bet on LNG transformed the country's fortunes and ultimately funded the majority of the new infrastructure (including a reported US\$6.5 billion on new stadia and facilities alone) required to host the World Cup.<sup>1</sup>

Qatar was highly indebted and heading towards bankruptcy in the early 1990s before QatarPetroleum (now known as QatarEnergy) decided to develop LNG for export from Qatar's North Field. The move was seen as a gamble – with BP pulling out of the project in 1992 over fears that it would not produce significant returns. In 1997, Qatar exported its first LNG to Spain, and the country became the world's biggest LNG exporter in 2006. However, the state group did not stand still. It maximised its domestic gas production for export and announced huge expansion plans in 2017. In so doing, it partnered with energy majors such as Shell and Total, who invited QatarEnergy to join their projects around the world. QatarEnergy has now built a global portfolio of exploration projects.

Saad al-Kaabi, Qatar's Energy Minister and Chief Executive of QatarEnergy, told the FT that the next chapter in the company's evolution will be focused on international expansion, with plans to increase its production outside of Qatar from 45 000 boe/d to 5000 000 boe/d by 2030. The company is also looking to diversify its assets. It is exploring new crude oil finds in countries such as Namibia, as well as investing in petrochemical production and solar energy in Qatar. The company recently announced that it is proceeding with the construction of an integrated polymers facility on the US Gulf Coast, in partnership with Chevron Phillips Chemical Co. LLC (more details about this project can be found on p. 5 of this issue). This diversification of assets was highlighted by the company's decision to change its name from QatarPetroleum last year, reflecting its new strategy to focus on energy efficiency and environmentally-friendly technology. However, as the piece from the FT points out, QatarEnergy has currently not set net zero emissions targets, and the company firmly believes that natural gas will be central to the world's energy transition. Al-Kaabi said: "I agree with going green, but I always say gas is not a transition fuel, it is a destination fuel."

QatarEnergy has amassed its fortune through a series of shrewd moves, and it will be interesting to see if it continues to thrive in a changing world.

 WILSON, T. and ENGLAND, A., 'QatarEnergy: the company behind World Cup host's wealth', Financial Times, (18 November 2022).



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# **USA | Chevron Phillips Chemical and QatarEnergy to construct polymers facility**

hevron Phillips Chemical and QatarEnergy have announced that they are proceeding with the construction of a US\$8.5 billion integrated polymers facility in Orange, Texas, US.

The companies have made a positive final investment decision (FID) on the project and created a joint venture (JV) company, Golden Triangle Polymers Company LLC.

Chevron Phillips Chemical owns a 51% equity share in the JV, and QatarEnergy owns 49%.

The plant, expected to begin operations in 2026, will produce Marlex® polyethylene. The project is targeting to have approximately 25% lower greenhouse gas emissions than similar facilities in the US and Europe.

Construction of the plant will begin immediately near Chevron Phillips Chemical's existing facility in Orange, located 113 miles east of Houston.

Chevron Phillips Chemical will manage engineering, procurement and construction for the project, and operate the facility after start-up.

# South Korea | S-OIL to build one of the world's largest petrochemical crackers

A ramco is making its biggest ever investment in South Korea to develop one of the world's largest refinery-integrated petrochemical steam crackers through its S-OIL affiliate.

The US\$7 billion Shaheen project aims to convert crude oil into petrochemical feedstock and would represent the first commercialisation of Aramco and Lummus Technology's TC2C thermal crude to chemicals technology, which increases chemical yield and reduces operating costs. It follows an earlier US\$4 billion

investment into the first phase of the petrochemical expansion, completed in 2018

Located at S-OIL's existing site in Ulsan, the new plant is planned to have the capacity to produce up to 3.2 million tpy of petrochemicals, and include a facility to produce high-value polymers. The project is expected to start in 2023 and be completed by 2026.

The steam cracker is expected to process byproducts from crude processing, including naphtha and off-gas, to produce ethylene.

# UK|Wood appointed as integrated services partner for Centrica Storage

Wood has been appointed as integrated services partner by Centrica Storage for the company's UK Southern North Sea operations.

The five-year contract includes the provision of engineering, procurement and construction solutions, operations and maintenance services, as well as project management services for the Rough gas field and the Easington Gas Terminal in East Yorkshire, England.

Rough, the UK's largest natural gas storage site, was recently reopened to help bolster the UK's energy security. Wood has been deploying its experience in brownfield modifications to support the significant engineering designs and modifications required to enable the facility to store up to 30 billion ft<sup>3</sup> of gas ahead of this winter.

Wood's scope also includes working with Centrica Storage to support its ambition to drive the UK's clean energy transition by redeveloping Rough into the world's biggest hydrogen storage facility. To support the successful delivery of this contract, Wood will expand its engineering office in Hull, securing highly-skilled jobs for around 100 local people.

# Indonesia | Pertamina NRE and ACWA Power to support Tuban refinery

Pertamina New & Renewable Energy (Pertamina NRE) and ACWA Power have signed a joint development agreement (JDA) for core utilities supply to the Tuban grassroot refinery and petrochemical (GRR&P) project.

The scope of the JDA comprises power generation with a capacity of 575 MW, steam generation with a capacity of 3288 tph, and a water desalination plant with capacity of 12 000 tph, all to supply the Tuban GRR&P project. Located in Tuban, Indonesia, this is one of the country's national strategic projects aimed at building national energy security and advancing the domestic petrochemical industry.

As a subsidiary of Pertamina, Pertamina NRE is at the forefront of building green businesses and developing decarbonisation initiatives.

ACWA Power has a mission to reliably deliver electricity and desalinated water at a low cost, thereby contributing to the sustainable, social and economic development of communities and countries.



# **DIARY DATES**

#### 6 - 7 December 2022

15<sup>th</sup> Annual National Aboveground Storage Tank Conference & Trade Show

The Woodlands, Texas, USA www.nistm.org

# 6 - 7 February 2023

#### **NARTC**

Houston, Texas, USA www.worldrefiningassociation.com/nartc23

#### 20 - 23 February 2023

**Laurance Reid Gas Conditioning Conference** Norman, Oklahoma, USA pacs.ou.edu/lrgcc

#### 19 - 23 March 2023

#### **AMPP Annual Conference & Expo**

Denver, Colorado, USA ace.ampp.org

#### 08 - 12 May 2023

#### RefComm

Galveston, Texas, USA events.crugroup.com/refcomm

#### 07 - 08 June 2023

#### Valve World Americas Expo & Conference

Houston, Texas, USA www.valveworldexpoamericas.com

#### 07 - 08 June 2023

#### **Downstream 2023** Texas, USA

events.reutersevents.com/petchem/downstream-usa

#### 13 - 15 June 2023

#### **Global Energy Show**

Calgary, Alberta, Canada www.globalenergyshow.com

#### 10 - 13 July 2023

#### LNG2023

Vancouver, British Columbia, Canada www.lng2023.org

# 05 - 08 September 2023

## Gastech

Singapore www.gastechevent.com

# 26 - 28 September 2023

#### **Turbomachinery & Pump Symposia**

Houston, Texas, USA tps.tamu.edu

# **USA** | Sempra announces partnership with ConocoPhillips

Sempra has announced that its subsidiary, Sempra Infrastructure, and ConocoPhillips have executed a 20-year Sale and Purchase Agreement (SPA) for 5 million tpy of LNG from Phase I of the proposed Port Arthur LNG project that is under development in Jefferson County, Texas, US.

The parties have also entered into an equity sale and purchase agreement whereby ConocoPhillips will acquire 30% of the equity in Phase 1 of Port Arthur LNG, and a natural gas supply management agreement whereby

ConocoPhillips will manage the feed gas supply requirements for Phase 1 of the proposed liquefaction facility.

Sempra Infrastructure recently announced that it is expecting to make a final investment decision (FID) for Phase 1 of the liquefaction project in 1Q23. Additionally, it has finalised an engineering, procurement and construction (EPC) contract with Bechtel Energy for Phase 1, whereby Bechtel will perform the detailed EPC, commissioning, start-up, performance testing, and operator training activities.

# Asia | Vopak and Petronas sign CCS MoU

Vopak and Petroliam Nasional Berhad (Petronas) have signed a Memorandum of Understanding (MoU) for the development of the CCS value chain in the Southeast Asia region.

As part of the MoU, both companies will jointly study the development of the value chain, focusing on the carbon dioxide (CO<sub>2</sub>) emitted by industries in Singapore. This includes CO<sub>2</sub> transport from a Vopak terminal for potential injection into the regional storage hubs developed by Petronas.

The aggregation of  $\mathrm{CO}_2$  emissions from various emitters in the region is also part of the feasibility study. Both companies have the intention to invest in the development of CCS value chain solutions.

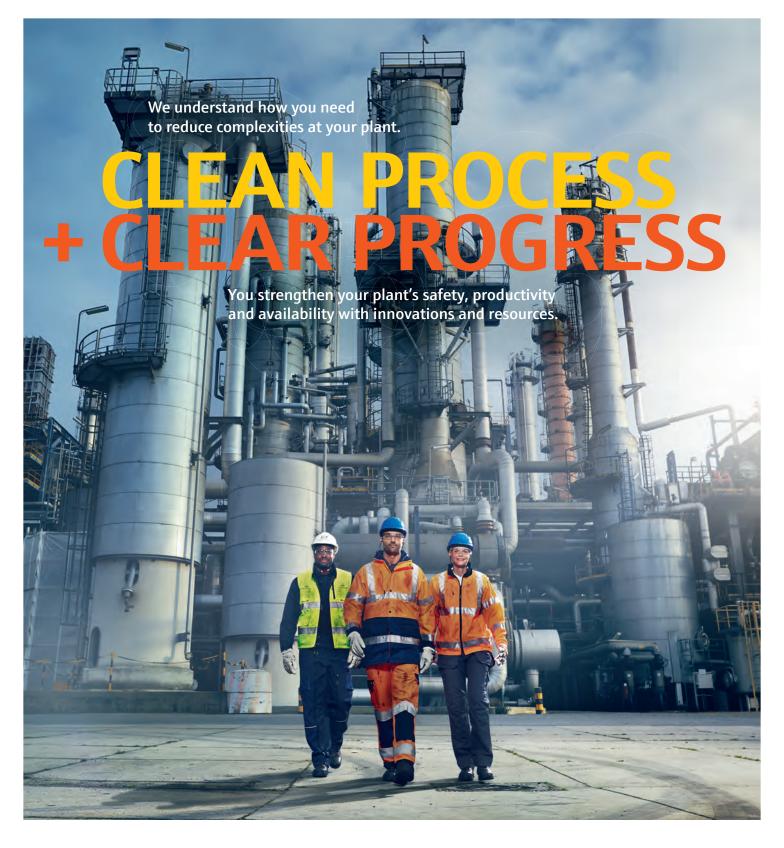
Chris Robblee, President Vopak Asia & Middle East, said: "We are excited about this project with our long-term partner Petronas to jointly collaborate. This is well aligned with our commitment to support the energy transition through development of CO<sub>2</sub> infrastructure for sustainable energy solutions and the decarbonisation of the industry."

# **USA** | Chart Industries to acquire Howden

hart Industries Inc. has signed a definitive agreement to acquire Howden – a leading global provider of mission critical air and gas handling products and services – from affiliates of KPS Capital Partners LP for a purchase price of US\$4.4 billion.

The acquisition, which is subject to the receipt of certain regulatory approvals and the satisfaction of other customary closing conditions, is expected to close in 1H23. It will result in an estimated combined revenue of US\$3.4 billion, based on the trailing 12 months as of 31 August 2022.

Jill Evanko, Chart's CEO and President, said: "The offerings of Chart and Howden are highly complementary, bringing multiple cost synergies, commercial synergies and efficiencies in the first year, along with significant aftermarket, service and repair exposure, which lifts the margin profile of the combined business, adds resiliency and broadens our end markets."



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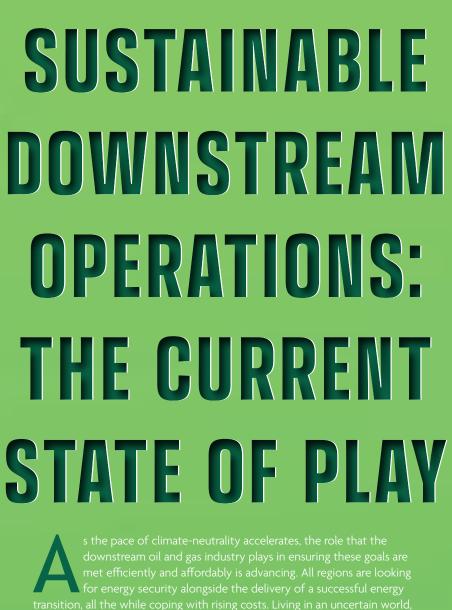
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**Stefan Chapman and Miro Cavkov, Euro Petroleum Consultants (EPC),** detail the role of downstream operations in promoting sustainability within the energy sector.





s the pace of climate-neutrality accelerates, the role that the downstream oil and gas industry plays in ensuring these goals are met efficiently and affordably is advancing. All regions are looking for energy security alongside the delivery of a successful energy transition, all the while coping with rising costs. Living in an uncertain world the energy sector is now faced with the complex pressures of balancing security and growth with decarbonisation. In this ever-changing environment, the downstream industry is also evolving, with boundaries between upstream, midstream, downstream and power becoming blurred. Whether it is reduce, recycle or remove, success will be defined by clear, significant and concrete targets.

Historically, the downstream oil and gas sector has always been considered a sustainability driver in terms of being an energy security supplier and a major provider of petroleum derivatives and products. Today, refining technologies have enabled producers to operate assets efficiently and reliably, where each drop of crude oil and each group of molecules is managed, almost eliminating lower-value products. The result is visible, and modern life simply would not be what it is today without the support of the downstream oil and gas industry. The majority of transportation – whether personal, commercial, by land, sea, air or rail – relies on liquid or gaseous fuels, produced by the downstream sector. This is also the case for petrochemical products, which facilitate our daily lives and touch every industry: health, communications, construction, etc.

Demand drives the market, and susequently production. Technology innovations from the last few decades have provided endless possibilities, most of which were unimaginable just a century ago. However, fossil fuels are not renewable and at some point crude output will begin to decrease. Predictions clearly show this trend — even if it will take some time. So, in truth, the current energy transition agenda is not just a technology issue, but

rather a global sustainability plan, whereby achieving climate goals (on time) will be crucial for future generations, and will need to be balanced with the increasing global energy demand.

# Downstream assets: an essential part of the solution

The question is: how can today's refineries play an integral role in reaching climate goals? Downstream producers have been proactive in looking at ways to reduce their environmental footprint, whilst being key energy providers and remaining competitive in difficult conditions. Each asset or complex should be treated individually – there is no 'silver bullet' solution that is applicable to every facility. The first step for all major refiners and petrochemical and chemical companies is to improve present operations by increasing energy efficiency and reliability, and reducing current emission levels from existing facilities. Reaching these 'low hanging fruit' is a priority.

Other routes are being evaluated, such as further refining and petrochemical integration opportunities, and diversification by way of co-processing with bio-feedstocks, and the implementation of plastic recycling technologies. In reality, the world is still heavily reliant on mid-distillates and diesel, even in a declining market, and this has to be balanced

with climate regulations that are being introduced, where Scope 1, 2 & 3 emissions will be part of the benchmark for success.

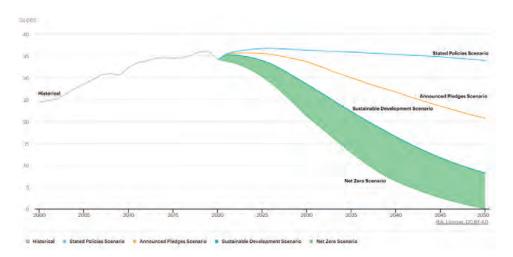
In order to remain competitive and meet changing demands, operators must adapt their existing assets in a sustainable way, requiring extra production and technology flexibility. As an example of this, the most used liquid fuels worldwide are gasoline, diesel, jet and marine fuel, and these can now be produced from sustainable feedstock — either 100% sustainable, or as a blend with conventional feedstocks.

Currently, there is general interest in hydrotreated vegetable oil (HVO) and bioethanol, since these fuels (or components) can be designed in such a way that they can be a drop-in solution, meaning that internal combustion engine (ICE) powered vehicles will not require any interventions in order to run on these sustainable and blended fuels.

There is clear evolution in the field, with the elimination of issues from first-generation biofuels. Newer generations have great cold filter plugging point (CFPP) standard properties, which have unlocked a major new opportunity: sustainable aviation fuel (SAF). Sustainable fuel technologies are available, scaled up, and will be ready to meet future demand. In terms of implementing these new technologies, the question that operators face is whether it is better for them to be the front runners or the fastest followers. Each company needs to

weigh up the pros and cons of this.

Producers are having to balance securing their business and remaining competitive whilst looking to reshape the downstream industry into a lower-carbon model – and this is no easy task. An added difficulty is that even in a disrupted oil market, renewable feedstocks and fuels remain less cost competitive when compared to their fossil counterparts. In this case, businesses and society have to understand that the sustainable and renewable future we are aiming for will have different dynamics and different variables, compared to the traditional forms of energy.



**Figure 1.** CO<sub>2</sub> emissions in the IEA's World Energy Outlook 2021 scenarios: 2000 – 2050.

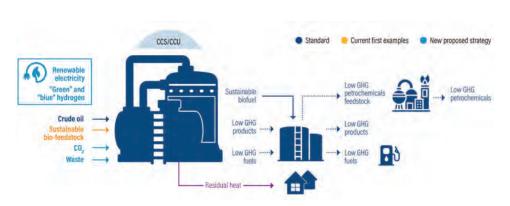


Figure 2. Concawe's conceptual low-carbon refinery, feedstock and products in 2050.

# Hydrogen: the designated game changer

Hydrogen, especially green, has been touted as the 'Holy Grail' of the sustainability journey – a major decarbonisation medium and possibly the ultimate solution. This can be seen in many high-level industry



# **SBW Group** Seven Decades of Progress

In 1960, SBW manufactured their first own-design centrifugal compressor in the original Shenyang factory (background image).

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1979 – Olefin plant compressors (115 000 tpy)

1982 - Ammonia/urea plant (520 000 tpy)

1989 – Hydrocracker compressor (800 000 tpy)

2003 – Axial/centrifugal ASU compressor (40 000 nm³/hr oxygen)

2010 - First PTA plant compressor (600 000 tpy)

2011 - High-thrust reciprocating compressor (125 t thrust)

2017 - Air separation for 100 000 nm<sup>3</sup>/hr oxygen



2021 – PDH plant, 900 000 tpy (world's largest using Lummus-process) DMCL1706+2MCL1707



2021 – first 1.4 million tpy Olefin plant (74 MW cracked gas; 39 MW propylene; 24 MW ethylene) CNPC Guangdong

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discussions, current investments, and potential projects. However, as aforementioned, a successful future energy mix will be a combination of several alternative energy solutions.

In the case of hydrogen, there remain a number of hurdles to overcome. These include the scalability of green hydrogen production, existing and future infrastructure, market demand, consumer willingness, and the ability to cope with the energy transition. Scaling up of electrolysers is already underway, confirmed by Norway's HydrogenPro project – the largest industrial electrolyser built so far, with a diameter of 2 m. Additionally, there is Germany's 24 MW installation in the Leuna facility, and the 8.75 MW PEM electrolyser in Wunsiedel.

Western Europe is very much at the forefront in terms of green hydrogen production. Many countries are investing and developing infrastructure to allow for further implementation. Building sustainable infrastructure is critical, and reliable government and EU regulations are required for its successful implementation.

Europe already has a strong gas transmission network, which could potentially be used in certain circumstances. However, these existing pipeline networks have been designed to transport natural gas, and so simply switching to 100% pure hydrogen is not possible, as hydrogen can easily diffuse through metal surfaces. Additionally, hydrogen is a much smaller molecule than methane in natural gas, which means that leakage rates though pipeline walls and joints may be greater, resulting in increased safety concerns and economical issues. Certain metal pipes used for transporting natural gas may also degrade over time when exposed to hydrogen, especially in the presence of high temperatures and pressures.

However, if blending of hydrogen and natural gas is considered then these networks could potentially become an option. Of course, complex engineering challenges remain in the repurposing of existing networks, in order to safely transport natural gas blended with hydrogen through more than 200 000 km of transmission pipelines across 2 million km of distribution network that has over 20 000 compressor and pressure reduction stations in Europe.

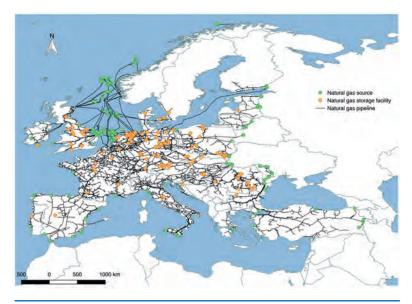


Figure 3. Europe's existing gas transmission network.

Unfortunately, there is no quick method to investigate whether a pipe might become compromised due to hydrogen exposure, as this damage takes time to manifest. As such, precise studies and empirical tests are currently being performed. In-depth knowledge of pipeline systems, as well as the implementation of accurate risk assessment and gap analysis, will enable network owners and operators to determine the safe proportions of natural gas to hydrogen when blending. This solution could result in the supply of lower-carbon-intensity energy to end users.

The green hydrogen solution has merit. Once the engineering challenges are overcome, and the technology, infrastructure and consumer behaviour is in place, hydrogen will deliver significant environmental benefits. Notably, green hydrogen can leverage periods of low sunlight and wind, and can also act as a battery. It is an energy carrier that can ensure energy supply in times where renewable sources are not in their highs. As an energy carrier, it can be stored in a liquid organic form as ammonia (NH $_3$ ), which requires 125 psi (862 kPa) of constant pressure and temperatures of below -33.6 °C, while pure hydrogen requires temperatures of as low as -252.87°C and a pressure of 14.7 psi (10.3 kPa) to transform into liquid form.

From this simple comparison it is clear that the storage and transportation options for liquid organic hydrogen carriers (LOHCs) suggest that this is a more promising solution. One thing is for certain: hydrogen will be a substantial part of our future, but it will not be the only sustainable solution.

#### Conclusion

The downstream industry has a role to play in securing a sustainable future, and should be seen as part of the solution. At the last COP26 conference, the lack of downstream sector representatives elevated concerns that governments intend to solve the energy issue without the expertise and experience of the sector, and in the case of carbon, the complexity of the problem is not being fully recognised.

There is a distinct mismatch between the want to have zero emissions, and the transition that must happen in order

to realise it, as well as a lack of dialogue between those making policies and those required to deliver it. Without the input of the industry, poor decisions are likely to be made, with sub-optimal outcomes. A recent example of this is the ban of plastic straws, which had no material impact on consumer polymer use. Rather, the replacement material created more carbon emissions.

An open dialogue is needed in order to deliver a more logical and efficient energy transition that will result in lower emissions. By keeping some of the cleaner fossil fuels active, the most carbon-intensive fuels would be displaced. There is a lot that can be achieved at present that may not result in neutrality, but would escalate progress. Ours is a transition that demands acceptance that it will not gain overnight; it will instead require a number of steps in order to land upon sustainable solutions that will solve our sustainability challenge.



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Daisy Chen, Amazon Web Services (AWS), **USA**, discusses how cloud-enabled equipment

s with many capital-intensive industries, the energy sector relies on highly available and reliable equipment in order to reach production targets and meet customer demands. Downstream operations comprise of a complex network of equipment infrastructure, technical data and business workloads to support the transport, separation and processing of hydrocarbons to produce finished products. Additionally, equipment within a facility is constantly subject to feed rate and quality shifts, online process fluctuations, equipment modifications, or capital expansions. As such, improving reliability, optimising equipment performance, controlling maintenance costs, and improving overall field safety are top business

Maximising value from ageing equipment is fundamental for downstream profitability, but achieving this goal often means that operators are caught in an ongoing battle to optimise equipment performance, minimise unplanned equipment failures and downtimes, and control maintenance costs. This conundrum occurs for two reasons: the scale and complexity of accumulated technical data makes real-time access to relevant equipment health data challenging and inefficient; and ageing legacy equipment monitoring and maintenance tracking systems utilise disparate tools, disjointed technology and data systems, and antiquated equipment analytics.

Today, finding the right balance between production and equipment maintenance strategies depends on sophisticated data and analytics. Enabling advanced analytics invariably requires digital transformation and more often than not, the migration of legacy systems to the cloud. Among the most promising innovations in downstream transformation are cloud-native equipment health and maintenance (EHM) solutions that help improve critical equipment reliability and performance through real-time visibility to equipment performance and early indications of equipment failure.





EHM is playing a key role in the implementation of predictive maintenance. The US Department of Energy (DOE) has stated that predictive maintenance saves 8 - 12%



Figure 1. Predictive maintenance applications for downstream oil and gas operations can help operators reduce costs and downtime by identifying equipment failures before they occur.



Figure 2. The EHM solution from AWS is a cloud-based offering that provides predictive equipment analytics to monitor equipment health and performance and boost preventative maintenance strategies, which helps reduce equipment downtime and optimise performance.



Figure 3. Leveraging AWS for a customised, condition-based maintenance project, a leading Australian natural gas producer reduced the cost of routine inspection and service by 80%.

over preventative maintenance costs, and upwards of 40% over reactive maintenance costs.

EHM utilises advanced machine learning (ML), analytical applications, visualisation, and alerting capabilities for critical equipment monitoring and proactive anomaly detection in order to enable effective maintenance scheduling. By overlaying operational insights provided by EHM with equipment maintenance history records, companies have lead-time to take field action such as equipment optimisation and proactive maintenance planning. EHM gives downstream companies the ability to reduce unplanned downtimes and optimise equipment life cycles which, in turn, help them to optimise maintenance planning and the associated costs.

EHM solutions help downstream companies maximise value from existing equipment infrastructure. EHM aggregates operational data from data historians or equipment sensors, equipment records, and maintenance work histories, to provide contextualised insights that support predictive maintenance efforts. With the ability to model and view field equipment performance, companies can increase equipment utilisation, prioritise maintenance efforts, optimise maintenance costs, and reduce operational risks.

The EHM solution from Amazon Web Services (AWS) utilises a variety of services to drive its cloud-based applications. These include AWS IoT Core, AWS Database Migration Service, Amazon Aurora, Amazon Simple Storage Service (Amazon S3), AWS Lambda, Amazon Lookout for Equipment, and Amazon SageMaker, all of which provide performance monitoring and enable predictive maintenance at scale, which is critical for downstream companies seeking to leverage digital transformation to improve equipment reliability and overall performance.

# Case study: predictive maintenance at an Australian natural gas facility

When a leading Australian natural gas producer announced an ambitious goal to increase operational efficiencies by 30% over three years through technology innovation and analytics, it faced the following common technology challenges:

- Different teams were using several manual processes across different systems, and they needed a workflow that could run across the top, integrating all of these manual steps into an automated process.
- Data needed to flow continuously from onsite equipment to analytics systems, but much of its infrastructure was old and was not designed to support real-time data capture, transfer and access.
- Data was stranded in disparate siloes, and a multi-layered solution was required to bring data to a central location quickly and securely, and make it accessible to analytics teams and decision makers across various systems, such as maintenance and permit.

To address these challenges, the company developed a cloud-based condition-based maintenance (CBM) system to improve equipment visibility for analysis, troubleshooting and maintenance for 1500 cooling fans in its LNG

processing facility. The CBM project goals included detecting equipment failures before they occur, reducing time from detection to repair, automating mundane processes, and minimising the number of hours to which staff in the field are exposed.

Leveraging cloud-based IoT infrastructure and services, the company developed and implemented wireless IoT vibration sensors to understand the condition of the fans. The sensors transmitted data back to a centralised cloud-based data lake across a wireless LoRaWAN network and managed cloud-based IoT data services to handle edge applications, device data routing, and storage.

The company used a managed ML development service to build customised ML models to perform continuous analysis on data in production in order to determine equipment condition, detect defects, and assign a health score to every machine every three hours. This enabled the company to automate responses so that detected defects could be entered into the CBM app to generate a fully-resourced work order with a permit and isolation certificate. ML models were also developed to automate the company's work planning process, and enabled templated, automated steps and responses, eliminating the need to build artefacts and work orders from scratch.

Collecting and analysing cooling fan data was performed manually every three months. The company was able to increase the interval of cooling fan field data capture to every 15 minutes to provide near real-time monitoring. ML-driven workflow automation reduced the average work planning process from 80 days to one day. The cost of routine inspection and service was reduced by 80%, and the company expects to reduce that to 90% as it continues to train the CBM algorithms. The company is also able to utilise staff for more productive activities, with capacity for further innovation – including beginning similar CBM work on its pumps, valves and turbomachinery.

# **Conclusion**

Disruptive digital transformation has become a business imperative in the energy industry, and cloud-native EHM solutions are creating a new dimension of capability to solve critical industry challenges. Migrating field equipment monitoring and maintenance operations to the cloud enables downstream companies to optimise equipment performance, reduce unplanned downtimes, and extend equipment life cycles. Instead of reacting to equipment failures as they occur, which is inherently dangerous, costly, and directly impacts margin performance, near real-time failure detection allows companies to proactively plan maintenance, which helps control expenditures and optimise downtime impacts. Workflow automation helps reduce operating costs, increase production throughput and plant efficiency, and increase labour productivity.

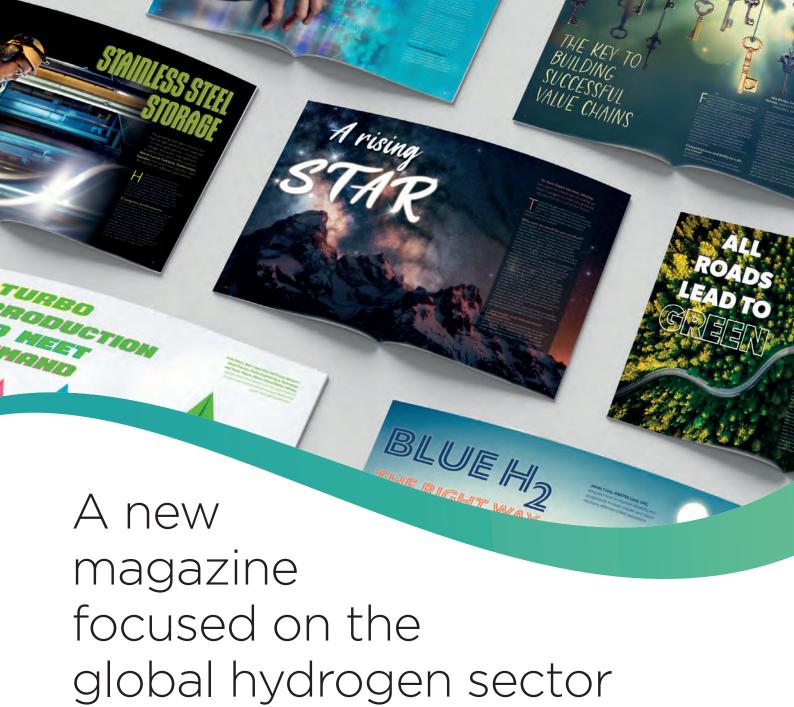
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**Praveen Sam, Honeywell Connected Industrial, USA,** details the new role of the cloud for industries, and five capabilities that must be created by industrial organisations adopting the cloud.

he 'industrial cloud' has been used as a broad term for the application of cloud technologies in industries such as energy, mining, metals, chemicals, and other manufacturing industries. The role of the cloud in industries began with the promise of reducing infrastructure costs

and increasing IT efficiencies by shifting computing workloads from on-premises data centres to cloud service providers.

Today, in addition to the infrastructure benefits, moving computing to the cloud also unlocks new benefits such as delivering more productive, high-performing, and cost-effective

technology assets. The cloud enables the re-engineering and modernising of both industrial data and applications. With these new capabilities, it increases the speed of adoption and reduces the time-to-value of industrial software, which addresses new business realities.

# New industry realities are accelerating the shift to cloud

Industries today are responding to unprecedented levels of change in the world, driven by factors such as an increased focus on improving sustainability, responding to pandemic-induced economic realities, and adapting to the changing social, political and demographic landscape. These factors have contributed to the need to look differently at digitally-enabled business transformations.

Solving these challenges requires industries to expand across the boundaries of their site, organisation and geography, and these problems must be solved jointly with customers and partners from multiple industries. As a result of these factors, now is the time for industries to increase the adoption of cloud technologies. Looking at some industry challenges reveals why the cloud is more relevant than ever.

# Solving challenges such as improving sustainability and strengthening the supply chain

Improving sustainability requires addressing challenges such as emissions reduction and waste management. These challenges are globally distributed in nature. As an example, consider the end-to-end supply chain, which generates most of its carbon emissions either through sourcing of raw material, distribution of the product, or through the usage of sold products such as fuels. If industries must shift to a lower carbon footprint and develop lower-carbon products, the effort to monitor emissions spans geographic and organisational boundaries in bringing transparency, reinventing products, and jointly creating new business models.

Similarly, if we look at supply chains, they require seamless workflows of information both up and downstream of the supply chain. An industry's business performance is directly linked to how well a supply chain performs and responds to changes. Collaboration on planning for anticipated demand or supply disruptions and faster access to information improves end-to-end supply chain visibility. The global availability of cloud applications allows business processes to become more integrated across the supply chain network. This can create end-to-end visibility across all supply chain participants, with the cloud providing the necessary technical foundation.

# Improving digital inclusion of industrial workers from the field to the boardroom

The COVID-19 pandemic highlighted how critical digital technologies are for remote working and ensuring business continuity. While the pandemic enabled many millions of people to immediately participate in the economy remotely, it also exacerbated the digital divide

for those that do not have this option. The World Economic Forum references that more than 47% of the world's population remains unconnected. This has brought a renewed sense of urgency to improve the digital inclusion of people across geographic and cultural boundaries, and include people of different skill types and age groups.

In the context of industries, this will mean addressing challenges such as how to sufficiently build competency, enable productive work, and ensure safety. Capabilities such as remote workforce management and remote operations help industries to address these challenges by baselining operations and enabling business continuity. With these technologies, achieving work outcomes requires supporting an inclusive digital workforce that can adopt these new operating models.

Another aspect of digital inclusion is the ability to provide training for operators across the world. As the population of the world increases with major demographic shifts, the need to increase the availability of specialised operator training becomes even more important. Cloud technologies provide the foundation to enable the delivery of global competency programmes that reduce training time and enable the start-up of operations from almost anywhere in the world.

# Increasing business resilience in a highly-volatile and changing world

Recent global events have reiterated that the most important thing is to always keep people safe. Events such as the pandemic, the supply chain crisis, and changing geopolitical landscape place additional stress on the business to respond fast. Despite these challenges, businesses and operations must go on.

Industries that develop capabilities in the cloud benefit from the speed and flexibility in adapting their business with capabilities such as remote operations, production insights, and supply chain insights at a global level. The cloud provides elasticity, which enables industries to scale up and down easily while consuming only those computing resources that they need. During periods of uncertainty, the cloud enables people to function and ensures that industries do not lose the opportunity to innovate by quickly scaling up when necessary.

# Technology trends are also accelerating the shift

In the past decade, cloud technology has matured with several capabilities available as Software-as-a-Service (SaaS), which makes it easier to increase the adoption of the cloud for industries. This has contributed to increased readiness for industries to adopt cloud technologies.

# Enterprise-grade software is now available on the cloud and extends to the edge

With the advent of cloud hyperscalers, the ability to serve a globally-distributed or large organisation is now



# Service for peace of mind



easily possible at lower costs than before. Their capabilities now extend to on-premises and the edge, which increases the possibility of transitioning critical business services to the cloud while ensuring the least disruption.

# Software product categories are converging, which is simplifying cloud migration

Fewer separate point solutions are required as major product categories have started to become increasingly integrated and are available as a seamless capability on the cloud and often as SaaS. For example, Asset Performance Management is becoming more integrated with products that integrate asset registers, strategy libraries, real-time performance monitors, integrity risk tools, as well as predictive maintenance. Similarly, Manufacturing Execution Systems are becoming far more integrated with the ability to plan, schedule, manage production operations, and extend into dispatch and supply chains from within a single product. These trends make it easier for industries to adopt purpose-built cloud technologies.

# Embedding AI/ML capabilities across software applications is easier

As analytics becomes mainstream in industries, it is increasingly being embedded within major software products in the market. The cloud allows for building and scaling industry-specific analytics capabilities. This reduces barriers of availability of skills and the need to create artificial intelligence (AI)/machine learning (ML) use cases that are specific for each site and manage disparate sets of data.

# Cybersecurity capabilities on the cloud have significantly improved

Cybersecurity compliance is becoming more streamlined with increased adoption of standards such as IEC 62443 for industrial automation and control system cybersecurity, ISO-27001/270002 for information security management, ISO-27017 for information security controls for cloud services, and ISO-27018 for the protection of personally-identifiable information in public clouds. Availability of AICPA SOC 2 audit reports also helps when companies consider SaaS or other cloud vendors in their journey to adopt cloud technologies.

#### Availability of industrial SaaS applications

Industrial companies are often perceived as late adopters of digital technology. Most industries have preferred to stick with on-premises software solutions, largely due to the lack of suitable SaaS options at a cost that is viable to many of them. This is rapidly changing with several industrial software capabilities delivered as a service. These capabilities include foundational infrastructure such as data, analytics and production insights, in addition to major software applications such as manufacturing execution systems, asset performance management, and remote operator training.

# Five capabilities for the industrial cloud

Strategically thinking about the role of the cloud for industries requires more than a consideration of technology. Most industries have already initiated some form of digitally-enabled business transformation programmes. An incremental and agile approach to cloud transformation reduces risk and avoids business disruption when compared with large and expensive rip and replacement of existing systems.

Making cloud for industries easy to adopt across the organisation requires tailoring capabilities that address long-term needs for the industry. These clouds must bring together common industrial data models, industry-specific standards, business workflows, application programming interfaces, and interoperability with multiple clouds. There are five capabilities that industrial organisations adopting the cloud must create:

#### Industry-specific building blocks

Each organisation must develop common capabilities that scale across the boundaries of its enterprise to address industry needs. These are modular building blocks that speed up the development of industry-specific digital solutions. Examples of these are shared building blocks such as asset models, process models, simulation engines, and/or planning and scheduling models, which allow applications to consume as a common resource on the cloud.

#### Cross-application architecture blueprint

An industry-specific architecture that covers all aspects beginning with data, network, computing infrastructure, and the range of applications will serve as a blueprint for enabling industrial cloud transformations. Industry clouds require an industry-specific blueprint, against which organisations can modernise and innovate capabilities that are most relevant for their business.

#### Openness and interoperability

Cloud applications for the industry must be thought of as a highly-interoperable ecosystem of applications that must be capable of maximising existing software investments such as their current on-premises environment. A successful industrial cloud will drive an increased level of openness and interoperability, while promoting a common view across the enterprise.

# Cybersecure foundation for connectivity, data and access

Building an enterprise-wide data, analytics and connectivity model is critical in order to function in the new world of cloud. Cybersecurity threats are risks that must be managed for both information and operational technology applications. These threats are ever-changing. In order to fully exploit the benefits of the cloud, a foundation to manage cybersecurity must be built, starting with connectivity and then extending to data and access.

# Secure integration for partners

There are currently multiple cloud environments from different providers. The landscape is even more complex if we consider the overlap between many SaaS and Infrastructure-as-a-Service (laaS) providers. Most companies who started their cloud journey seem to have focused on proving their success with a single cloud provider. Over time, the ability to integrate and operate across multiple cloud ecosystems is an important building block in order to fully exploit an open ecosystem with partners.

# Where to start?

One of the most important questions that industries try to answer is where to start. Generally, business leaders either expand their cloud transformation efforts to cover operational technology and industrial applications or start with a new industrial cloud journey. In order to develop a phased roadmap with the right governance, there are five principles to follow:

# Start with a business context and a problem to solve

Cloud transformation journeys must be aligned with business objectives and have a shared context with the overall strategy for the organisation. As a first step, picking a problem to solve with a cloud-enabled business value will help set the stage for future transformation. For example, enterprise-level production insights to improve economic planning across multiple production sites will provide a basis for additional capabilities.

# Build the data foundation and establish interoperability

Operational technology and industrial software applications are largely built on-premises where they have been used for several years. Expanding their availability using the cloud requires breaking down siloes and creating broad availability of industrial data for consumption by new software applications and users

A clear strategy for how to connect to different equipment and applications to collect, contextualise, store and scale data must be established. Wherever possible, common master data must be used between applications, with shared assets and process models utilised through extensible application interfaces. This will enable increased levels of interoperability.

# Select new capabilities to build on the cloud

Add new technology capabilities to the cloud that can be shared across the entire organisation. These are capabilities such as data science tools, common enterprise applications, data visualisation templates, and ML models. This helps future-proof investments by adopting new capabilities that can be exploited using the cloud at a scale that was not possible before.

# Shift workloads with a roadmap, and plan for a transition period

Moving to the cloud does not have to be wholesale. While workloads are moved between on-premises and the cloud, industries should plan for a hybrid period where an overlap will exist between the current infrastructure and the new cloud infrastructure. The goal of a successful transition includes setting up new infrastructure and software management processes to minimise disruption such as high availability, disaster recovery, and testing on the cloud.

Capabilities to have on the cloud must be determined in order to build a migration roadmap. Industries that adopt software must shift from a focus on software applications to a focus on outcomes. With a focus on outcomes, industries must choose which applications to transform in the cloud, which to simply migrate, and which to keep as-is. Certain legacy systems may never be migrated to the cloud for technology, commercial, or regulatory reasons. Regional differences for data sovereignty or regulatory requirements must be assessed for each industry and the products that are produced. A roadmap must be built which defines how to sequence these capabilities and regions. During the transition period, deployments to existing data centres must be by exception, and all new investments must be cloud-first or cloud-ready.

# Build the organisation around these new capabilities

New capabilities built on the cloud will require changes to the current organisation to enable adoption and realise value. For example, adoption of an open and interoperable ecosystem across multiple industry stakeholders will require setting up business processes that facilitate collaboration with customers and partner organisations. This will also require governance around aspects such as cybersecurity through intrusion prevention, and detection and response. The organisation structure must be built with the right incentives to ensure that new opportunities presented by the cloud are utilised.

# Why the time is now?

We are now in a phase of mainstream adoption of the cloud within industries. The increased maturity of industrial cloud technologies makes adoption easier and provides faster time to value. Preparing for volatility and uncertainty in the world also requires industries to adopt new cloud-enabled capabilities such as remote operations and production insights while increasing the digital inclusion of people.

All of these factors make now a suitable time to adopt cloud transformations. These allow industries to achieve operational excellence, improved sustainability, end-to-end process optimisation, increased reliability, and better workforce productivity. In utilising the cloud, industries can embrace bold strategies which create a future that is more efficient, safer, and sustainable, and is also inclusive of all people in the workforce and society.

# CARBON BLACK MARKET

# **Stefano Sassi, Eurotecnica, Italy,** explores the environmental benefits of carbon black production within a refinery.

here is no doubt that the most important development in carbon black production has been the introduction of furnace blacks.

Today, the furnace black process accounts for more than 95% of carbon black production worldwide, this process being the most modern way of manufacturing this important building block.

Eurotecnica's proprietary ET Black<sup>TM</sup> Carbon Process is a high-yield furnace black process. It combines a high degree of economy of scale with the flexibility of producing a wide spectrum of carbon black grades with a single reactor.

The production of carbon black in the ET Black process is accomplished by the partial combustion and thermal decomposition of highly-aromatic residual oils at high temperatures, in horizontal closed reactors. Temperatures range from 1400°C to 2000°C, depending on the type of carbon black produced, whether it is a soft black or hard black grade, and the specific reaction times for each grade.

In the downstream part of the reactor, at selected intervals, water is injected to perform quenching of the carbon black laden gases. The sequence, intensity and duration of quenching confers the carbon black product-specific characteristics that differ from grade to grade. Several specifically-designed heat exchangers allow for the efficient recovery of the massive amount of heat that is generated in the reaction.

A carbon black plant designed and implemented for ADNOC's refinery in the UAE has proven the level of performance that is achievable by the ET Black process, and its ability to produce high-end grades (N115, N220) out of relatively poor, low Bureau of Mines Correlation Index (BMCI) feedstock.

This experience has demonstrated the benefits that a refinery can experience by taking advantage of the so-called 'bottom of the barrel' as feedstock to produce carbon black – a valuable group of commodities applied in several industrial sectors.

There are many advantages to investing in a carbon black plant – for the refinery itself, for the local community and, broadly, for the global environment. For instance, low-value residuals, such as FCC decant oil, are difficult streams to use in a refinery for anything other than burning it completely, generating large amounts of greenhouse gases. As this type of feedstock has certain characteristics of high aromaticity, it is perfect as carbon black feedstock.

The advantages for those refineries considering setting up an ET Black carbon black plant are numerous:

- The production of a valuable commodity that is priced at US\$2000/t on average, which is generally in high demand.
- The refinery is enriched with top technology and several highly-qualified jobs that it generates.
- Entry into a growing market.
- The production of carbon dioxide (CO<sub>2</sub>) is halved; roughly half the feedstock becomes carbon black instead of simply being burned.

- Around half the sulfur contained in the feedstock is captured.
- The residual emissions are virtually zero.

While the first advantages are rather obvious, the latter demand further detail.

# Emissions to air: halve the production of CO,

When a refinery cannot sell oil residues to the market, there are no alternatives to burning it, resulting in the 100% transformation of the carbon into CO<sub>2</sub>. However, adopting a carbon black plant is a way to use such streams and turn them into a valuable product. Since the yield is around 50% – depending on the grades produced – only the balance



**Figure 1.** An operator at an ET Black carbon black plant.

becomes  $\mathrm{CO}_2$ , allowing for a significant reduction of that greenhouse gas (GHG). Other types of emissions from a carbon black plant are produced in very low quantities, if not traces. Table 1 lists these.

# Tail gas venting

An important potential source of emission to the air is the 'tail gas'. Tail gas comes from the reactor following product separation, and is a low calorific gas with a high moisture content due to the quench water vapour. It contains hydrogen (H<sub>2</sub>), carbon oxides (CO and CO<sub>2</sub>), reduced sulfur compounds (H<sub>2</sub>S, CS<sub>2</sub> and COS), sulfur dioxide (SO<sub>2</sub>), nitrogen compounds (N<sub>2</sub>, NO<sub>3</sub>, HCN and NH<sub>3</sub>) and volatile organic compounds, such as ethane and acetylene.

The tail gas composition can vary considerably according to the grade of carbon black produced, and the feedstock used. Carbon black yields can be up to 65%, depending on the grade produced and the raw materials used. The presence of sulfur compounds in the tail gas (sulfur oxides, H<sub>2</sub>S and volatile organic sulfur compounds) depends on the feedstock sulfur content.

As a rule of thumb, only half of the sulfur contained in the feedstock does turn into sulfur oxides ( $SO_{\chi}$ ), as the balance stays in the final carbon black product. Around 2.5% sulfur content in the feedstock is still acceptable, because for several grades of carbon black – those applied in the rubber applications – the sulfur takes part in the downstream process of vulcanisation.

In many standalone plants, the standard requirement for tail gas treatment is flaring. However, methods for recovering the energy content of the tail gases are more frequently employed than in the past. For instance, tail gas combustion is

becoming common practice. The combustion of tail gas generates flue gas with different environmental characteristics

Venting of non-combusted tail gas may be allowed during emergencies, start-up and shutdown periods, and during periods of grade change. Typical ranges of carbon black tail gas composition are provided in Table 2. However, these values do not reflect the full range of tail gas compositions encountered in all the carbon black facilities. Significant variations occur due to the different feedstocks used and carbon black grades produced.

# Emissions from dedicated tail gas combustion devices

Gaseous toxic and odorous emissions from the tail gas, such as H<sub>2</sub>S, volatile organic sulfur compounds (CS<sub>2</sub>, COS), and CO are controlled with thermal combustion such as flares, boilers or incinerators. Thermal combustors can achieve complete oxidation of organic compounds, and can oxidise sulfur compounds in the flue gas process.

Table 1. Emissions produced by a carbon black plant				
Emission	Origin			
СО	<ul> <li>Product of incomplete combustion in the reactor</li> <li>Product of incomplete combustion in dryers, boilers, flares, etc.</li> </ul>			
SO <sub>x</sub>	<ul><li>Oxidation of feedstock sulfur compounds in the reactor</li><li>Oxidation of sulfur compounds present in the tail gas</li></ul>			
Reduced sulfur compounds (H <sub>2</sub> S, CS <sub>2</sub> , COS)	<ul> <li>Decomposition and partial oxidation of feedstock sulfur compounds in the reactor</li> </ul>			
NO <sub>X</sub>	<ul> <li>Oxidation of feedstock nitrogen compounds in the reactor</li> <li>Thermal NO<sub>x</sub> from the reactor</li> <li>Fuel NO<sub>x</sub> from dryers, boilers, flares, etc.</li> <li>Thermal NO<sub>x</sub> from dryers, boilers, flares, etc.</li> <li>Oxidative post-treatment of carbon black with NO<sub>2</sub> or HNO<sub>3</sub></li> </ul>			
Volatile organic compounds (VOCs, e.g. methane, acetylene, ethylene	■ Incomplete decomposition of feedstock in the reactor			
Polycyclic aromatic hydrocarbons (PAH)	■ Incomplete decomposition of feedstock			
Particulate matter (e.g., carbon black dust)	<ul> <li>Slip through filter system behind reactor</li> <li>Slip through dedusting filter systems, e.g., behind dryer</li> <li>Slip through thermal combustor (e.g., boiler, flare)</li> <li>Fugitive emissions due to storage, transportation and packaging</li> </ul>			
Heavy metals	Present as trace impurities in some feedstock			

Combustion efficiencies of 99.6% for H<sub>2</sub>S and 99.8% for CO have been measured for a flare of carbon black. Particulate emissions may also be reduced by the combustion of some of the carbon black particles. However, SO<sub>2</sub> emissions are increased due to the oxidation of H<sub>2</sub>S and volatile organic sulfur compounds.

Additionally, it is important to realise that the combustion will also increase the emissions of nitrogen oxides. In Europe, the recovery of energy from the tail gas in the form of heat, steam and/or electricity is common, and the same applies to the ET Black plant at ADNOC facilities. The combustors usually treat some 70% of the generated tail gas; the remaining 30% is normally used as fuel in the dryers of the wet pelletising unit.

# **Emissions from the dryers of the wet** pelletising unit

The wet pelletised carbon black is transported to a rotary drum dryer, where the wet pellets are dried. Tail gas is generally used as a heat source, as it aids the reduction of fossil fuel consumption. The flue gases' heated dryer can be combined into one common stack with the evaporated water from inside the dryer.

# Filter system vents

Carbon black is separated from the tail gas in the main bag filter, consisting of a special type of bag filter. Carbon black that is not captured in this filter is entrained in the tail gas. Normally, levels of carbon black in the tail gas after the filter are < 100 mg/m<sup>3</sup>. As the slip of carbon black in this filter represents a loss of product, there is a drive for the operator to keep the level as low as



Figure 2. Tyres are by far the largest single market for carbon black.

possible. The collected (fluffy) carbon black is pneumatically-transported by air to another bag filter system, where the carbon black is separated from the transport air and subsequently fed to the pelletiser. The emissions from this filter are released into the atmosphere. Emission levels from this filter are generally  $< 50 \text{ mg/Nm}^3$ .

# **Fugitive emissions**

Fugitive emissions of carbon black (particulate matter) originate from cleaning, spills, and leaks in handling, packaging, storage and transportation. Fugitive emissions can be insignificant when the operator adheres to ET Black guidelines.





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#### Emissions to air

Due to the large variety of plant configurations, feedstock compositions and product types, it is difficult to present an overview of emissions from carbon black plants that fits all plants. Some plants operate with separate stacks for the tail gas combustion units and for the product dryers, whereas others combine the flue gases from these sources.

#### Emissions to water

Water is used in relation to the production process or used for non-process-related utilities. The following two sections discuss the process-related and the non-process-related discharges to water

### **Process-related water streams**

In the production process, the following water streams are distinguished:

- Quench water (reactor tail gas).
- Scrubber water during start-up/warming up of the reactor.
- Water used for pelletisation.
- Boiler feed water (if present).
- Cooling water for the power plant or thermal combustor.

# **Potential discharges**

Some water streams can be reused as process water for quenching the reactor's gas/carbon black mixtures if it does not affect product quality. Prior to being reused for quenching, the effluent water streams are filtered. It has been proven that zero discharge to water is possible for ET Black plants.

Table 2. Typical ranges of carbon black tail gas composition

Compound	Minimum (vol%, wet)	Maximum (vol%, wet)
Moisture (H <sub>2</sub> O)	29.6	50
N <sub>2</sub>	32.7	46.2
H <sub>2</sub>	6.6	14
CO	6.1	11.7
CO <sub>2</sub>	1.5	3.9
O <sub>2</sub>	0	1.85
CH <sub>4</sub>	0.07	0.78
Acetylene (C <sub>2</sub> H <sub>2</sub> )	0.03	0.7
	Minimum (ppmv, wet)	Maximum (ppmv, wet)
SO <sub>x</sub>	5	260
H <sub>2</sub> S	63	2500
COS	3	300
CS <sub>2</sub>	11	800
Mercaptans (R-SH)	Traces	180
NO <sub>X</sub>	5	310
Ammonia	42	60
Hydrogen cyanide (HCN)	130	564
Ethane/ethene (C <sub>2</sub> H <sub>6</sub> /C <sub>2</sub> H <sub>4</sub> )		
Propane/other C <sub>3</sub> S		
Butane/other C <sub>4</sub> S	50	3612
Pentane/other C <sub>5</sub> S		
Hexane/other C <sub>6</sub> S		

However, the production of some rubber black and nearly all specialty black grades requires clean quench water.

#### **Solid wastes**

According to European legislation, waste can be divided into hazardous and non-hazardous waste, and this is discussed in the following two sections:

#### Hazardous waste

The following types of hazardous waste can be distinguished:

- Spent or used oil.
- Oil sludge (e.g. due to the cleaning of storage tanks or leakage).
- Hazardous waste generated in workshops, laboratories and offices.

Carbon black processes generate very little direct hazardous waste. This is mainly due to the reuse of spent oil. As such, nearly all hazardous waste in carbon black plants are only generated in the workshops, laboratories or offices that support the production process. The amounts are relatively small in relation to the amounts of carbon black produced.

#### Non-hazardous waste

The following non-hazardous waste can be distinguished:

- Sub-standard carbon black.
- Refractory waste.
- Used bag filters (carbon black filter systems).

Carbon black processes generate non-hazardous waste from producing substandard carbon black. This material is typically reprocessed. The amounts of non-hazardous waste are relatively small in relation to the amounts of carbon black produced. Compared to carbon black production, the amount of refractory waste is approximately 0.02 – 0.1%. Nowadays, this refractory waste is pure alumina, which can be considered non-hazardous waste.

#### **Conclusion**

Carbon black is a more than 13 million tpy market, and it is expanding to cover a wide spectrum of growing applications. Tyres are by far the largest single market for carbon black. As long as the world maintains its appetite for mobility, there will always be the need for tyres, and therefore for carbon black.

Refineries and petrochemical operators are potential investors in carbon black manufacturing, as they have abundant and cheap raw materials to produce. ET Black complies with the most stringent environmental regulations now and in the future. Additionally, it has the flexibility to produce all ASTM and specialty grades, with a single plant.

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# EQUIPPED FOR A CLEANER FUTURE



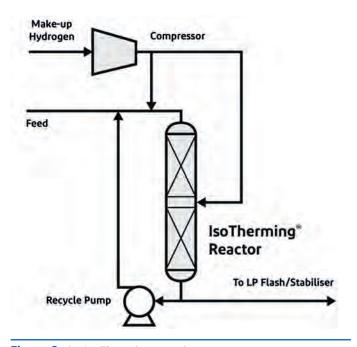
**Patrick Downey, Elessent Clean Technologies, USA,** introduces a sustainable solution for producing cleaner fuels.

new age of fuel production is here with the introduction of policy changes pushing refineries to reduce emissions and ultimately achieve net zero goals. These policies include compliance and voluntary carbon markets that play an important role in driving refineries to make investments towards a more sustainable future. The carbon markets utilise tax credits that are available to refineries that can produce fuels in a more

efficient and sustainable manner. One avenue to receiving carbon market tax credits is to improve energy efficiency by reducing emissions generated through utilities. This can be done by measuring and optimising utility consumption, such as fuel gas, steam, cooling water and electricity, and then converting to the equivalent amount of carbon dioxide (CO<sub>2</sub>) emissions that were reduced. In addition to this, traditional fossil fuel feedstocks can be replaced by feedstocks made

from renewable resources that are harder to process, such as vegetable oils, bioethanol, and animal fats, but that are also eligible as carbon market tax credits. As the market undergoes further energy transition and evolving policy

Figure 1. An IsoTherming reactor in commercial service.



**Figure 2.** An IsoTherming reaction zone.

enforcement, it will be important for the refining sector to explore more economical processes to produce fuel.

This article describes the principles of the IsoTherming® hydroprocessing technology and highlights the energy

efficiency, versatility and robustness of the process. Two recent revamp case studies will be showcased that demonstrate its benefits, specifically in the areas of energy efficiency and the ability to process difficult feedstocks into Euro VI compliant fuels. In addition to this, refiners across the globe are under pressure to look for ways to comply with renewable fuels mandates. The technology is well suited to provide refiners with a cost-effective option for co-processing renewable feedstocks in the existing hydrotreater units, and is capable of managing the high heat of reaction that comes with processing these renewable components, which has proven to be a challenge to those operating hydroprocessing units with the traditional trickle bed technology. A discussion of co-processing renewable components and its impact on unit design and operation will also be presented.

# Introduction to the technology

IsoTherming hydroprocessing technology is a commercially-proven process that provides refiners worldwide with a more economical means to produce today's transportation fuels. Implementing this technology enables refiners to not only produce high-quality, low-sulfur fuels that are compliant with local environmental regulations, but also decrease energy consumption and operating costs when compared with historical trickle bed hydroprocessing technologies. The proven reliability and operational flexibility of the technology also enables refiners to meet business sustainability and social responsibility objectives.

The fundamental principle of the technology is the ability to provide the hydrogen that is necessary for chemical reactions using a liquid stream, rather than a recycle gas system. The reactor feed is saturated with hydrogen, which eliminates the need for a recycle gas compressor and amine absorber. To satisfy hydrogen requirements within the reactor, additional hydrogen can be added by means of an external liquid recycle stream and/or inter-bed hydrogen injection. Feed types that have low hydrogen demand, such as kerosene, do not require an external recycle stream to satisfy hydrogen availability requirements.

Operating the reactor liquid-full also acts as a heat sink for the exothermic reactions. Thus, the reactor operates closer to isothermal conditions, which reduces uncontrolled cracking reactions and lowers the production of light ends.

The type of hydroprocessing application, product objectives, and chemical hydrogen requirements dictate optimal reactor design considerations, such as number of catalyst beds and recycle ratio. The IsoTherming reactor design is robust and has been commercially-proven to successfully provide over 160% of design chemical hydrogen consumption, while processing fluctuating feedstocks. This flexibility offers refiners the ability to

process a wide variety of feeds to maximise refinery profits.

The technology currently has 29 licenses comprised of 24 grassroots units and five revamp units. There are 16 commercial installations of the technology currently in operation. The following case studies will detail how two refineries have revamped their existing hydroprocessing units.

# Case study 1

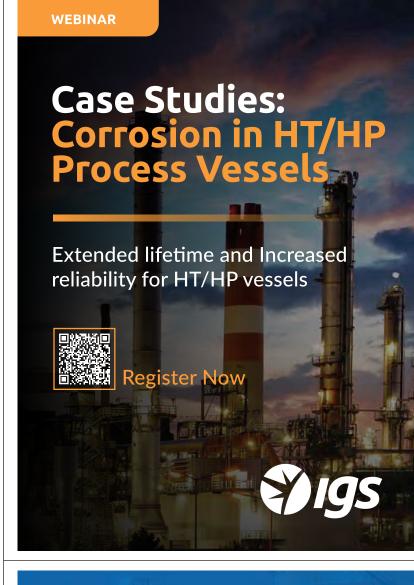
The first case study is for Refinery A, located in Western Europe. Refinery A has an existing trickle bed diesel hydrotreater that lacks a recycle gas compressor. This unit currently produces ultra-low-sulfur diesel with poor cycle length. Even at reduced throughput rates, current cycle lengths range from 12 to 14 months. An evaluation by catalyst suppliers concluded that a catalyst upgrade by itself could not achieve the desired product and operating targets due to unit constraints. Therefore, the refinery decided to evaluate the option of a unit revamp for its low-pressure diesel hydrotreater unit.

Refinery A extensively studied the revamp solution with the current trickle bed technology, and compared this to a revamp solution offered by Elessent Clean Technologies with the IsoTherming technology. A full conversion of the unit to liquid phase with this technology would provide the customer with extended cycle length, as well as a return to nameplate capacity and the ability to process cracked feedstock. A summary of the key benefits can be seen in Table 1.

Feedback from Refinery A indicated that the proposed trickle bed revamp solution was more capital cost intensive and comprised a longer list of new equipment, including a new recycle gas compressor (and associated high-pressure auxiliary equipment, such as an amine absorber and heat exchangers). Even with a new recycle gas compressor, the trickle bed technology was unable to offer the same extension in cycle length at the nameplate capacity as the IsoTherming technology, and additional catalyst volume or reduced feedstock rates were required to meet a similar cycle length.

In addition to offering a low capital cost, revamping with the IsoTherming technology provides additional operating efficiency benefits to Refinery A. The feedstock under review has very high levels of hydrogen consumption and thus a high volume of heat release. Due to the energy-efficient nature of the IsoTherming technology, coupled with this high level of heat release, the feed-fired heater is only required to operate at minimum operation rates outside of start-up conditions. Even at this minimum rate, there is surplus heat after pre-heating the feed. As such, a cost/benefit analysis was conducted, and it was deemed economical to utilise the excess heat from the reaction to produce medium-pressure steam in the unit. Table 2 quantifies the high-pressure energy savings expected post-revamp with the new technology, compared against current trickle bed operation.

Based on the assumed cost values of fuel gas and steam, the revamp would save Refinery A



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US\$1.7 million (US\$51/bbl of feedstock) annually in high-pressure utilities alone. Additional savings are also expected from low-pressure utilities.

This revamp solution is not only attractive from a capital and operating cost standpoint, but it also lowers the carbon footprint of the refinery due to the reduction in combustion of fuel gas from the fired heater. Based on the normal operating duties shown in Table 2, the reduction of 5520 tpy of  $\rm CO_2$  emissions is equivalent to the removal of over 1200 light passenger vehicles annually (based on heat content of propane of 139 million Btu and 4.6 tpy of  $\rm CO_2$  emissions from a single light passenger vehicle). Support for the revamp of Refinery A's diesel hydrotreater unit with the new technology continues, in anticipation of a 2025 start-up date.

**Table 1.** Refinery A – current operation vs IsoTherming revamp

Parameter	Current	IsoTherming revamp				
Capacity	149 Sm <sup>3</sup> /hr	205 Sm³/hr († 38%)				
% cracked feedstock	0%	8.1%				
Feed density @ 20°C (kg/m³)	860	909 (+49 points)				
LHSV hr <sup>-1</sup>	0.34	0.78				
Cycle length	12 – 14 months	36 months (↑ 3x)				
Recycle hydrogen	Once through	Recycle pump				

**Table 2.** Refinery A – utility comparison: current operation vs IsoTherming revamp

Parameter	Current trickle bed	IsoTherming
Normal operating charge heater duty (million kcal/hr)	4.936	1.780
% savings	-	64%
Fuel gas (kg/hr)	414	149
Fuel gas value (US\$/yr¹)	1 233 224	444 711
Steam produced (kg/hr)	-	10 281
Steam value (US\$/yr²)	-	891 035
Annual net value of utility consumption/production (US\$)	1 233 224	446 324
<sup>1</sup> Based on a fuel gas value US\$/million kcal of US\$297		

Table 3. Refinery B – current operation vs IsoTherming revamp

<sup>2</sup> Based on steam value US\$/1000 kg of US\$10.3

rable 3. Kermery by correct operation vs isotherming revails			
Parameter	Current	IsoTherming revamp	
Diesel yield (wt%)	96.7	98.5	
Additional diesel value (US\$/yr¹)	-	701 527	
Fuel gas (Gcal/hr)	10.0	6.4	
Fuel gas savings (US\$/yr²)	-	1 128 325	
CO <sub>2</sub> emissions (tpy)	21 003	13 442	
CO <sub>2</sub> tax savings (US\$/yr³)	-	39 338	
Annual net value of diesel yield/fuel gas (US\$)	-	1 869 190	

<sup>1</sup>Based on a diesel value of US\$558/t, and off-gas value of US\$426/t

<sup>2</sup>Based on 11.1 Gcal/t heating value for fuel gas, and fuel gas value of US\$426/t

# Case study 2

The second case study is for Refinery B, located in Eastern Europe. Refinery B has an existing trickle bed diesel hydrotreater with an approximate capacity of 229 standard m³/hr (Sm³/hr), which equates to 35 000 bpd. The refinery is investigating options to reach its decarbonisation targets and optimise operating expenses, while maintaining its current capacity.

Elessent Clean Technologies worked closely with Refinery B to evaluate multiple revamp scenarios geared toward its decarbonisation and sustainable operating objectives. A comparison of the final revamp conditions compared to current operation is presented in Table 3.

Based on the assumed values of diesel and fuel gas, the revamp saves Refinery B US\$1.9 million (US\$53/bbl of feedstock) annually from increased diesel yield, fuel gas savings and tax savings from reduced carbon footprint of the unit.

In addition to a reduction in operating expenses and carbon footprint, the revamp cost and effort from trickle bed to the IsoTherming technology was proven to be minimal. It was confirmed that the heat exchangers and air coolers supporting the existing trickle bed unit can be utilised with the new technology, with the only additional equipment required being the reactor recycle pump and proprietary IsoTherming Reactor internals.

Due to the low CAPEX required for this conversion, the calculated payback for the effort is only three years given the value provided with increased diesel yield, reduced fuel gas consumption and CO<sub>2</sub> tax savings. Support for the revamp of Refinery B's diesel hydrotreater unit with the technology is ongoing, as a revamp from trickle bed is anticipated in the near future.

#### Conclusion

The global market demand for biofuels continues to increase as mandates and renewable fuel credits are being implemented across the world. Whether mandated or not, renewable fuel production is likely on the mind of all refiners. The IsoTherming technology is well-suited to assist refiners in the production

of renewable distillate range products. The liquid-full technology is capable of handling the high hydrogen consumption and temperature rise that is associated with processing lipid-based feedstocks – whether in conjunction with a petroleum-derived feedstock or in a standalone unit. It also unlocks the ability to co-process without the concern of the trickle bed's recycle gas compressor limitations. The capital cost savings, energy efficiency and sustained catalyst life highlighted in the aforementioned case studies will also be apparent in a renewable processing application.

 $<sup>^3</sup>$  Based on 2.58 t CO $_2$ /t fuel gas (CO $_2$ , SO $_2$ , NO $_X$ ), and tax of fuel gas of US\$150.50/t

# SEARCHING FOR COLUTIONS



**Dennis Snijders, Integrated Global Services (IGS),** offers solutions for process vessel corrosion protection, and highlights a project that the company carried out in the Middle East.

ission critical equipment, including process vessels, towers and columns, play a major part in maintaining the uptimes and levels of production of oil and gas plants worldwide. These vessels typically operate at elevated temperatures and pressures, and are constantly subjected to a wide variety of aggressive, corrosive chemicals produced or added into the process.

One of the primary causes of process disruption is the issue of corrosion and metal wastage. There are several viable options available to address the corrosion mechanisms with a corrosion resistant alloy (CRA) barrier. The technique used to apply this CRA will predominantly be determined by the shutdown time that is available to carry out the application.

There are many different technologies that can be utilised to provide surface protection solutions for mission-critical equipment. Each technology has its advantages and

disadvantages that need to be well understood by customers so that they can make the best decision for their unique facility.

Process vessels operating at elevated temperatures and pressures represent one of the most arduous service environments and major challenges for asset owners and operators. These vessels, and those involved in the separation of oil/water and gas as it enters the process stream, are constantly subjected to a wide variety of aggressive conditions that can ultimately lead to severe internal corrosion.

# **Corrosion mechanisms**

In the FEED stage, refineries and oil/gas processing plants are designed to provide a minimum operating life (design life). However, conditions rarely match the FEED parameters in service. Plants operate well beyond the original design life, and challenges in vessel fabrication, design and process operation

typically lead to higher internal corrosion rates than anticipated. This introduces the requirement for maintenance, repairs or replacement of process equipment to prevent loss of containment, as well as maintain asset integrity and process operation.

#### The cost of corrosion

Corrosion ultimately leads to metal wastage and a loss of shell thickness. Plant and process shutdowns caused by issues with these critical assets can quickly run up losses of tens of millions of dollars. It is reported that a 29-day turnaround at Valero's

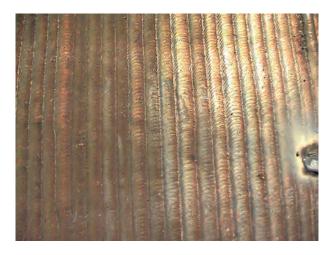


Figure 1. Welding repair.

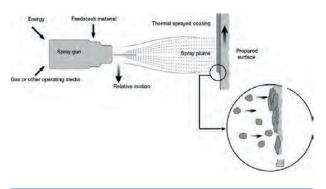


Figure 2. Thermal spray application.



**Figure 3.** The 2021 inspection of HVTS applied by IGS in 2015 shows the cladding in excellent condition.

St. Charles refinery in the US cost US\$39 million, and it was estimated that the company lost US\$1.2 - 3 million/d if the turnaround went beyond its projected timeline.<sup>1</sup>

# **Preventing/stopping corrosion**

There are a variety of solutions available on the market to help prevent the process of corrosion, including welding, various coatings, and Integrated Global Services (IGS)' High Velocity Thermal Spray (HVTS).

Welding is a commonly-used solution in the oil and gas industry, both for rebuilding degraded areas of wall thickness and providing a corrosion-resistant alloy barrier. Welding carries some fundamental drawbacks. A common issue is distortion of the shell due to heat input during the welding process, which can further require crane support to the equipment. A high degree of stress is added into the process during welding, especially on thinner wall vessels. Additionally, the weld procedure, code or environmental conditions may require heat treatment prior to or after the application as an additional step to the repair solution.

There is also a question of time and costs. Welding is a relatively slow process with an application time of  $10-16~\rm ft^2$   $(1-1.5~\rm m^2)$  per weld head per shift, and can cause additional delays in bringing the asset back into service. During a critical path period, using welding for corrosion protection can have a significant financial impact.

# Thermal spray

Thermal spray technology has been utilised for the application of CRA since the 1980s, spraying metals that are widely used in the welding process. However, it was quickly noted that the thermal spray process itself can negatively affect the condition of the material being sprayed. The resulting cladding, when using traditional metal alloys and commercially-available thermal spray equipment, is permeable. This permeability, coupled with internal stress and a lower bond strength with the base metal, creates a path for corrosion and premature failure.

These early failures have resulted in an understandable and rather universal distrust of early iterations of commercially-available thermal spray technology. The issues with thermal spray cladding raised some important questions, including whether it was possible to eliminate the permeability, porosity and internal stress of the thermal spray applied coating, and improve bond strength.

# The best solution for preventing corrosion

With corrosion causing disruption to many refineries, the industry needed a solution that could eliminate the permeability, porosity and internal stress of commercial thermal spray without compromising bond strength, delivering a robust solution similar to welding.

IGS understood this industry problem and developed its own proprietary solution – a corrosion-resistant HVTS technology. Designed to protect the base metal in highly-corrosive environments, this technology involves the simple application of a non-porous, high-nobility metal alloy.

The application process is considerably faster than welding, and no stresses are imposed on the base material during the application process. Furthermore, the process does not

generate any dilution. The quality of the cladding remains uncompromised, and there is no potential for galvanic corrosion due to dissimilar metals.

# Case study: comparing solutions for amine vessel corrosion in the Middle East

In 2015, a gas plant in the Middle East identified internal corrosion in two of its amine process columns and contracted IGS to apply HVTS alloy cladding to protect the base metal. The cladding was applied, and in 2016 the plant went out to public tender for the completion of a similar work scope on six more columns. The plant decided to use a local thermal spray contractor on a cost basis which involved using a conventional low velocity thermal spray process technology.

#### Amine vessel corrosion mechanisms

In the amine system, most of the corrosion is related to acid gas breakout and the subsequent attack of the metal surface, usually at elevated temperatures. Since corrosion is a chemical reaction, high temperatures always accelerate corrosion activity because reactions occur faster and more aggressively at higher temperatures.

There are often several factors that contribute to failure by corrosion. Statistics show that almost 50% of corrosion incidents occur in the hottest part of the plant: the reboiler and the bottom of the amine regenerator. In amine plants, most

corrosion is related to hydrogen sulfide  $(H_2S)$  or carbon dioxide  $(CO_2)$  breakout, and the subsequent attack of the metal surfaces – usually in areas of elevated temperature or a high pressure drop (leading to condensation).

Further potential corrosion mechanisms exist in amine columns. In the lower section of a regenerator, for example, carbon steel surfaces not wetted by the amine solution may be attacked by water vapour and the formation of carbonic acid. Acid gas ratio, choice of amine (DEA, MEA, MDEA, DGA, AGR, etc), contaminants, two-phase flow, flashing, high velocities, vessel design and insulation are all contributing factors. Pitting, crevice corrosion, flow-enhanced corrosion and general corrosion loss are frequent problems.

In this case, the plant in the Middle East conducted a planned inspection and noticed pitting in its amine process columns, which would eventually lead to failure if left untreated, and potentially cost the plant millions of dollars to replace the columns.

#### The solution

Some mechanical options include the installation of temporary clamps and plugs, vessel section replacement, and the application of internal weld overlay. The time required for these, together with the post weld heat treatment (PWHT) needed to remove heat affected zones (HAZ) and structural support considerations, often demand extended turnaround or shutdown schedules and associated production losses.

Table 1. Comparison of corrosion protection methods						
	HVTS	Welding	Organic coating			
Corrosion resistance	High	High	Medium (temperature and % concentration dependent)			
Erosion resistance	High	Medium (depending on alloy)	Medium (material dependent)			
Typical alloys utilised	Modified hastelloy and monel alloys	316, 625, 622, 52, monel, hastelloy with Fe dilution	N/A			
Bond	Mechanical and chemical (>35 MPa)	Metallurgical	Mechanical and chemical (> 15 MPa)			
Heat treatment before/after application	No	Yes (or HAZ becomes weak corrosion resistance area)	No			
Dilution into base metal	No	Yes	No			
HAZ	No	Yes	No			
Stress/distortion of base material	No	Yes	No			
Application speed	32 – 64 ft² (3 – 6 m²) per shift/machine	$5 - 21 \text{ ft}^2 (0.5 - 2 \text{ m}^2) \text{ per shift/machine}$	$53 - 107 \text{ ft}^2 (5 - 10 \text{ m}^2) \text{ per shift/gun}$ and variable curing time			
Repairability	Blast prep, build-up and/or local reapplication	Blast prep, grind and re-weld if not cracked/contaminated	Blast, surface preparation and reapplication			
Durability	Mechanically tough and resistant to high temperatures	Mechanically tough	Vulnerable to mechanical and heat damage			
Steam-out resistance	Yes	Yes	No			
Thermal resistance	> 932°F (500°C)	> 932°F (500°C)	< 284°F (140°C)			
Curing requirements	Not required	Not required	Up to five days			
Application requirements	Minimum environmental controls	Minimum environmental controls	Strict environmental controls (including temperature, humidity, surface salts, amine bloom, surface release)			
External inspection capability during normal operation	Yes	Yes	No			

Temperature and chemical compatibility limitations have prevented the effective use of organic coatings. Due to the nature of the sour feed, loss of containment poses a major safety and environmental risk.

The gas plant in the Middle East chose to use an alloy cladding solution to fix the issue of corrosion in its amine process columns. This solution provides the same benefits as a high-nobility weld overlay corrosion barrier, with several additional advantages including no HAZ or requirement for PWHT; no distortion of base materials; and a rapid application speed. The following section will discuss the results of the application of HVTS to two of the columns vs the low velocity thermal spray applied by a local contractor to six of the columns in 2016.

### The inspections: high velocity vs low velocity thermal sprays

The first inspection of the two columns protected by HVTS took place in 2018, with no signs of further corrosion. The protective cladding was in excellent, as-applied condition. Further inspection by the plant's senior corrosion engineer in November 2021 revealed a significant contrast between the two columns sprayed with HVTS in 2015 and the other columns applied with the low velocity thermal spray in 2016. The HVTS



**Figure 4.** The 2021 inspection of the six columns coated with a low velocity thermal spray shows severe corrosion and risk of failure.



Figure 5. HVTS application.

was still in excellent condition, with no signs of cracking or failure. However, the other columns sprayed with the low velocity thermal spray showed extreme signs of breakdown of the applied cladding and corrosion of the substrate, with the wall thickness loss threatening to exceed its maximum corrosion allowance.

If left, the ongoing corrosion could result in an unplanned shutdown, potentially costing millions of dollars in lost revenue. In the best-case scenario, the column would need to be stripped of the remaining cladding, undergo mechanical repairs (which is both costly and time consuming), and then be protected with a long-lasting HVTS.

#### The science

This scenario is a common occurrence at many oil and gas plants, refineries and petrochemical sites. Although the initial cost is often far less, the long-term expense outweighs the short-term savings. To understand why the low velocity system failed, it is important to understand the science behind various types of materials and application methodology.

#### Material modification

Standard welding alloys are unsuitable materials for thermal spray application in critical internal process equipment, as the cladding particles form oxides on their surface in flight, creating a fundamental weakness in the microstructure and permeability.

#### True high velocity application technology

HVTS conveyance technologies atomise the bespoke wire feedstock in a supersonic gas stream, producing a cladding that consists of flat and tightly-packed, micro-sized particles. Conventionally-available thermal spray application systems cannot produce equivalent particle sizes — they have a more open microstructure and do not impart sufficient energy to flatten the particles that are inherently highly stressed. These shortcomings lead to premature failure due to permeation from microstructural weaknesses and cracking of the coating.

#### Conclusion

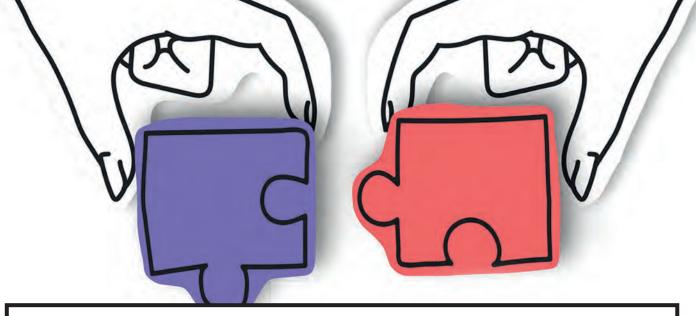
The high cost of corrosion for refineries around the world emphasises the importance of asset maintenance and protecting process materials from degradation and loss of performance. Unplanned shutdowns can have a significant financial impact in terms of lost productivity and emergency remedial works.

There are several solutions available on the market today, namely weld metal overlay (WMO), which is a reliable albeit time consuming and costly method. Thermal spray is another solution which, in theory, is a better alternative to WMO but can lead to premature failure. HVTS is the next evolution of thermal spray coatings which provides reliable, long-term protection from corrosion.

As asset failure continues to be a costly problem for the downstream oil and gas industry. It is crucial that preventative measures are taken to improve asset life, reduce downtime, and deliver significant savings.

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# The material selection puzzle

**Karen Picker, Alleima, USA,** explains the thought that goes into selecting the optimum material for heat exchangers.

number of different types of heat exchangers are used in the petrochemical and chemical industry to add or remove energy from a process. These include coolers, condensers, evaporators, preheaters, reboilers, and air coolers.

The transfer of energy can happen between two different process fluids, or in cases where energy needs to be added to the system, an external heating source such as steam can be used to heat the fluid. If, on the other hand, energy needs to be removed from the system, this can be dissipated using an external cooling source such as water or air.

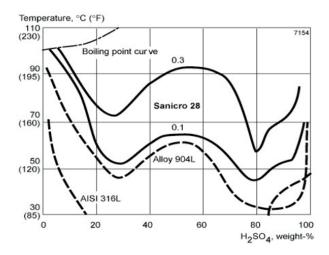
Heat exchangers are categorised depending on the type of process fluid, physical changes happening to such fluid, and whether a cooling or heating medium is being used. However, the overall transfer of energy concept remains.

For example, in general, when the fluids on both sides of the metal are single-phase and are both process streams, the equipment is simply called a heat exchanger. However, if the aim is to reduce the temperature of a process stream using water or air, this equipment is known as a cooler. Condensers, on the other hand, use cooling water or air as the cooling media. In this case, the process fluid on the other side of the tube is a vapour stream that condensates due to the temperature drop that it is being exposed to. Finally, heaters and reboilers carry a process fluid on one side of the tube, and steam or hot oil on the other side of the tube, which is used to bring the process fluid up to the desired temperature.\frac{1}{2}

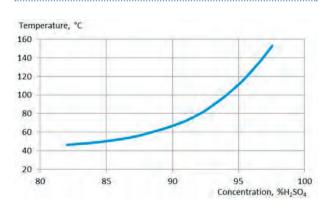
Given the complexity of the application, choosing the right material for the construction of heat transfer equipment is important for reliable operations. The selected grade must offer



adequate corrosion resistance combined with mechanical and physical properties that are able to withstand variations in temperature, pressure, and the aggressiveness of the process fluid. Some of the more common corrosion issues that cause premature failures in heat exchangers are general or uniform corrosion, pitting, crevice, under deposit, and erosion corrosion.



**Figure 1.** Isocorrosion diagram for Sanicro 28 in. deaerated sulfuric acid with corrosion rates of 0.1 and 0.3 mm/yr. For alloy 904L and AISI 316L, the curves represent a 0.1 mm/yr corrosion rate.



**Figure 2.** Isocorrosion diagram, 0.1 mm/yr, for Alleima SX base in concentrated  $\rm H_2SO_4$  at static conditions.

Table 1. Minimum PREN values for commonly

used Alleima stainless steel grades						
Alleima Grade	PRE	Cr	Мо	N		
304L	18	18	-	-		
316L	24	17.5	2.1	-		
Alloy 825	28	20	2.5	-		
SAF 2205	35	22	3.2	0.18		
Sanicro 28	39	27	3.5	-		
254 SMO*	43	20	6.1	0.2		
SAF 2507	43	25	4	0.3		
SAF 2707 HD	49	27	4.8	0.4		
Sanicro 35	53	27	6.5	0.3		
*2E4 CMO is a trademark owned by Outokumpy OV						

#### **General corrosion**

General corrosion takes place when the material is exposed to strongly acidic or alkaline solutions and a uniform mass loss per unit surface area occurs. General corrosion is expressed as mean metal loss per unit time in millimeters per year (mm/yr) or milli-inch per year (mpy).

Isocorrosion curves are typically used to represent the resistance of the metal to the intended service conditions. For example, to select material for a heat exchanger in sulfuric acid ( $H_2SO_4$ ) service with 93 – 98.5% concentration, operating temperatures of between 60 – 120°C in the shell side, and cooling water at temperatures between 25 – 45 °C in the tube side, the isocorrosion curve shown in Figure 1 offers good guidance to start material selection based on the shell side process conditions.

This figure shows the isocorrosion curve of three different grades in H<sub>2</sub>SO<sub>4</sub>. Sanicro® 28 is shown with two curves representing 0.1 and 0.3 mm/yr corrosion rates. Alloys 316L and 904L are shown with dashed curves, representing a 0.1 mm/yr corrosion rate. This isocorrosion graph suggests that Sanicro 28 performs better at different temperatures and concentrations of H<sub>2</sub>SO<sub>4</sub>. However, should one of these materials be used under the process conditions presented in this case, the high concentrations and temperature of the acid will cause premature failure of the bundle.

For  ${\rm H_2SO_4}$  services with high concentrations (> 90%) and high temperatures, silicon-based alloys such as Alleima® SX are a better choice, as shown in Figure 2. When selecting material, it is important to characterise the entire system and take into consideration contaminants and the corrosivity of both the shell side and tube side. In this instance, the cooling media used in the tube side is water. Depending on the level of chlorides present in this water, silicon-based alloys might not be the right choice, since their pitting resistance is not sufficient if the chloride content in the water is higher than 100 ppm.

#### **Pitting corrosion**

Pitting corrosion is a type of localised attack on a small area of the metal surface due to localised breakdown of the passive film, usually caused by the presence of chlorides. Pitting corrosion is most likely to initiate at weak points such as weld heat affected zones or at surface defects and inclusions. Controlling the concentration of aggressive ions such as chlorides and pH, and selecting alloys with the right chemical composition, are key to addressing or preventing pitting corrosion.

Seawater coolers used in the process industry, or gasifiers used in the LNG industry, are examples of the types of equipment that are commonly affected by this form of corrosion. Seawater contains large amounts of sodium chloride (NaCl) and solid particles, such as sand and organic solids. As a result, it is more likely to induce pitting corrosion in the metal. However, even equipment that uses freshwater or city water can be prone to this issue.

When selecting material for chloride-bearing environments, the Pitting Resistance Equivalent Number (PREN) of each grade can be compared to ease the decision making process. The PREN is calculated using equation 1, which relates the alloy's chromium (Cr), molybdenum (Mo), and nitrogen (N) content, with its resistance to pitting corrosion. This number is used for



an approximate ranking of stainless steels in chloride-bearing environments, as shown in Table 1. The alloys with the higher PREN are expected to have a higher resistance to pitting corrosion when exposed to the same environment.<sup>2</sup> However, the alloy's mechanical properties and the expected operating temperatures of the equipment must also be considered.

$$PREN = %Cr + 3.3%Mo + 16%N$$

For example, duplex stainless steels (DSS) are a great choice for seawater cooling applications in the process industry, due to their excellent mechanical properties (which make them more resistant to erosion corrosion), and their high PREN (which indicates their high pitting resistance). Moreover, the operating temperatures of heat transfer equipment in the process industry are typically well within the temperatures that DSSs are designed for (-50  $-280\,^{\circ}$ C).

However, in the case of LNG gasifiers, for example, this family of alloys is not a good fit due to the cryogenic temperatures that the application sees. In this case, the new grade programme for LNG from Alleima, including Sanicro® 35 (a new family of super austenitic [highly-alloyed] seamless stainless tube with 5 – 7% Mo) would be the right material choice due to superior corrosion resistance and high mechanical strength – even at cryogenic temperatures.

Another way to select the most appropriate material for heat exchangers based on the equipment operating temperature is to evaluate grades by their Critical Pitting Temperature (CPT). CPT is the temperature determined through accelerated laboratory testing such as ASTM G48 (6% FeCl<sub>3</sub> solution), at which a material is expected to initiate pitting corrosion. CPT values are specific to the environment and the test method used. When comparing alloys, it is important to note the environment in which the test was performed. In addition to pitting corrosion, the corrosive seawater used in this LNG application usually presents the challenge of crevice corrosion in the tube-to-tubesheet section of the equipment. However, these grades can substantially extend the service life of vaporisers, without the need to upgrade the entire equipment to high nickel grades such as Alloy C-276.

#### Crevice and under-deposit corrosion

Crevice corrosion occurs due to oxygen depletion in the localised environment that prevents the re-passivation of the alloy and promotes the formation of a corrosive cell. The

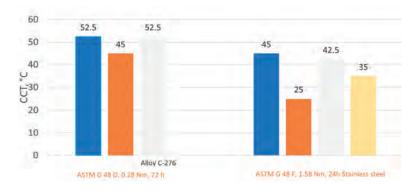


Figure 3. Comparison of CCT of different alloys in ASTM G48 - D, F.

difference between this and pitting corrosion is that crevice corrosion, as the name suggests, will always initiate at crevices found in the equipment, due to design limitations or flaws.

For shell and tube heat exchangers, the weak point is the tube-to-tubesheet interface on the shell side, which happens to be the problem area for LNG vaporisers. Another form of crevice corrosion found in heat exchangers is one that forms under deposits. Salt deposits and fouling are common causes of the failure of heat exchanger tubes. Ammonium chloride (NH $_4$ Cl) and sodium chloride (NaCl) salt precipitation are common in refinery processes. While the best way to address salt deposits is to prevent salt formation in the first place, this is not always achievable, as this requires adjustments to the process operating parameters, which may impact the overall efficiency of the process. Generally, a higher alloyed grade will have better resistance to under-deposit corrosion, and similarly to pitting corrosion.

One test that can be used to indicate the crevice corrosion resistance of different alloys is ASTM G48 methods D and F. These methods help to determine the critical crevice temperature (CCT) of the alloy when exposed to a 6% FeCl<sub>3</sub> solution utilising a crevice former. Method D, which is intended for testing nickel alloys, utilises 0.28 newton-meter (Nm) force applied for 72 hours. Method F, as designed for the testing of stainless-steel grades, requires the use of 1.58 Nm force for 24 hours. Figure 3 shows a comparison of the CCT of different alloys from 6Mo grades to high nickel alloys in the two test methods. Both tests demonstrate how the high-alloyed super austenitic grade Sanicro 35 has superior performance in crevice corrosion to that of high-nickel grade Alloy 625, and similar performance to Alloy C-276.

### Advancing through materials technology

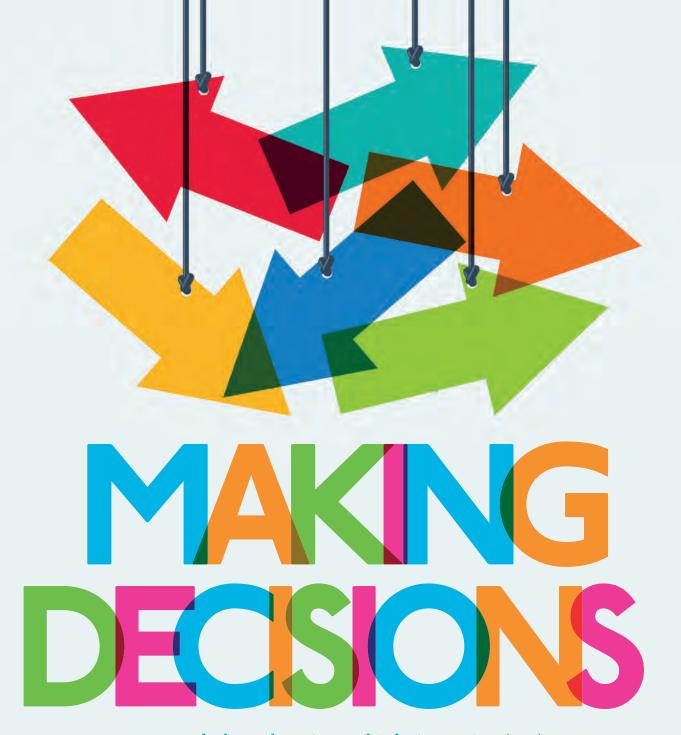
Heat transfer equipment is instrumental in the petrochemical and chemical process industry. A significant part of its reliability depends on proper material selection for the intended service conditions. When selecting material, it is important to take each piece of the puzzle or, in this case, the process streams, and analyse how their characteristics will impact the equipment's performance in service.

The very first step of the process includes evaluating whether the material of choice is resistant to the general service that the equipment will be used in (i.e. sulfuric acid, nitric acid, or hydrocarbons). However, the material selection process does

not stop there. The material selector must also account for the possible causes of localised corrosion. While some of the issues can be prevented or addressed through design and operating parameter adjustments, these options are not always feasible. Selecting higher alloyed materials with proven increased corrosion resistance is the logical approach. Standardised tests, isocorrosion curves, and innovative material solutions exist to help ease the process.

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# **Byron Black, Koch Engineered Solutions, USA,** details the reasons for choosing a hairpin heat exchanger.

here are many different types of heat exchangers on the market today, but the traditional go-to tubular option for the process industry is the Tubular Exchanger Manufacturers Association (TEMA)-style shell and tube. Shell and tube exchangers are versatile in that they are capable of handling a wide range of process conditions in an economical way. Additionally, due to the fact that they have been around for more than a century, they are well known and ubiquitous in most plants. However, there are cases where another exchanger type, such as a hairpin (double pipe or multitube) heat exchanger, is a more efficient, cost-effective option.

In simple terms, a hairpin exchanger is a long, skinny, single-pass shell and tube heat exchanger that has been folded in half, giving it a hairpin configuration. All connections, shell side and tube side inlet and outlet, are located at the front end

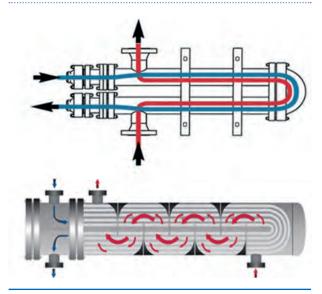
of the exchanger, and a bonnet covers the U-bend end of the exchanger. While a conventional shell and tube exchanger bundle is removed from the front end of the exchanger, the bundle of a hairpin exchanger is removed from the back end of the exchanger by first disconnecting the bolting on the front end of the exchanger, then removing the bolts connecting the bonnet on the back end of the exchanger, and finally detaching the bundle.

There are numerous reasons for considering a hairpin heat exchanger rather than a conventional shell and tube. A long-held paradigm exists that hairpins are exclusively for small surface area requirements with small shell diameters. For many years, this translated into a preconceived notion that hairpins should only be specified when the surface area required is 500 ft² or less. Anything larger should be specified as a shell and tube. This rule of thumb is long outdated, and hairpin

heat exchangers are now designed and sold with shell diameters up to – and even exceeding – 36 in., and surface areas in excess of  $10\,000\,\mathrm{ft^2}$ . It is the process conditions and



**Figure 1.** Cutaway showing details of a hairpin heat exchanger.



**Figure 2.** Top: counter-current flow hairpin. Bottom: conventional shell and tube with counter-current/co-current arrangement.



Figure 3. Top and middle: tube inserts.
Bottom: TWISTED TUBE® Heat Exchanger tubes.

unique mechanical features of the hairpin that dictate when one should be used, rather than the required surface area.

As the old guidelines are no longer valid, designers should question when a hairpin should be considered over a conventional shell and tube. The answer can be broken down into two categories: process optimisation and mechanical integrity.

#### **Process optimisation**

Many heat exchanger applications, such as feed-to-effluent or lean-to-rich applications, are geared towards maximising heat recovery. The desire is for the outlet temperature of one stream to get as close as possible to the inlet temperature of the other stream, which is also known as the approach temperature. This often results in a temperature cross, which occurs when the outlet temperature of cold stream is higher than the outlet temperature of the hot stream. In other words, the temperatures of the hot stream and the cold stream cross inside the exchanger at some point.

The optimal way to handle a temperature cross is with true counter-current flow, which is defined as having the shell side and tube side fluids moving in opposite directions of each other through the exchanger. Counter-current flow maximises the temperature difference between the streams through the entire length of the heat exchanger.

In a conventional shell and tube heat exchanger design, multiple tube side passes are typically employed, resulting in a combination of co-current and counter-current passes with the shell side fluid. In this arrangement, multiple shells in series are typically required to achieve the temperature cross by avoiding a temperature cross in any single exchanger.

A counter-current flow arrangement is also achieved in a TEMA 'F' style shell, which employs a longitudinal baffle on the shell side, effectively dividing the shell side in half. By routing the shell side flow through two passes instead of one, counter-current flow can be achieved in the exchanger. However, in order to prevent bypass of the shell side fluid from the first shell pass to the second shell pass, the use of seal strips to seal the long baffle to the shell ID is required. As these components are made from a thin metal, the required removal and reinsertion of the bundle for cleaning and maintenance can lead to damage of the seal strips over time. This results in shell side fluid bypass, which can significantly degrade the performance of the heat exchanger. For this reason, the use of TEMA 'F' shells is not allowed in many plants.

As a hairpin exchanger matches a single shell side pass with a single tube side pass, counter-current flow is achieved, maximising the temperature efficiency without requiring multiple shells or a TEMA 'F' style shell.

In addition to counter-current flow, hairpin vendors often have tools to optimise the design that can increase the heat transfer coefficient, reduce shell side pressure drop, and eliminate flow-induced vibration. These include:

- Low pressure drop tube supports.
- Longitudinal fintubes.
- Various tube inserts.
- TWISTED TUBE® Heat Exchanger tubes.

Longitudinal finned tubes are utilised in applications that are shell side controlled, meaning that the shell side heat



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transfer coefficient is much lower than the tube side heat transfer coefficient and thus controls the design of the exchanger. Adding fins increases the surface area to compensate for the low coefficient.

Tube inserts can be used to enhance the tube side heat transfer coefficient either by inducing swirl flow for high viscosity or vaporising fluids, or by blocking flow area to increase velocity.

TWISTED TUBE® Heat Exchanger tubes act in a similar way to a swirl flow type insert on the tube side of the heat exchanger, thus increasing the tube side coefficient, while the shell side generally flows in a longitudinal, interrupted swirl flow path.

#### **Mechanical integrity**

The most significant differences between a hairpin heat exchanger and a conventional shell and tube are the configuration and available closure technologies. The configuration of a hairpin provides a number of advantages over that of a conventional shell and tube, such as:

 Large radius U-bends allow for tube side cleaning and the ability to handle the thermal expansion from large



Figure 4. Hairpin bundle with large radius U-bends.





**Figure 5.** Top: removable bonnet. Bottom left: external split ring closure design. Bottom right: internal split ring closure design.

- tube side temperature differences, unlike the much smaller U-bend radii of a U-tube style shell and tube exchanger.
- Tube side and shell side nozzles are on the same end of the exchanger, which not only simplifies piping, but also reduces thermal stresses on the shell side nozzles in the event of expansion or contraction of the shell.

Closure technologies for hairpins differ as compared to the various TEMA designations and result in these advantages:

- Separate, independent terminal tube side and shell side closures address applications with high terminal temperature differences and/or cyclic conditions resulting in thermal shock. These separate closures result in smaller flanges, thinner tubesheets and smaller bolts. This is a significant advantage in high-pressure applications.
- External bolting: all bolting on a hairpin heat exchanger is external and can be tightened while the exchanger is in operation. TEMA-style floating head designs use internal bolting that comes in contact with the shell side fluid, and cannot be tightened unless the tube bundle is pulled or the floating head cover removed – both of which require the process to be shut down.
- The return bonnet closure is a compact through-bolted design, allowing for visual inspection of the shell side condition of the U-bends without removing the tube bundle or disconnecting the piping.
- High-pressure closure technology: the closure technologies offered by various hairpin vendors are unique to each vendor. However, each typically has a high-pressure closure offering. Although TEMA-style closures are often limited to pressures of below 3000 psi, hairpin closure designs have been used for pressures of up to 11 000 psi. This is particularly applicable to offshore well stream heaters as oil and gas producers seek to harvest reserves in deeper waters.

Another point to consider is that, unlike TEMA, there is no standard that dictates the model designations, nomenclature or closure types for hairpin heat exchangers, so it is recommended that users do their due diligence on the closure technologies being offered. For example, through bolting vs studs, external split rings vs internal, and separated head vs single bolted closures are all things to consider.

#### **Conclusion**

For hairpin heat exchangers, the industry standards include API 663, ISO 12212 and PIP VESHP001. Many manufacturers also have their own standards, which can be requested to ensure that they are suitable for the particular application in mind. In summary, operators should consider a hairpin when one or more of the following conditions exist:

- A temperature cross or a close temperature approach is desired.
- High-pressure tube side conditions.
- Cyclic or thermal shock conditions are present.
- High terminal temperature differences exist.
- Operators wish to avoid the use of an expansion joint.
- Ability to clean U-tubes is required.
- All external bolting is desired.
- An augmentation device would improve heat transfer or reduce pressure drop.

# DRIVING THE WAY FORWARD

#### Tom Starr, Tommy Chen and Anupam Prakash, Nalco Water, an Ecolab Company,

discuss how to drive productivity and profitability with digitally-enabled insights.

n energy and chemical processing, productivity and profitability are directly tied to water and energy efficiency. Heat exchanger performance is one key component behind ensuring efficiency. Industrial businesses can manage their heat exchanger performance more effectively with digital diagnostic tools and data-driven visibility.

Chemical processors and energy companies constantly strive to operate safely and sustainably while meeting productivity and profitability goals. One way to achieve these objectives in tandem is to ensure that equipment is well maintained so that it can operate efficiently with minimal downtime. Although maintenance downtime and costs are unavoidable, companies can detect anomalies by

closely monitoring performance data and acting before situations escalate.

Advancements in digital technology are enabling companies to gain better visibility into their operations, including asset performance and operations efficiency. Using predictive analytics and other data-driven tools, companies can mitigate the loss of production, avoid unscheduled downtime, and ultimately improve business outcomes.

Water systems are a prime example of where companies can integrate digital technology to optimise their daily operations. Cooling water systems are an integral part of the production process, and yet the heat exchangers that utilise this process are often monitored manually or not at all, typically with less scrutiny than other critical equipment.



Often, this is due to a lack of readily-available data, which makes predictive maintenance (such as cleaning or retubing a heat exchanger) challenging to track and manage.

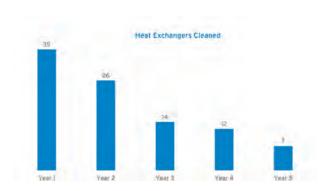
To address these challenges, Nalco Water, an Ecolab Company, offers a holistic approach that combines



**Figure 1.** A visual of the OMNI Heat Exchanger Reliability digital analytics solution.



**Figure 2.** Diagram illustrating all components of the OMNI Heat Exchanger Reliability program.



**Figure 3.** Chart illustrating how OMNI Heat Exchanger Reliability reduced the frequency of heat exchanger cleaning from 35 to 7 times per year.

continuous data acquisition with digital technology. Specifically, Nalco Water's OMNI<sup>TM</sup> Heat Exchanger Reliability program, powered by the ECOLAB3D<sup>TM</sup> intelligence platform, leverages IoT data and advanced analytics to continuously measure heat exchanger performance.

To implement OMNI Heat Exchanger Reliability, the teams at Nalco Water survey the full plant strategically with various survey frequencies on different heat exchangers, according to their situations. A stress profile of system heat exchangers is created with a comprehensive flow and temperature survey. The survey provides a snapshot of heat exchanger stresses and helps to identify critical exchangers. Then, using non-invasive sensors and proprietary diagnostic tools, Nalco Water provides continuous on demand visibility of critical heat exchanger and water treatment system performance. Working collaboratively with plant operators, OMNI data helps to optimise the chemical and mechanical operations within the heat exchange process. OMNI Heat Exchanger Reliability communicates using the same platform as other OMNI premium services and water management systems, such as 3D TRASAR<sup>TM</sup> automation and control technology. When combined, these solutions help companies to gain a detailed view of their enterprise utility operations. The ECOLAB3D platform and OMNI performance information is readily available, 24 hr/d.

Recognising the substantial benefits of integrating tools that provide greater visibility, many chemical processors and energy companies have already implemented solutions such as the OMNI Heat Exchanger Reliability into their daily operations.

# Optimising maintenance at a US petrochemical plant

In one example, a North American petrochemical plant routinely cleaned a large number of cooling water heat exchangers as part of its normal maintenance practice. However, the company lacked metrics and performance data to make precise performance evaluations. Without sufficient data to determine whether an exchanger needed to be cleaned, numerous exchangers were routinely cleaned unnecessarily, wasting company time and resources.

To resolve the inefficiency in the maintenance cycle, the company worked with Nalco Water to optimise its cooling water process. Through a comprehensive cooling system audit, the plant could review the performance data of each heat exchanger and rearrange the cleaning schedule. The company could then prioritise cleaning the heat exchanger, and eliminate unnecessary maintenance.

An assessment conducted with OMNI Heat Exchanger Reliability discovered that 95% of the plant's heat exchanger issues were due to iron scale accumulation on the cooling water inlet tubesheet, which caused heat exchangers to experience excessively low water velocity and high skin temperature.

Working closely with plant personnel, the Nalco Water team collected water samples and ran multiple what-if scenarios in its Cooling Water Optimizer (CWO) modelling system. The company proposed a series of recommendations, including upgrading to a patented high-charged polymer scale inhibitor to minimise mineral scaling issues, as well as

implementing a plant-wide backwashing programme for all capable heat exchangers. In addition to this, the plant began to use OMNI Heat Exchanger Reliability data to closely monitor heat exchanger performance in daily operations.

The company halted unnecessary cleanings and significantly increased production time and efficiency. By year five, total heat exchangers cleaned per year were reduced from 35 to 7, while maintaining unit performance and reliability. This resulted in an 80% reduction in cleaning costs, which translated to approximately US\$600 000 in annual cost savings.

## Avoiding downtime at a Texas VCM plant

In another example, a chemical plant in Texas, US, that produces vinyl chloride monomer (VCM) uses propylene as a refrigerant to selectively condense impurities, allowing them to be removed later in the process. The plant produces more than 4 million lb/d of VCM, and the propylene refrigerant condenser is critical for maximising process efficiency. If the propylene is not efficiently condensed, impurities are not removed effectively, resulting in production inefficiency or operational shutdowns.

The plant experienced a near unplanned shutdown, and a decision was made to remove the condenser from service for cleaning. During the 90-day period before maintenance, the site operated at increasingly greater load reductions, which was ultimately at about 10% of the nominal production capacity. Production loss was quantified at

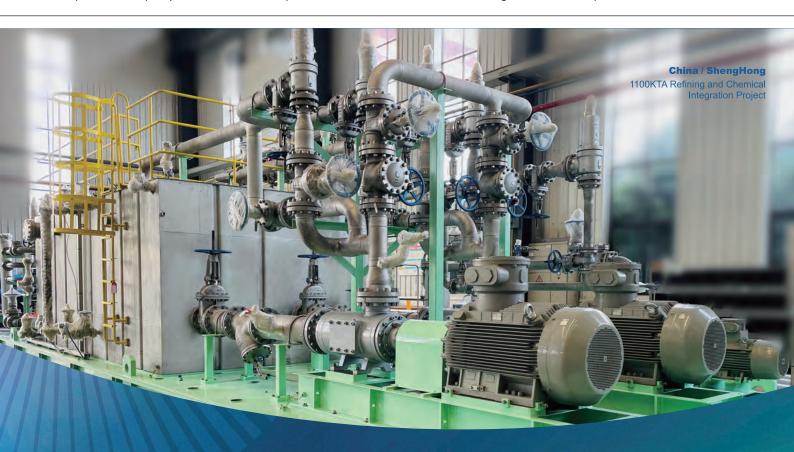
approximately US\$3.6 million during this period. After performing an inspection and analysing available data, the producer and Nalco Water determined that the cooling water inlet tubesheet had likely accumulated debris, causing decreased cooling water flow. OMNI Heat Exchanger Reliability was installed, enabling the producer to track the performance and detect debris accumulations before they disrupted condenser efficiency and caused production losses.

With this program, the team also discovered that the condenser was using approximately 25% greater-than-design cooling water flow. The program calculated U-Value trends, determining that less cooling water flow would not significantly decrease condenser heat transfer efficiency. As a result, the Nalco Water team suggested that the customer manually reduce the cooling water flow to the propylene condenser and redirect excess flow to other heat exchangers in need

With all of the recommendations provided by OMNI Heat Exchanger Reliability, the plant made critical data-driven decisions concerning how the propylene condenser must operate to achieve maximum efficiency and productivity. Nalco Water helped the company realise estimated savings of over US\$5 million/yr.

## Discovering hidden risks in a US petrochemical plant

Another large North American petrochemical plant, located on the Gulf Coast, was struggling to track the status of over 1000 heat exchangers. The risk of unplanned shutdowns due



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to heat exchanger failure could have cost the company millions of dollars in both lost production and environmental penalties. To address this potential risk, the company collaborated with the Nalco Water team to implement the OMNI Heat Exchanger Reliability program in its operations.

The first step was to collect and validate the data for all heat exchangers across the company's facilities. The performance data was loaded into the program on the ECOLAB3D platform.

The solution detected a 90% decrease in the designed water velocity of a critical heat exchanger. After further investigation, the team discovered that the inlet tubesheet



**Figure 4.** Debris in the inlet of the critical heat exchanger.



**Figure 5.** Cooling tower fill observed in the heat exchanger.

of the heat exchanger was obstructed with cooling tower fill that was drawn into the system during routine cooling tower maintenance. The issue was corrected by removing the debris, which returned the heat exchanger to its design cooling water flow. The corrective action ensured asset performance and operation reliability. The plant saved over US\$1 million in production losses and approximately US\$50 000 in heat exchanger replacement costs. These savings were generated by correcting just one critical issue. With more than 1000 other heat exchangers, the plant stands to save additional costs and decrease downtime in the future.

## Avoiding revenue loss due to microbiological fouling

In another example, when a nitrogen producer based in North America decided to expand its production cycle, this increased stress on the company's assets, including heat exchangers. Because the facility used unfiltered river water as a make-up water source and consequently had a history of fouling, the company decided to implement OMNI Heat Exchanger Reliability in its process to closely monitor the conditions.

The Nalco Water team started with a comprehensive survey that compared current heat exchanger operations to historical and design data. The survey indicated that the monoethanol coolers were the most stressed heat exchangers in the system. To better understand the situation, the team installed OMNI Heat Exchanger Reliability sensors on the coolers to extract additional performance data and insights.

During the first three weeks after the sensors were installed, the performance data remained steady. In week four, however, plant operators observed a slight but consistent decrease in U-Value. After correlating chemistry indicators, the cause was determined to be microbiological fouling. Microbiological slime is one of the most insulating substances encountered in cooling water systems. A customised system of bio-cleaning was implemented, and the U-Value gradually returned to a value that was sufficient enough to enable maximum production through the next planned outage. As a result of OMNI Heat Exchanger Reliability, the company was able to proactively detect the anomalies and prevent production loss.

#### **Conclusion**

Digital tools such as OMNI Heat Exchanger Reliability provide a new perspective for chemical processors and energy companies pursuing enhanced productivity and reliability. With access to strategically-obtained heat exchanger data, producers have increased visibility on the location of problem areas, which allows for implementation of proactive corrective actions. Although heat exchanger performance is only one component of an entire production process, optimising it with the support of digital predictive tools brings substantial benefits to the entire process. As more companies choose to embrace this new trend, there is no doubt that digitalisation and predictive analytics from services such as OMNI Heat Exchanger Reliability help improve production processes and create new industry standards.

# Treating your sulfur storage pits right

**Thomas Kline, Structural Technologies, USA,** details the process of hardened sulfur and carsul removal from below-grade reinforced concrete sulfur storage pits.

elow-grade reinforced concrete sulfur storage pits provide containment and bulk conveyance of molten sulfur products in the elemental sulfur process stream. With the appropriate detailing, these critical equipment assets can provide long-term service in incredibly harsh process environments, allowing for dependable process throughput. Unfortunately, either due to cold temperature environmental conditions, power interruptions, and/or process upsets, the realisation of a cold sulfur pit with hardened sulfur and carsul deposits (a byproduct delivered in the process stream) can be a source of major anxiety for sulfur process professionals and plant management.

#### The nature of elemental sulfur

Historically, sulfur was also called brimstone, which means 'burning stone'. In the past, it was mined from deposits associated with volcanic activity. Presently, most elemental sulfur is produced as a byproduct of removing sulfur-containing contaminants from natural gas and petroleum processing/refining streams by the largest producers in the world (Kazakhstan, Russia, Canada, Qatar and the US).<sup>2</sup>

#### Sulfur containment safety

Prior to working in and around any sulfur recovery unit (SRU) infrastructure, a safety execution plan (SEP) should be developed that identifies task hazards, as well as environmental and ergonomic concerns associated with the planned scope of work (SOW). Essentially, the SEP establishes a series of steps/practices that closely follow industry best practices and Occupational Safety and Health Administration (OSHA) safety protocols to ensure worker safety and environmental stewardship. The SEP is integral to the daily toolbox meetings, along with manager/supervisor safety audits, in order to

educate, inform and implement task hazard analysis checkpoints associated with the SOW.

When reviewing molten sulfur containment, several 'red flags' surface regarding safety, due to the fact that sulfur and sulfurous compounds are frequently corrosive to materials that they are in direct contact with. Specifically, containment materials that are typically unreactive to molten and/or sulfur cake forms are often readily attacked when sulfur co-mingles with moisture/water sources. The result of these materials co-mingling is the formation of acidic compounds that can be corrosive, especially when contact occurs at elevated temperatures. When hardened sulfur cake needs to be removed from sulfur containment structures, mechanised equipment (i.e. skid-steers, backhoes, excavators, etc) should be employed for the most part, and craft labour used in those areas that are inaccessible by mechanised equipment – wherever possible. The goal is to minimise the exposure of craft labour to known task hazards and reduce, when possible, the level of personal protective equipment (PPE), by employing engineering controls.

Sulfur differs from most combustible dust by having a relatively low autoignition temperature of 482°F (250°C), and a flash point of 405°F (207°C). The handling of solid sulfur in pits and tanks can create a dust cloud which can then produce a static charge among the air-suspended sulfur particles. The static discharge can readily cause ignition of the dust cloud and create explosive conditions, and sulfur dust explosions do occur in the refining and gas industry. Research has determined that dust concentrations of as low as 35 mg/l of sulfur dust in air are explosive.<sup>3</sup>

Owing to the pyrophoric nature of sulfur cake and metals affected by sulfurous contact, moisture must often be used to provide spark/fire suppression during hardened sulfur cake removal. The working

surface should be kept wet so that dust is not allowed to accumulate. A slight spray of water should be applied to the working surface prior to excavating the sulfur. A continuous spray is not necessary, but the sulfur should always be wet. Diligence in protective PPE usage and adhering to appropriate safety protocols by craft labour is key to reducing the possibility of acidic compound contact and providing overall hazard mitigation. Safe practices typically include the following:<sup>3</sup>

- Clean/dirty room dressing trailers and/or rooms for PPE gearing-up/removal.
- Single or multiple-use chemical suits, gloves and boots. External clothing that has become impregnated with sulfur should be removed or replaced.
- Duct-taped sealed seams at protective PPE transitions.
- Barrier skin cream application to potentially exposed skin 'patches' adjacent to respirator face and neck areas
- Full-face respirators, organic vapour/acid-gas and HEPA cartridge filters, or full-face supplied-air respirators.
- Individual personnel hydrogen sulfide (H<sub>2</sub>S) monitors attached within 12 in. (30 cm) of facial regions.
- Confined space retrieval/extraction body harnesses.
- Easy access or escape routes in the verified work area.
- Confined space air movement via high-capacity fans/air horns.
- Atmospheric testing that should include monitoring for sulfuric acid (Dräger Tubes) and sulfur dioxide (SO<sub>2</sub>) in addition to oxygen, LEL, etc.
- Use SO<sub>2</sub> analysers to monitor the atmosphere around the pit or tank. Since sulfur burns with a dim blue flame, it may not be detectable if the area is well lit.
- Eye washing stations.
- Emergency shower locations.
- Compressed air should not be used to remove or clean dust from any surface since the agitation may create a dust cloud.
- Ground all areas that may develop a static charge.
- Avoid use of plastic tarps that are not anti-static.
   General purpose plastic can generate a static charge that could ignite a sulfur dust cloud.





**Figure 1.** View of solidified sulfur in an extracted sulfur leg (left), and sulfur cake accumulated at the base of a sulfur pit that went 'cold' during a unit-wide power outage (right). Note the extensive damage to the sulfur pit walls due to sulfurous acidic attack exposing embedded steel bars (for reinforcement).

Hot surfaces can easily ignite dust clouds and/or dust accumulation on horizontal surfaces. The result of this can be a small fire that could ignite a dust cloud. Poorly ventilated electric motors, uninsulated steam lines, or electric lighting are examples of hot surfaces that can cause a fire.

It is also important to note that vacuum trucks should not be used in removing water and any hardened sulfur debris due to industry-reported fires and explosions associated with their use. Industry best practice is to diaphragm-pump (i.e. trash-pump) water out from within sulfur pits, and shovel remaining debris onto intrinsically-safe conveyors, or into waiting debris receptacles (i.e. tip-hopper dumpsters, wheelbarrows, or small buckets) rather than using vacuum removal techniques that can build and release static charges during operation.<sup>3</sup>

#### Typical approaches to 'cold' sulfur pits

The sulfur process stream is typically maintained in a molten state within sulfur pits via steam coils, steam-jacketed process lines, and heat-tracing. When molten sulfur temperatures fall below 250°F (121°C) for extended periods of time, molten sulfur solidifies and 'cakes'. In its solid form, sulfur can no longer be pumped but instead requires mechanical means and methods to dislodge the product from process piping, equipment and vessels (see Figure 1). While the degradation process involving sulfurous compounds is well understood in operating sulfur pits both metallurgically<sup>4</sup> and on cementitious products<sup>5</sup>, material corrosion will be initiated in the presence of moisture and oxygen in and around these civil/mechanical assets.

When plant operations determine reductions in sulfur pit operating process temperatures, difficult decisions are often made to raise internal sulfur pit temperatures. These measures can include using temporary heating coils (see Figure 2), placing new molten sulfur over the top of cooler sulfur products, or bypassing current storage containments in lieu of auxiliary storage vessels (i.e. adjacent sulfur pits, above-grade sulfur tanks, railcars, or heated barges). Having process bypass options is always prudent.

However, these attempts frequently fail to provide long-term relief from cold pits filled with caked sulfur and carsul.

### **Experience with cold sulfur pits**

Cold sulfur pits filled with sulfur cake are frequently thought of as something that can be remelted, and the product pumped from the pit into waiting containment vessels. Unfortunately, the inherent crystalline form of hardened sulfur makes solid sulfur an excellent insulator and therefore difficult to remelt on a large-scale. This is also why it can be hazardous to walk on top of a perceived hardened level of sulfur cake. There may in fact be 'hot spots' (i.e. still molten sulfur) below the crust of the sulfur cake that

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have not cooled sufficiently, due to this insulating characteristic. There have been reported incidents over the years of scalded contractors/operations personnel that have 'broken through' these hardened crust formations.

#### **Excavating sulfur cake and carsul**

When approaching sulfur cake and carsul removal activities, a project execution plan (PEP) needs to be developed and implemented, following the industry motto 'Plan-the-Work and Work-the-Plan'. A typical PEP will focus on the steps or 'milestones' during a project so that important features are not missed, and accountability is maintained so that efforts will be the safest and most cost-effective possible, and within the parameters set by the facility.

#### Case study: a dormant cold sulfur pit

A refinery in Midwest US was in the process of restarting a decommissioned SRU when it realised that a significant amount of hardened sulfur cake remained in the sulfur pit, along with underlying carsul deposits. Plant operators had very little success with remelting attempts using steam coil augmentation, and so they engaged contracting specialists for the removal of their hardened sulfur cake and carsul within the SRU's sulfur pit.





Figure 2. View of a cold sulfur pit filled with solidified sulfur cake at a roof slab portal location (left). The adjacent portal revealed temporary heating coils in-place, with little effect on melting subsurface sulfur cake deposits (right).





Figure 3. View of sulfur cake and carsul removal from a four-year decommissioned sulfur pit that was recommissioned and brought back online at a Midwest US refinery.

When reviewing project requirements, the use of mechanical excavating equipment was selected over manual excavation in accessible areas for sulfur cake and carsul removal. However, in difficult-to-access regions involving small sulfur pit access portals and around piping and process equipment, manual excavation 'means and methods' were employed. These efforts frequently require the workforce to use pickaxes, shovels, and small pneumatic chipping guns to remove hardened sulfur and carsul materials (see Figure 3). To provide effective spark suppression, water was sprayed onto sulfur cake surfaces to prevent these areas from drying out and becoming a source of fire ignition.

Excavated materials within sulfur pits are typically placed onto intrinsically safe conveyors, tip-hopper dumpsters, wheelbarrows, or even into buckets for removal, depending on access requirements. It should be noted that carsul has a higher specific gravity than molten sulfur, and settles to the bottom of the pit. When encountering carsul in sulfur pits, the deposit tends to be light-to-dark grey in colour and extremely hard when compared to the overlying sulfur cake. Carsul core sampling reveals these deposits to be frequently more than 5000 psi (35 MPa) in compressive strength. This hardness makes hydro-blasting carsul very difficult.

Additionally, carsul is a hydrocarbon byproduct and

requires removal to perform reinforced concrete repairs and to restore sulfur pits to their originally-designed volumetric dimensions. Often, during sulfur cake and carsul removals, concrete surface areas are exposed and repaired while the sulfur pit is down operationally. During an outage, mechanical process equipment (i.e. steam coils, pumps, etc) can also be evaluated and repaired and/or upgraded at that time. This was the case at this refinery, and 'just-in-time' engineering for concrete repair design detailing and 'hot shot' delivery of sulfate-resistant concrete repair materials was required which were site batched, placed, and cured on a 'fast-track' basis to meet outage schedule milestones. 👯

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# QUALITY CONTROL

**Felix Trainer, Servomex, Germany,** introduces an integrated quality control solution for gas cylinder filling.

ncreasingly, cylinder filling plants for industrial gases are looking to improve production output and efficiency by incorporating highly-automated gas quality measurements with fully digitalised data acquisition and monitoring systems.

Barcode scanners have become an industry standard to reduce paperwork documentation typing errors while increasing efficiency, and are widely used in production sites to identify and track the filling process of gas cylinders. This is in conjunction with the quality assurance laboratory information management system (LIMS), which allows the customer to digitally acquire and store information about the gas cylinder and its content.

Servomex's Multigas Analytical System (MAS) is an all-in-one solution that offers functionality,



expandability and integration with existing systems such as LIMS, in a package that is tailored to the customer.

The MAS works in conjunction with Servomex's proprietary Intuitive Gas Software (IGS), which is installed on a Windows PC to facilitate network integration. This PC supports the use of a remote barcode scanner, enabling the customer to scan gas cylinders and measure specified impurities. The IGS currently supports up to 40 measurements, with up to eight impurities per measurement.

In addition to the PC with IGS installed, the MAS consists of four 19 in. racks with partially orbital-welded and electropolished SS-piping, stream-switching diaphragm valves with multiple bypass flow meters for fast purge, two barcode scanners, and a number of gas analysers.

#### Gas analysers

The DF-745 SGMax, a digital moisture analyser optimised for diverse gas mixtures in specialty gas blending applications, measures trace water ( $H_2O$ ). The Gen-7 model is based around Servomex's tunable diode laser absorption spectroscopy technology, which delivers a broad measurement range of 0 – 100 ppm, with a lower detection limit (LDL) of 5 ppb – the lowest available without using a pump. Ultra-stable, zero drift



**Figure 1.** Servomex's Multigas Analytical System consists of four 19 in. racks including the SERVOPRO Chroma, MonoExact DF310E and DF745SGMax.



**Figure 2.** Based in Dagmersellen, Switzerland, PanGas AG is a major gas producer and the Swiss subsidiary of Linde plc.

sensing technology helps to extend calibration periods and reduce ongoing maintenance needs.

The moisture analyser includes a database of 17 standard background gases – with blends of up to eight gases – providing an adaptable solution for diverse application needs. Up to 30 custom gas mixtures can be predefined directly via the user interface.

The DF-745 SGMax is optimised for fast and efficient operation with pure and specialty gas blends, minimising downtime when switching between cylinder measurements, ensuring adaptable, high-performance analysis.

The MonoExact DF310E, a digital analyser designed specifically for accurate measurements of oxygen in industrial gas applications, delivers precise, trace-level measurements of oxygen (O<sub>2</sub>) to the MAS. Using a coulometric digital oxygen sensor, it offers enhanced user control and a reduced cost of ownership. It has analog and digital communication options – including Modbus and Profibus – for simple integration into a wide range of systems, and uses an icon-driven guided user interface for easy operation.

Multiple SERVOPRO Chroma models are used in the MAS to provide trace measurements of carbon monoxide (CO), carbon dioxide (CO $_2$ ), nitrogen (N $_2$ ), argon (Ar), methane (CH $_4$ ), non-methane hydrocarbon

(NMHC), and hydrogen ( $\rm H_2$ ). Offering a non-depleting plasma emission detector (PED), flame ionisation detector (FID), and thermal conductivity detector (TCD), the Chroma analyser is configurable to a wide range of applications, supporting these sensing technologies with gas chromatography techniques.

Sophisticated configuration and performance options are facilitated through a fully automated, tune-to-the-application system for simplicity of operation.

The Chroma's software permits full device interaction remotely via Ethernet/internet, and a full range of reporting options for simplified statistical data analysis.

#### Case study

Servomex supplied PanGas AG with an all-in-one solution that met demanding quality requirements for its gas cylinder filling facility in Dagmersellen, Switzerland. PanGas is a major gas producer and the Swiss subsidiary of Linde plc. Its operations are divided into the production of products through air separation, and their further processing operations. This involves the unloading, transfer and mixing of the gases, gas purification, and ultimately their recovery.

#### The challenge

PanGas is continuously striving to improve its processes and productivity within its gas cylinder filling facility, and was looking to replace its existing gas analyser with a future-proof solution capable of handling complex tasks.



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HYDROCARBON ENGINEERING A particular challenge that the company faced was the change between the different high-purity (Grade 6.0) gases and its tight specifications, since, for example, the main components of the first measurement interfered with the measurement results as secondary components of the second measurement.

PanGas selected Servomex's MAS to replace its existing gas analyser. This offers extensive functionality, expandability, and integration with existing systems such as LIMS, in a package tailored to the customer.

The MAS was installed on a Windows PC to facilitate network integration. This PC supports the use of two control stands in two separate parts of the PanGas facilities, each equipped with a touchscreen panel, wireless keyboard, and remote barcode scanner, enabling the customer to scan gas cylinders and measure specified impurities.

Different sources such as storage tanks, truck trailers, laboratory quick connectors, and the multi-gas cylinder station can be analysed sequentially by utilising a stream-switching valve box for distribution of the sample gas to the corresponding Servomex gas analysers, and forwarding the measurement results via serial interface to the IGS.

The solution used parts of the client's existing set-up by reusing the hardware of a 12-port multi-cylinder analysis station. A new, remote input/output module was used to implement the local operation and control of the existing actuators.

IGS allows the customer to perform one of the prepared measurement applications or a sequentially programmed measurement sequence, including one or more gas sources, enabling 24 hr/d production with the

measurement results automatically transferred into the LIMS system, without the need for paperwork. The MAS also allows the customer to perform single gas cylinder analysis by connecting gas bottles via Quick-Connector at the front of the cabinet and then starting the gas analysis via IGS by choosing the corresponding measurement application. The measurement data is then forwarded to the LIMS.

The adaptability of the IGS and the MAS allows PanGas to respond to changes in the product portfolio or add additional gas sources. The issue of changing between the different high-purity gases was also solved by a sophisticated purging process, which was developed and optimised in cooperation with PanGas.

#### **Conclusion**

The improvement of processes and productivity are essential for modern gas cylinder filling facilities. This relies upon accurate gas quality measurements supported by a high level of automation to ensure optimum output and efficiency.

The MAS delivers an all-in-one solution that meets demanding quality requirements, while the customer only needs to deal with a single supplier. It offers automated gas quality control that allows the customer to operate continuously, on a 24 hr/d basis, with a flexible approach to changes in the customer product portfolio.

The adaptability of the IGS and the MAS allows operators to respond to changes in the product portfolio or add additional gas sources. It is also possible to extend the system so that its functionality can be expanded as future applications arise.



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