Lecture 7

Membrane Application

High Purity Water Production

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Presentation Menu

Part 1: Introduction

Part 2: Membrane configurations

Part 3: Membrane systems





Part 1: Introduction





High Purity Water Production

(Also known as ULTRAPURE water)

- Boiler feed water
- Laboratory
- Process water
- Cleaning / rinse water
 - electronic
 - pharmaceuticals



Applications of High Purity Water Production

(Also known as ULTRAPURE water)

- Boiler feed water
- Electronics
- Metal finishing
- Medical and pharmaceuticals
- Packaging
- Cleaning processes
- Painting materials
- Food industry





Boiler feed water

Steam generator water quality guidelines

Drum pressure	Silica (ppm SiO2)	Total alkalinity (ppm CaCO3)	Specific conductance (µmhos/cm)
0-300	150	350	3,500
301-450	90	300	3,000
451-650	40	250	2,500
651-750	30	200	2,000
751-900	20	150	1,500
901-1000	8	100	1,000
1001-1500	2	0	150
1501-2000	1	0	100



Electronic Industry

Ultrapure water specifications for IM DRAM Manufacture

Parameters	Attainable	Acceptable
TOC (ppb)	<10	<30
Particles/liter by SEM		
0.2-0.3 μm	-	<2,000
0.3-0.5 μm	<200	<200
>0.5 μm	<1	<1
Bacteria/100 ml		
By culture	0	<6
By SEM	<1	<10
By EPI	<5	<50
Silica, dissolved (ppb)	<4	4



Metal finishing industry

- Products: doorknobs, lighting fixture, electrical relay contacts etc.
- Plating materials: gold, copper, cadmium, copper, chrome etc.
- High purity water: 1 10 megohm
- For rinsing operation



Medical & pharmaceuticals

- Medicinal preparations, e.g. lotions & creams
- Pharmaceutical products: eye drops, contact lens, laboratory practice etc.
- Hemodialysis machines use membrane technology (for producing high purity water and separating the blood cells)
- Medical uses: water for procedures, water for cleansing and cleaning



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Conventional treatment flow scheme for ultra pure water production

- Feed water: Tap water
- Quality problems:
 - Residual chlorine
 - Total dissolved solids
 - Organic fractions
 - Microorganisms
- Treatment:
 - Thermal process
 - Chemical and ultraviolet process
 - Membrane



Module on High Quality Water



Conventional treatment flow scheme for ultra pure water production

Tab water

Treatment Process

- Thermal
- Chemical
- Membrane

Ultra pure water

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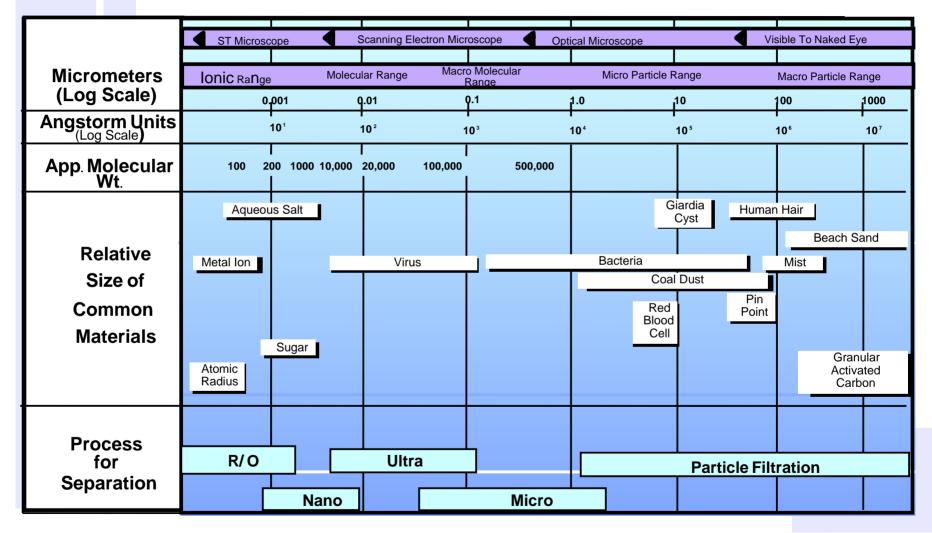


Advanced Water Treatment (4)

Coagulation Solid/liquid separation Solid/liquid separation Organic, taste & odor removal RO NOM removal Disinfection (UV) Bacterial removal



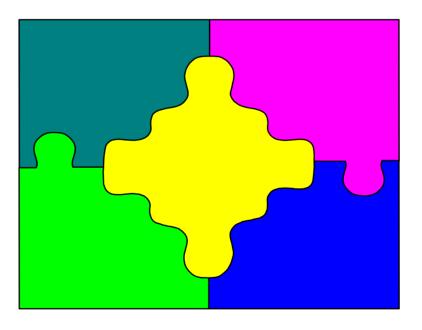
Filtration Spectrum



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Part 2: Membrane configurations, designs, operations

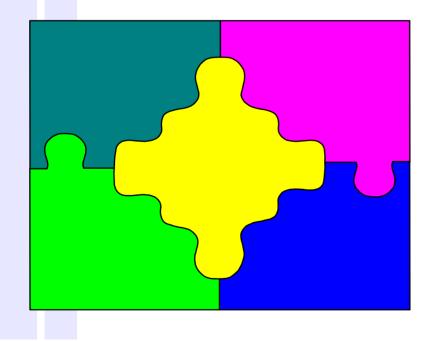




14

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Part 3: Membrane Systems





Reverse osmosis

- Normally used for high purity water in many industries at the moment, coupled with UV
- Purposes:
 - Ionic removal
 - Organic removal
 - Silica removal
 - Particles and bacteria



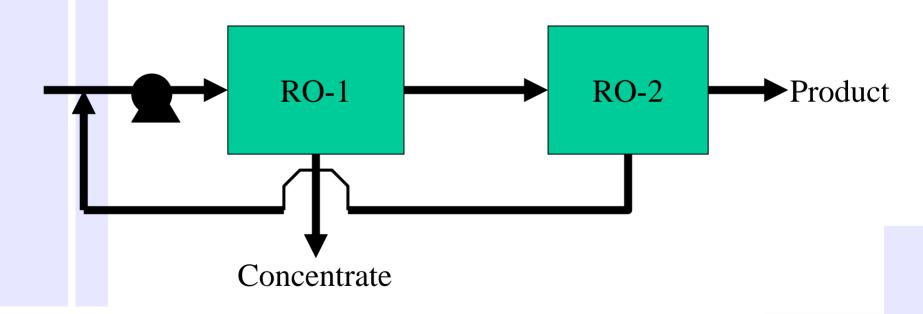
Problems in high purity water systems

- Post treatment contamination
- Membrane bypass
- Differential passage of silica and carbon dioxide



Double-pass reverse osmosis

Increase rejection level



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Pre-treatment and post-treatment

- Particle stabilization
- Ionic stabilization
- Biological control
- Polishing treatment

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Market size and projections

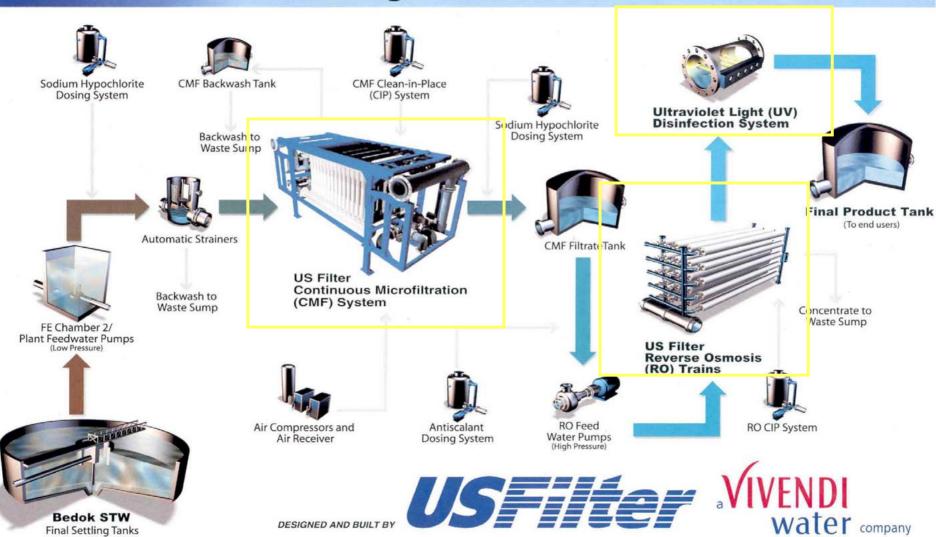
- 2.5% annual growth (global)
- RO is replacing ion exchange
- The more industrial growth in electronic, medical & pharmaceutical industries – the more market for membrane technology



BEDOK NEWATER FACTORY

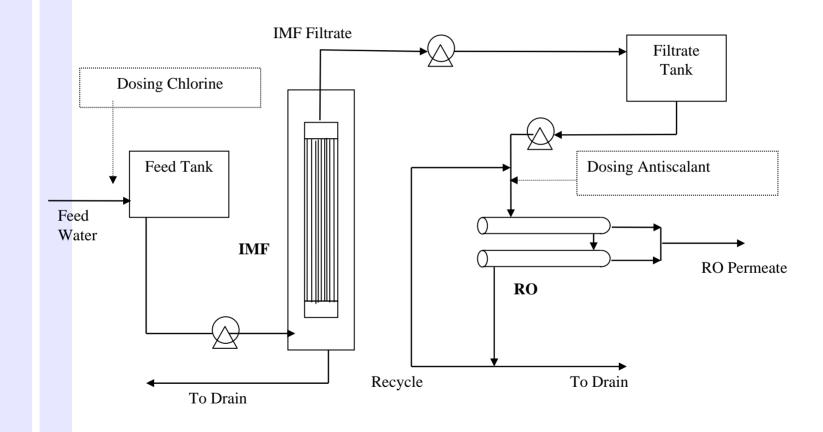
Water Reclamation Demonstration Plant

NEWater Factory - PROCESS FLOW SCHEMATIC



Final Settling Tanks

The pilot plant



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Membrane Specification

Manufacturer	-	Memcor
Commercial Designation	-	1S10X CMF-s
Active Membrane Area (outside)	m ²	31.3
Flow Direction	-	outside-in
Nominal Membrane Pore size	μm	0.2
Membrane Material/Construction	-	polypropylene, hollow fiber
Membrane Charge	-	slightly negative
Design Flux	L/hr.m ²	31.1

Specification for the IMF

Specification for the RO

Manufacturer	-	Hydranautics
Commercial Designation	-	LFC1-4040
Active Membrane Area (outside)	m ²	7.9 per module
Memrane Material	-	Polyamide (thin film composite)
Operating pH Range	-	2.0-10.0
Maximum Operating Temperature	deg C	45
Free Chlorine Resistance	mg/L	<0.2



IMF operating conditions

Parameters	Value	
IMF Unit		
Filtrate flow rate	0.8 m ³ /hr	
Backwash interval setting	18 minutes/2 minutes	
Filterate temperature	30 − 35 °C	
Backwash liquid flow	2.20-2.25 m ³ /hr	
Feed chlorine level	0.5-1.0 ppm	



RO operating conditions

Parameters Value	
RO Units	
Feed flowrate	28 L/min
Permeate flowrate	4.5 L/min
Rejection flowrate	5.0 L/min
Recycle flowrate	15.5 L/min
Feed pressure	8 – 9 bar
Permeate & rejection pressure 1 bar	
Silt density index	3.7 – 5.5



The pilot plant







The components







The components





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The experimental results

Parameters	Feed	Effluent	% Rejection
BOD, mg/l	25	1	95
COD, mg/l	70	14	80
Suspended solids, mg/l	20	1	95
Hardness	998	12	88
TOC	20	1	95
Ammoniacal Nitrogen	33	<3	92
Nitrate, mg/l	0.3	0.1	>66
Total Phosphorus, mg/l	5.18	0.46	>90
Iron	0.47	0.03	93
Manganese, mg/l	0.08	0.02	75
Silica, mg/l	8.29	0.54	94
Total plate count	775 x 10 ³ cfu/100mL	291 x 10 ³ cfu/100mL	>62

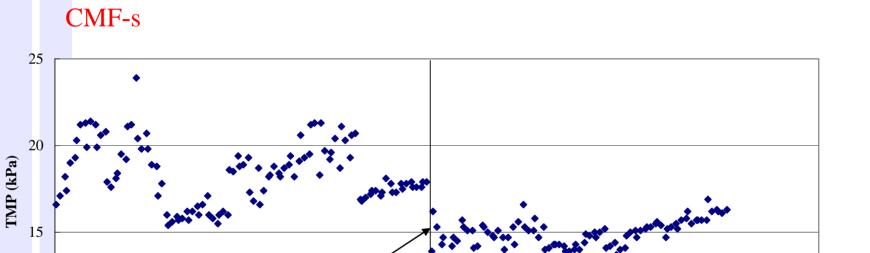
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CIP Cleaning

200

Experimental results on TMP



300

Operating Hour (hr)

400

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Production by Prof. Zaini Ujang

500



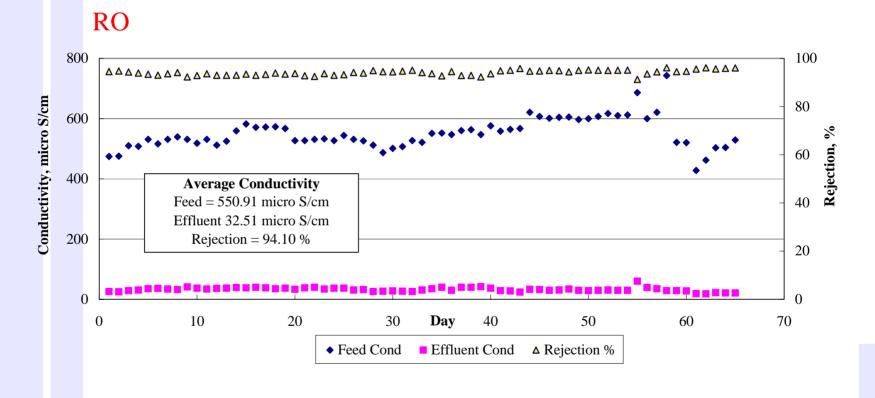
600

10

0

100

Experimental results on conductivity



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Discussions

- pH of reclaimed water slightly acidic (pH 6 6.5)
- permeate of RO always slightly acidic (drop by ~0.5) vs influent due to:
 - the removal of silica
 - the usage of acid as RO anti-scalant.
- Ammonical nitrogen in reclaimed water averaging 2.5 mg/L (WHO guideline at 1.5 mg/L)
- Unexpected high ammonical nitrogen in the influent (with 32 mg/L).
- STP should produced effluent with ammoniacal nitrogen down to 5 - 10 mg/L.

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Excellent removal rate of ammonical nitrogen with RO have been achieved (average 90 – 93 %)



Discussions

High plate count in reclaimed water

Theoretically, RO would remove all bacteria and virus. However, the pilot plant is running only 8 hr/day and as such substantial bacteria growth in the post RO piping system as the pilot plant is not equipped with disinfection (UV, chlorination)



The overall results



Meeting the requirement of both effluent Standard A and drinking water

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Rockeffeller Foundation Team Residency: Exploration of the potential of membrane technology for sustainable sanitation

- Politecnico di Milano, Milan, Italy
- April 23-26, 2003
- Only 14 participants representing various global fractions!



