

NMRWA PUMPS & MOTORS REFRESHER



Presented by: TP Pump
SPEAKER: JIM BASSETT

AGENDA

SECTION VII PUMPS & MOTORS

- CENTRIFUGAL vs.. POSITIVE DISPLACEMENT
- TYPES OF CENTRIFUGALS & APPLICATIONS
- TYPES OF POSITIVE DISPLACEMENT & APPLICATIONS
- PUMP COMPONENTS & PART I.D.
- HEADS & PUMP CURVES
- COMMON OPERATIONAL PROBLEMS

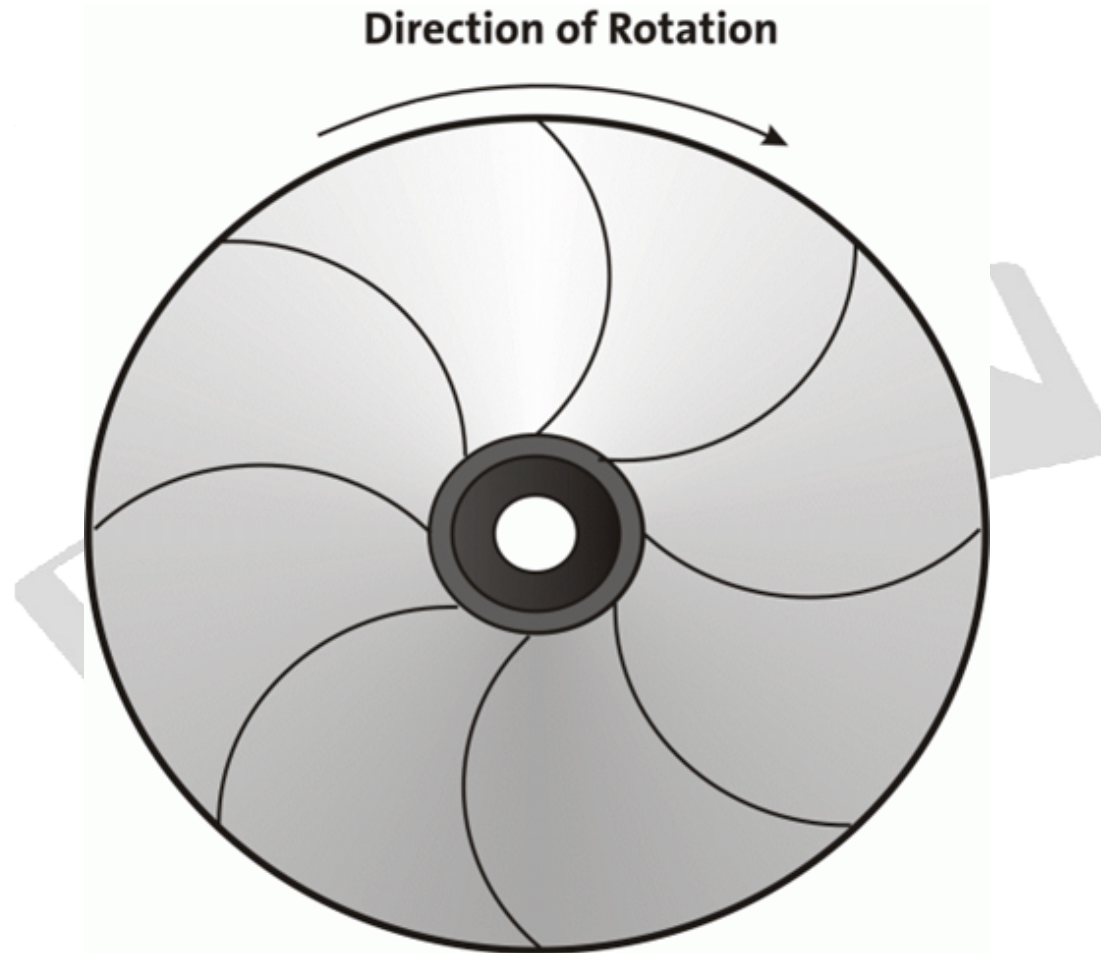


CENTRIFUGAL PUMPS

- LARGE VOLUMES @ RELATIVELY LOW HEADS
- FLOW CHANGES WHEN HEAD CHANGES
- SINGLE OR MULTIPLE STAGES



Impeller Direction of Rotation

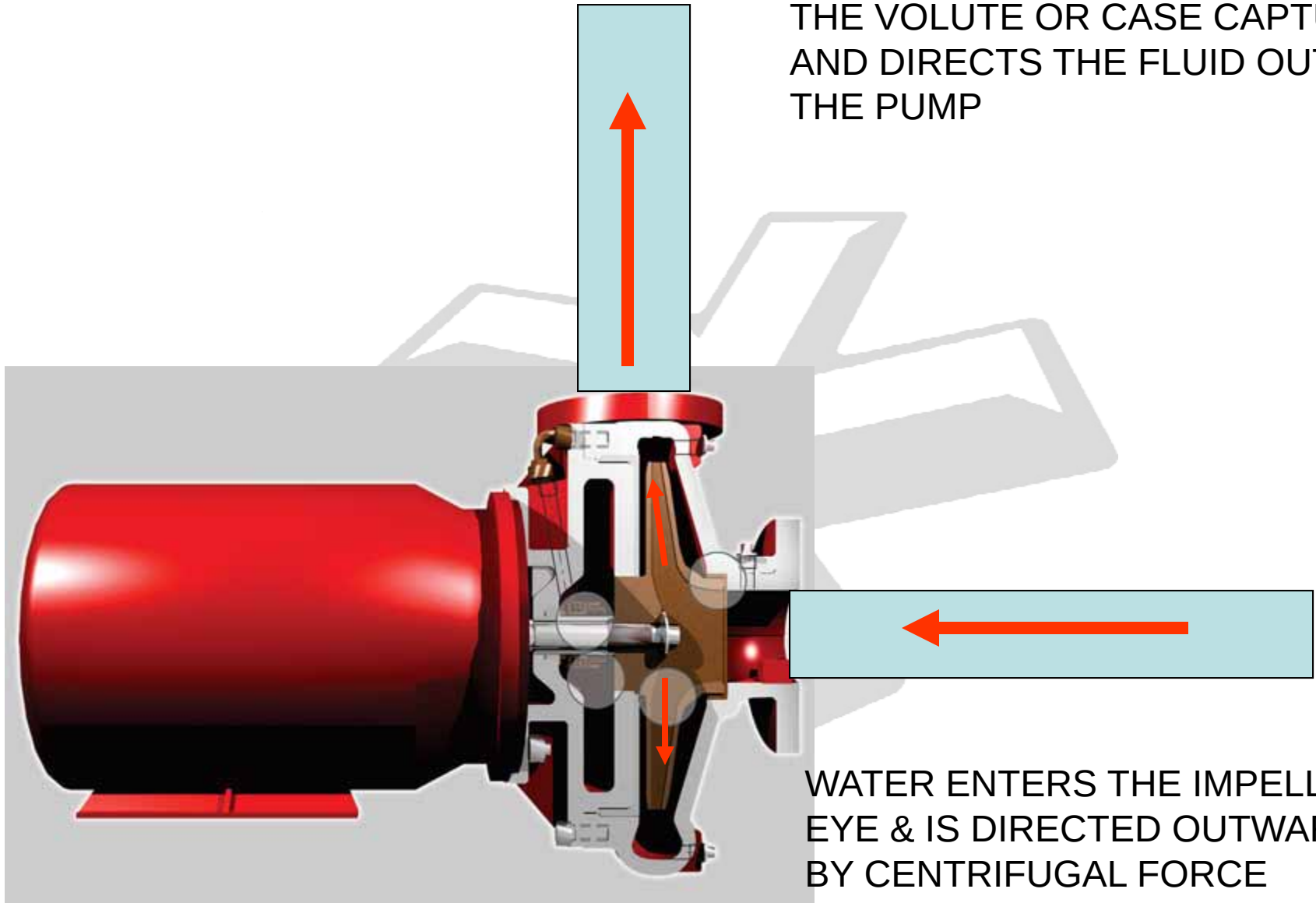


**Centrifugal
Force**

CW ROTATION



THE VOLUTE OR CASE CAPTURES
AND DIRECTS THE FLUID OUT OF
THE PUMP



WATER ENTERS THE IMPELLER
EYE & IS DIRECTED OUTWARD
BY CENTRIFUGAL FORCE



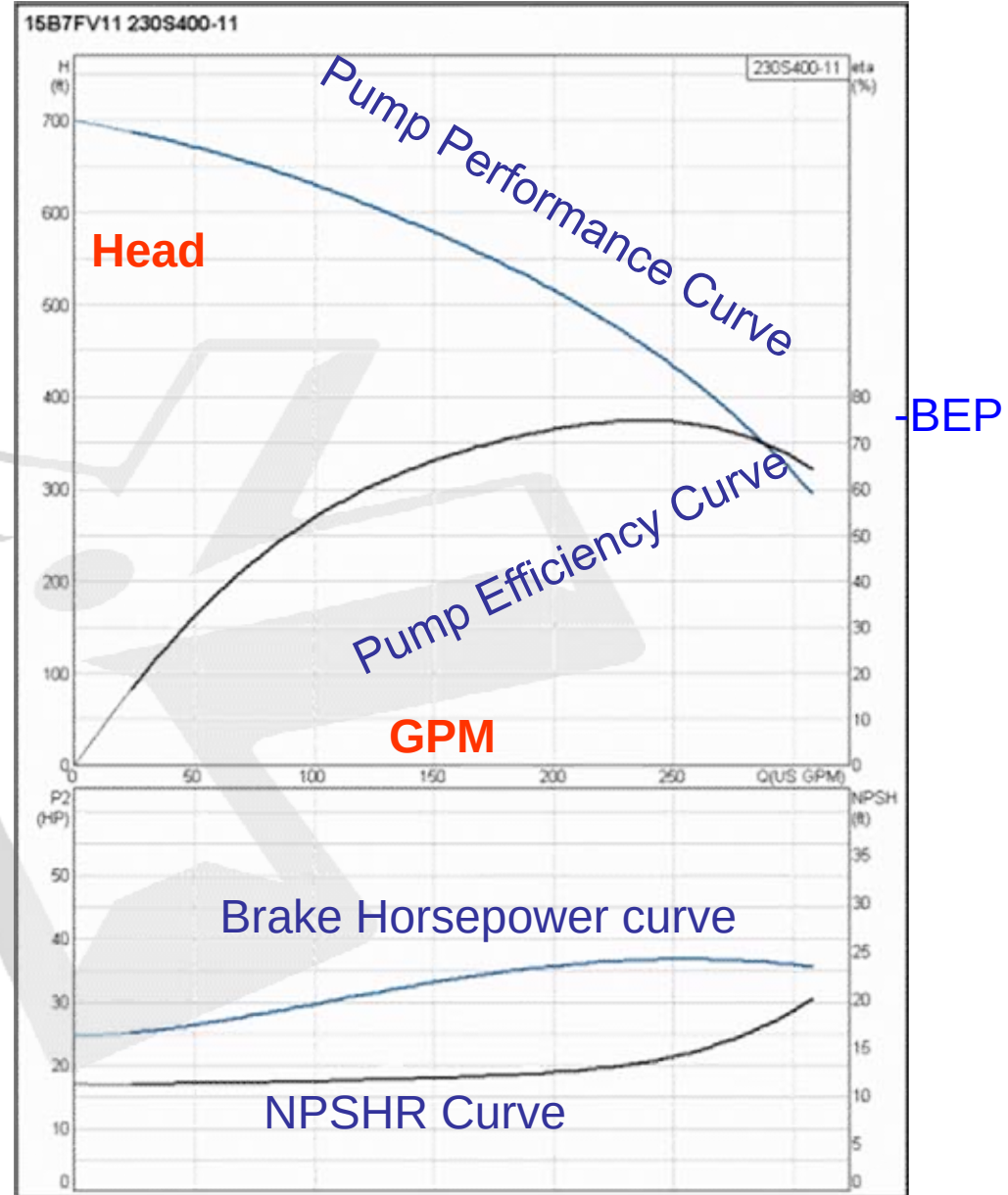
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Typical Pump Submersible Curve Format

Note: model shown
230S400-11
40 HP
11 STAGE

BEST EFFICIENCY POINT
(BEP) : 230 GPM
77% @ 480 FT.

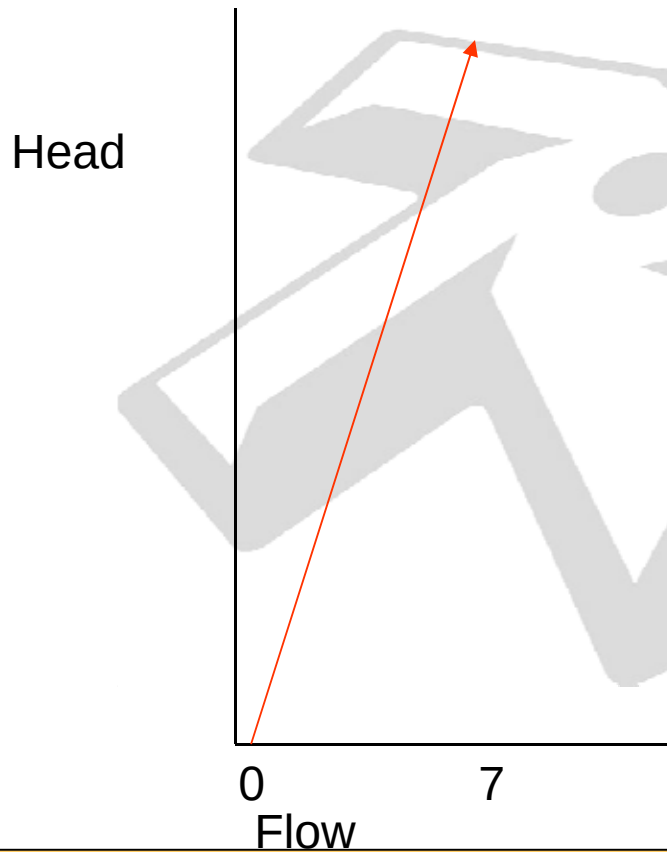


POSITIVE DISPLACEMENT PUMPS

- HIGH HEAD @ LOW FLOWS
- FLOW DOESN'T CHANGE WHEN HEAD CHANGES



Typical **POSITIVE DISPLACEMENT** Pump Curve Format



APPLICATIONS & TYPES OF CENTRIFUGALS



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Rural Water Supply



Suction side
Storage tanks
50,000 gallons
each

Grundfos
Submersible
Well pumps



Discharge side
Storage tank

BoosterpaQ



2 miles of
pipe line



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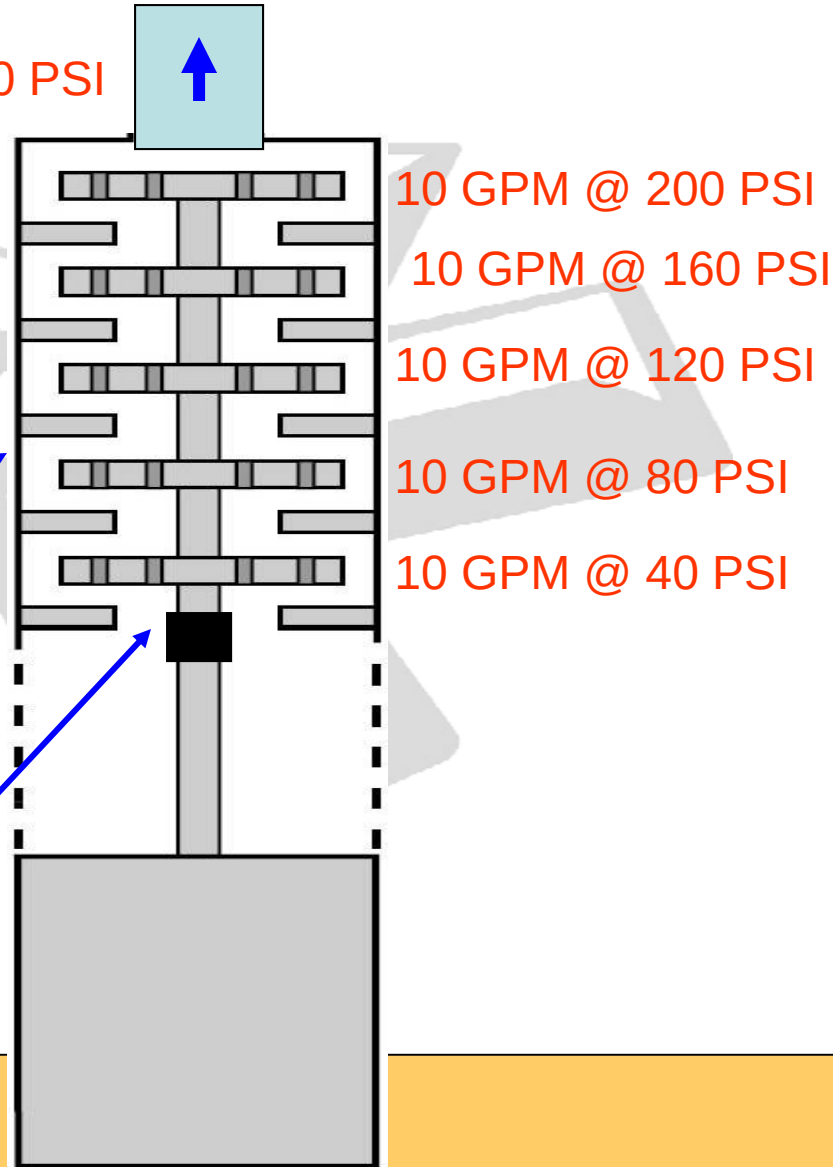
Centrifugals - Series

Example:

Each stage is rated 10 GPM @ 40 PSI

Each stage progressively
boost the pressure

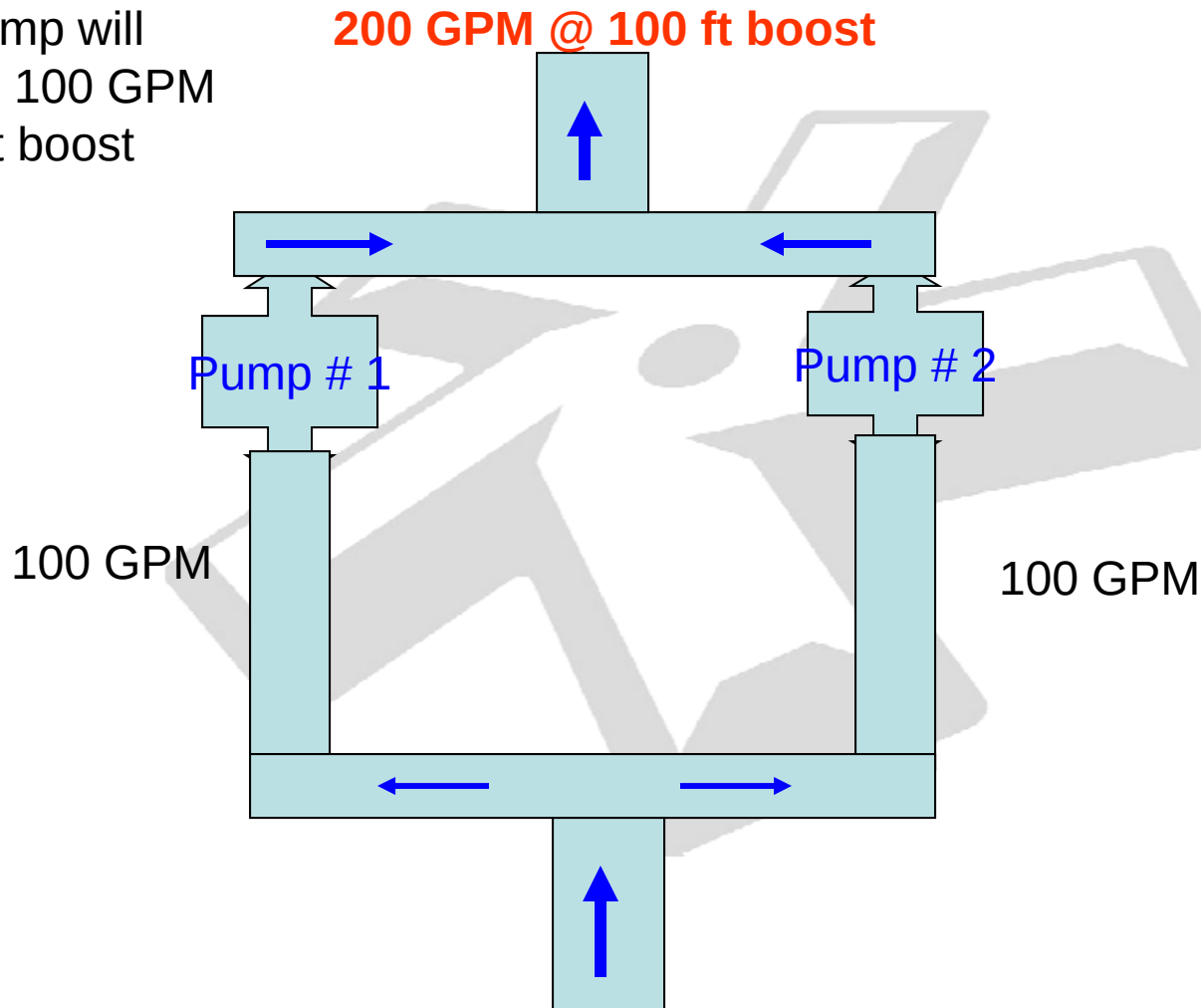
Water enters thru bottom of
the pump end





Centrifugals - Parallel

Each pump will
Produce 100 GPM
@ 100 ft boost







CENTRIFUGAL TYPES

BASIC TYPES OF CENTRIFUGALS

- END SUCTION
- SPLIT CASE
- TURBINE



TYPES OF CENTRIFUGALS

END SUCTION



BASE / FRAME MOUNTED



CLOSE COUPLED



TYPES OF CENTRIFUGALS

END SUCTION vs.. SELF
PRIMING



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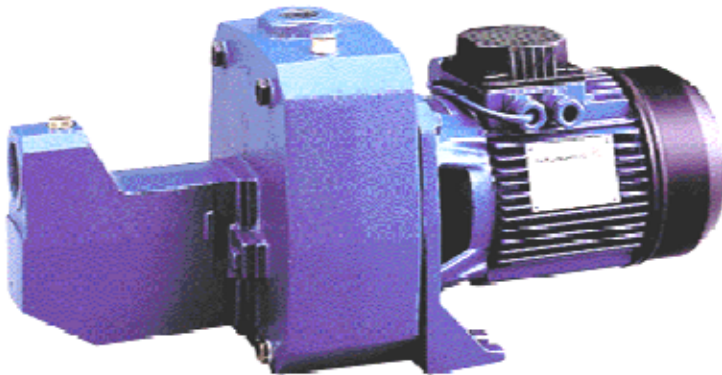
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TYPES OF CENTRIFUGALS

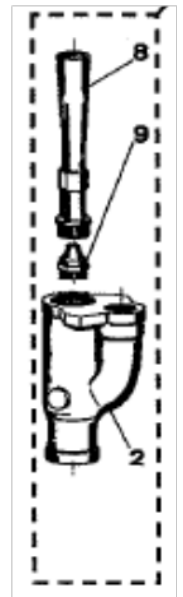
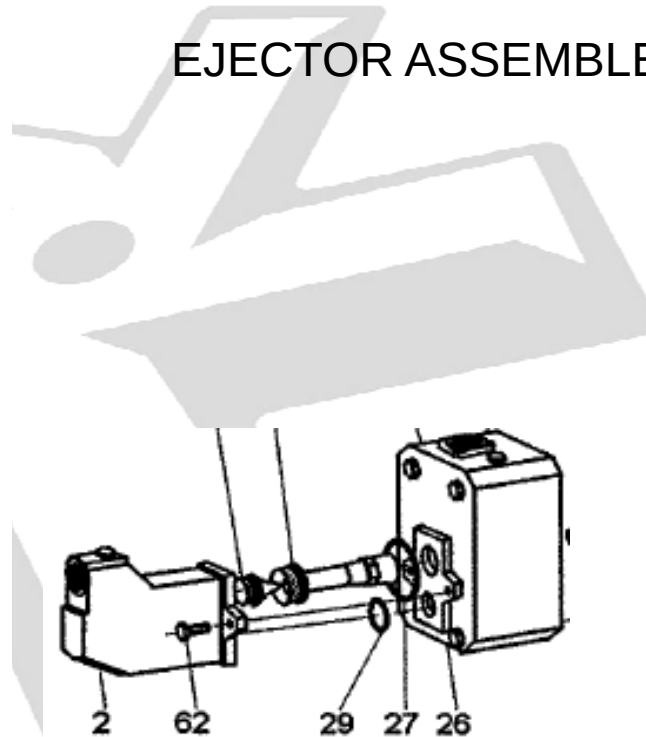
END SUCTION

EJECTOR ASSEMBLY

DEEP WELL



RESIDENTIAL
SHALLOW WELL JET



TYPES OF CENTRIFUGALS

VERTICAL IN LINE



SINGLE IMPELLER



MULTI-STAGE

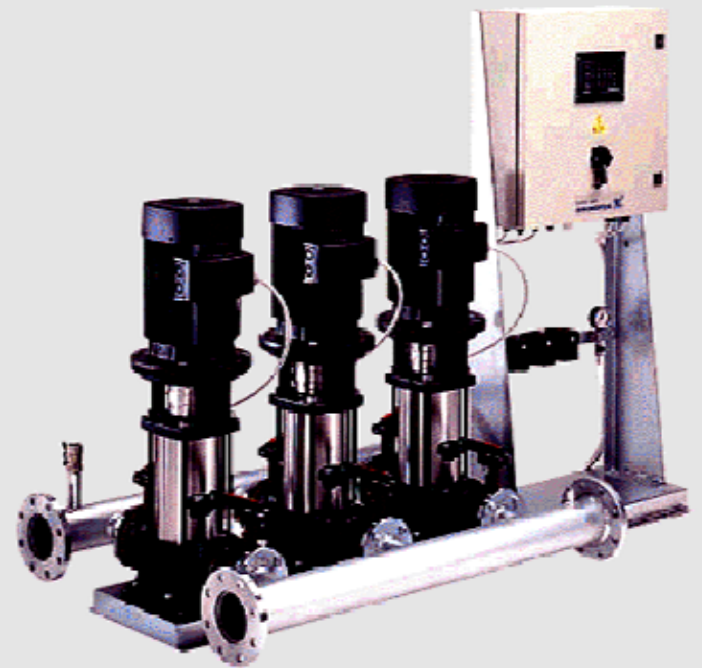


TYPES OF CENTRIFUGALS

PACKAGED SYSTEMS



Single Pump Package



Multiple Pumps

TYPES OF CENTRIFUGALS

SUBMERSIBLE



MULTI-STAGE WELL



SUMP



TYPES OF CENTRIFUGALS

SHORT SET
W/ VHS MOTOR



SUBMERSIBLE

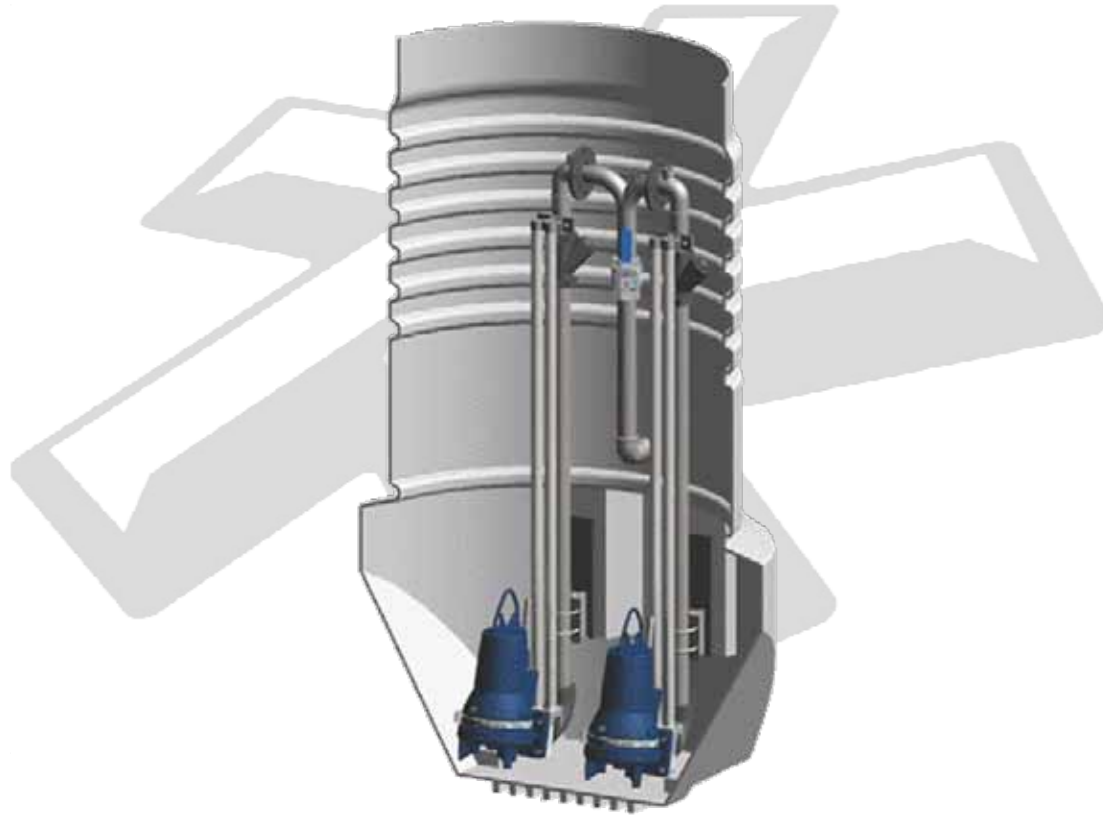


TURBINE



TYPES OF CENTRIFUGALS

SEWAGE / EFFLUENT



Submersible Non-Clog Pumps

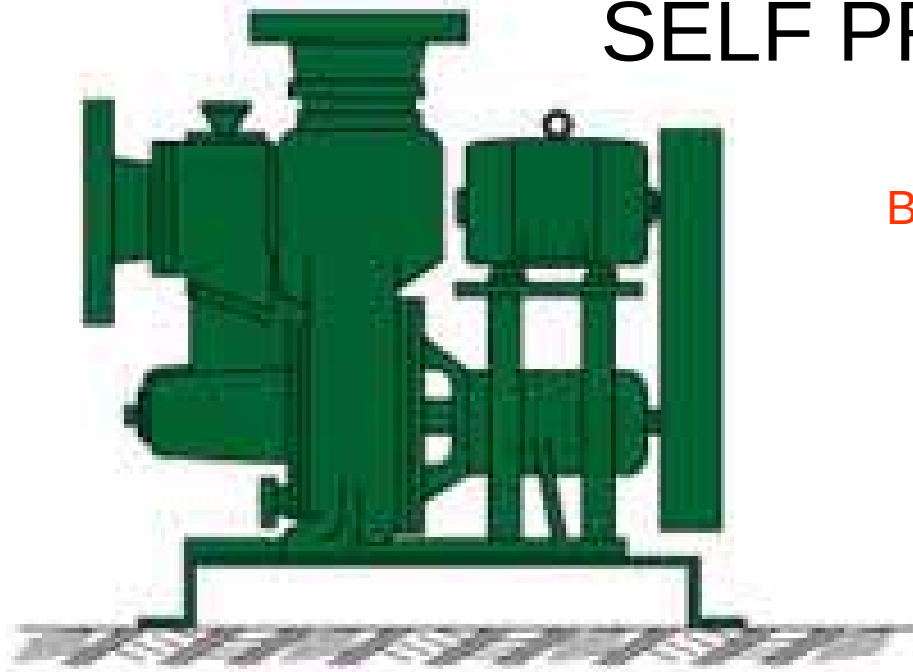


S8FX

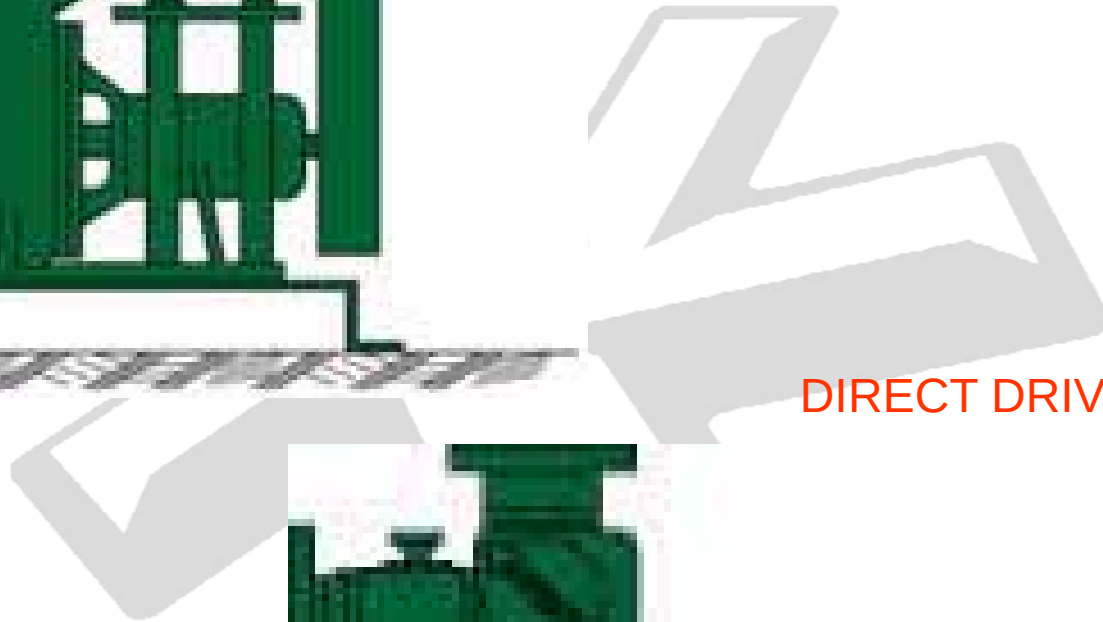


S12L

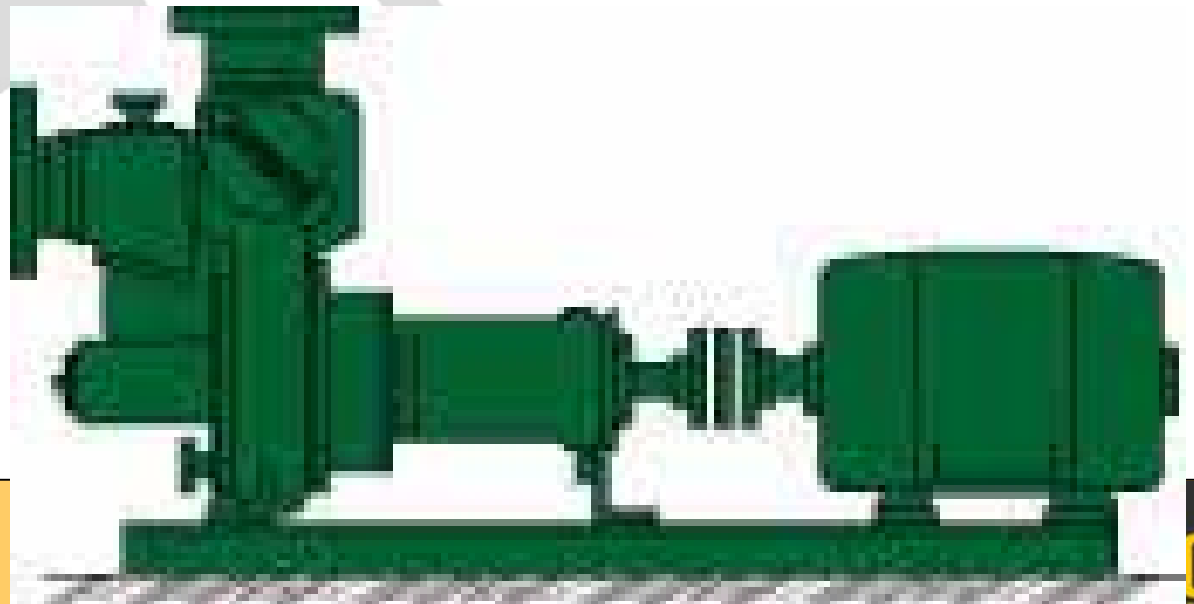
SELF PRIMING TRASH PUMPS



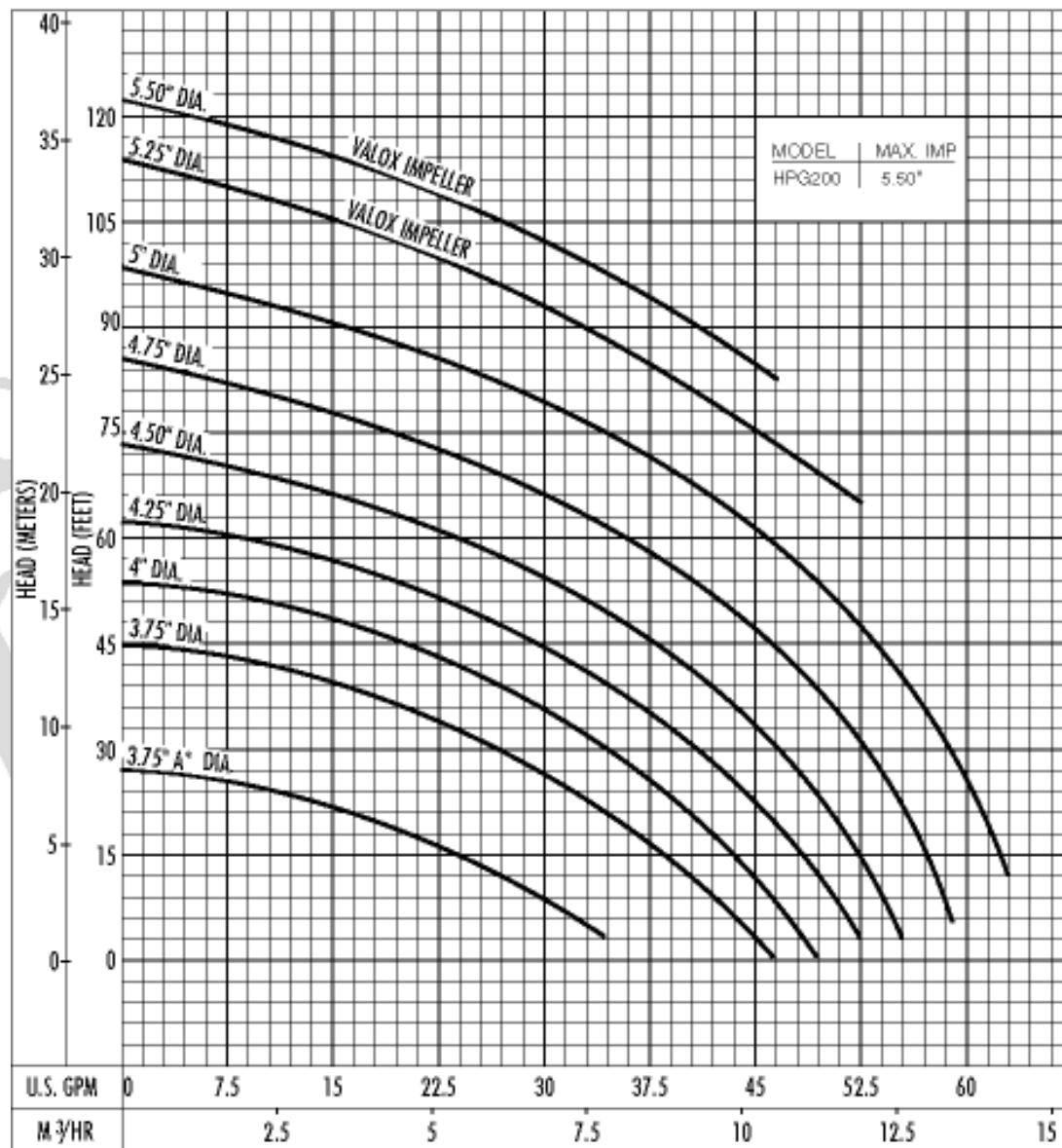
BELT DRIVEN / REDUCED RPM



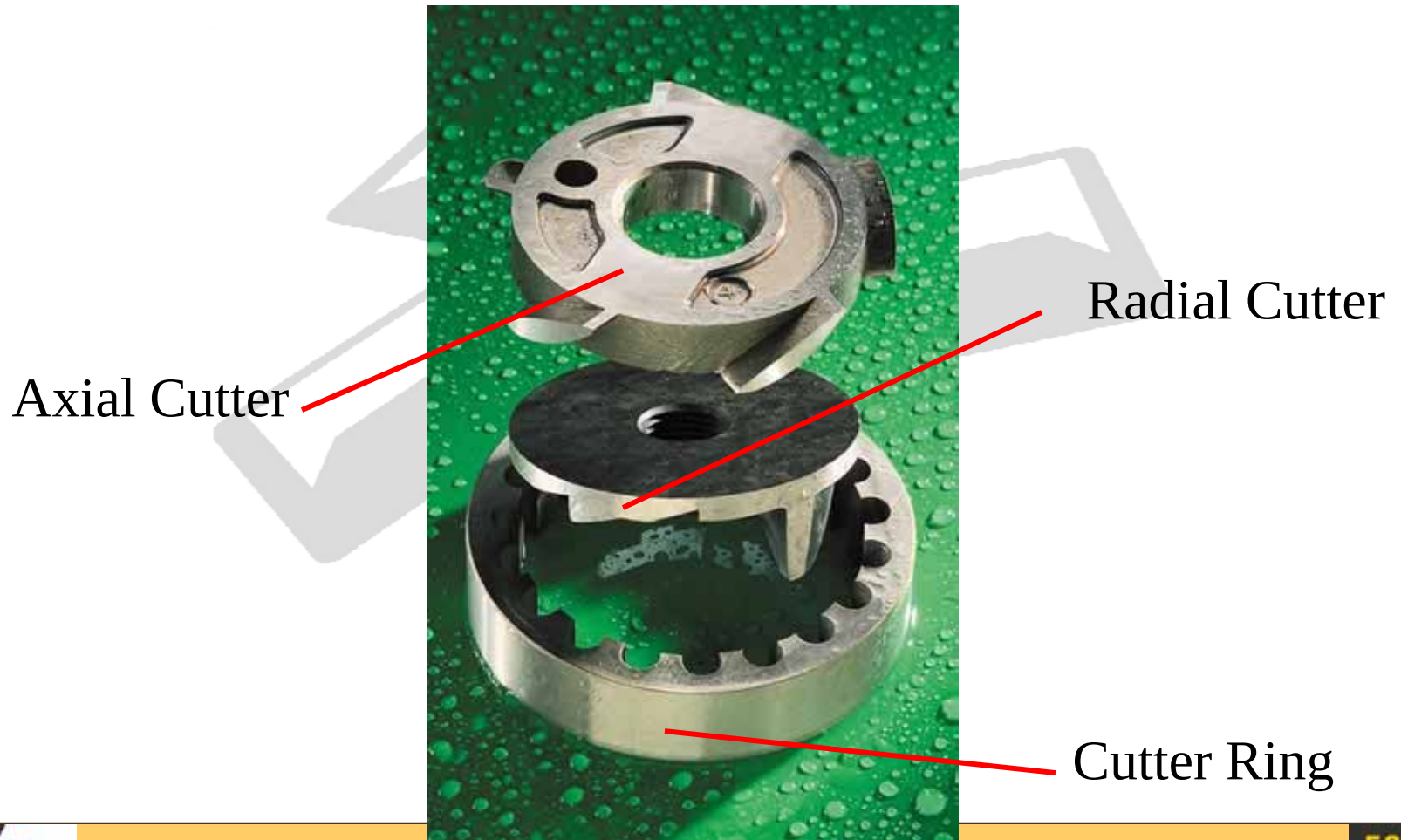
DIRECT DRIVEN



Hydromatic Grinder: HPG



Submersible Sewage Grinder Pumps



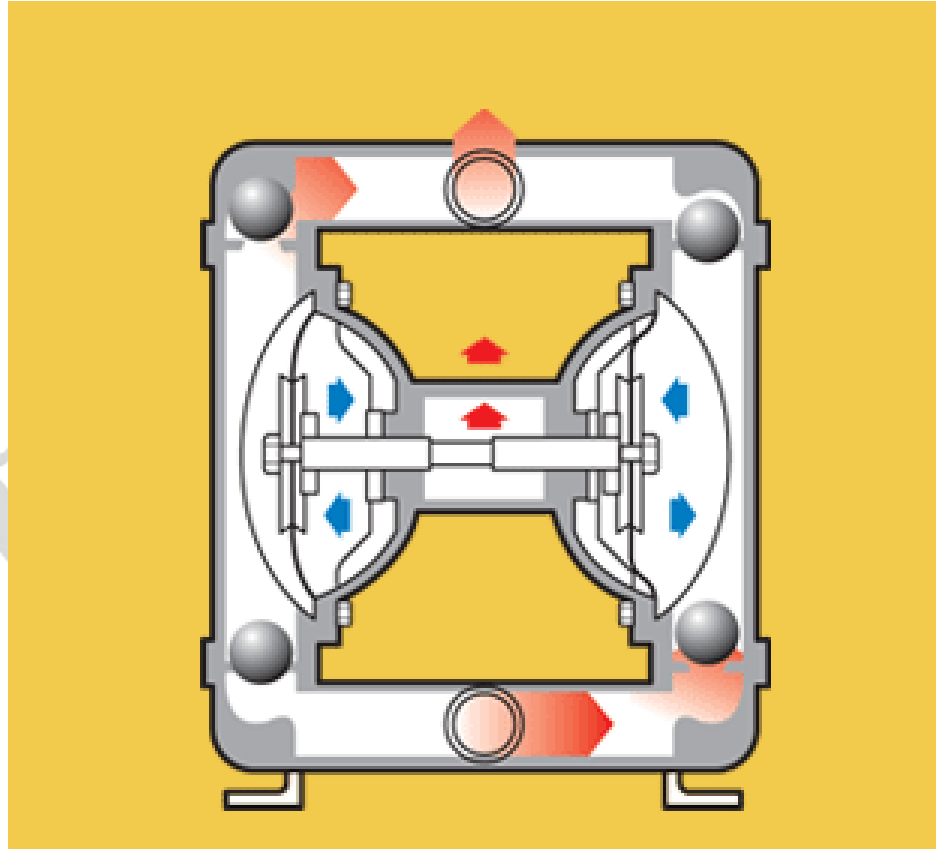
APPLICATIONS – POSITIVE DISPLACEMENT



POSITIVE DISPLACEMENT TYPES

- DIAPHRAGM
- ROLLER / PERISTALTIC
- PISTON / PLUNGER
- PROGRESSIVE CAVITY
- GEAR OR LOBE
- ROTARY SCREW





POSITIVE DISPLACEMENT PUMPS

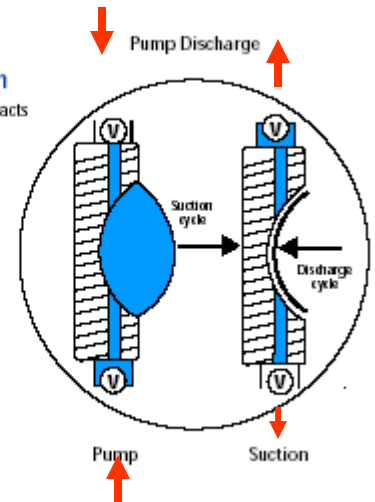
DIAPHRAGM PUMPS – Chemical Metering



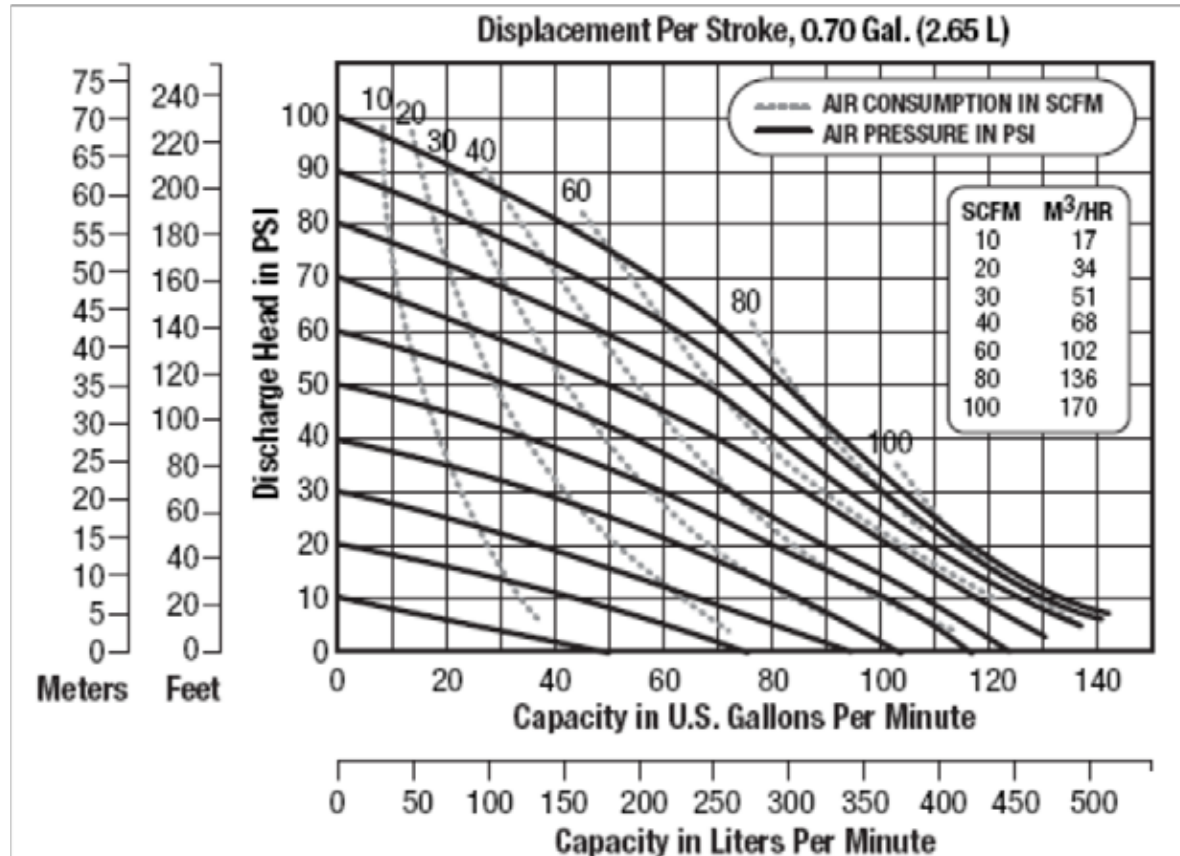
SUCTION DISCHARGE

Principle of Operation

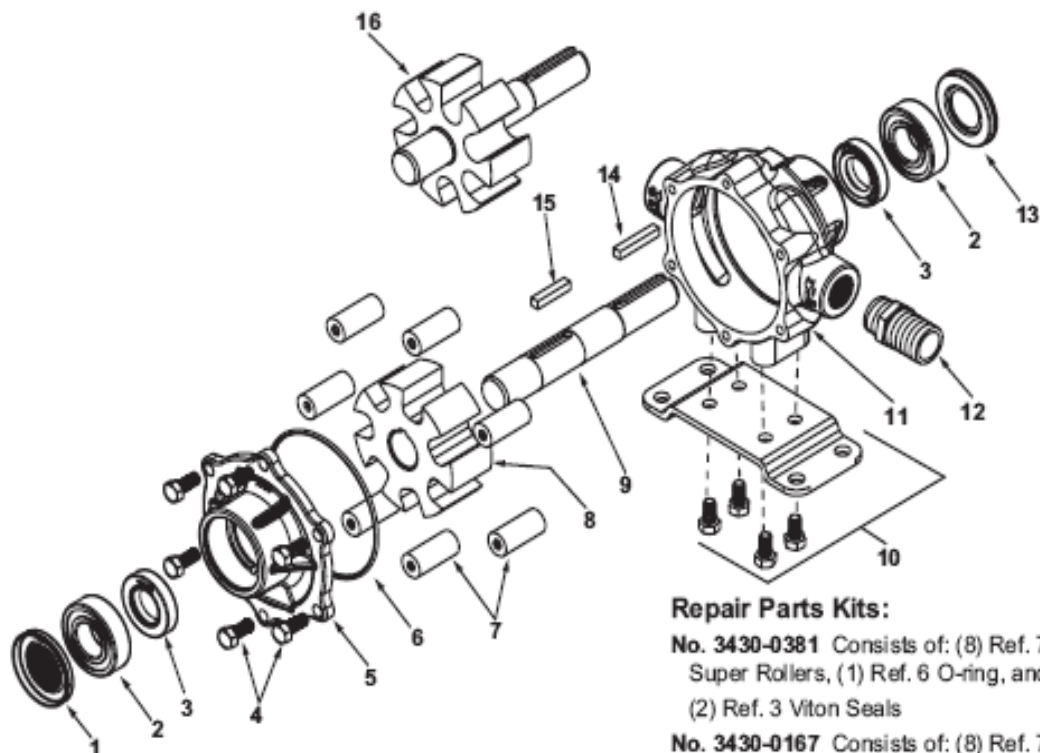
1. The electronic solenoid retracts the diaphragm when power is applied.
2. This causes the suction valve(s) to open and fluid flows into the diaphragm cavity.
3. When the solenoid is deactivated, a spring returns the diaphragm and forces fluid out the discharge valves.



POSITIVE DISPLACEMENT PUMPS



ROLLER



Note: When ordering parts, give quantity, part number, description and complete model number. Reference numbers are used ONLY to identify parts in the drawing and NOT to be used as order numbers.

Repair Parts Kits:

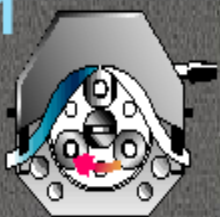
No. 3430-0381 Consists of: (8) Ref. 7 Super Rollers, (1) Ref. 6 O-ring, and (2) Ref. 3 Viton Seals

No. 3430-0167 Consists of: (8) Ref. 7 Polypropylene Rollers, (1) Ref. 6 O-ring, and (2) Ref. 3 Viton Seals

No. 3430-0623 Consists of: (1) Ref. 8 Phenolic rotor, (1) Ref. 9 Shaft, and (1) Ref. 15 Key

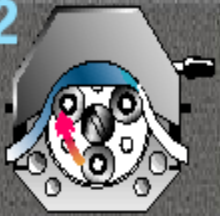
PERISTALTIC

1



A Masterflex pump head consists of only two parts: the rotor and the housing. The tubing is placed in the tubing bed—between the rotor and housing—where it is occluded (squeezed).

2



The rollers on the rotor move across the tubing, pushing the fluid. The tubing behind the rollers recovers its shape, creates a vacuum, and draws fluid in behind it.

3

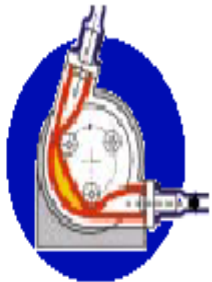


A "pillow" of fluid is formed between the rollers. This is specific to the ID of the tubing and the geometry of the rotor. Flow rate is determined by multiplying speed by the size of the pillow. This pillow stays fairly constant except with very viscous fluids.



Dry-Running Design

This pump design incorporates a unique tube bed that always ensures that one roller is occluding the hose. Termed dry-running because rollers that do not operate in a lubricated bath occlude the hose. Dry running pumps are available in models capable of discharge pressures up to 60 psig. Unique dual-hose versions provide a nearly pulse-free flow stream.

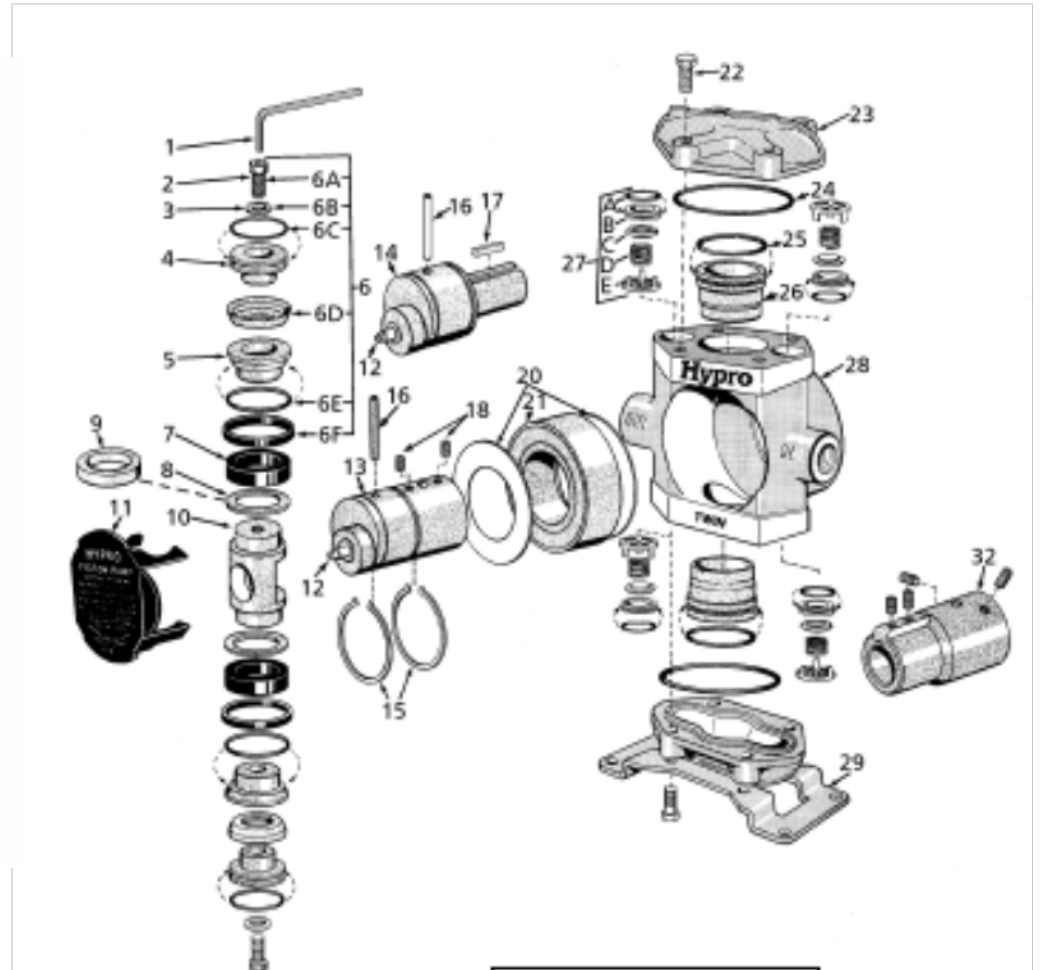


Lubricated Bath Design

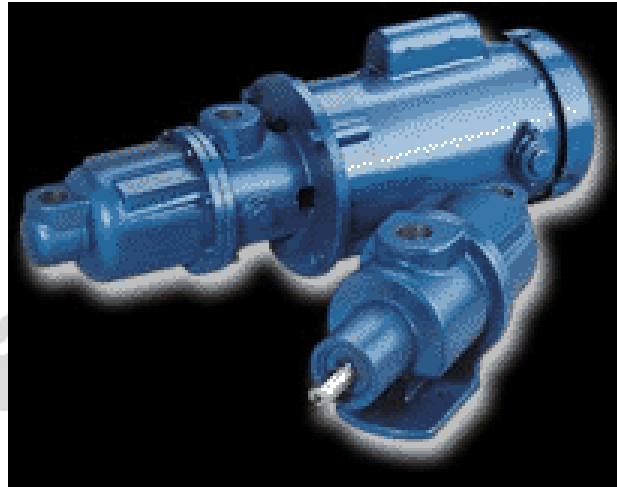
Used in PK series only, this design uses two sliding shoes on the rotor to occlude the hose. The rotor and hose operate in a lubricated bath that reduces friction on the hose and provides the long life typical of this type of hose pump design. These pumps are capable of operating at discharge pressures up to 220 psig (15 bar).



PISTON / PLUNGER



PROGRESSIVE CAVITY TYPE



HOPPER

PUMP END

DRIVE

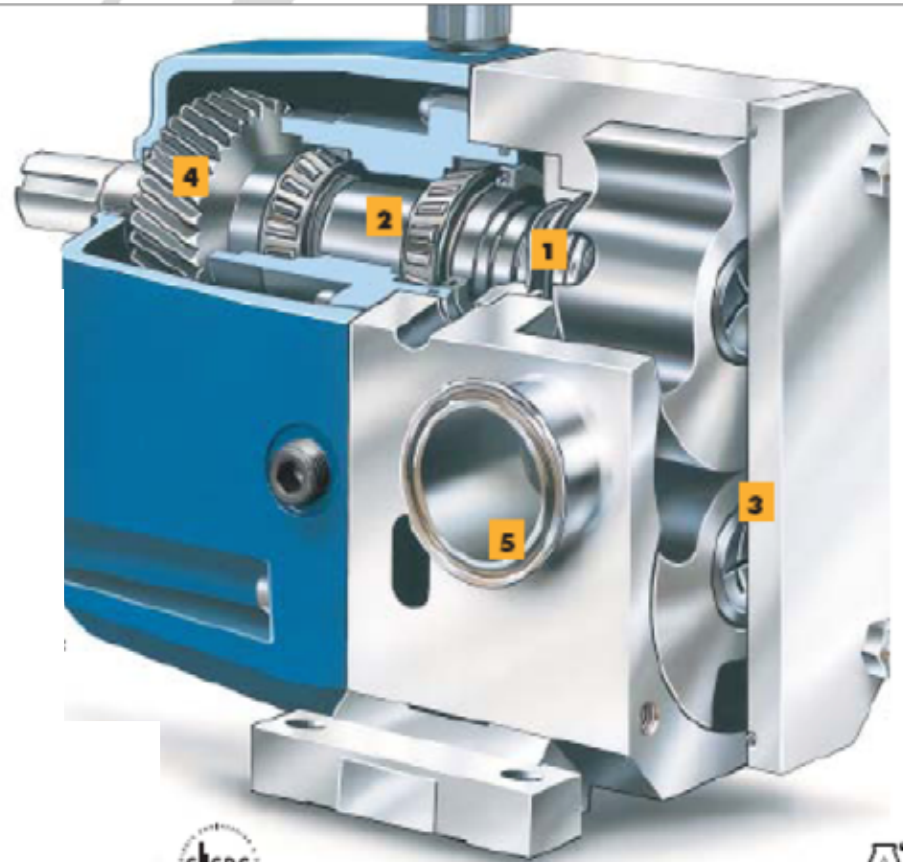
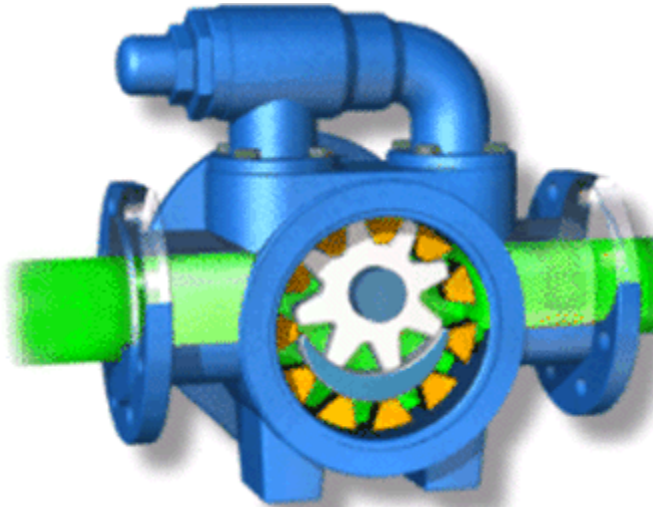


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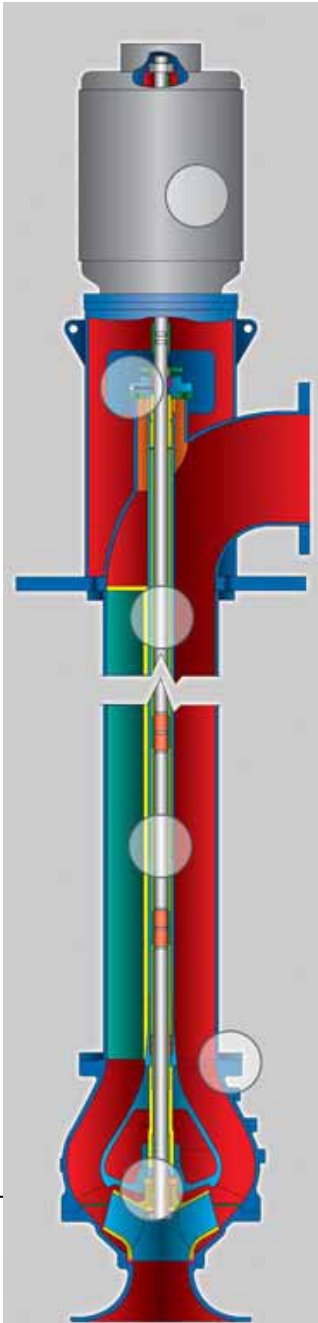
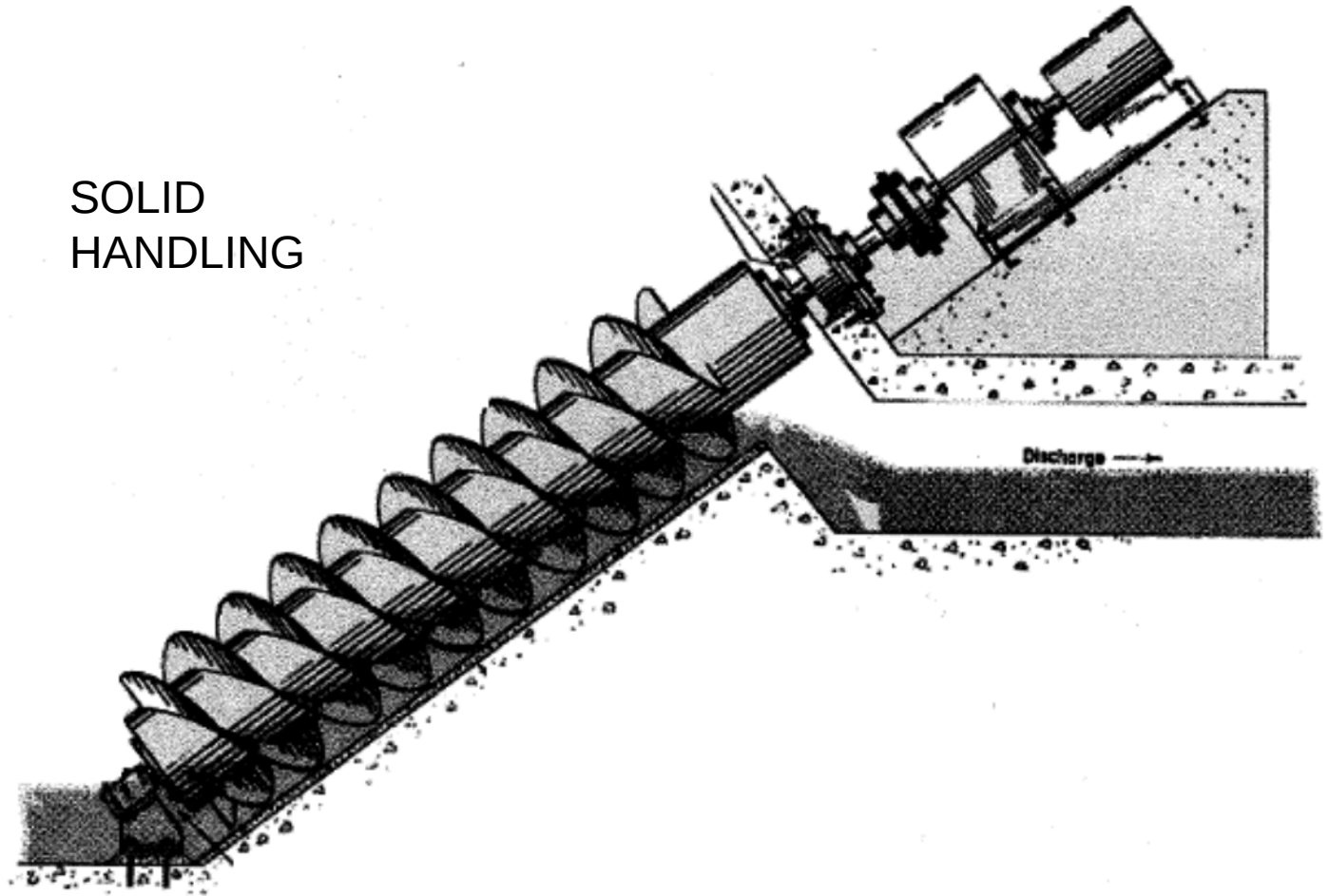


GEAR / LOBE PUMPS



Rotary Screw

SOLID
HANDLING

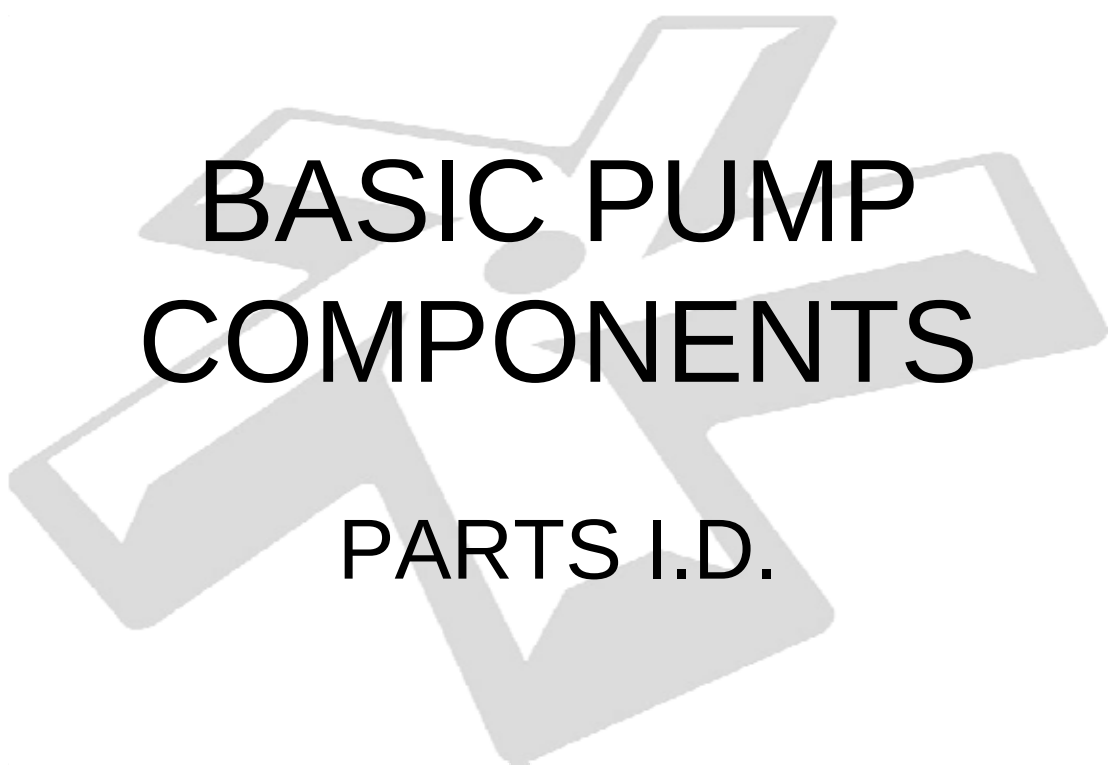


HYBRID PUMP

SUBMERSIBLE GRINDER/ PROGRESSIVE CAVITY UNIT



The HPD200 is a completely submersible sewage grinder pump for residential applications. Complete packaged systems also available.

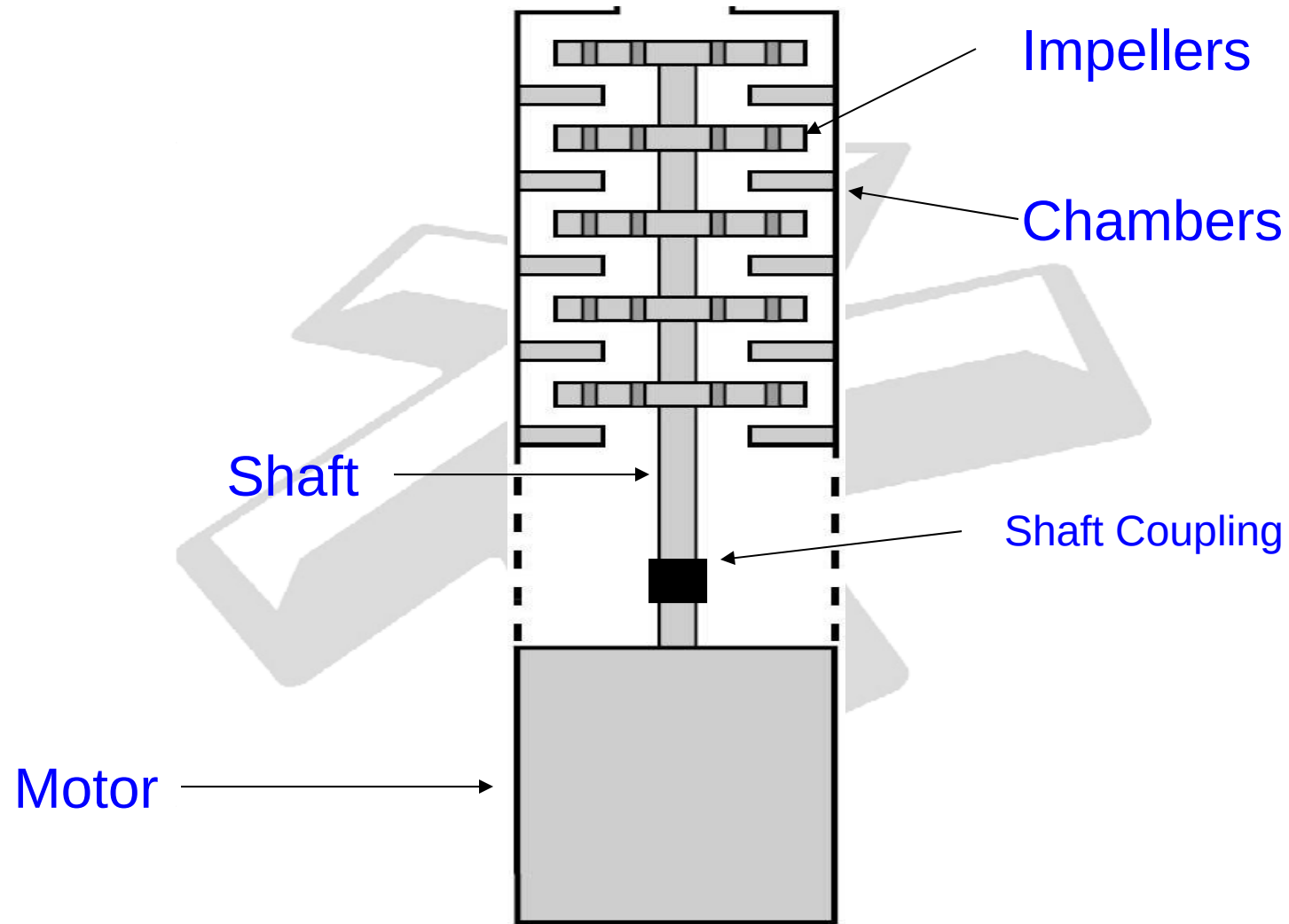


BASIC PUMP COMPONENTS

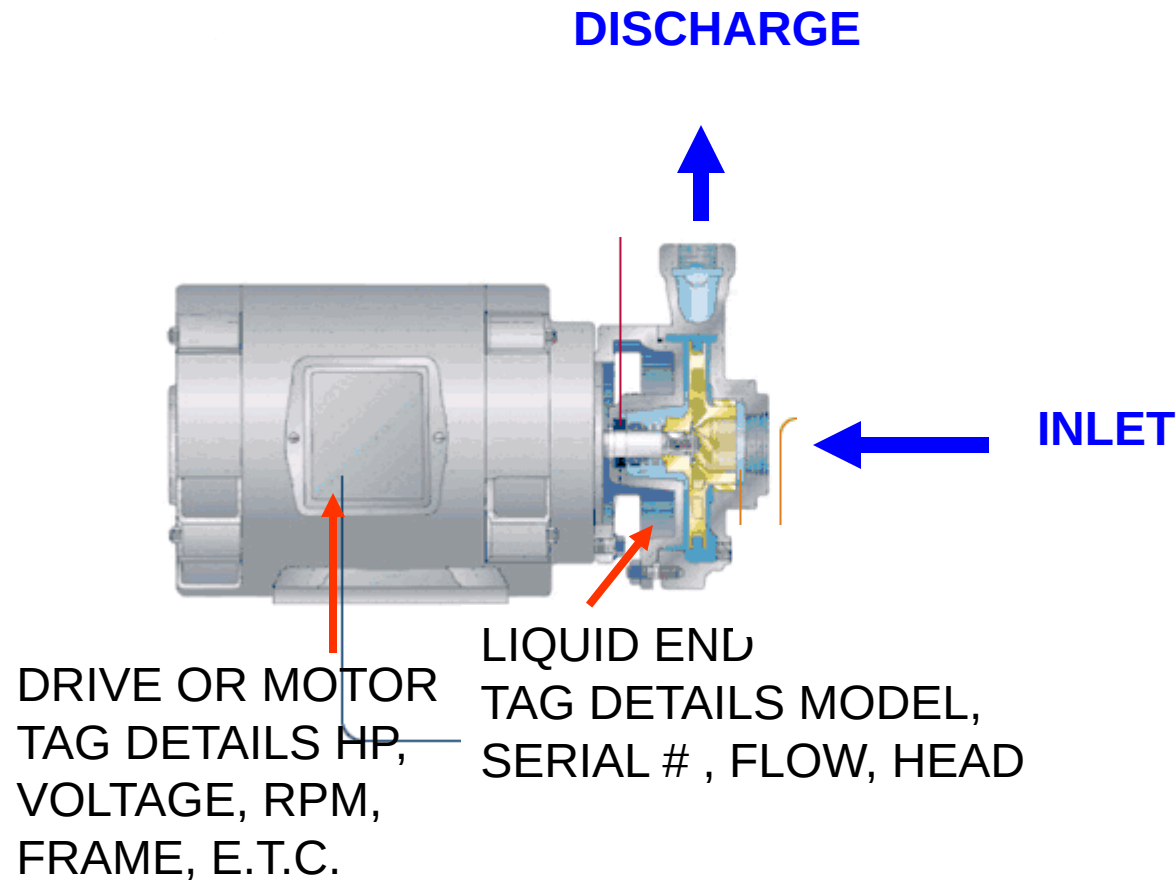
PARTS I.D.



Main Parts of a Submersible Pump



END SUCTION

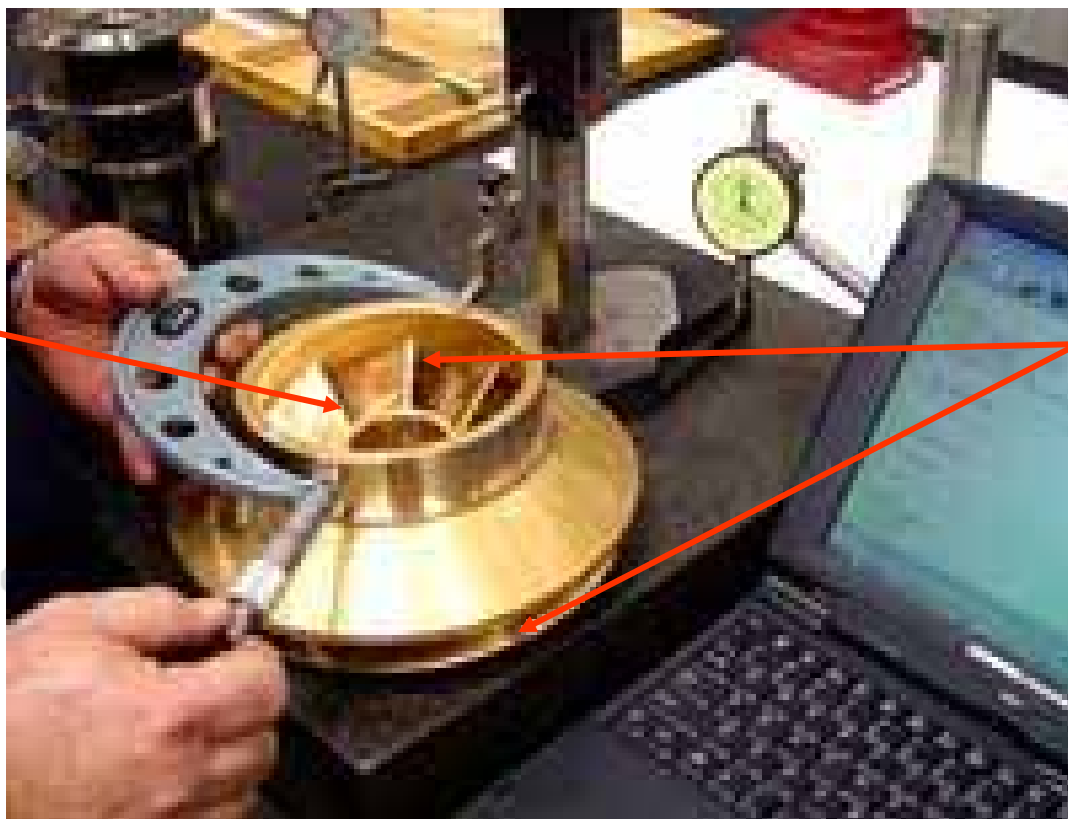


BASIC PARTS

- **IMPELLER** – CREATES THE FLOW OF LIQUID
- **IMPELLER EYE** – CHANNELS FLUID INTO IMPELLER VANES
- **IMPELLER VANES** – ASSIST IN ADDING CENTRIFUGAL FORCE TO FLUID

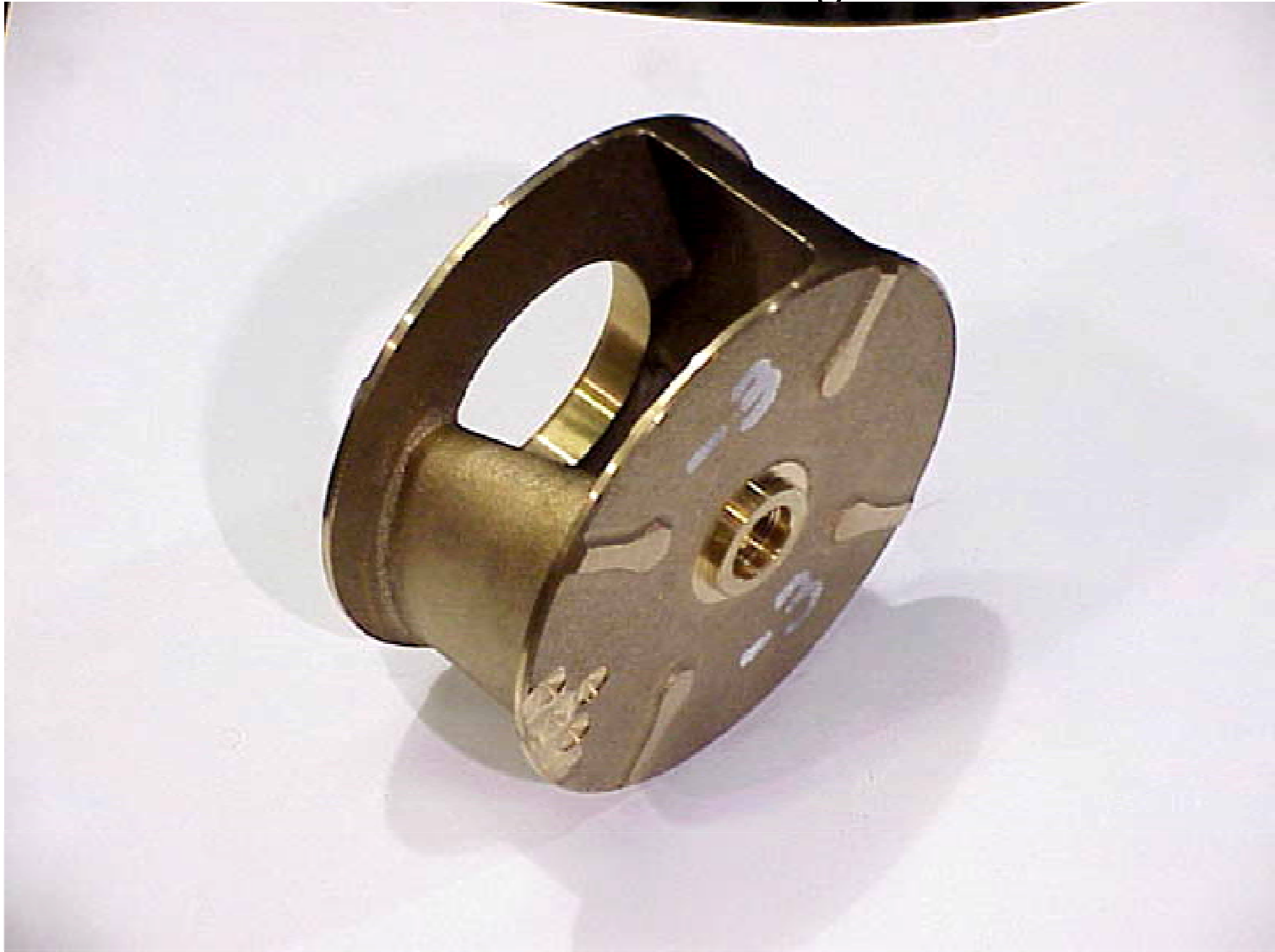


Impeller Eye

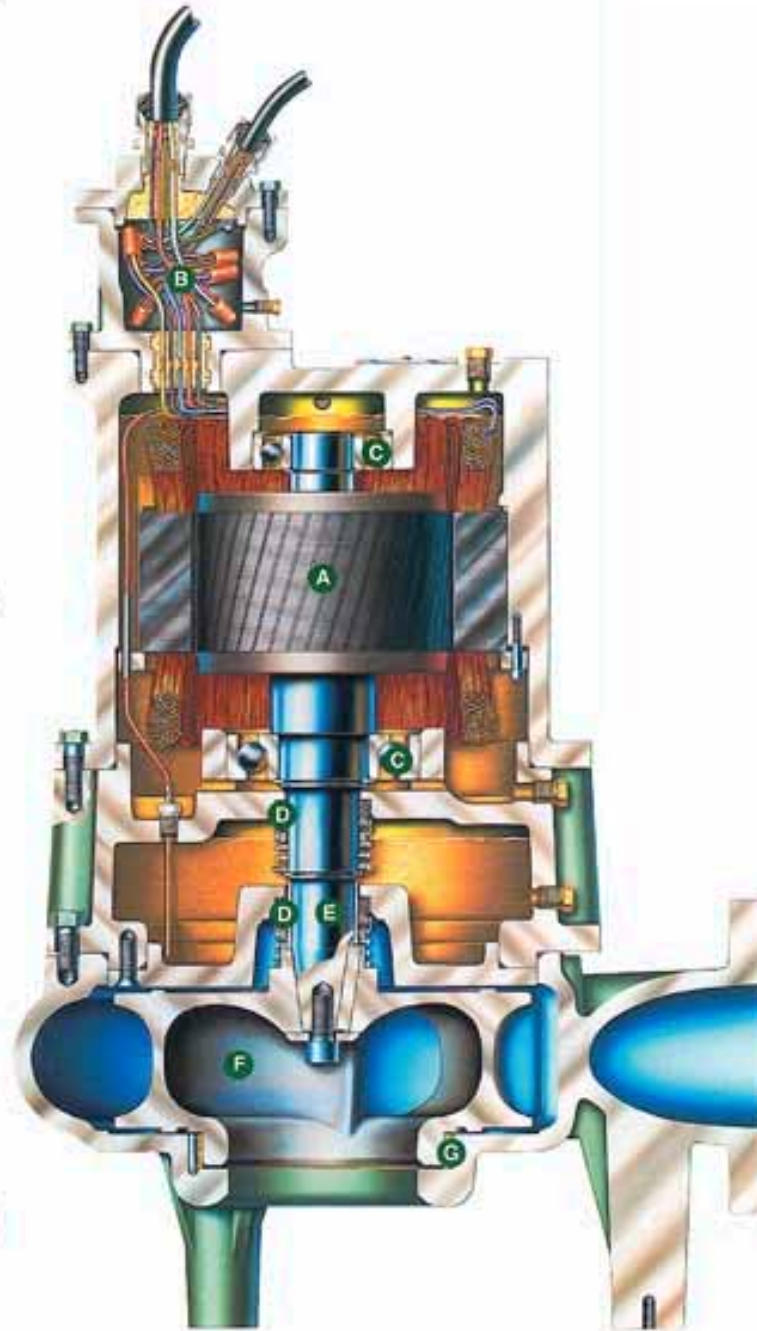


Impeller Vanes

IMPELLER - Non-Clogs



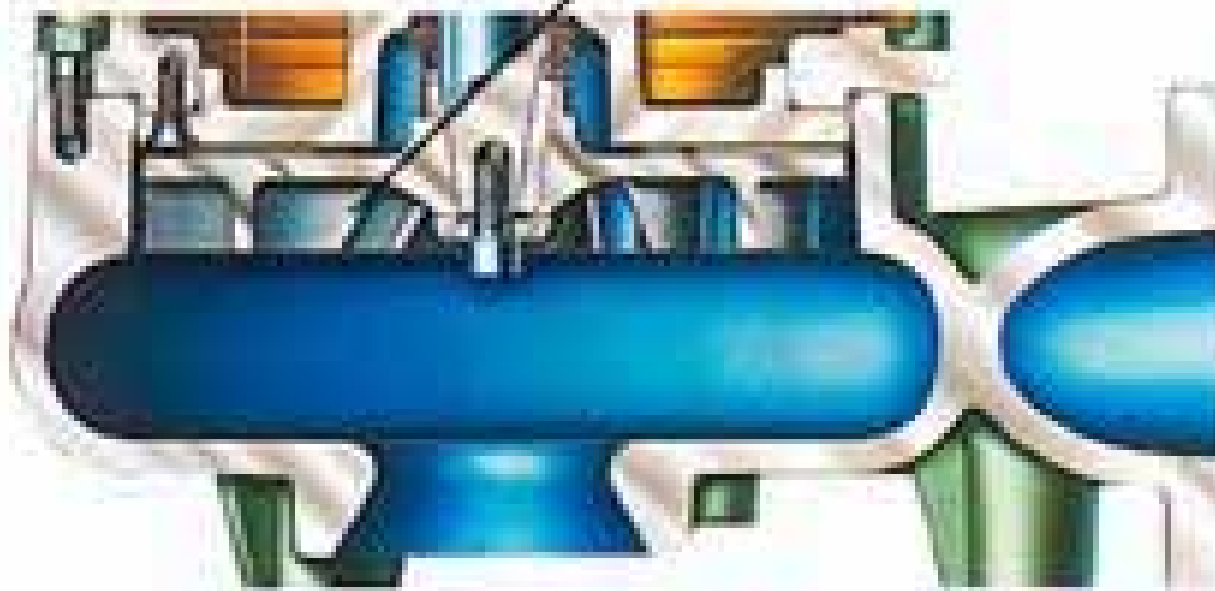
Dual Seal Non-Clog Pumps



IMPELLER – VORTEX OR OPEN



Recessed Impeller



HP HYDROMATIC
Pentair Pump Group

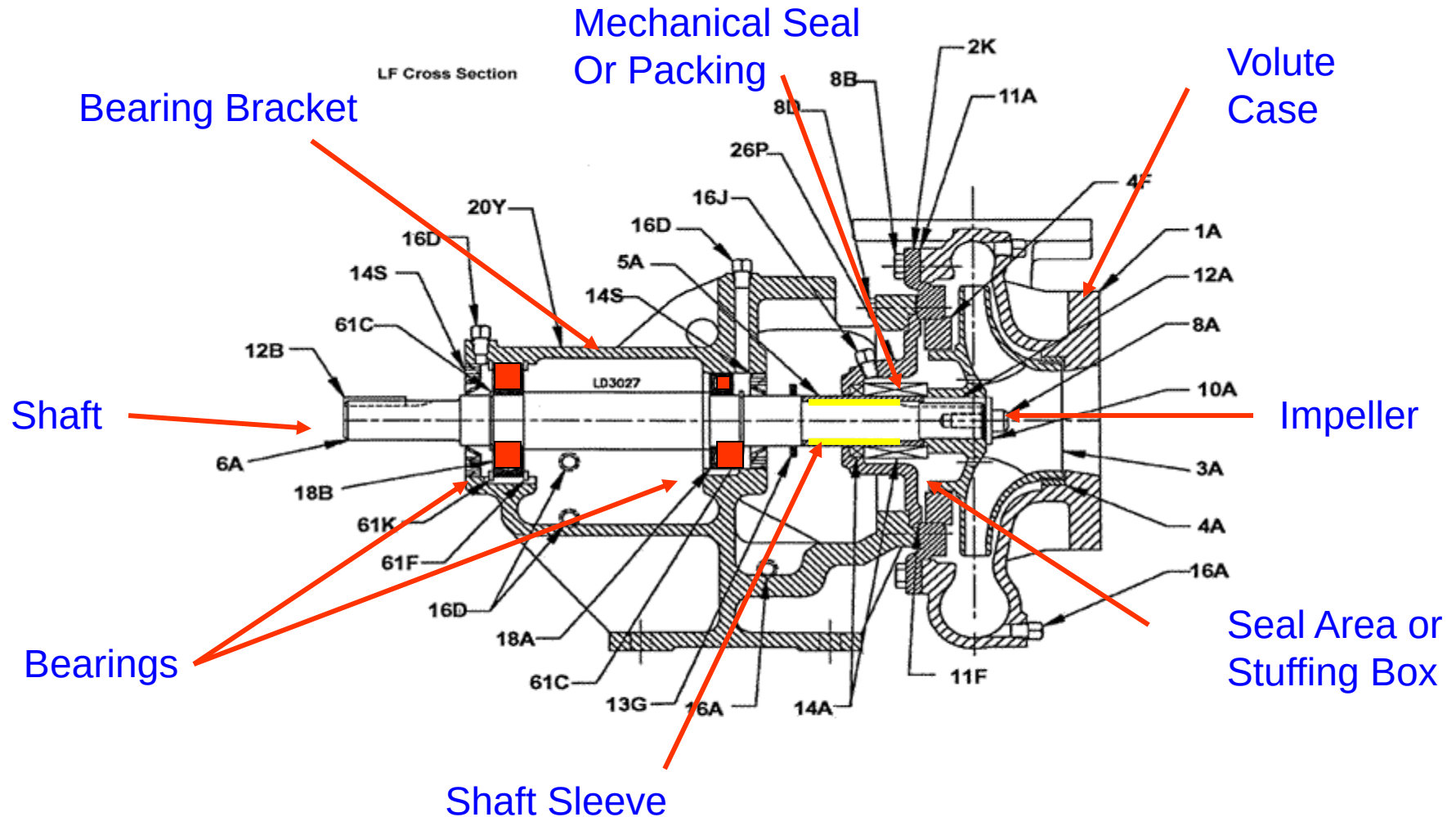
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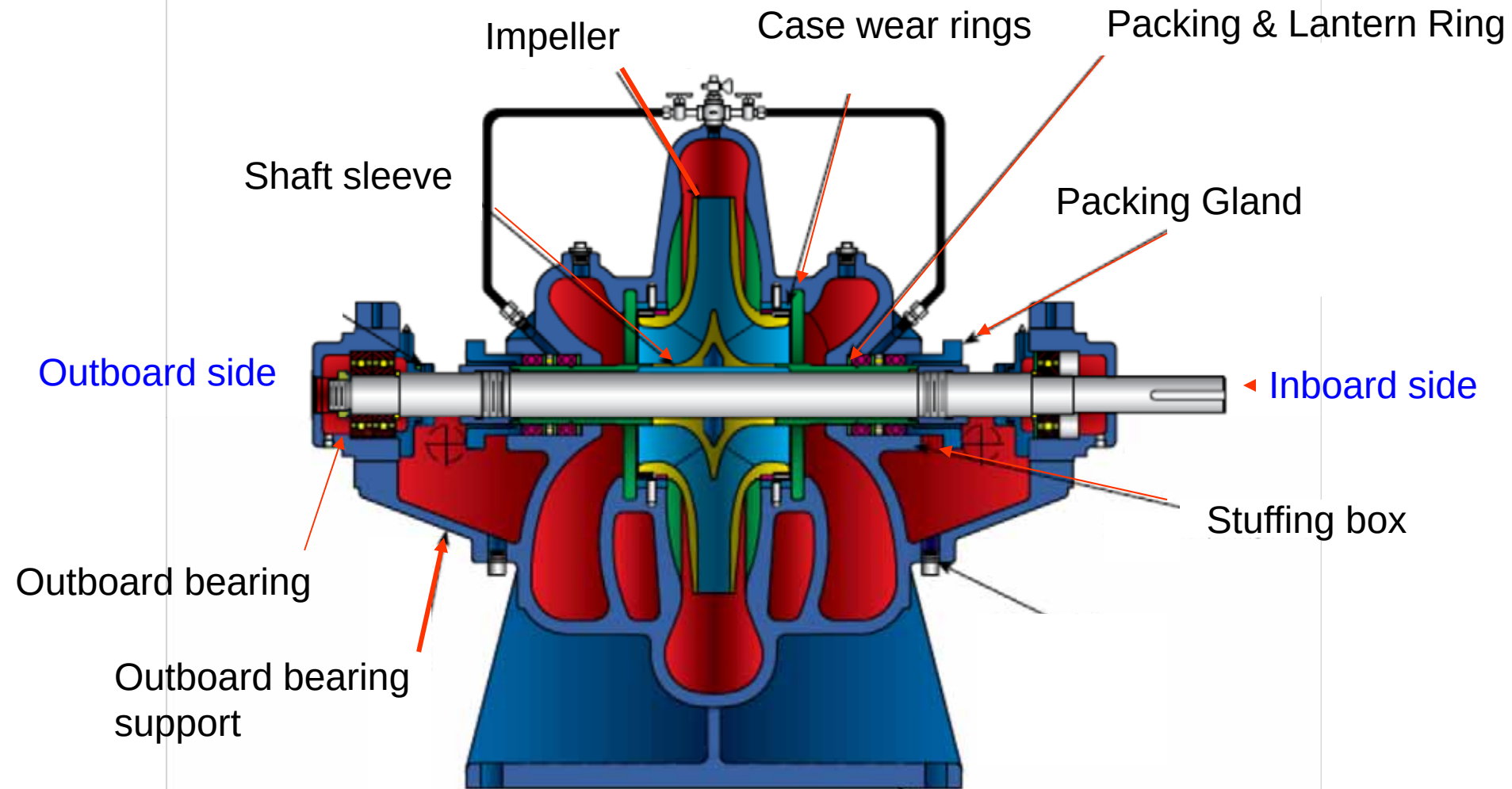
BASIC PARTS

- **SHAFT** – THIS ALLOW THE TRANSFER OF ENERGY FROM THE MOTOR TO THE IMPELLER
- **SHAFT SLEEVE**- THIS IS A WEAR ITEM TO PROTECT THE SHAFT.
- **BEARINGS**- THESE KEEP THE BASIC ALIGNMENT THRU-OUT THE ROTATING ASSEMBLY & HANDLE THRUST & AXIAL LOADS

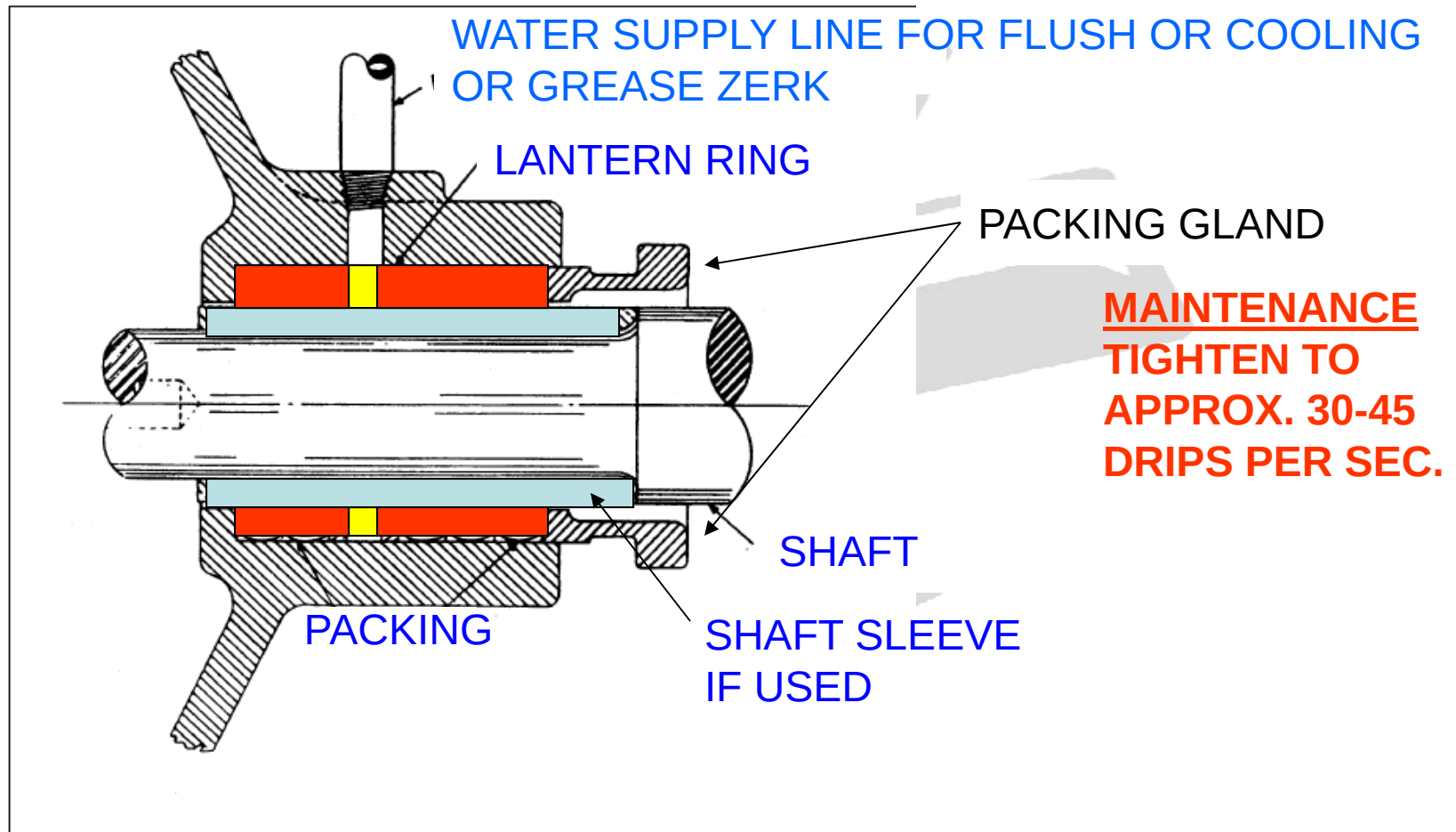
End Suction Parts Break Down



HORIZONTAL SPLIT CASE



STUFFING BOX WITH LANTERN RING



MECHANICAL SEALS

STATIONARY
SEAT

ROTATING
HEAD

SPRING



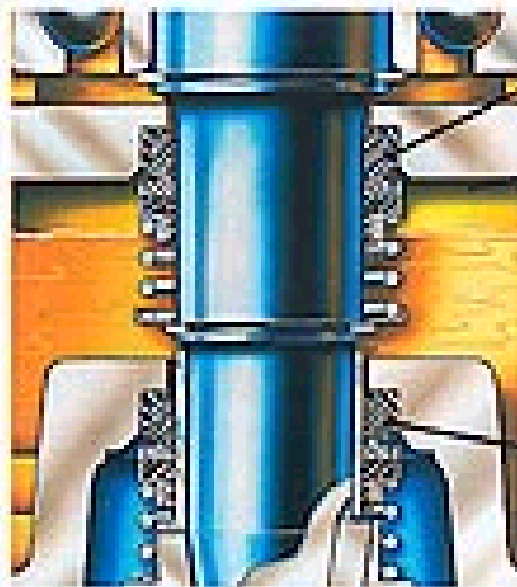
JOHN CRANE TYPE 21



CARTRIDGE TYPE



DUAL SEAL DESIGNS

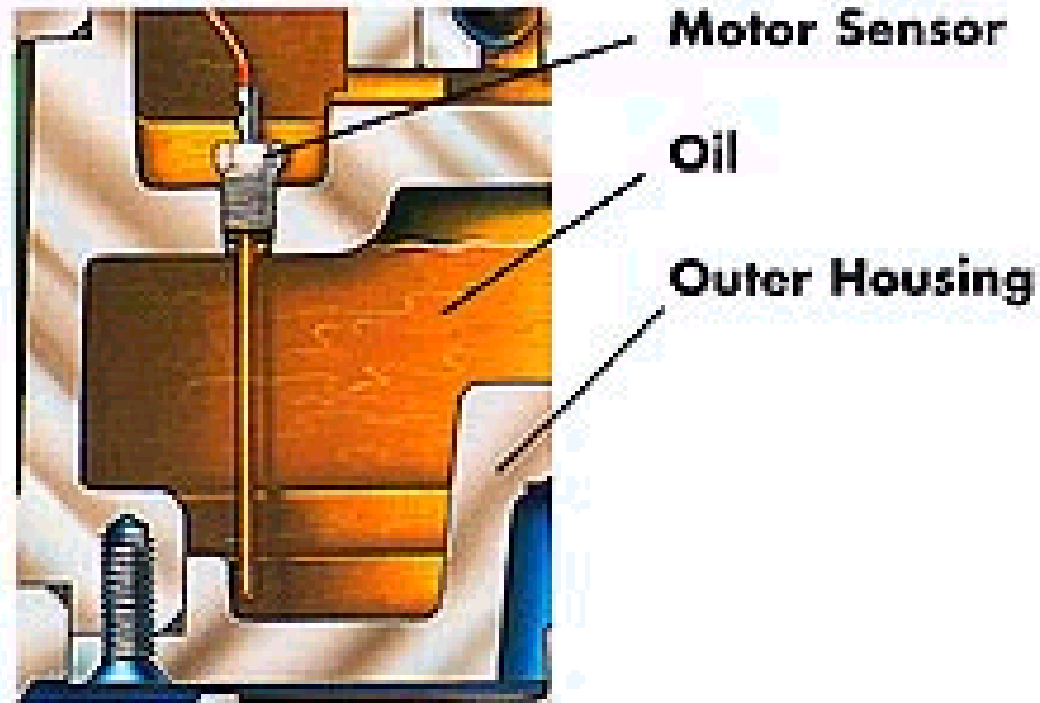


Upper Seal

**Air Pocket
compresses
with pressure
to serve as damper**

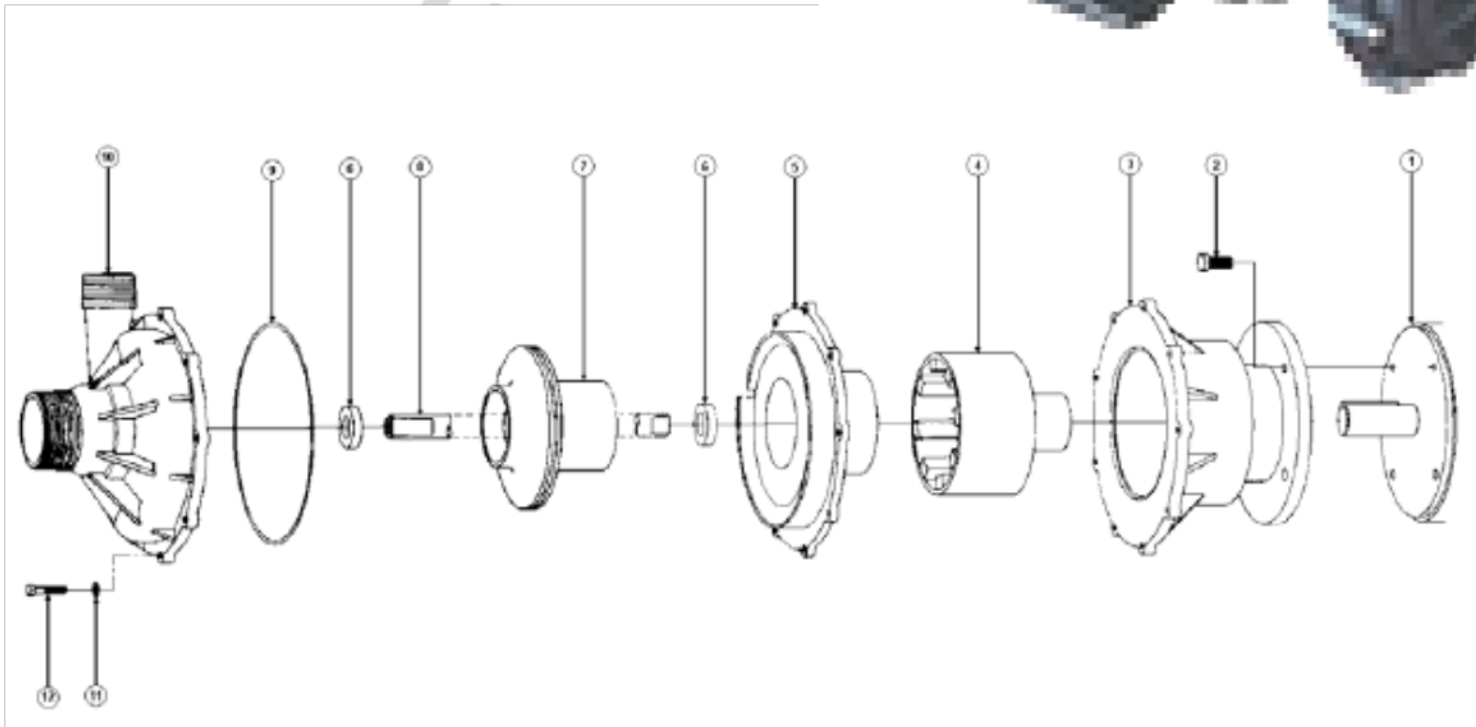
**Lower Seal is
outside the chamber**

The mechanical dual seal system protects your motor from media contamination to provide you exceptionally long pump service.

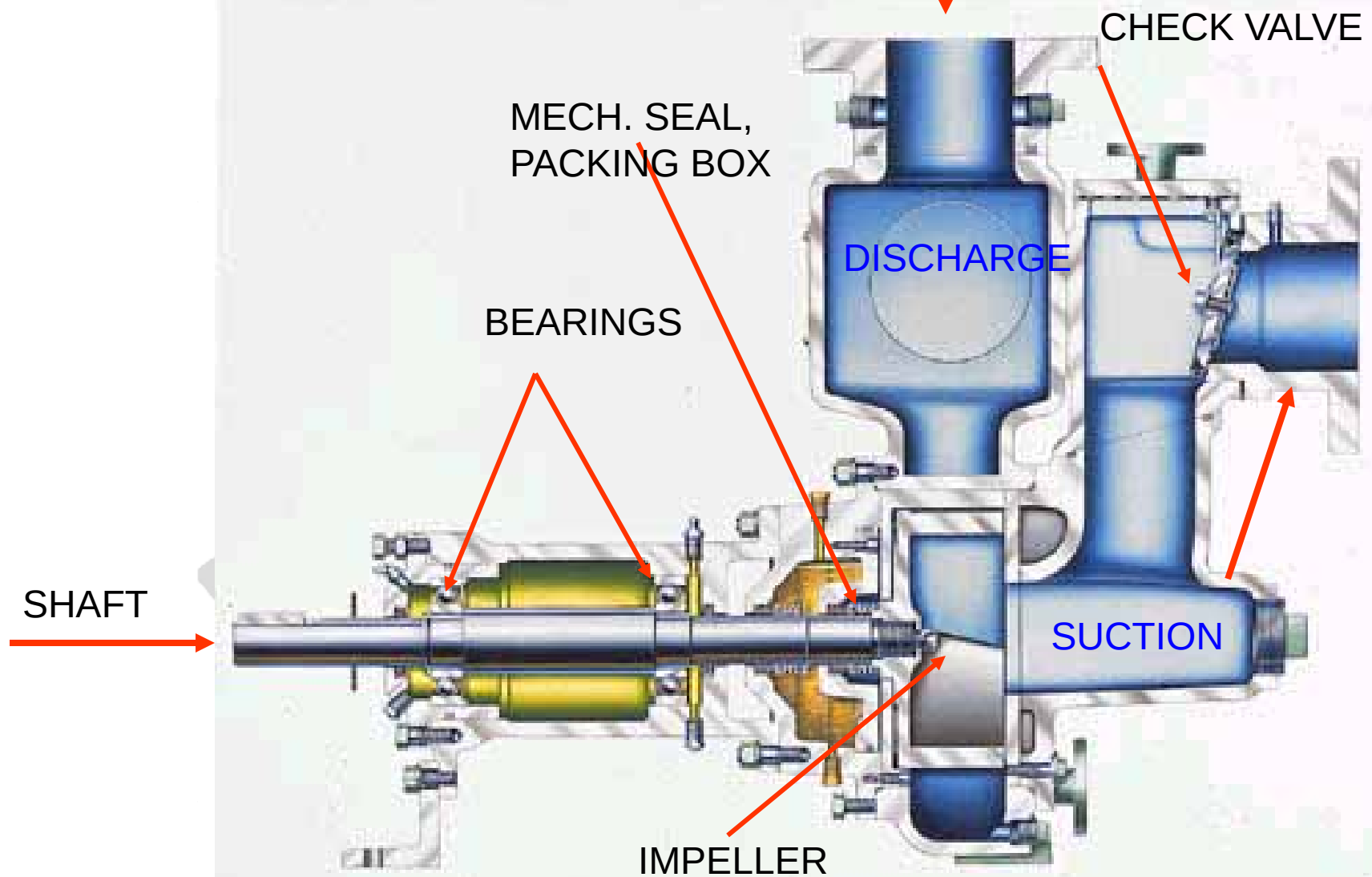


SEAL FAILURE PROBES

Seal-less Magnetic Driven



GUESS THE PART NAME



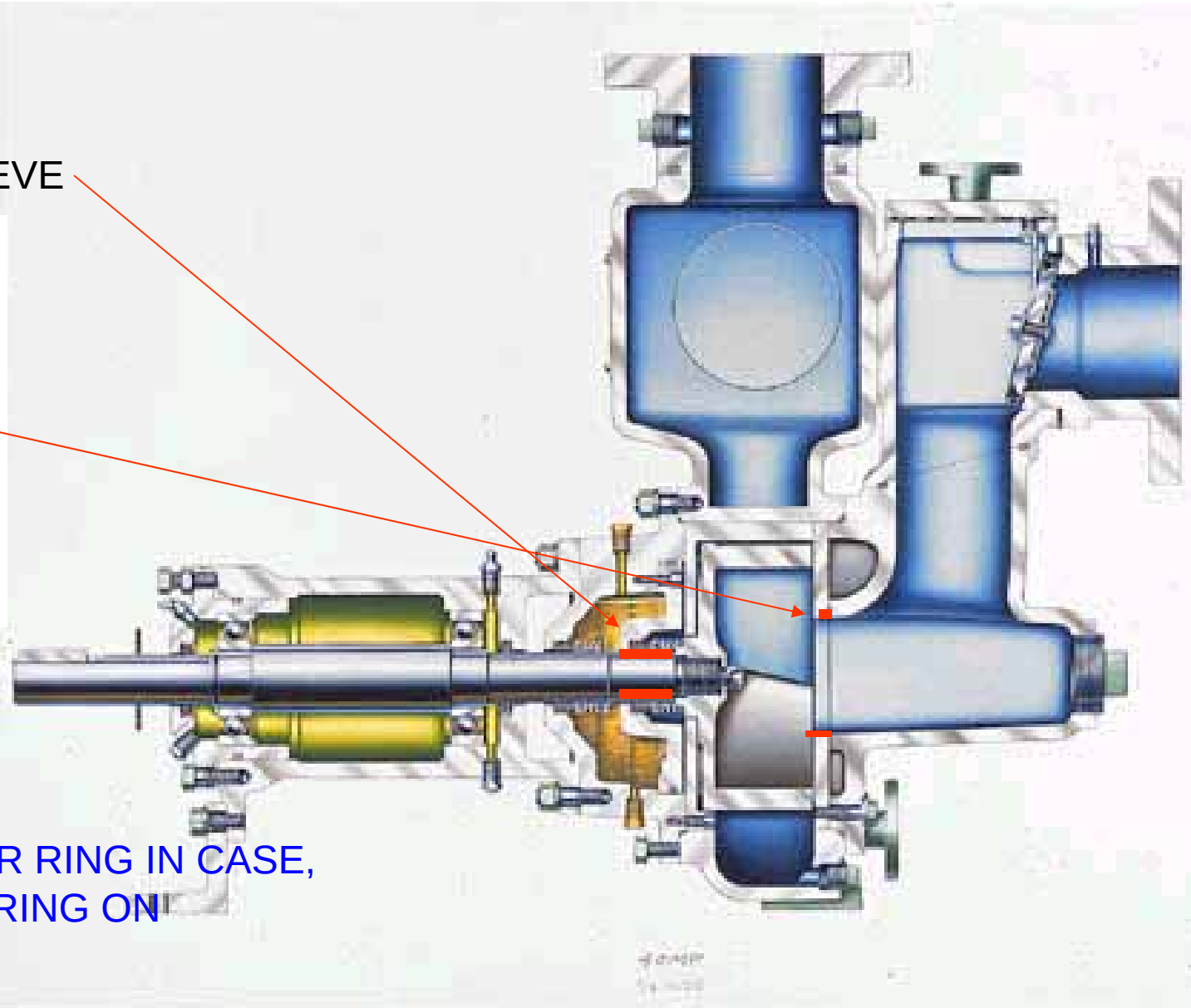
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WHERE WOULD THIS PART GO?

SHAFT SLEEVE

WEAR RINGS

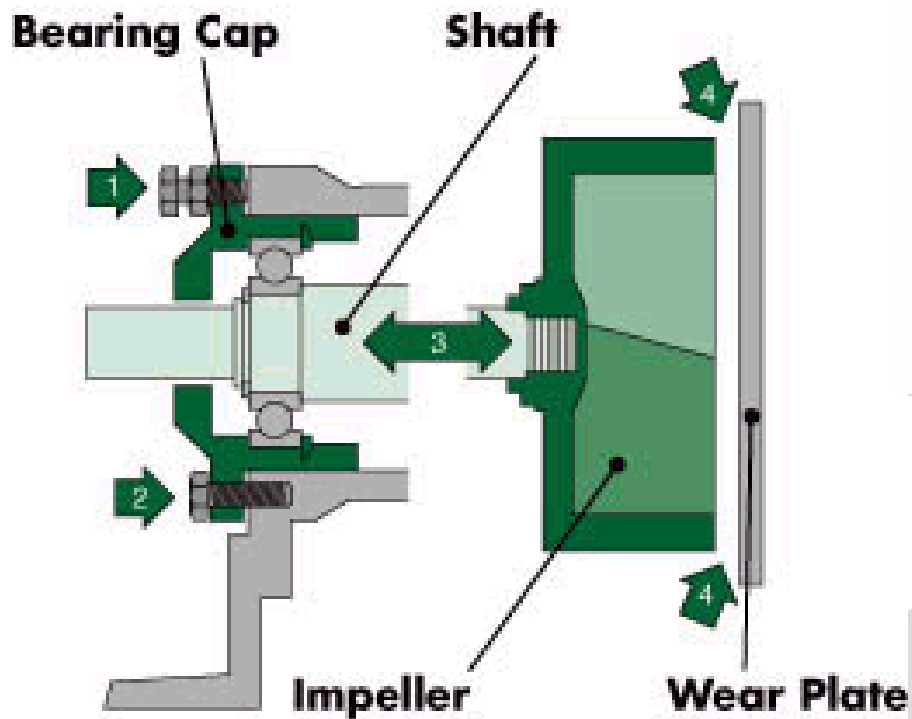


NOTE: CASE WEAR RING IN CASE,
IMPELLER WEAR RING ON
IMPELLER



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HEADS / FLOWS & PUMP CURVES



THE FOLLOWING STEPS MUST BE TAKEN WHEN SIZING A PUMP

- DETERMINE THE GPM (GALLONS PER MINUTE) REQUIRED.
- DETERMINE THE SUCTION HEAD
- DETERMINE THE DISCHARGE HEAD
- DETERMINE THE TOTAL HEAD
- DETERMINE THE FRICTION LOSS
- DETERMINE THE TDH (TOTAL DYNAMIC HEAD)

Save this Formula

- $\text{PSI} \times 2.31 = \text{FEET HEAD}$

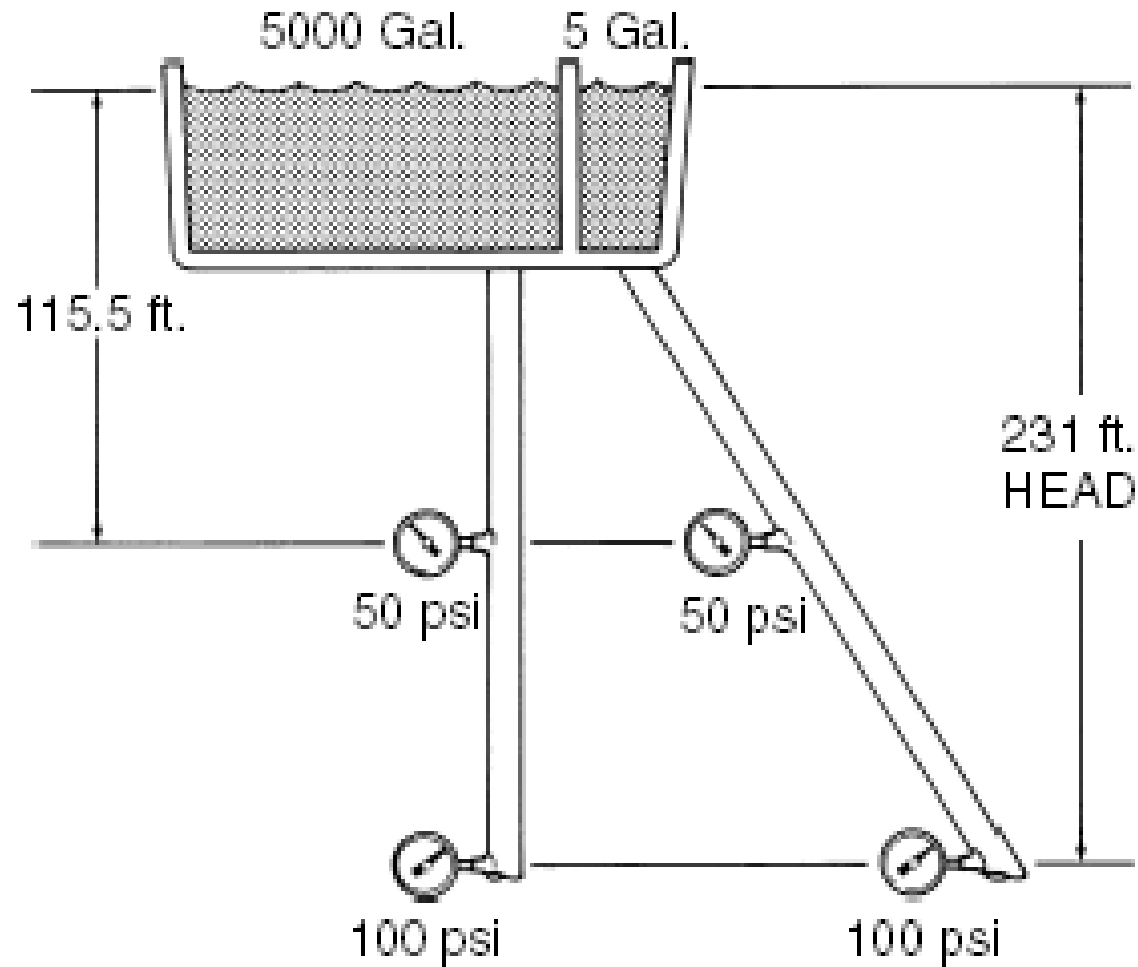
Example $43.3 \text{ PSI} \times 2.31 = 100'$

- $\text{FEET} \times .433 = \text{PSI}$

Example $100' \times .433 = 43.3 \text{ PSI}$



PRESSURE VS FEET OF HEAD



Head (H)

Centrifugal pumps are not rated in developed pressure (P), but rather in developed head.

A pump will develop only as much head as required to overcome resistance to flow.

Total Dynamic Head (TDH) is found by adding:

Pumping level (Well Static Level or draw down level)

Elevation (Additional feet required to delivery flow)

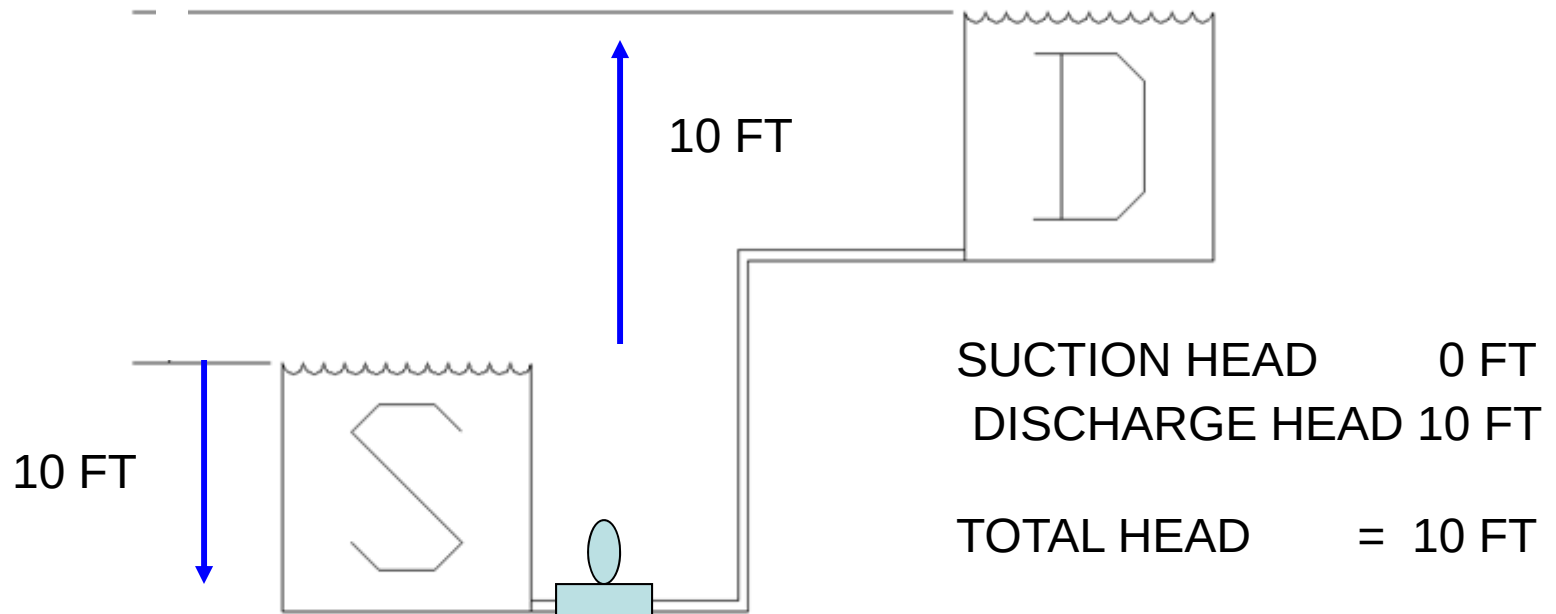
Pressure (PSI converted to feet for controls / storage)

Friction Loss (Feet of resistance from pipe, fittings, valves)



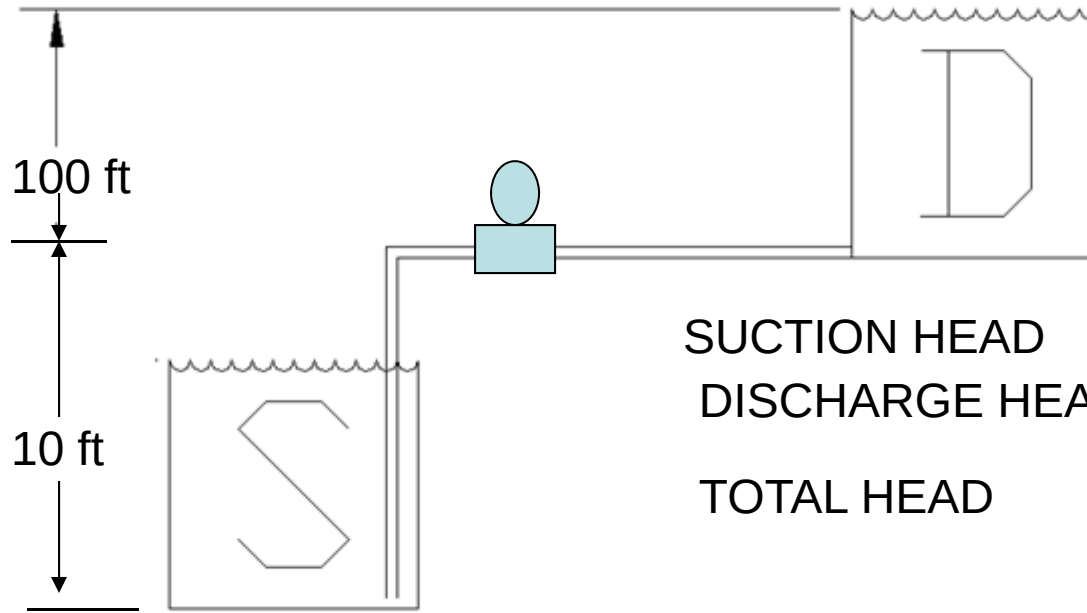
SUCTION vs. DISCHARGE HEAD

Note Piping Arrangements



SUCTION vs. DISCHARGE HEAD

Note Piping Arrangements



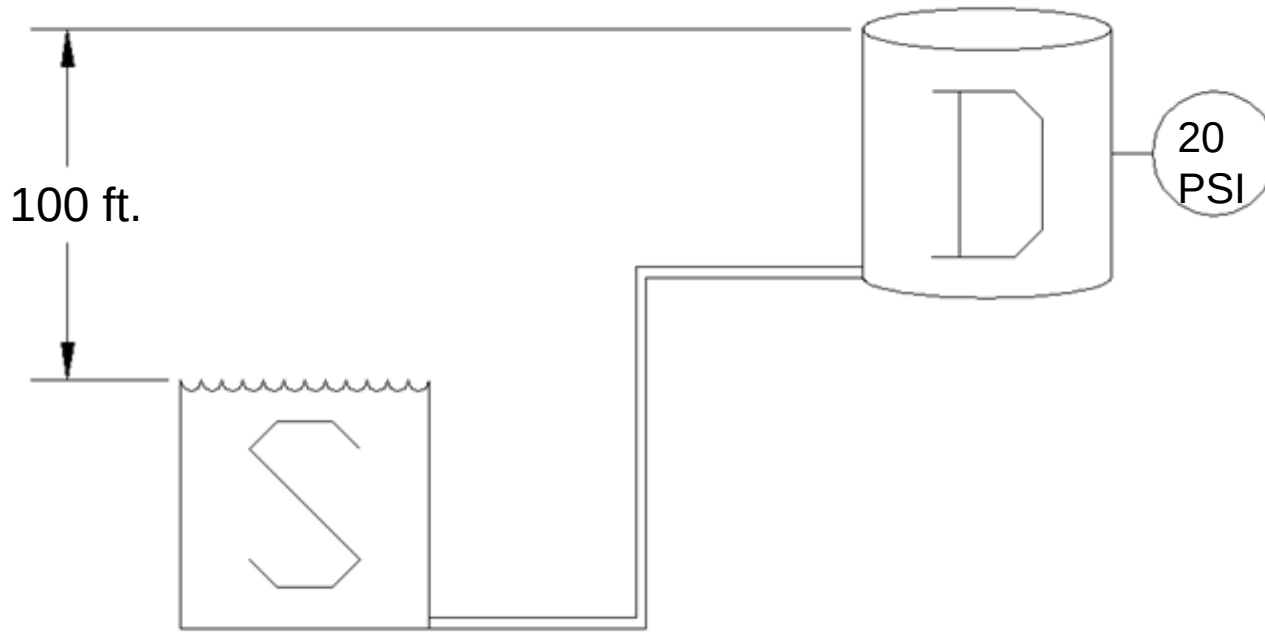
SUCTION HEAD = 10FT

DISCHARGE HEAD = 100 FT

TOTAL HEAD = 110 FT



Determining Pressure Head



$P = 20 \text{ PSI}$ or $P = 46 \text{ ft}$

Add $H = 100 \text{ ft}$

Pressure Head = 146 ft

THE C FACTOR?

- AS WATER MOVES THRU A PIPE, IT RUBS AGAINST THE INSIDE OF THE PIPE.
- THERE ARE FOUR FACTORS TO CONSIDER WHEN DETERMINING FRICTION LOSS.



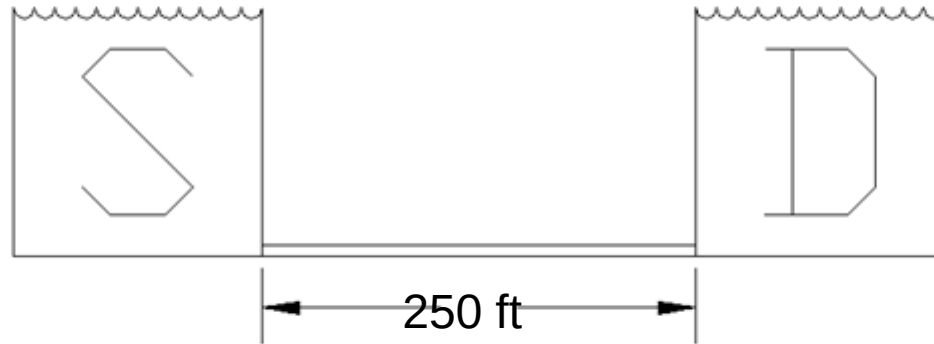
THE C FACTOR?

- THE PIPE SIZE OR INSIDE DIAMETER.
- THE FLOW (VOLUME) THRU THE PIPE.
- THE LENGTH OF THE PIPE.
- **THE C FACTOR:** IS KNOWN AS THE COEFFICIENT OF FRICTION. IT REPRESENTS THE ROUGHNESS OF THE INSIDE OF THE PIPE WALL.



Friction Head

Is the resistance to flow thru a given diameter of pipe, fittings or valves



Example: @ 16 GPM

1" Sch 40 pipe F.L. = 16.5 ft per 100 ft or $16.5 \times 2.5 = 41.25$ ft F.L. 17.86 PSI

1" Sch80 pipe F.L. = 26.3 ft per 100 ft or $26.3 \times 2.5 = 65.75$ ft F.L. 28.47 PSI

Determining Friction Head

VELOCITY CHART & FRICTION OF WATER

(new steel pipe) at 60° F

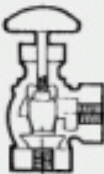
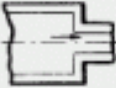
1 INCH

FLOW U.S. GPM	STANDARD WEIGHT STEEL - SCH. 40			EXTRA STRONG STEEL - SCH. 80		
	1.049" Inside Diameter			.957" Inside Diameter		
	VELOCITY (Ft./Sec.)	VELOCITY (Head Ft.)	HEAD LOSS (Ft./100 Ft.)	VELOCITY (Ft./Sec.)	VELOCITY (Head Ft.)	HEAD LOSS (Ft./100 Ft.)
2	0.74	.009	.385	.89	.01	.599
3	1.11	.019	.787	1.34	.03	1.19
4	1.48	.034	1.270	1.79	.05	1.99
5	1.86	.054	1.90	2.23	.08	2.99
6	2.23	.077	2.65	2.68	.11	4.17
8	2.97	.137	4.50	3.57	.20	7.11
10	3.71	.214	6.81	4.46	.31	10.80
12	4.45	.308	9.58	5.36	.45	15.20
14	5.20	.420	12.80	6.25	.61	20.40
16	5.94	.548	16.50	7.14	.79	26.30
18	6.68	.694	20.60	8.03	1.00	32.90
20	7.42	.857	25.20	8.92	1.24	40.30
22	8.17	1.036	30.30	9.82	1.50	48.40
24	8.91	1.23	35.80	10.70	1.80	57.20
26	9.65	1.45	41.70	11.60	2.10	66.80
28	10.39	1.68	48.10	12.50	2.40	77.10
30	11.10	1.93	55.00	13.40	2.80	88.20
35	13.00	2.62	74.10	15.60	3.80	119.00
40	14.80	3.43	96.10	17.90	5.00	154.00
45	16.70	4.33	121.00	20.10	6.30	194.00



Fitting Friction

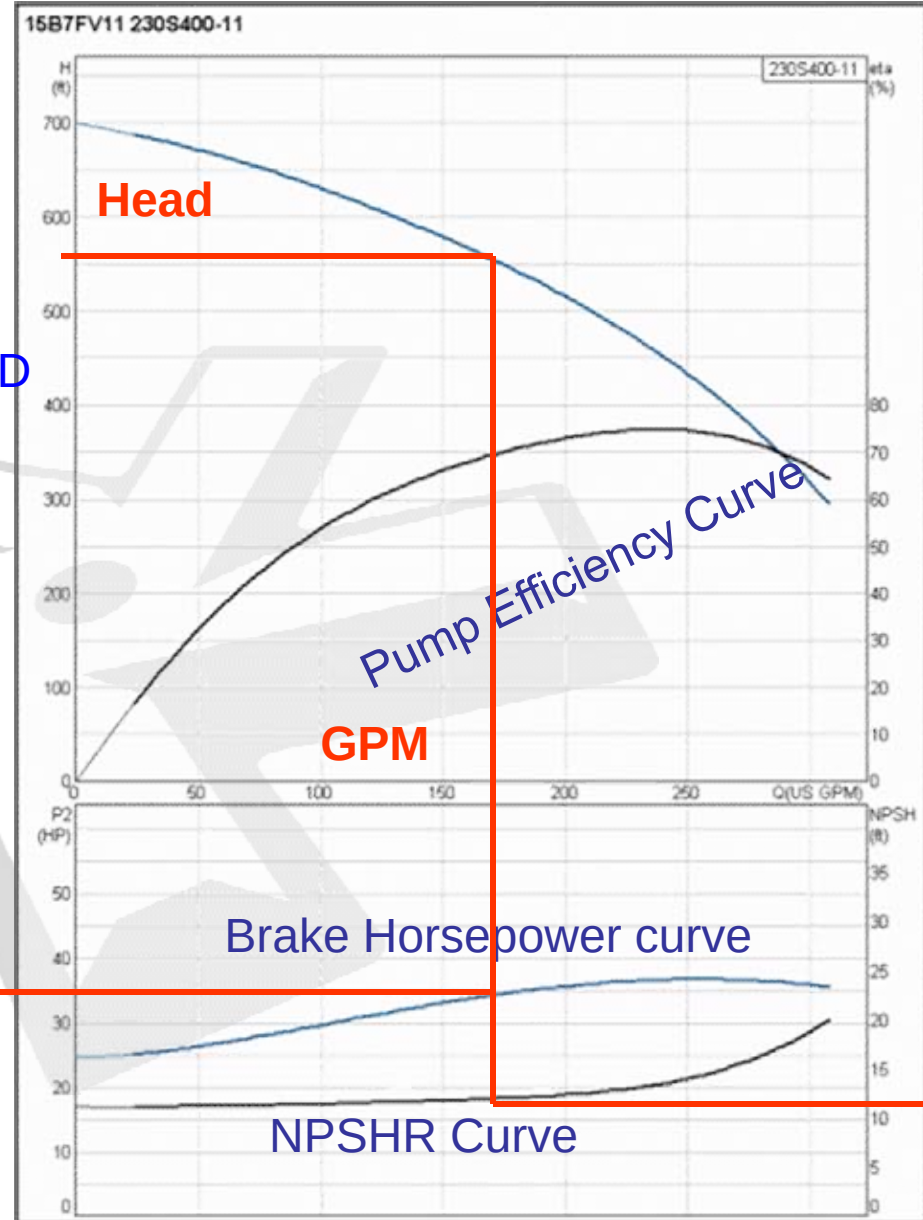
FRICION LOSSES THROUGH PIPE FITTINGS & VALVES

SIZE OF PIPE (Inches)	 GATE VALVE				 GLOBE VALVE- WIDE OPEN	 ANGLE VALVE- WIDE OPEN	 CHECK VALVE- WIDE OPEN	 ORDINARY ENTRANCE TO PIPE LINES	 STD. 90° ELBOW	 MEDIUM SWEEP 90° ELBOW	 LONG SWEEP 90° ELBOW
	WIDE OPEN	1/4 CLOSED	1/2 CLOSED	3/4 CLOSED							
STRAIGHT PIPE IN FEET (EQUIVALENT LENGTH)											
1/8"	.14	.85	5.00	19.00	9.00	5.00	2.00	.46	.74	.65	.50
1/4"	.21	1.25	7.00	26.00	12.00	6.00	3.00	.60	1.00	.86	.70
3/8"	.27	1.80	9.00	36.00	16.00	8.00	4.00	.75	1.40	1.15	.90
1/2"	.41	2.10	12.00	44.00	17.60	7.78	5.18	.90	1.60	1.55	1.10
3/4"	.55	2.90	14.00	59.00	23.30	10.30	6.86	1.40	2.30	2.06	1.50
1"	.70	3.40	18.00	70.00	29.70	13.10	8.74	1.60	2.70	2.62	2.00
1-1/4"	.92	4.80	24.00	96.00	39.10	17.80	11.50	2.50	3.60	3.45	2.50
1-1/2"	1.07	5.60	28.00	116.00	45.60	20.10	13.40	3.00	4.50	4.03	2.90
2"	1.38	7.00	36.00	146.00	58.60	25.80	17.20	3.50	5.40	5.17	3.60
2-1/2"	1.65	8.40	41.00	172.00	70.00	30.90	20.60	4.00	6.50	6.17	4.40
3"	2.04	10.00	52.00	213.00	86.90	38.40	25.50	5.00	8.50	7.67	5.50
3-1/2"	2.10	12.50	60.00	246.00	100.00	52.00	24.00	5.50	10.0	8.50	6.30
4"	2.40	14.00	70.00	285.00	116.00	57.00	27.00	6.50	12.0	9.50	7.20



WHEN SELECTING A PUMP

1. START WITH TDH NEEDED
2. DROP DOWN TO GPM NEEDED
3. CHECK % EFFICIENCY
4. CHECK HORSE POWER
5. CHECK NPSHR



What is NPSHR?

(Net Positive Suction Head)

CAN BE DEFINED AS THE HEAD THAT CAUSES LIQUID TO FLOW THROUGH THE SUCTION PIPING AND FINALLY ENTER THE EYE OF THE IMPELLER.

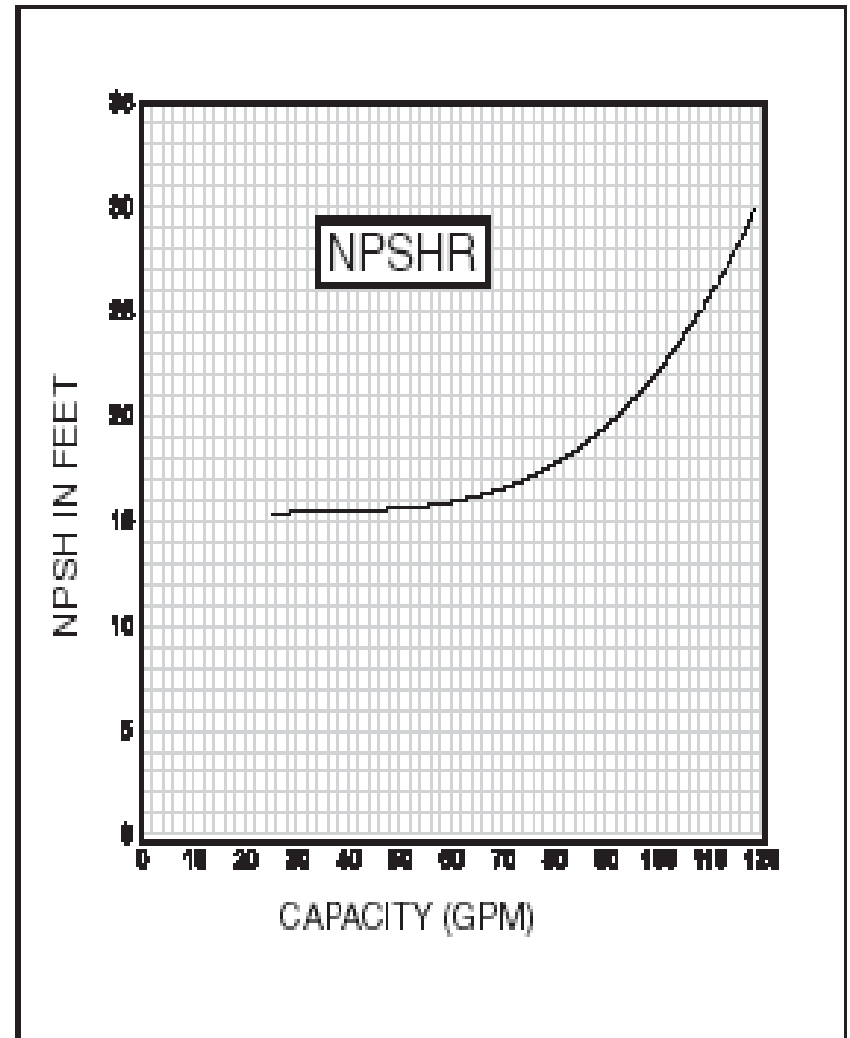
TWO TYPES

NPSHR =
NET POSITIVE SUCTION HEAD REQUIRED.

NPSHA =
NET POSITIVE SUCTION HEAD AVAILABLE.

OR in the case of submergible

MINIMUM SUBMERGENCE.



What is NPSHA?

Atmospheric pressure assist fluids in flowing into the eye of a pump

Take NPSHA 28.2

Minus NPSHR 15.0

A positive # 13.2

Indicates volume can be passed thru impeller

- Atmospheric Pressure Charts at various altitudes

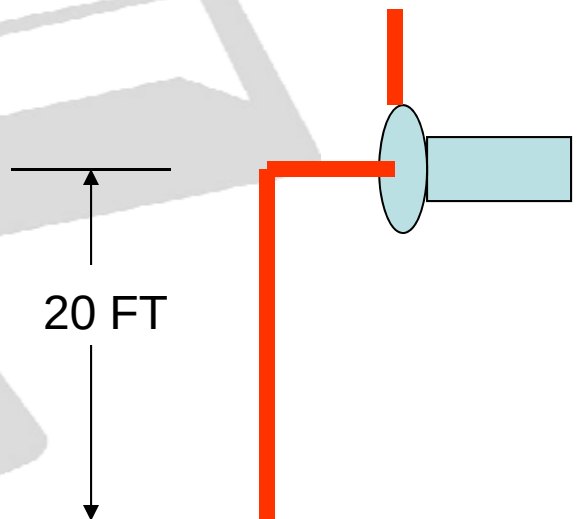
- @ sea level = 33.9'

- @ 4000' = 29.2'

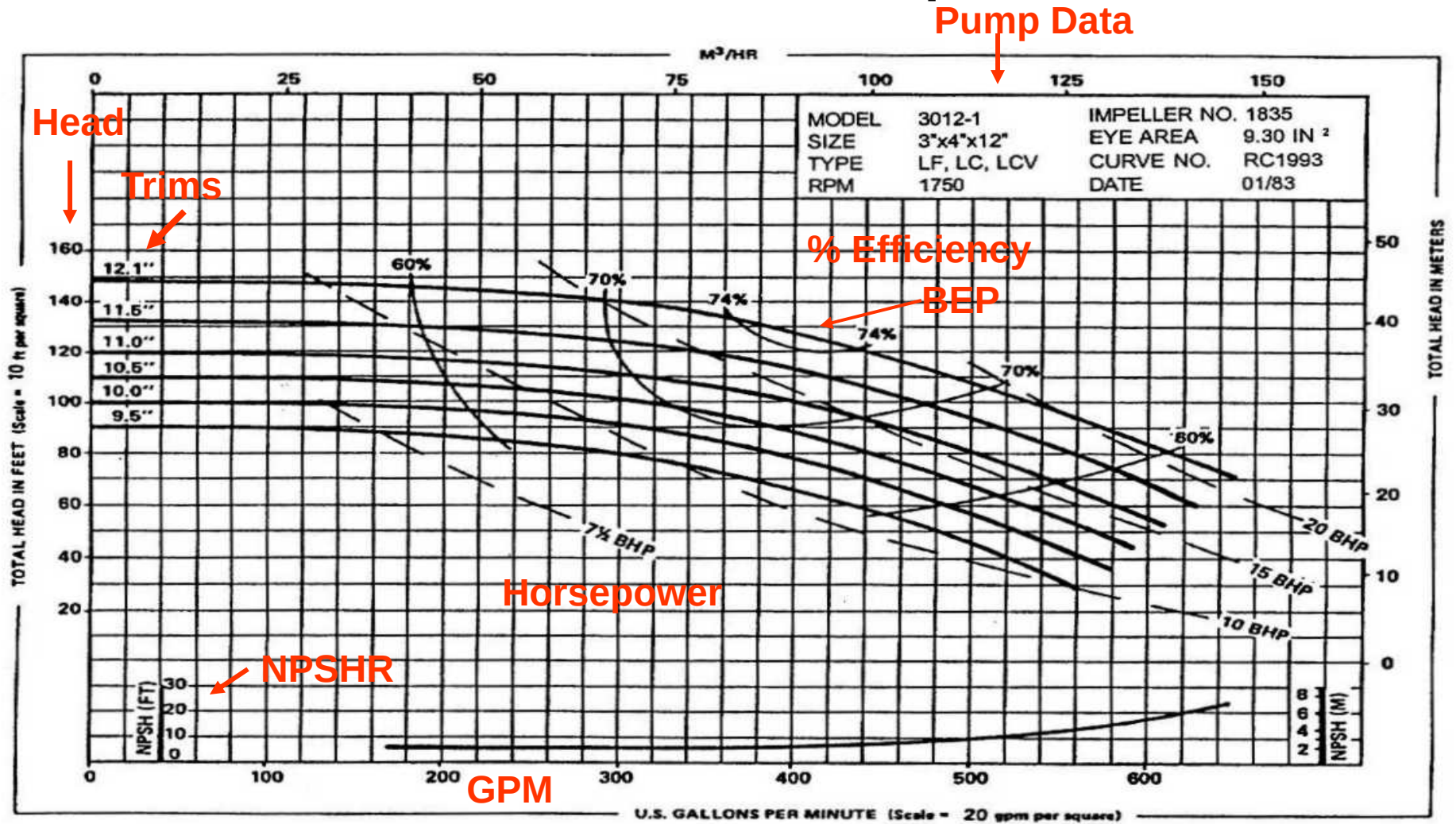
- @ 5000' = 28.2'

- @ 6000' = 27.2'

Negative Suction Head

- Atmospheric Pressure Charts at various altitudes
 - @ sea level = 33.9'
 - @ 5000' = 28.2'
 - @ 6000' = 27.2'
- 
- **TEST QUESTION DO NOT EXCEED 20 FT**

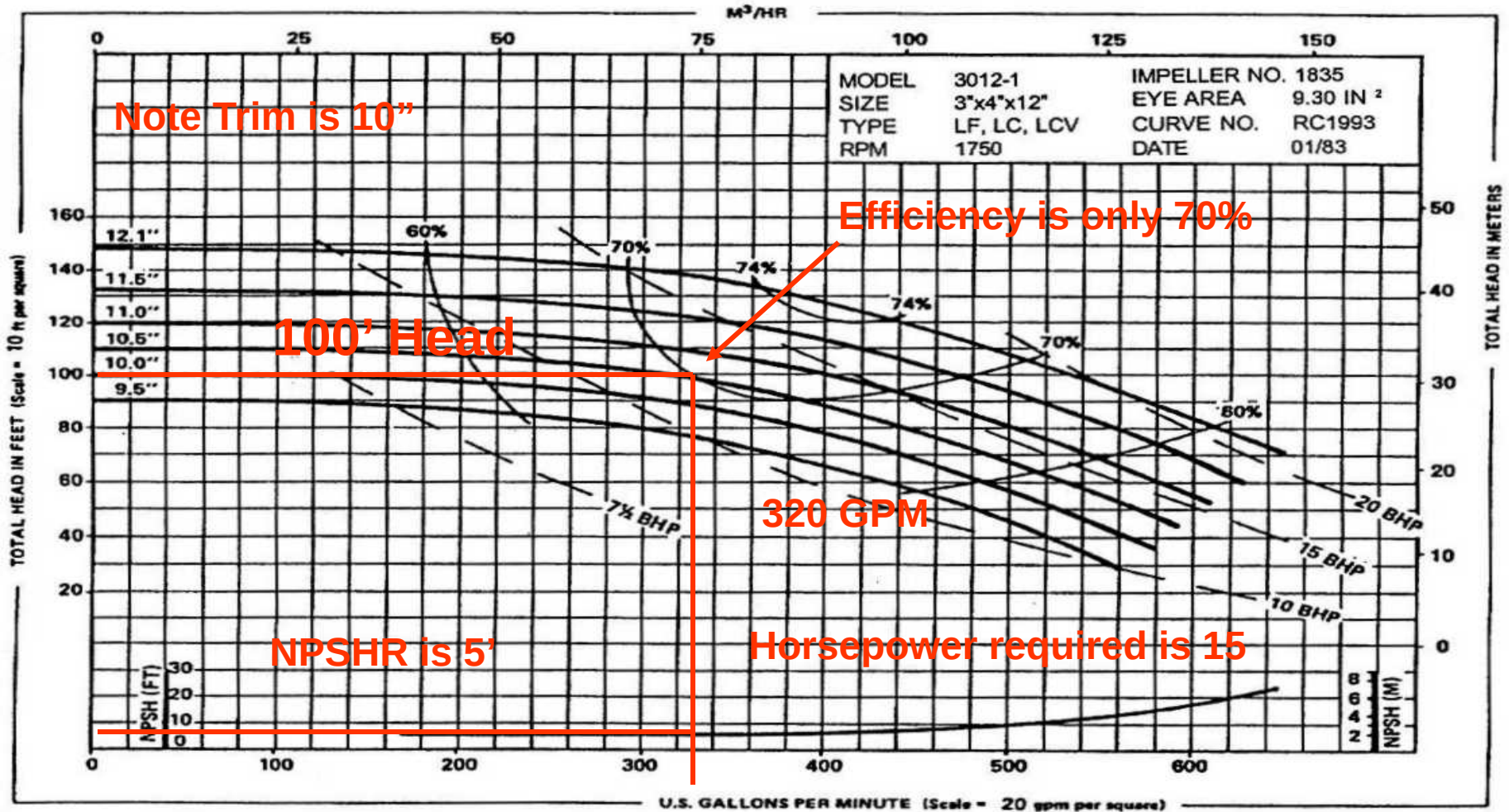
End Suction Pump Curve

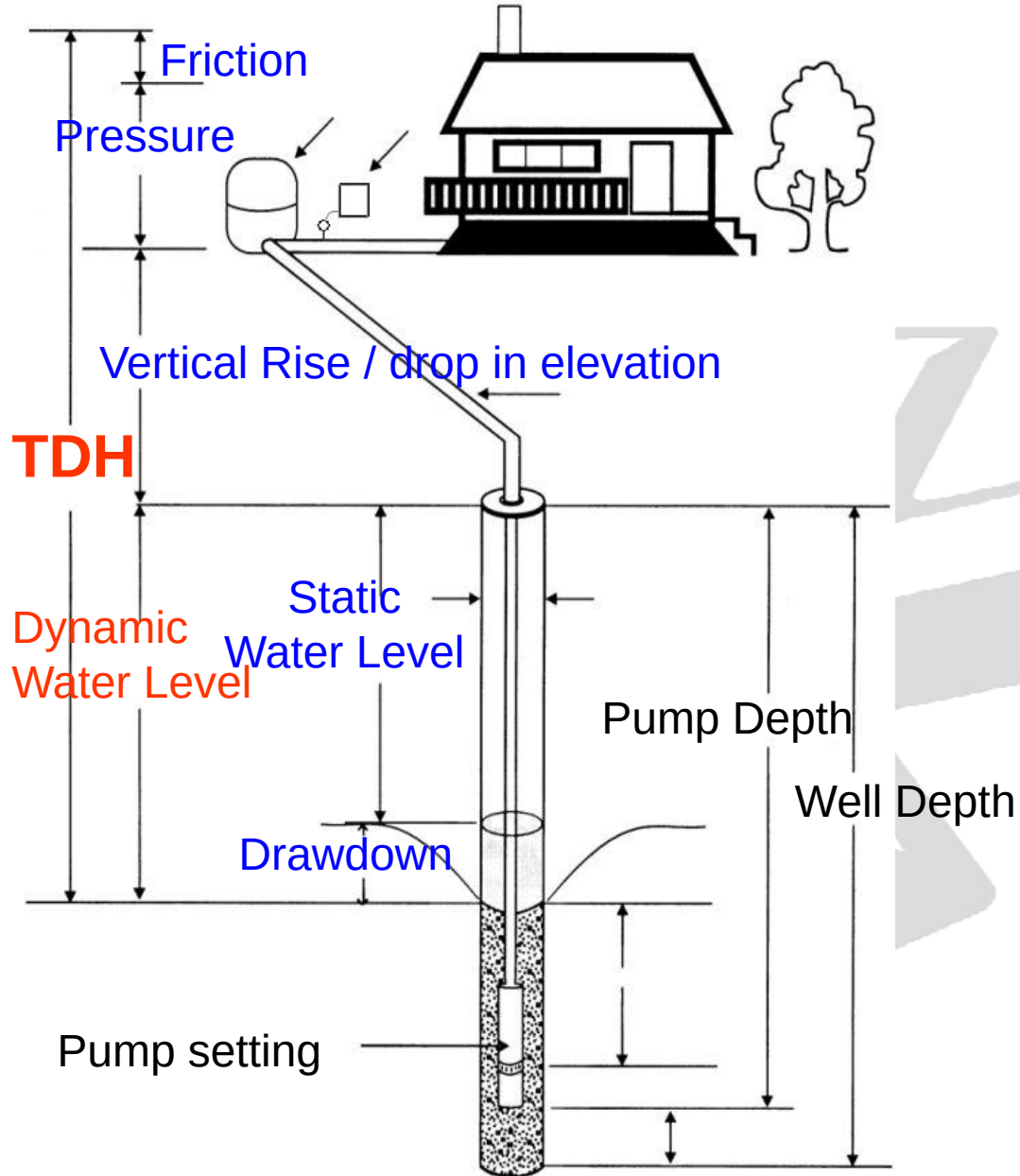


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Sizing with a trimmed pump curve

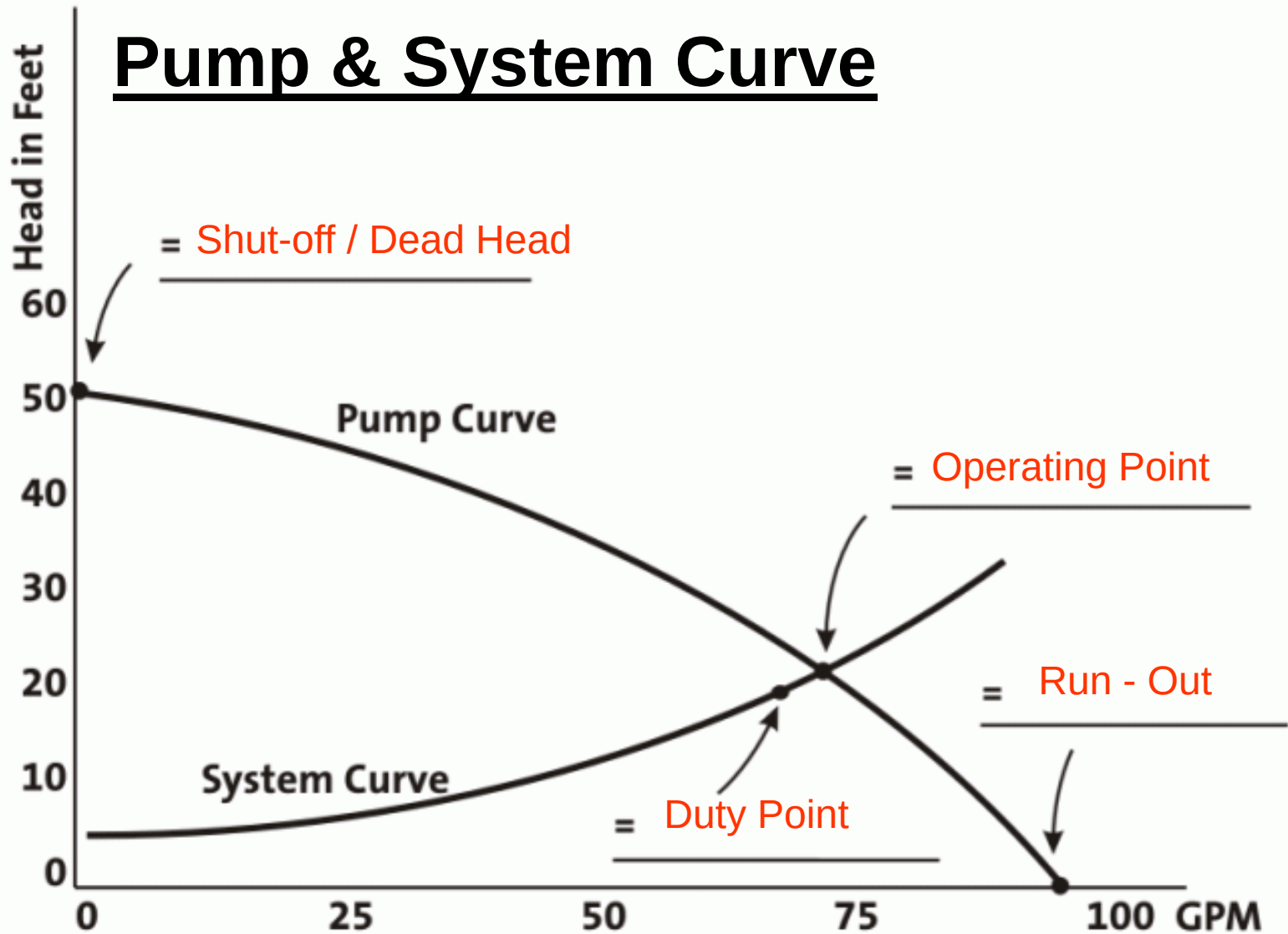




Summary

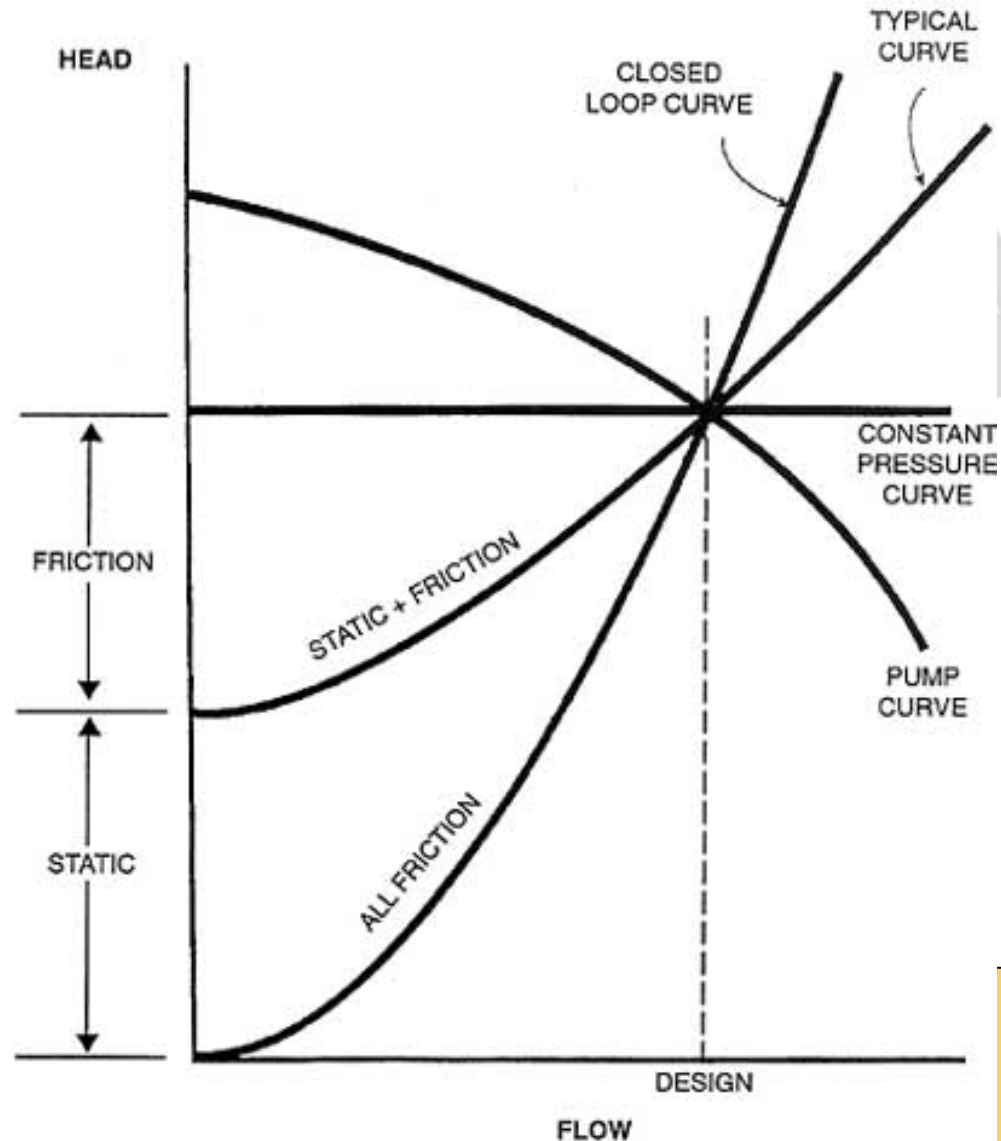
Calculating TDH
(Total Dynamic Head)

Pump & System Curve



BASIC SYSTEM HEAD CURVES

Variance can be anywhere from a flat horizontal line depicting constant pressure to an almost vertical curve when the head is predominantly frictional resistance.



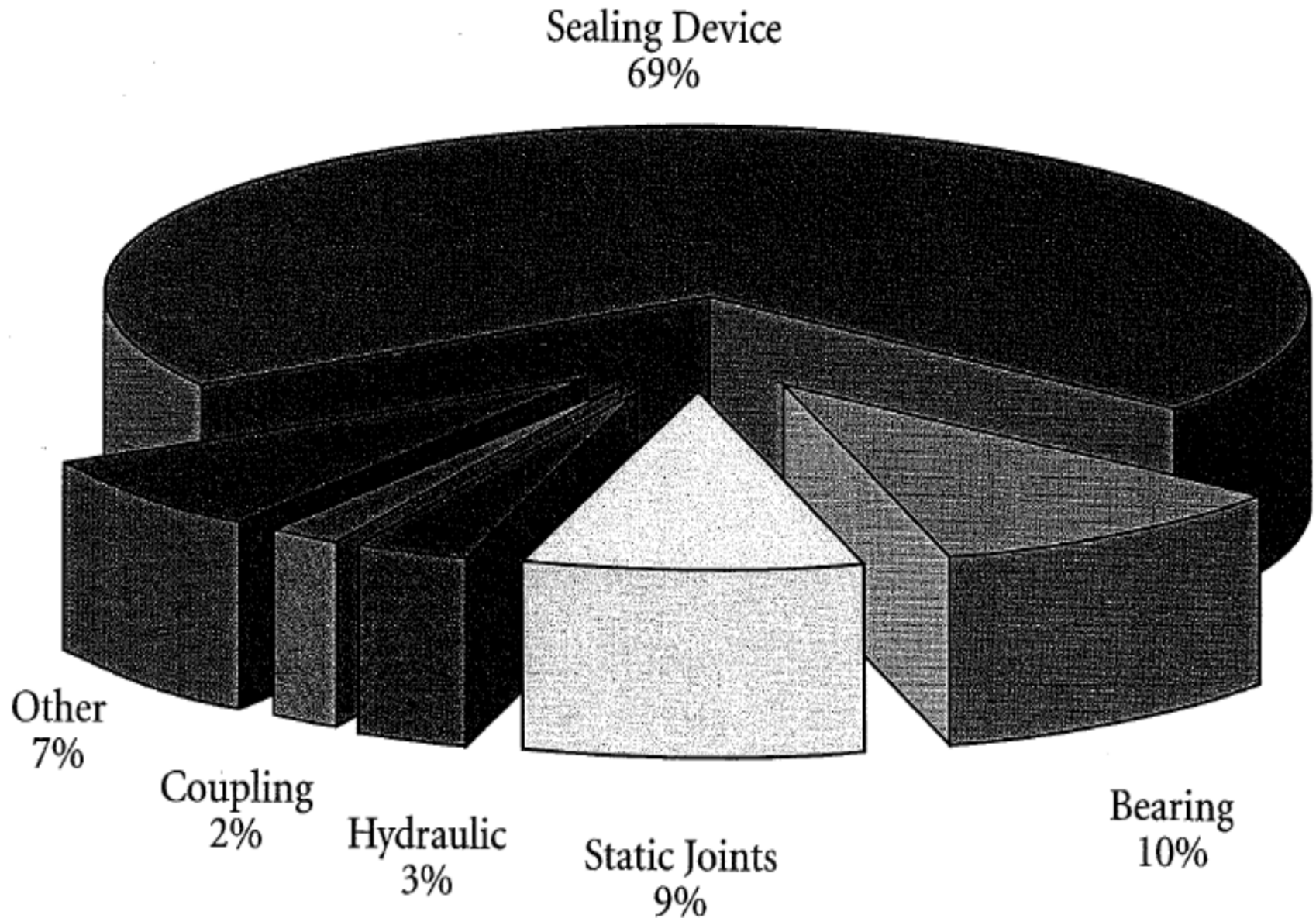
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COMMON OPERATIONAL PROBLEMS



MOST COMMON CAUSE OF EQUIPMENT FAILURE'S



What is Cavitation?

- The affects of cavitation vary from mild to extreme, under mild conditions the pumps may last for years with only a slight reduction in efficiency and no noticeable noise.
- Extreme cavitation will result in rapid destruction of impellers and or diffusers and is normally accompanied by audible (rattling) noise (sounds like gravel).

What is Cavitation

(as relates to water)

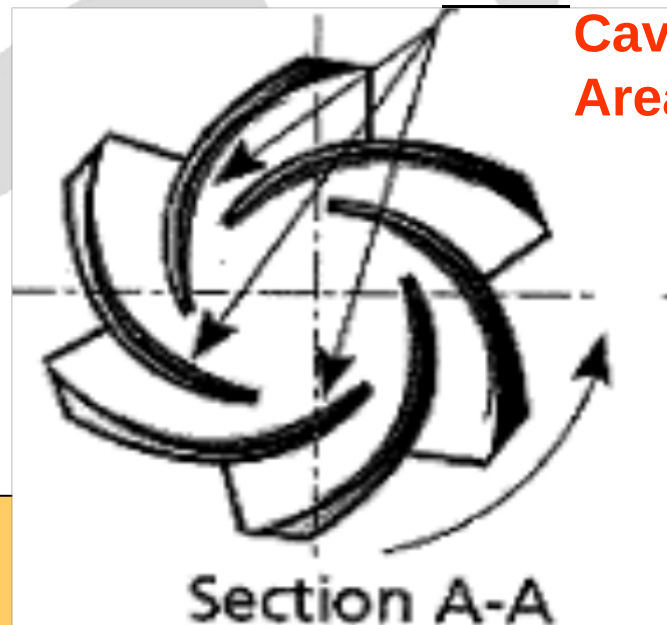
- Cavitation begins as the formation of vapor bubbles due to low pressure (Boiling off the liquid).
- The bubbles form at the position of the lowest pressure, normally in the vicinity of the impeller eye.
- The bubbles collapse as they move to a higher pressure zone.



What is Cavitation?

- This collapse is so rapid and violent that the forces generated are large enough to cause minute pockets of fatigue failure, pitting metal surfaces that are adjacent to the collapsing vapor/bubbles.

Potential
Cavitation
Areas



CAUSES OF Cavitation

- LOSS OF DISCHARGE PRESSURE DUE TO OPEN HYDRANTS OR LINE BREAKS
- CLOSED SUCTION VALVE
- OBSTRUCTION IN THE SUCTION LINE
- LOW SUCTION HEAD DUE TO DROP IN WATER LEVEL



Cavitation

- You can control pump cavitation by throttling the discharge valve.
- Can cavitation be a problem in piping & valves?

Yes



AIR LOCKING

AIR LOCKING IS CAUSED BY AIR OR DISSOLVED GASES THAT BECOME TRAPPED IN THE PUMP VOLUTE OR PIPING PREVENTING FLUID FROM ENTERING THE IMPELLER.

AIR LOCKING IS MOST OFTEN CAUSED BY LEAKS IN THE SUCTION LINE.

LEFT UNCHECKED AIR LOCKING CAN LEAD TO PUMP AND SEAL FAILURE FROM TEMPERATURE OR DRY-RUN.

REMEMBER THAT THE FLUID BEING PUMPED IS ALSO THE PRODUCT LUBRICATING AND COOLING THE EQUIPMENT AND IT'S COMPONENTS.



LOSS OF PRIME

- LOSS OF PRIME HAPPENS WHEN WATER RUNS OUT OF THE PUMP VOLUTE & IMPELLER; USUALLY IN A SUCTION LIFT APPLICATION.
- CAUSES ARE FAILED CHECK OF FOOT VALVE, AIR LEAKS IN SUCTION LINE.



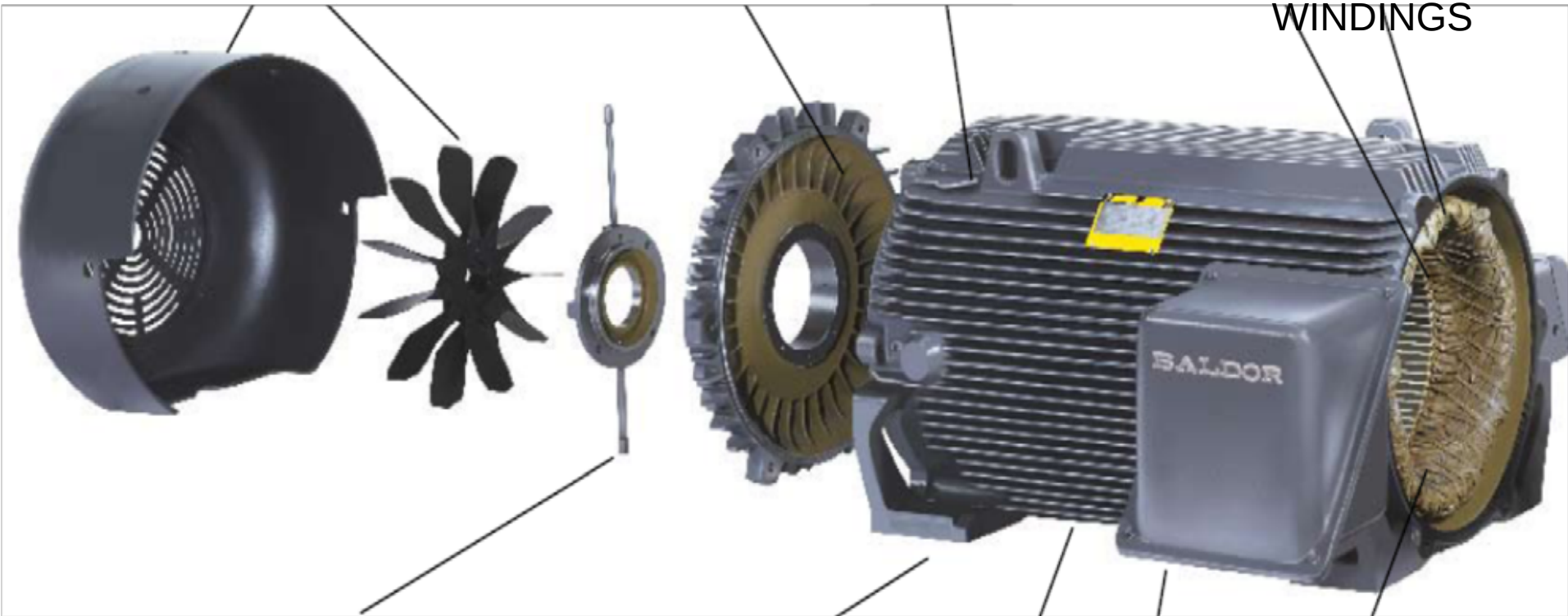
MOTORS

FAN &
COVER

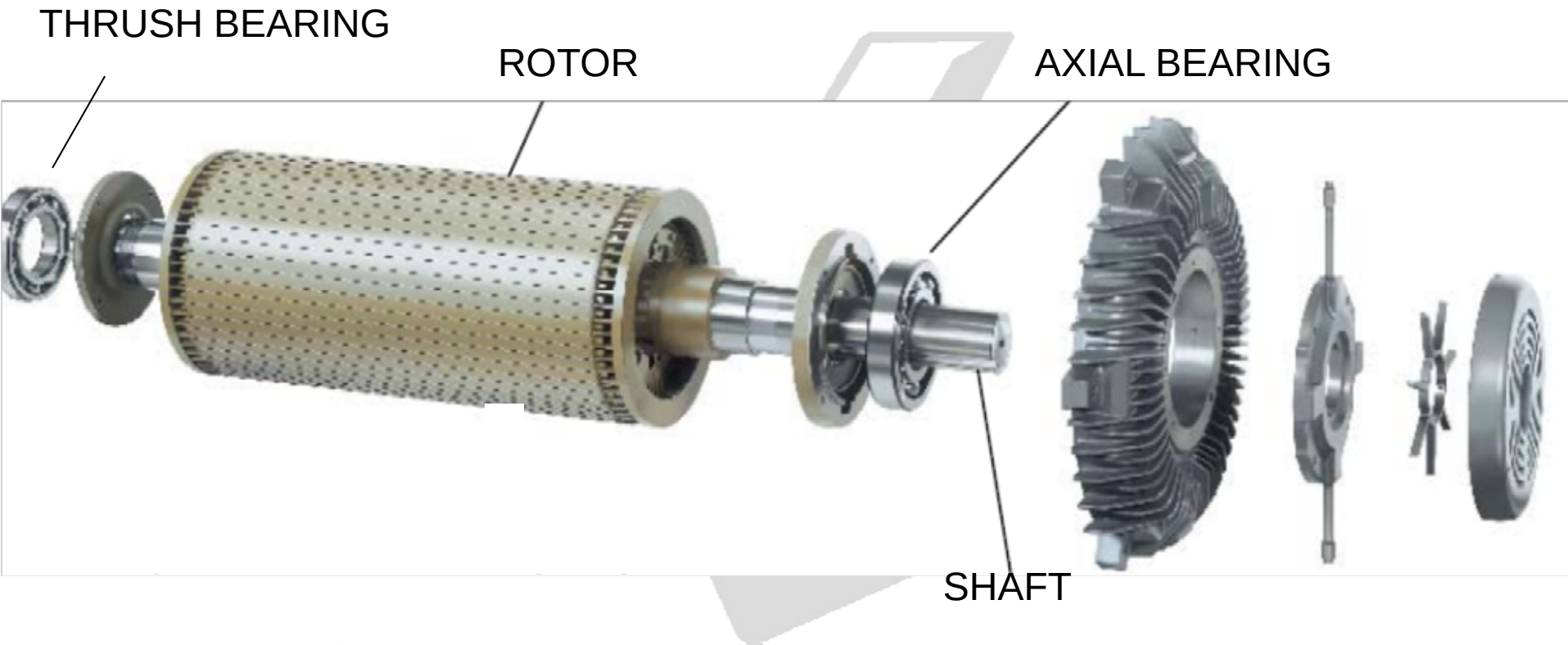
END BELL

COOLING FINS

STATOR /
WINDINGS



MOTORS



ELECTRIC MOTORS

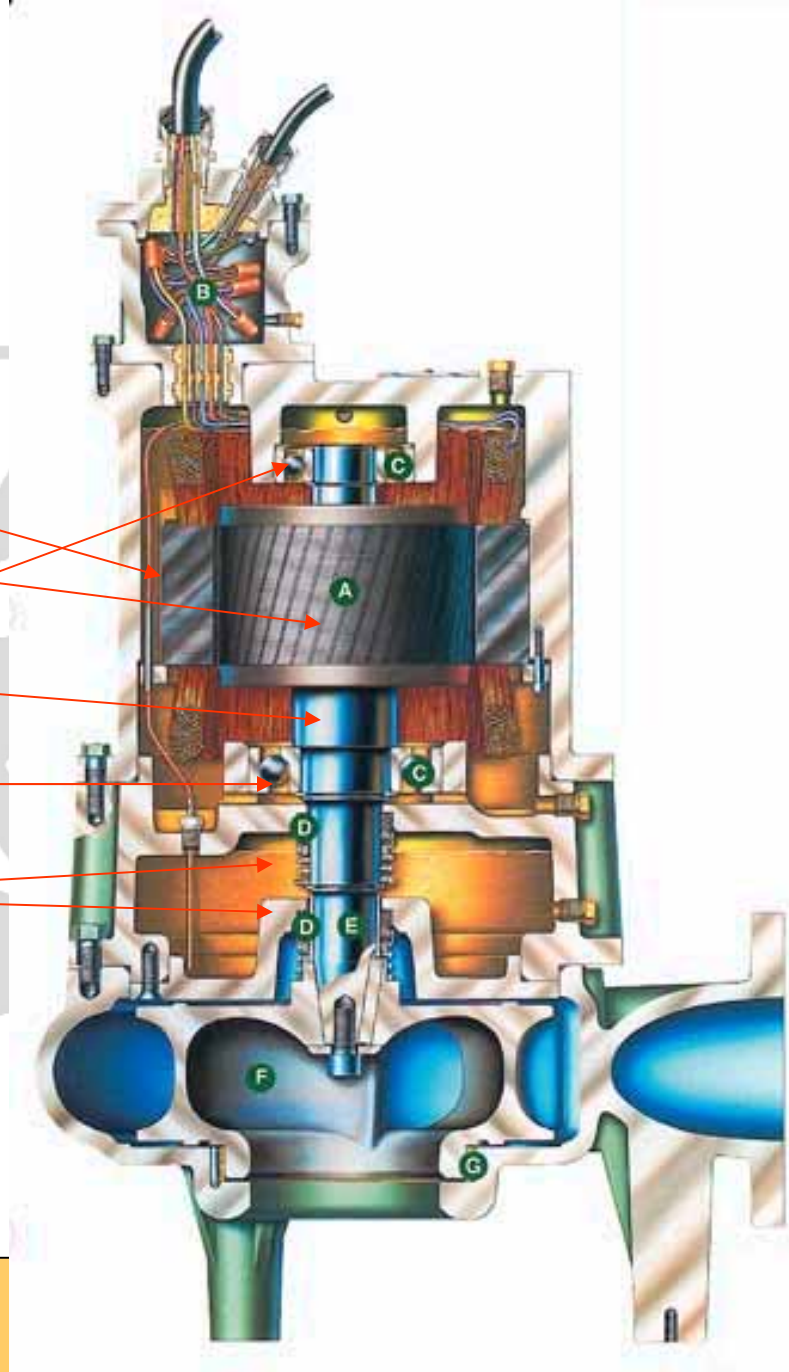
STATOR

ROTOR

SHAFT

BEARINGS

DUAL MECHANICAL SEAL



Motor Loading, Failure & Lifetime

The temperature of the windings are primarily dependent on the current (amp) draw through them and the ability of the motor to dissipate the heat generated to the ambient environment.

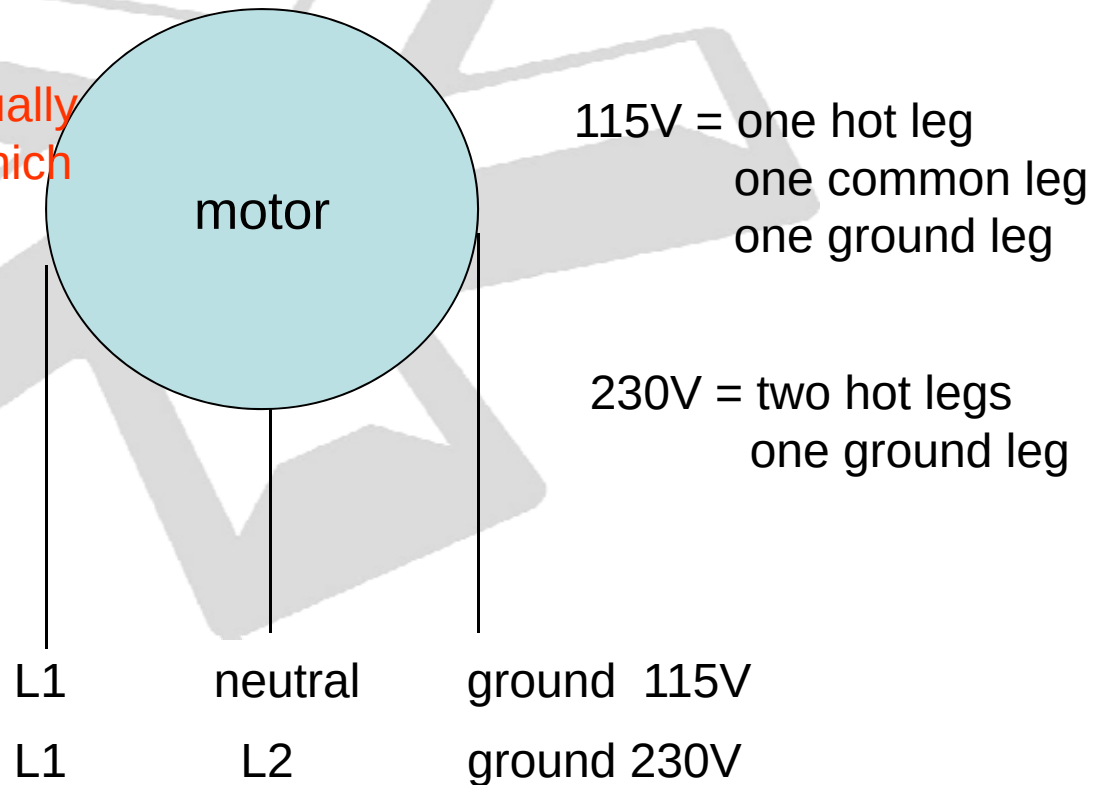
The higher the temperature the shorter the motor life.



ELECTRIC MOTORS

- SINGLE PHASE : 115 OR 230 VOLT AC

A single phase motor usually requires starting circuit which also ensures correct rotation.



Motor

Loading, Failure & Lifetime

- The voltage supplied to the motor terminals have a significant impact on the motor life.
- A rating of ± 10% is standard on motors
 - 115V (Range 103 to 127 VAC)
 - 230V (Range 207 to 253 VAC)



Submersible Motor Loading, Failure & Lifetime

- As voltage raise, current (amps) draw drops.

However, above a certain voltage, destructive arcing and insulation deterioration can occur.

- As voltage drops, current (amps) raises.
Means more amps / heat to dissipated.



Submersible Motor Loading, Failure & Lifetime

Three phase motors

- Single phasing
- Voltage Unbalance

Both of these can result in one leg carrying a higher current causing motor to run hotter, shortening life.

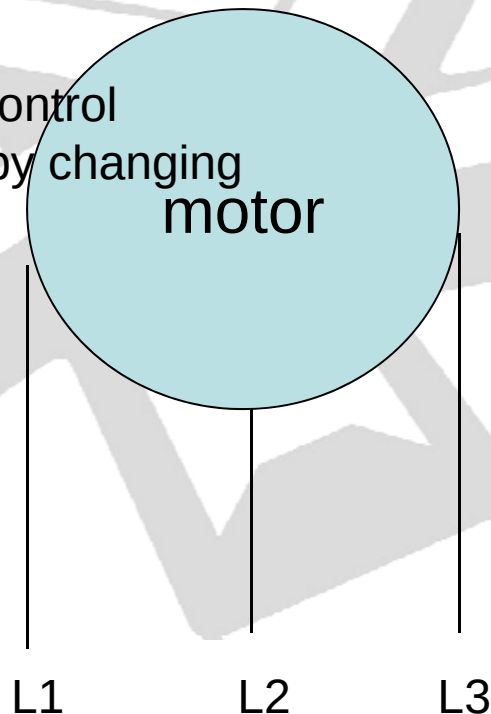
ELECTRIC MOTORS

- **THREE PHASE : 208 / 230 / 460 VOLT AC**

Requires external starter control

Rotation can be reversed by changing
any two leads

All three legs are hot

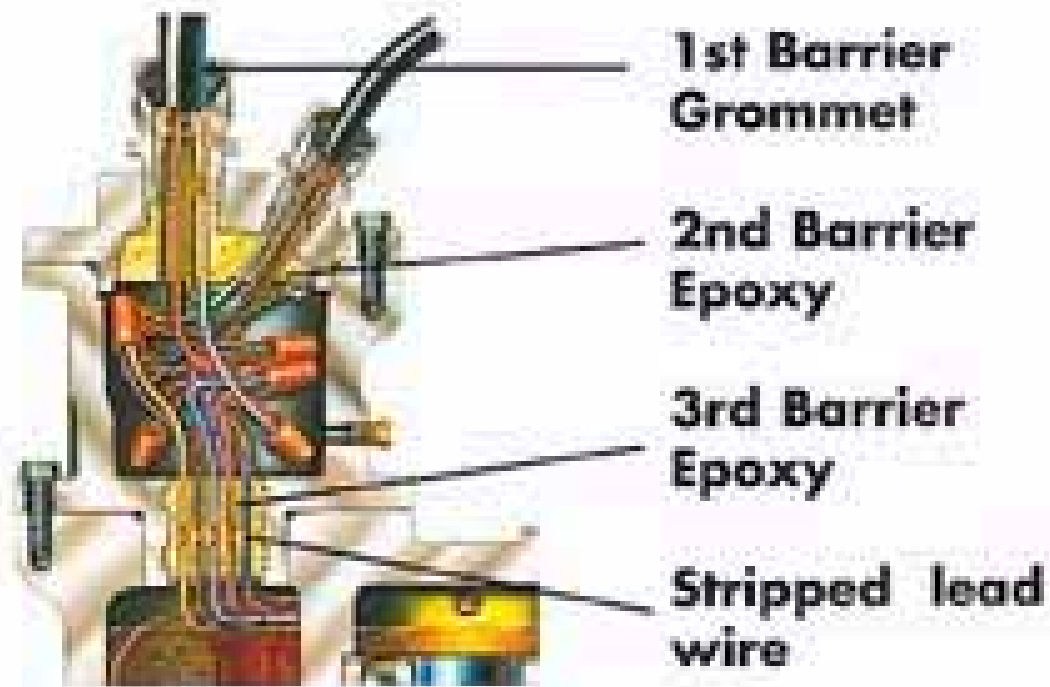


Incorrect Direction of Rotation

- >As a practical matter, applies to 3 Phase motors only (Some 1 phase motors)
- >Reduced flow and head
- >Noise
- >Inability to reach shutoff head



MOTOR LEAD SEALING



Three barriers ensure a dry motor for long-term, reliable operation.



System Components

Electrical

Additional Protective Devices:

- Circuit Breakers or Fused Disconnect Switch
- Run-Dry Protection
- Over Voltage Protection
- Under Voltage Protection
- Over Temperature Protection
- Phase Unbalance (three phase)
- Loss of Phase (three phase)



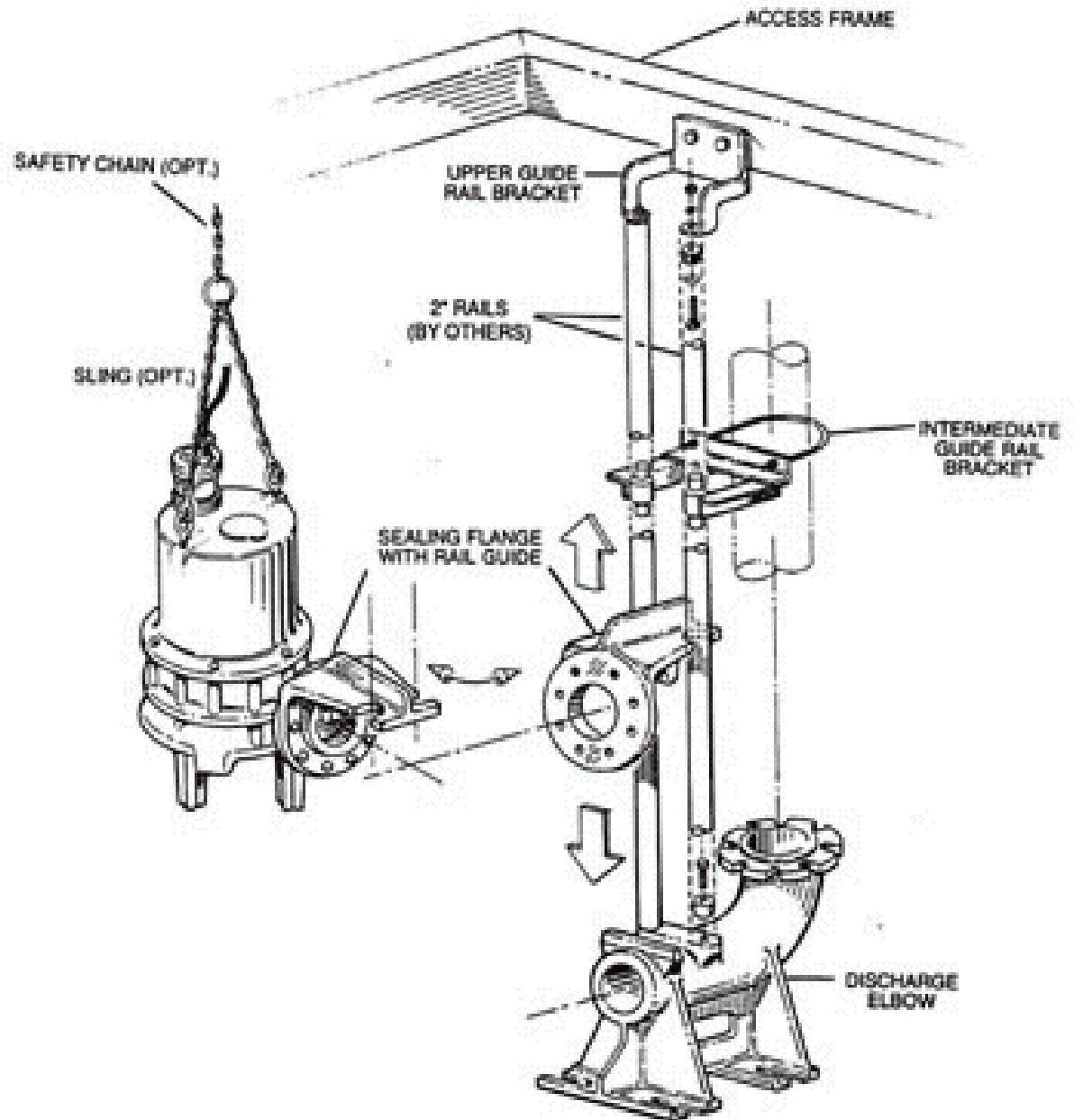
COMPONENTS ID LIFT STATIONS



FIBERGLASS BASINS



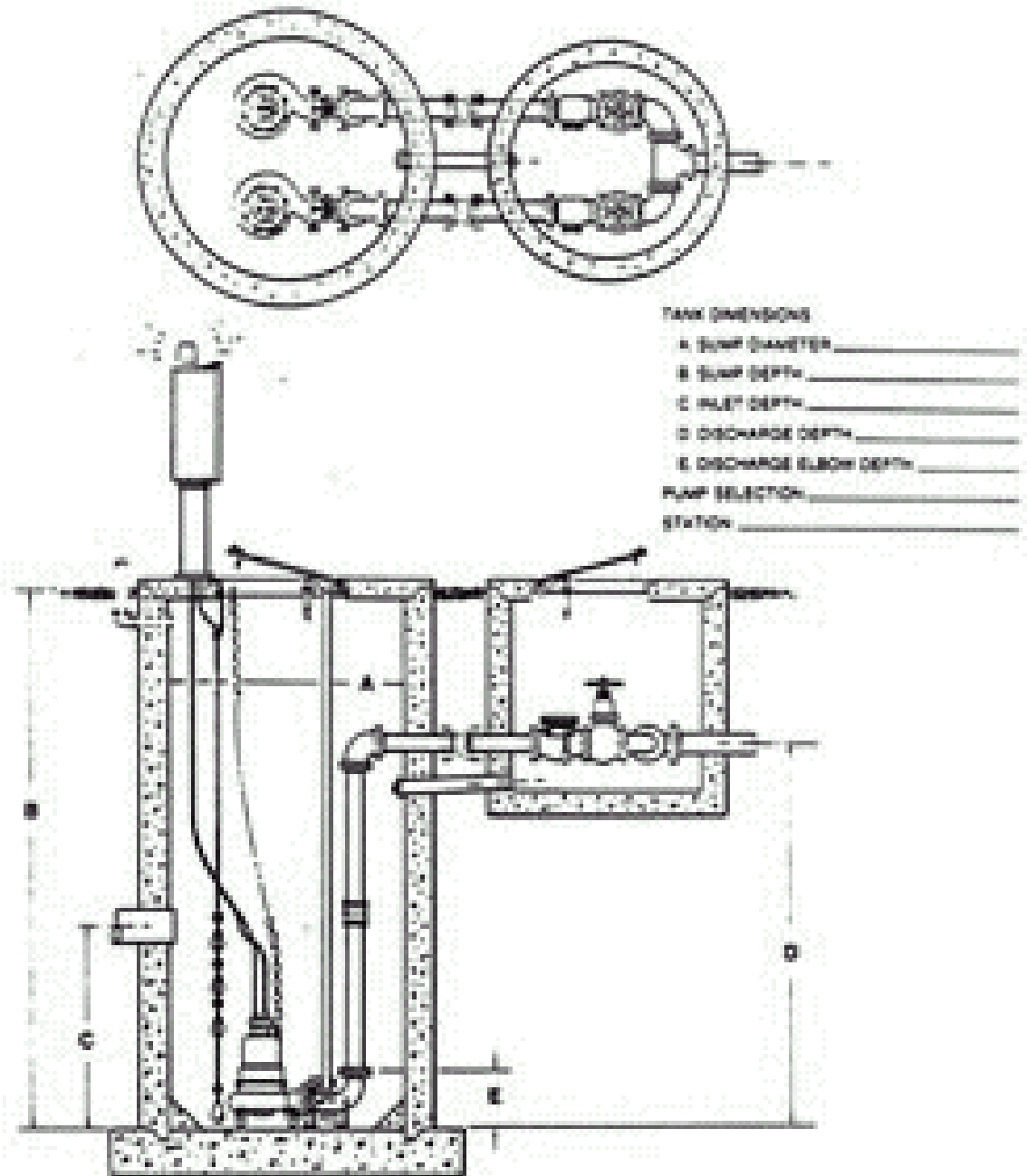
MTM



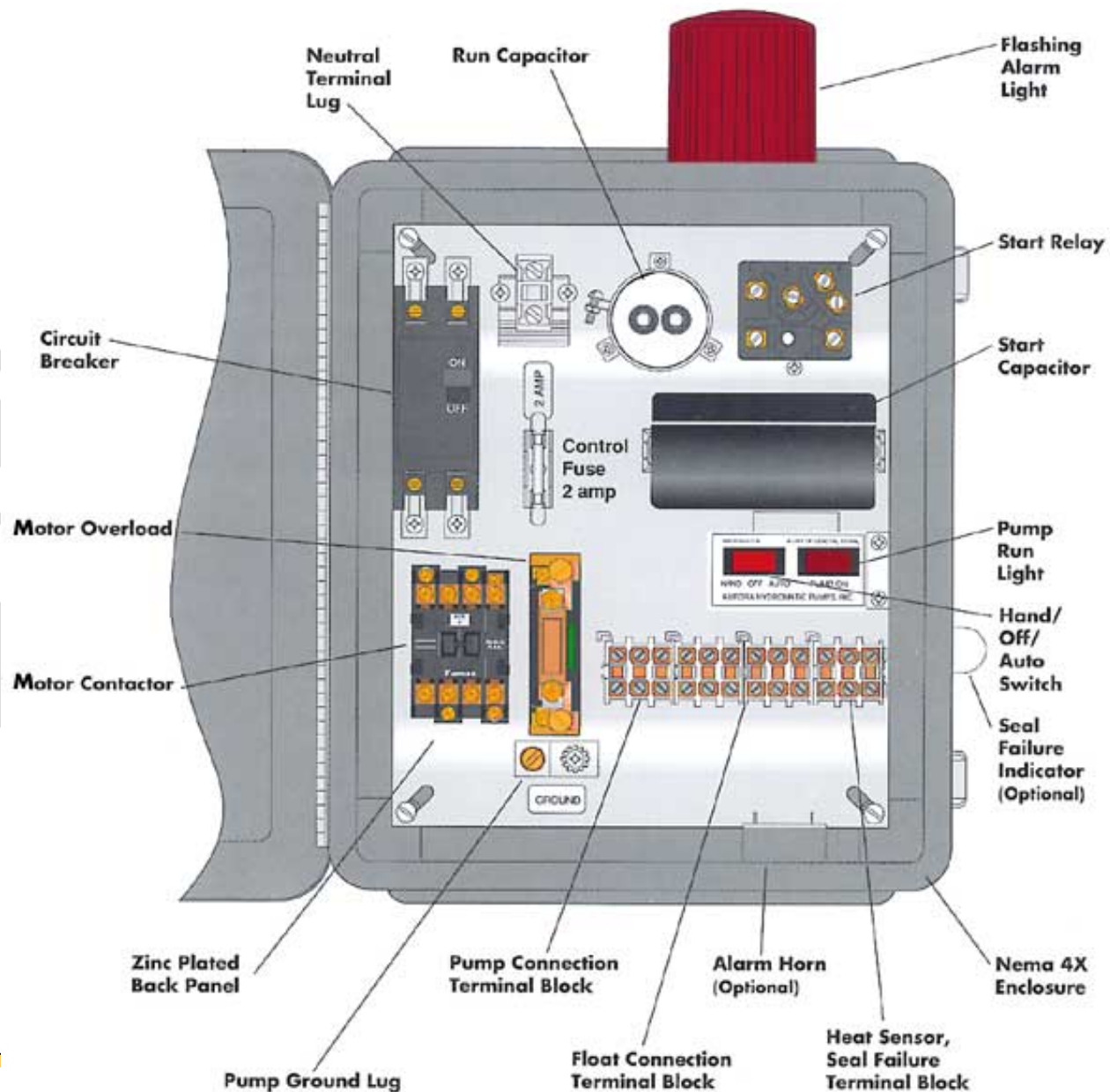
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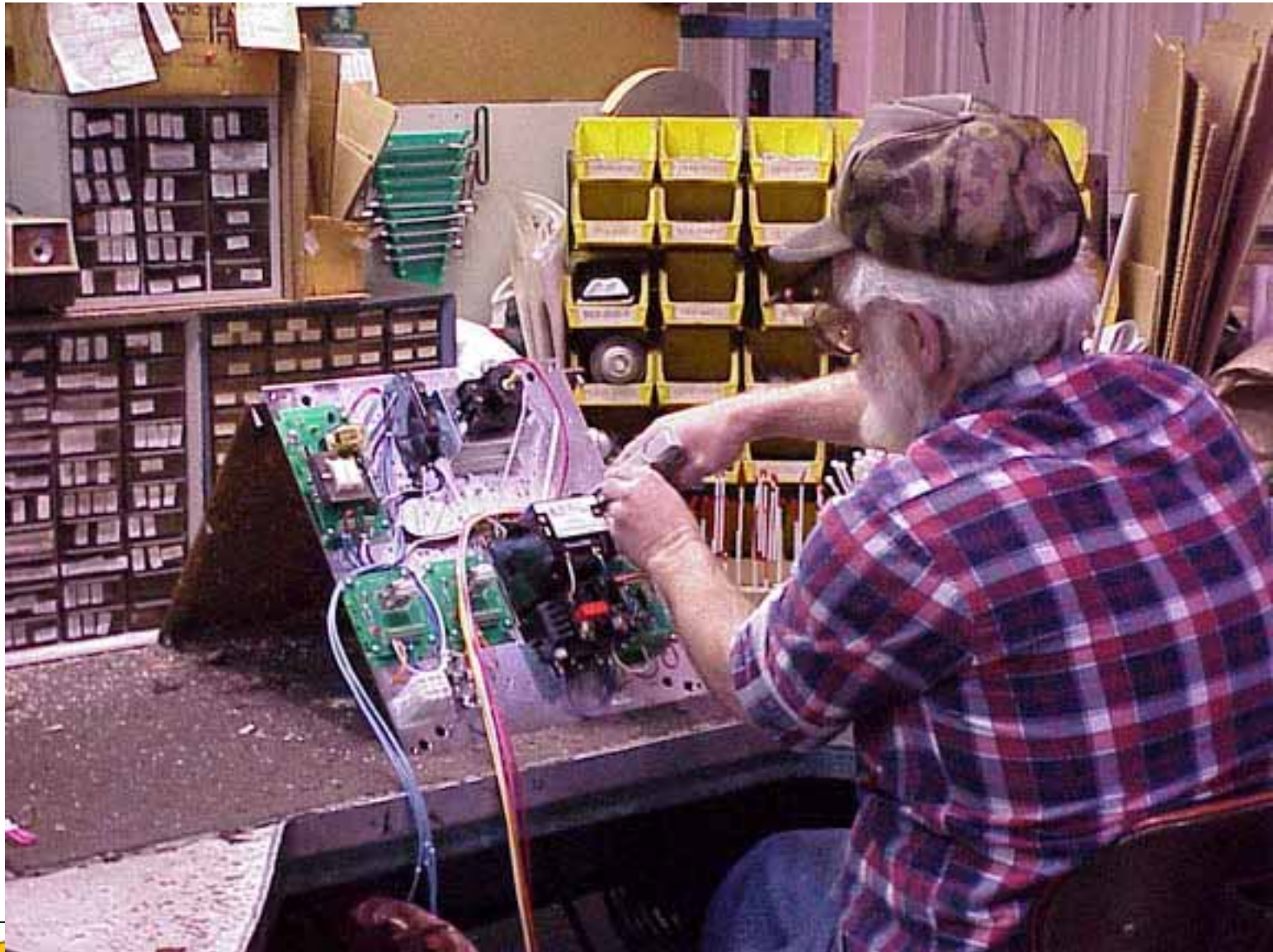
Duplex MTM



SPC-Panel



Virtual Tour Panels



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Virtual Tour Panels



Virtual Tour Panels



Virtual Tour Panels



HYDROMATIC®

3900/8300

Mercury Switch Level Switch



HYDROMATIC®
Pentair Pump Group



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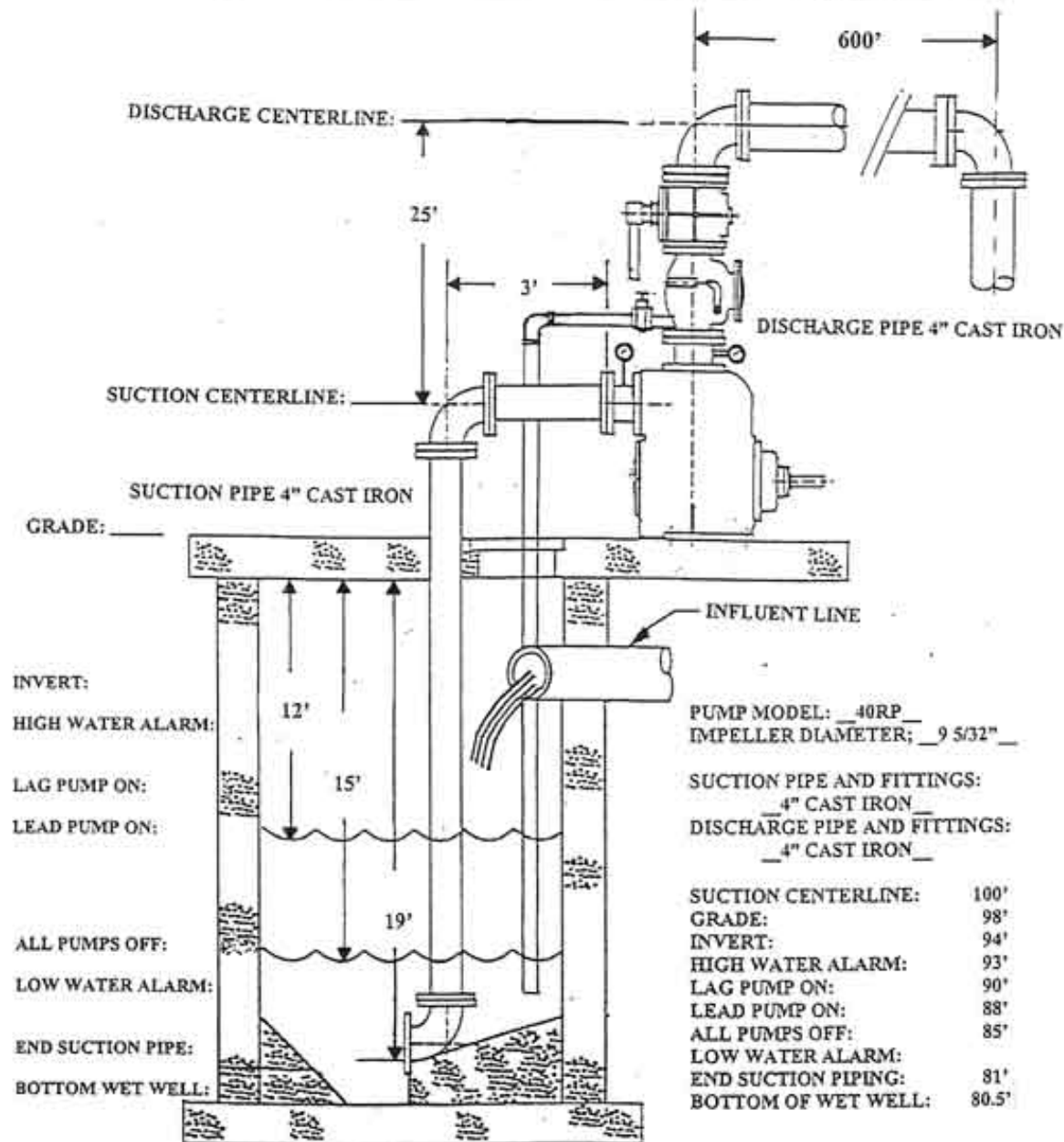


END

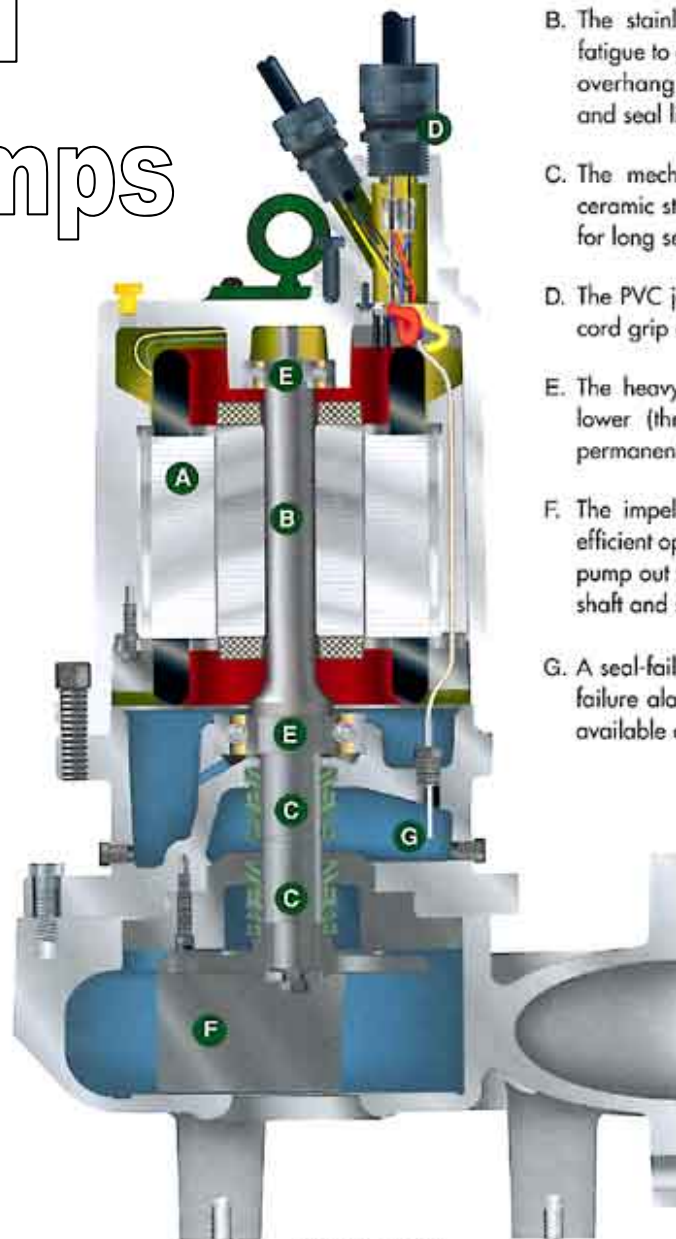


DATE: ____ / ____ / ____ LOCATION: ANYWHERE U. S. A.

JOB NAME: ZYX INC. GPM: 260 @ TDH: 62'



Dual Seal Sewage Pumps



Model: S3SD

- A. The fully enclosed oil-filled motor efficiently dissipates heat and locks out moisture so you receive reliable pumping service.
- B. The stainless steel shaft eliminates corrosion and fatigue to give longer pump life. The minimum shaft overhang decreases deflection and increases seal life.
- C. The mechanical dual seal is constructed with a ceramic stationary face and a carbon rotating face for long service life.
- D. The PVC jacketed power cord is sealed by both the cord grip and additionally by the epoxy barrier.
- E. The heavy duty ball bearings, upper (radial) and lower (thrust), are submerged in oil to provide permanent lubrication and insure long service life.
- F. The impeller is a two vane semi-open design for efficient operation without clogging. The impeller has pump out vanes to prevent material build up around shaft and seal.
- G. A seal-failure sensor probe (for connection to a seal failure alarm) is standard on three-phase units and available as a option on single phase models.

Virtual Tour - Non-Clogs



Virtual Tour - Non-Clogs



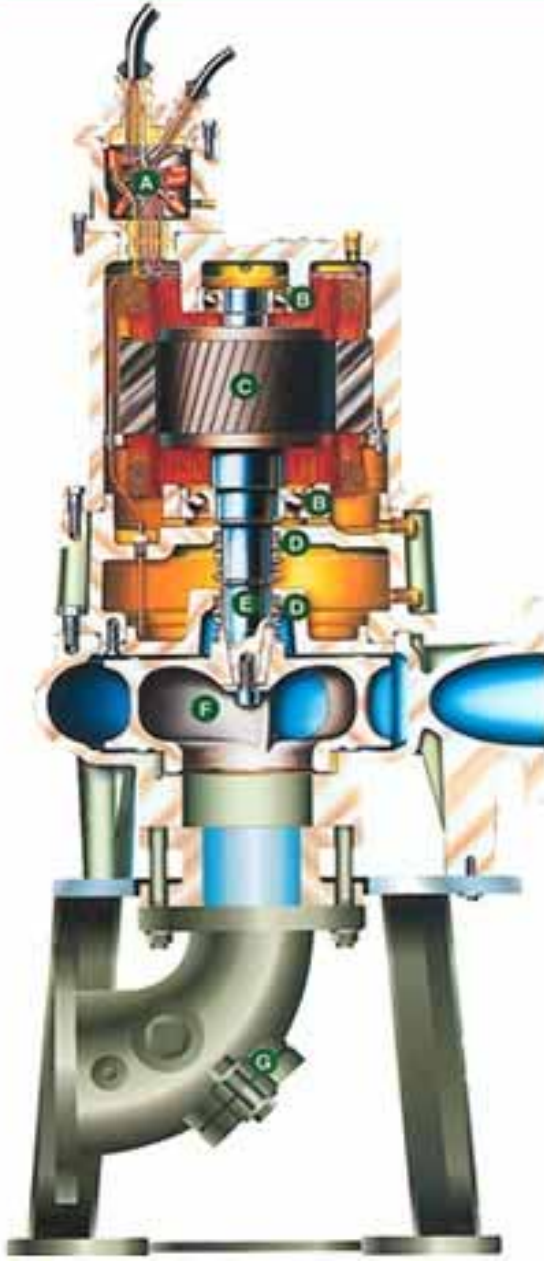
Virtual Tour - Non-Clogs



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BENEFITS



A. Connection Box

Two epoxy barriers and a compression fitting prevent water contamination of the motor area assuring long term reliable operation. Additionally, epoxy encapsulation and stripped leads positively eliminate “wicking” from the cable.

B. Bearings

Heavy-duty ball bearings, upper (radial) and lower (thrust), are submerged in oil to provide permanent lubrication and ensure long service life.

C. Motor

Hydromatic uses “Class H” Insulation for long life. Three phase pumps are suitable for use with VFD drives. Oil filled motor efficiently dissipates heat and locks out damaging moisture so you receive reliable pumping service.

D. Seals

Dual seal system operates in an oil chamber to provide long pump service life.

E. Shaft

The stainless steel shaft eliminates corrosion and fatigue to give longer pump life. The minimum shaft overhang decreases deflection and increases bearing and seal life.

F. Impeller

Two vane non-clog impellers provide the most energy efficient design. Pump-out vanes on the top shroud prevent the build up of materials in the seal area and extend the life of the thrust bearing by significantly reducing axial thrust.

G. Clean-Out

The pump is provided with a clean-out type cast iron suction elbow which is bolted directly to the pump suction flange. A clean-out hole is provided with a removable cover of the largest possible size.





