Performance Evaluation of the Hydrotech Belt Filter in Intensive Recirculating Aquaculture Systems

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Introduction

Problem: TSS in Aquaculture Discharged Effluent

- EPA: Best Management Practices (BMP)
- NPDES permits: state or regional NPDES permits
- Concentration of suspended solids
- Reduce quantity of discharge water
- Minimize storage volume

Hydrotech Belt Filter (Water Management Technologies)

Belt Filter System, Hydrotech Model HBF537-1H



Influent: 600 - 1400 mg/L

Effluent: 15% Solids





Objectives

- Summary of the current waste treatment systems
- Coagulation/Flocculation
- Performance evaluation of Hydrotech Belt filter

Freshwater Institute Intensive Recirculating Aquaculture Production Systems

- Partial-Reuse Fingerling System
- Recirculating Growout System





Partial-Reuse Fingerling System

Partial-reuse system:

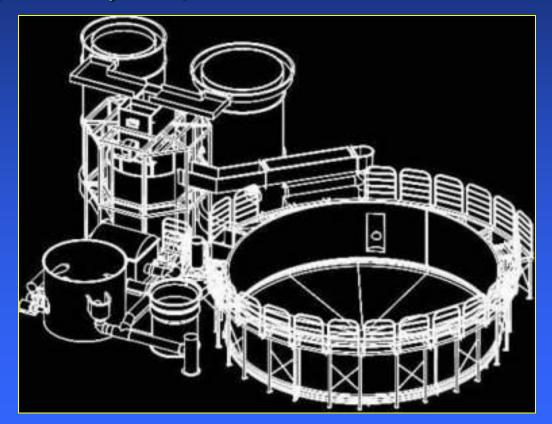
- NH₃-N controlled by pH
- pH controlled by CO₂
- 1500 lpm recirc
- bottom drain flow is discharged from system
- 12-15% of water flow
- sidewall flow is reused after microscreen filtration
- 45-50 kg feed/day



Recirculating Growout System

Fully-recirculating system

- 4 8% make-up rate on a flow basis (0.5-1.0 day HRT)
- 4,800 lpm recir. water flow
- 150 m³ culture volume
- 7% through bottom drain
- 93% through side drain
- 200 kg/day feed



Current Aquaculture Waste Management





Polishing Microscreen Filter Model RFM 4848, Manufacturing, Ltd.

Backwash Water Sump

Current Aquaculture Waste Management



Current Aquaculture Waste Management

Pumping Settling Cones





Land Application / Composting



Aerobic Lagoon

BOD In: 6 mg/L BOD out 2 mg/L

Waste Management – Discharge Parameters

| Parameter | Mean | | |
|---|--------------------------|-----------------------------------|--|
| pH Temp Alkalinity Turbidity | | 7.43 19.4 292 Over range | |
| TP RP | (mg/L - P) (mg/L - P) | 77.8 12.3 | |
| | (mg/L) (mg/L) | 1015 753 | |
| TN TAN NO ₂ NO ₃ | (mg/L - N) (mg/L - N) | 77.8 14.8 0.43 38.8 | |
| cBOD ₅ | (mg/L) | 548 | |





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Coagulation/Flocculation

Coagulation

Process of decreasing or neutralizing the electric charge on suspended particles

Flocculation

Process of bringing together the microfloc particles to form large agglomerations by the binding action of flocculants

Suspended Solids Removal

Alum in wastewater yields the following reaction:

$$Al_2(SO_4)_3 - 14 H_2O + 3Ca(HCO_3)_2 \Leftrightarrow 3Ca SO_4 + 2Al(OH)_3 + 6CO_2 + 14H_2O$$

Insoluble aluminum hydroxide is a gelatinous floc

Ferric Chloride in wastewater yield the following reaction:

$$2\text{FeCl}_3 \bullet 6\text{H}_2\text{O} + 3\text{Ca}(\text{HCO}_3)_2 \Leftrightarrow 3\text{CaCl}_2 + 2\text{Fe}(\text{OH})_3 + 6\text{CO}_2 + 12\text{H}_2\text{O}$$

Insoluble ferric hydroxide is a gelatinous floc

Phosphorus Removal

Basic reaction:

$$Al^{+3} + H_nPO_4^{3-n} \Leftrightarrow AlPO_4 + nH^+$$

$$Fe^{+3} + H_nPO_4^{3-n} \Leftrightarrow FePO_4 + nH^+$$

Simplest form of reaction, bench-scale test required to establish actual removal rate

Coagulation/Flocculation Aids

Advantages:

High Molecular Weight Long-chain Polymers

- lower dosages requirements
- reduced sludge production
- easier storage and mixing
- MW and charge densities optimized "designer" aids
- no pH adjustment required
- polymers bridge many smaller particles
- improved floc resistance to shear forces

Polymers

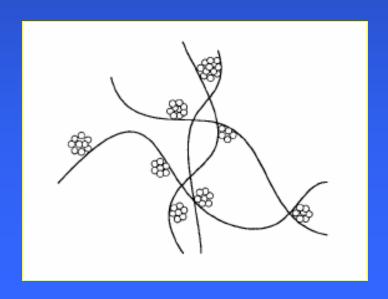
Process Efficiency depends on:

- polymer concentration
- polymer charge (anionic, cationic, and nonionic)
- polymer molecular weight and charge density
- raw wastewater characteristics (particle size, concentration, temperature, hardness, pH)
- physical parameters of the process (dosage, mixing energy, flocculation energy, duration)
- discharge water treatment levels required

How Polymers Work

• charge neutralization (low molecular weight polymers) neutralize negative charge on particle

bridging between particles (high molecular weight polymers)
 long loops and tail connect particles



Polymer Evaluation

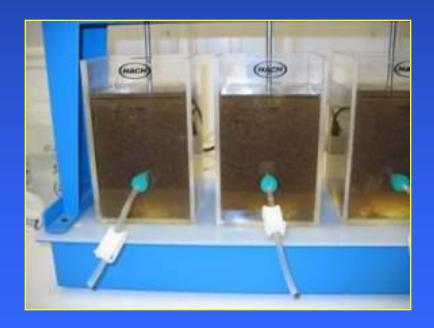
Similitude Studies with Jar Tests

- Jar Tests of coagulant and flocculant aids
 - Effect of mixing speed, (velocity gradient)
 - Effect of flocculation speed
 - Effect of coagulant type and dosage
 - Effect of flocculant (polymer) type and dosage

Jar Tests

Water Quality

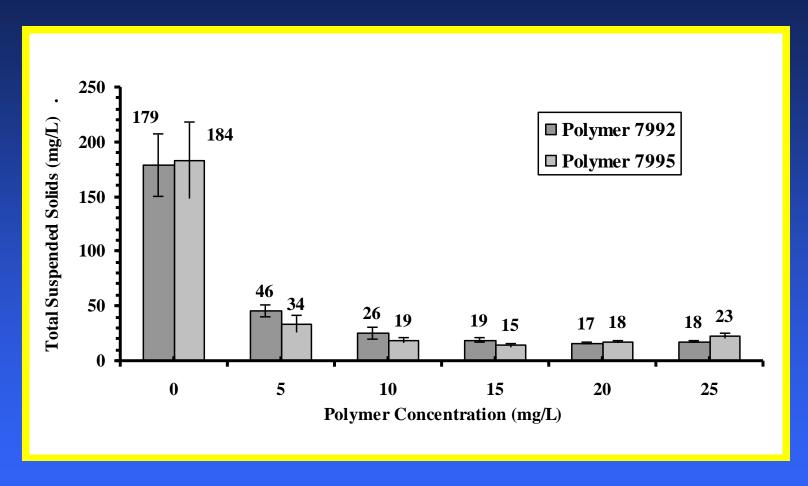
- □ pH
- Turbidity
- RP (orthophosphate)
- Alkalinity
- TSS





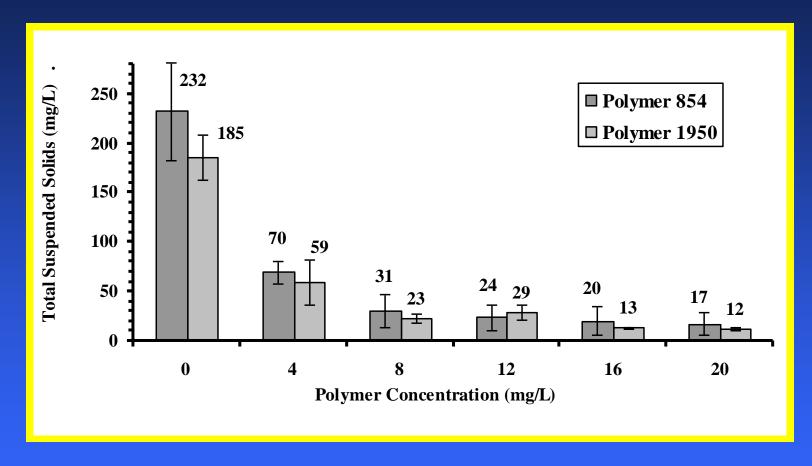
Phipps and Bird Six-Paddle Stirrer with Illuminated Base

Similitude Results



Total Suspended Solids removed using very high degree of cationic charge, very low Molecular Weight Polymers

Similitude Results



Total Suspended Solids removed using high degree of cationic charge, very high molecular weight Polymers

Objectives

- Summary of the current waste treatment systems
- Polymer Selection
- Performance evaluation of Hydrotech Belt filter

Hydrotech Belt Filter System







Coagulation/Flocculation Tank





Belt Filter

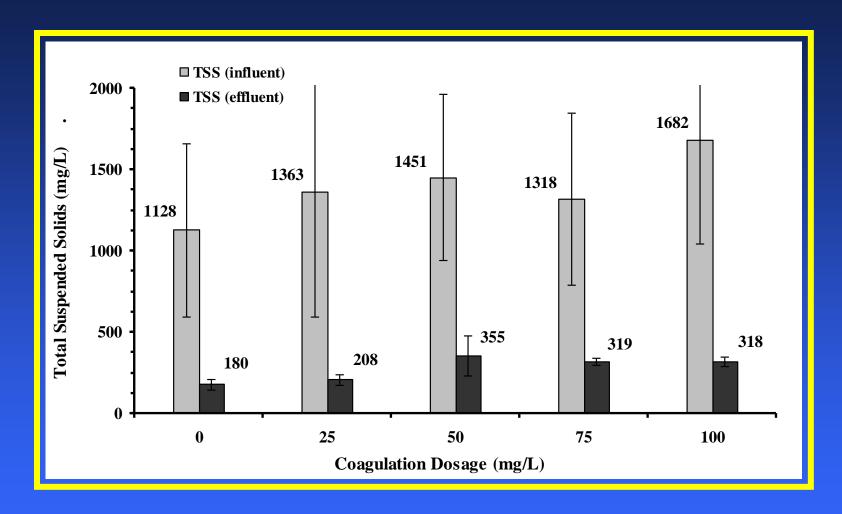


Objectives

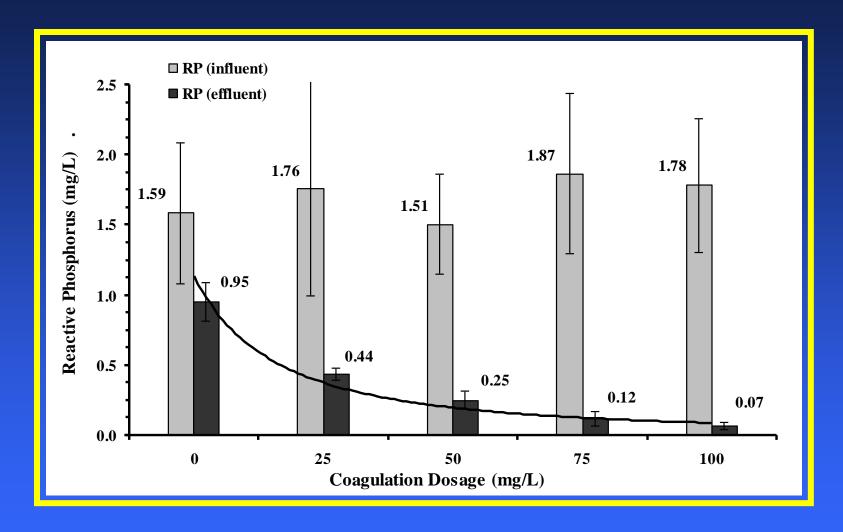
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 - Polymer as Coagulation Aid
 - Alum and Polymer as Coagulation/Flocculation Aids

Alum

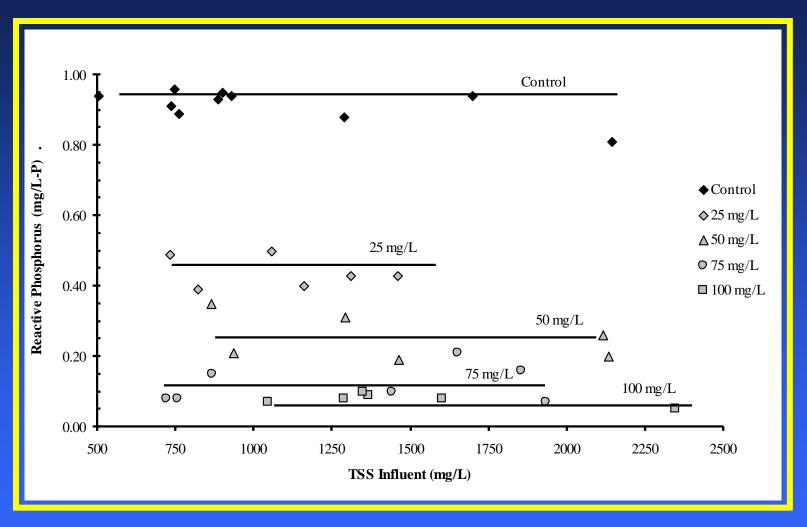
| Alum | | рН | Alkalinity | TSS (mg/L) RP (mg/L-P) | |
|----------|-----------|------|------------|------------------------|-------------|
| Dosage | | | (mg/L) | Mean: StDev: | Mean StDev: |
| 0 mg/L | Influent | 7.37 | 286 | 1128 534 | 1.59 0.50 |
| (11) | Effluent | 7.39 | 287 | 180 33 | 0.95 0.14 |
| | % Removal | | | 82% | 38% |
| 25 mg/L | Influent | 7.32 | 303 | 1363 768 | 1.76 0.77 |
| (7) | Effluent | 7.33 | 302 | 208 34 | 0.44 0.04 |
| | % Removal | | 1% | 83% | 71% |
| 50 mg/L | Influent | 7.29 | 283 | 1451 509 | 1.51 0.36 |
| (7) | Effluent | 7.24 | 270 | 355 122 | 0.25 0.07 |
| | % Removal | | 4% | 75% | 82% |
| 75 mg/L | Influent | 7.29 | 292 | 1318 527 | 1.87 0.57 |
| (7) | Effluent | 7.19 | 274 | 319 21 | 0.12 0.05 |
| | % Removal | | 6% | 72% | 93% |
| 100 mg/L | Influent | 7.30 | 288 | 1682 635 | 1.78 0.48 |
| (7) | Effluent | 7.06 | 242 | 318 31 | 0.07 0.03 |
| | % Removal | | 16% | 79% | 96% |



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of alum dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of alum dosage (mg/L).



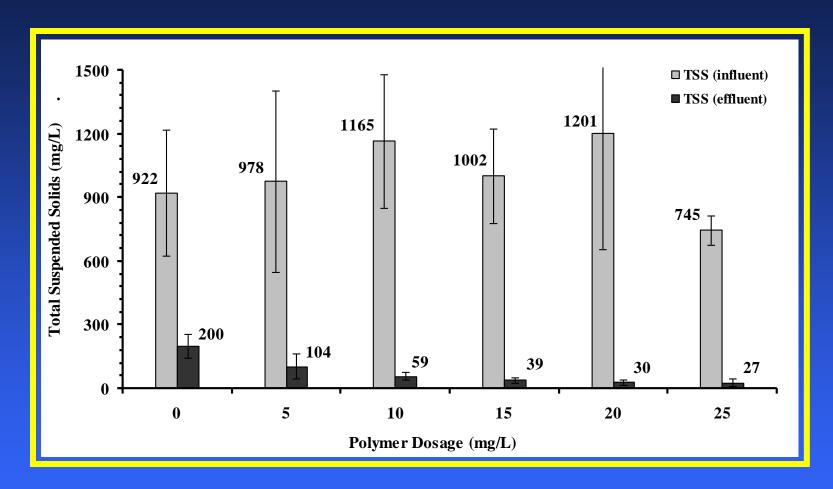
Reactive phosphorus for the effluent from the belt filter as a function of total suspended solids of the influent (mg/L).

Objectives

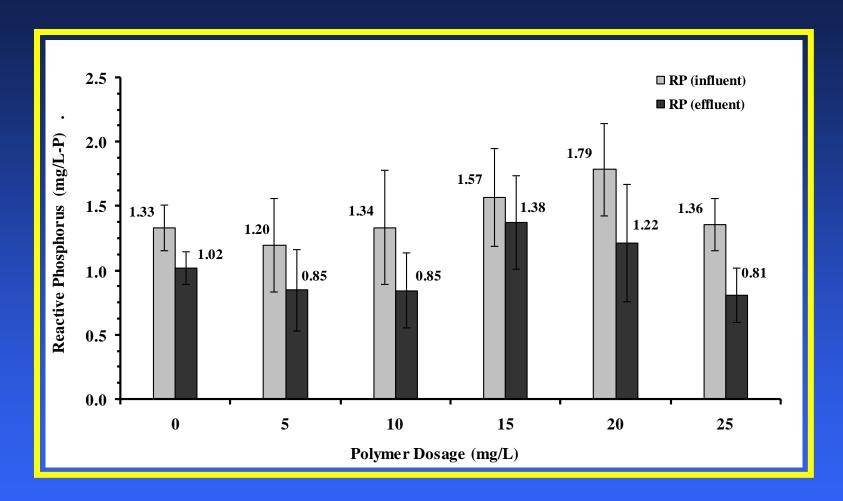
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Polymer

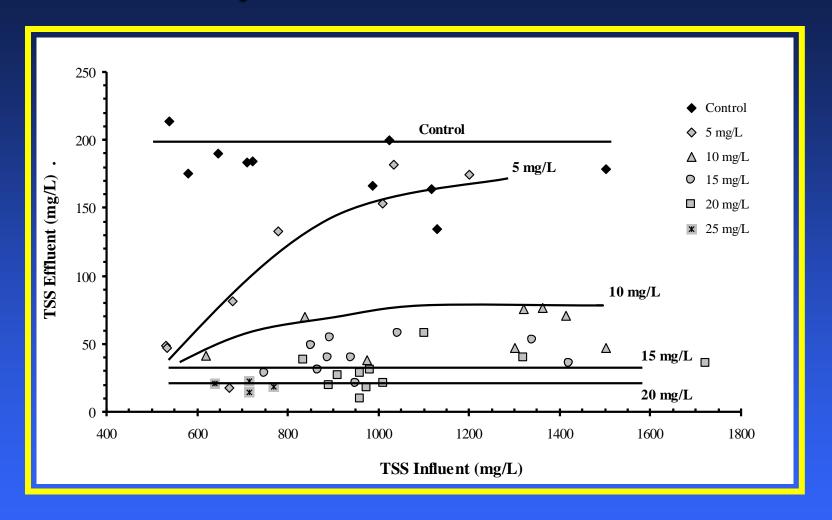
| | | рН | TSS (mg/L) | | RP (mg/L-P) | |
|----------------|-----------|------|------------|--------|-------------|--------|
| Polymer Dosage | | | Mean: | StDev: | Mean: | StDev: |
| 0 mg/L | Influent | 7.55 | 922 | 297 | 1.33 | 0.18 |
| (12) | Effluent | 7.62 | 200 | 55 | 1.02 | 0.13 |
| | % Removal | | 76.1% | | 23% | |
| 5 mg/L | Influent | 7.52 | 978 | 428 | 1.20 | 0.36 |
| (8) | Effluent | 7.55 | 104 | 60 | 0.85 | 0.31 |
| | % Removal | | 88.6% | | 26% | |
| 10 mg/L | Influent | 7.44 | 1165 | 316 | 1.34 | 0.44 |
| (8) | Effluent | 7.41 | 59 | 16 | 0.85 | 0.29 |
| | % Removal | | 94.7% | | 41% | |
| 15 mg/L | Influent | 7.45 | 1002 | 223 | 1.57 | 0.38 |
| (14) | Effluent | 7.31 | 39 | 12 | 1.38 | 0.36 |
| | % Removal | | 96.0% | | 14% | |
| 20 mg/L | Influent | 7.47 | 1201 | 548 | 1.79 | 0.36 |
| (12) | Effluent | 7.39 | 30 | 13 | 1.22 | 0.46 |
| | % Removal | | 97.3% | | 32% | |
| 25 mg/L | Influent | 7.42 | 745 | 69 | 1.36 | 0.20 |
| (8) | Effluent | 7.31 | 27 | 17 | 0.81 | 0.21 |
| | % Removal | | 96.3% | | 39% | |



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of polymer dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of polymer dosage (mg/L).



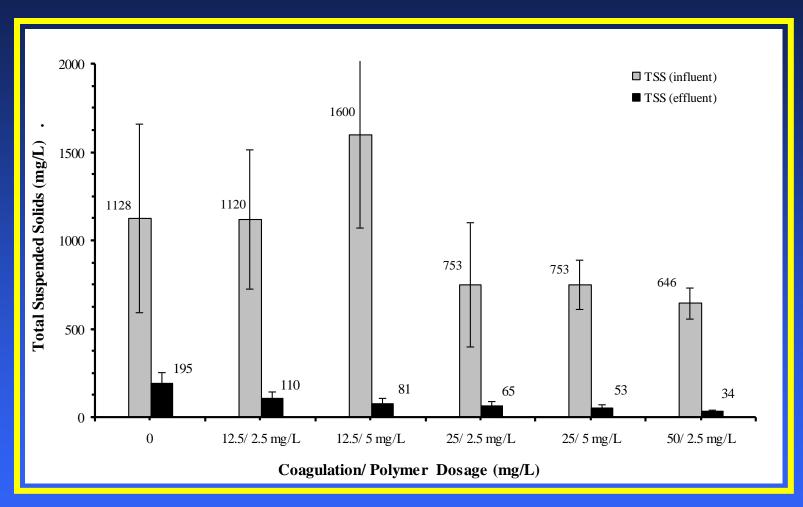
Impact of the influent TSS concentration on the effluent TSS from the belt filter as a function of polymer dosage (mg/L).

Objectives

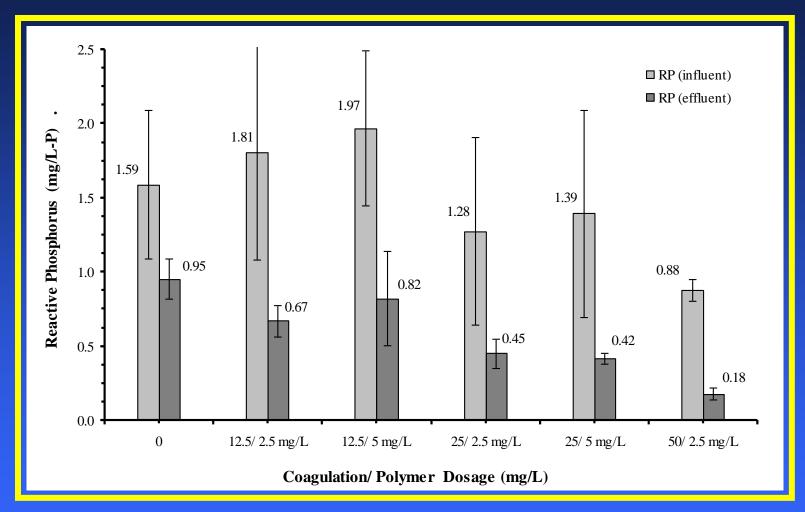
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Alum/ Polymer

| Alum/Polymer | | рН | TSS (mg/L) | | RP (mg/L-P) | |
|--------------|-----------|------|------------|--------|-------------|--------|
| Dosage | | | Mean: | StDev: | Mean: | StDev: |
| 0 mg/L / | Influent | 7.37 | 1128 | 534 | 1.59 | 0.50 |
| 0 mg/L | Effluent | 7.39 | 195 | 58 | 0.95 | 0.14 |
| | % Removal | | 81% | | 38% | |
| 12.5 mg/L / | Influent | 7.23 | 1120 | 396 | 1.81 | 0.73 |
| 2.5 mg/L | Effluent | 7.26 | 110 | 36 | 0.67 | 0.11 |
| | % Removal | | 90% | | 59% | |
| 12.5 mg/L / | Influent | 7.26 | 1600 | 526 | 1.97 | 0.52 |
| 5 mg/L | Effluent | 7.22 | 81 | 29 | 0.82 | 0.32 |
| | % Removal | | 94% | | 55% | |
| 25 mg/L/ | Influent | 7.34 | 753 | 352 | 1.28 | 0.63 |
| 2.5 mg/L | Effluent | 7.27 | 65 | 28 | 0.45 | 0.10 |
| | % Removal | | 91% | | 57% | |
| 25 mg/L / | Influent | 7.30 | 753 | 140 | 1.39 | 0.70 |
| 5 mg/L | Effluent | 7.13 | 53 | 20 | 0.42 | 0.04 |
| | % Removal | | 93% | | 65% | |
| 50 mg/L / | Influent | 7.38 | 646 | 87 | 0.88 | 0.07 |
| 2.5 mg/L | Effluent | 7.14 | 34 | 11 | 0.18 | 0.04 |
| | % Removal | | 95% | | 80% | |



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).

Sludge

- Alum
 - $13.2\% \pm 1.1$
- Polymer
 - $11.6\% \pm 2.2$
- Alum/Polymer
 - $12.6\% \pm 1.4$



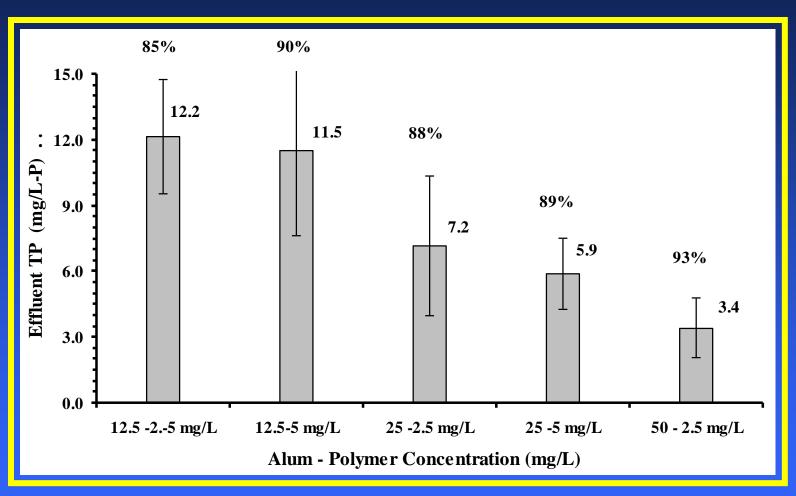


Secondary Objectives

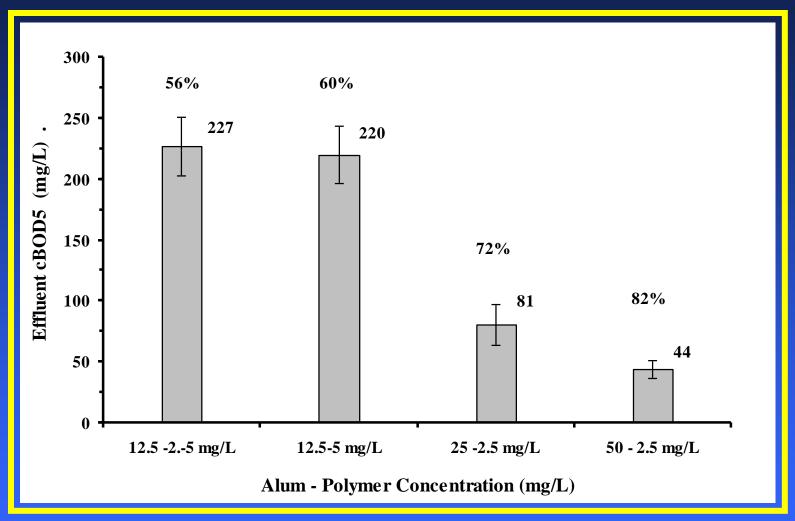
- Other Water Quality Parameters
 - Total Phosphorus
 - Total Nitrogen
 - cBOD₅
 - COD

Other Water Quality Parameter

| Alum/Polymer | | TP (mg | g/L-P) | P) TN (mg/L-N) | | cBOD ₅ (mg/L) | | COD | |
|--------------|-----------|--------|--------|----------------|--------|--------------------------|--------|-------|--------|
| Dosage | | Mean: | StDev: | Mean: | StDev: | Mean: | StDev: | Mean: | StDev: |
| 12.5 mg/L / | Influent | 95.1 | 39.9 | 49.1 | 20.6 | 498 | 89 | | |
| 2.5 mg/L | Effluent | 12.2 | 2.6 | 8.5 | 3.8 | 227 | 24 | | |
| | % Removal | 85% | | 81% | | 56% | | | |
| 12.5 mg/L / | Influent | 124 | 54 | 95 | 9.3 | 549 | 42 | | |
| 5 mg/L | Effluent | 11.5 | 3.9 | 16.4 | 1.7 | 220 | 23 | | |
| | % Removal | 90% | | 83% | | 60% | | | |
| 25 mg/L / | Influent | 705 | 46.4 | 36.2 | 19.8 | 359 | 214 | 758 | 162 |
| 2.5 mg/L | Effluent | 4.7 | 1.1 | 4.7 | 1.1 | 81 | 17 | 112 | 14 |
| | % Removal | 83% | | 83% | | 72% | | 85% | |
| 25 mg/L / | Influent | 37 | 19.8 | 37 | 19.8 | | | 880 | 140 |
| 5 mg/L | Effluent | 7.0 | 3.0 | 6.3 | 2.3 | | | 87 | 22 |
| | % Removal | 88% | | 83% | | | | 90% | |
| 50 mg/L/ | Influent | 50.3 | 12.4 | 31.1 | 6.8 | 251 | 50 | 808 | 170 |
| 2.5 mg/L | Effluent | 3.4 | 1.4 | 4.0 | 1.8 | 44 | 8 | 62 | 15 |
| | % Removal | 93% | | 87% | | 82% | | 92% | |



Effluent Total Phosphorus from the belt filter and percent removal for the microscreen backwash wastewater as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage.



Effluent cBOD₅ from the belt filter and percent removal for the microscreen backwash sump wastewater as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).

Economics

| Polymer | Cost of Polymers | Cost per kg | Cost per metric tonne of feed |
|---------|------------------------|-------------|-------------------------------|
| LT 7991 | \$247.50 / 450lb drum | \$1.21 | \$7.26 |
| LT 7992 | \$148.50 / 450 lb drum | \$0.73 | \$4.38 |
| LT 7995 | \$252.00/ 450 lb drum | \$1.23 | \$7.38 |
| CE 854 | \$418.50/ 450 lb drum | \$2.05 | \$13.08 |
| CE 1950 | \$418.50/ 450 lb drum | \$2.05 | \$13.08 |





Unexpected Difficulties

Polymer induced foam at high dosage



Conclusions

- Alum:

96% of RP, 0.07 mg/L-P

Polymer:

96% of TSS, 30 mg/L

Alum/Polymers:

95% of TSS and 80% of RP

Sludge:

13% solids

- □ TP 93%,
- □ TN 87%,
- BOD₅ 82%,
- COD 92%

Future Research

- Continued evaluation of other potential coagulant aids, such as Acid Mine Drainage Sludge
- Evaluation of other polymer
- Increase belt porosity to improve Hydraulic Loading Rate
- Additional performance evaluation of belt filter systems in terms of several operating parameters, including flow rates and belt speed.

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Questions?









