



Wastewater Treatment Technologies For Water Reuse In Saudi Arabia

Waleed M. Zahid

**Civil Engineering Department – College of Engineering
King Saud University**

**The 2nd Saudi International
Water Technology Conference 2014
King Abdulaziz City for Science and Technology
(KACST)**

23rd - 25th February, 2014 / 23rd - 25th Rabi' Al-Thani, 1435H

Content

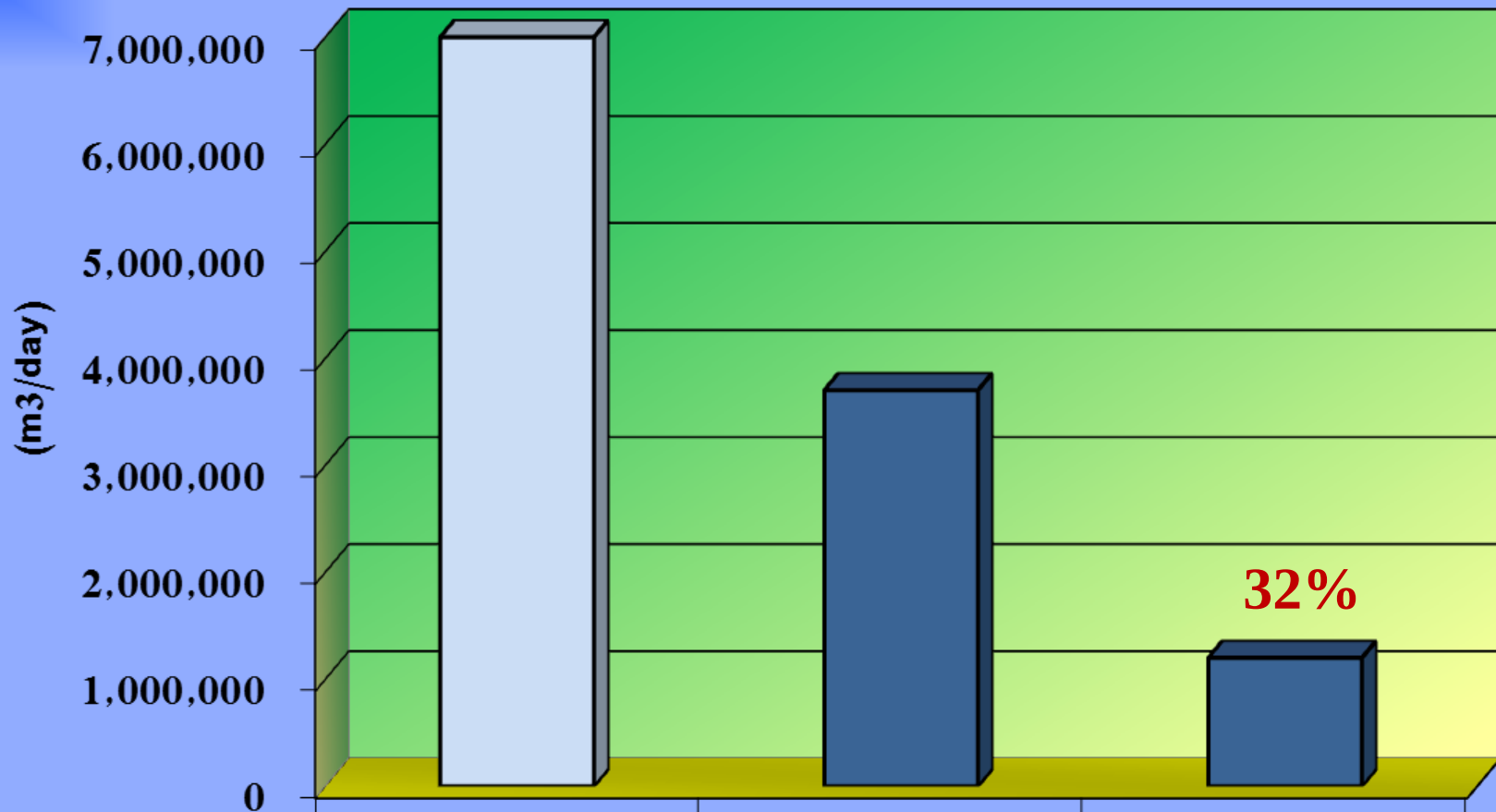
✓ Water Reuse in Saudi Arabia

- Quantity
- Types of Uses
- Treatment Plants

✓ Evaluation of Oxidation Ditch Plants in SA

- Performance
- Cost Effectiveness

Quantity of Reused Water In Saudi Arabia

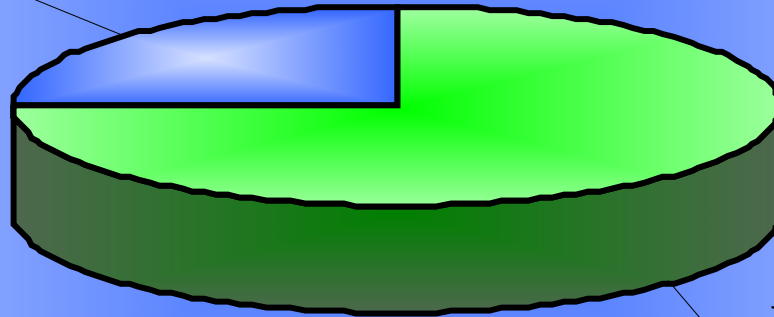


	Potable Water	Treated WW	Reused
Quantity	7,000,000	3,700,000	1,200,000

Uses of Reclaimed Water in SA

**Other
Purposes
25%**

- Industrial (cooling, processing, ...)
- Stream Flow Augmentation



**Irrigation
75%**

- Agriculture Irrigation
- Landscape Irrigation



Wastewater Treatment Plants

- ⊙ Approximately 73 plants
- ⊙ Design Capacity ≈ 5.0 million m³/day



Riyadh Plants

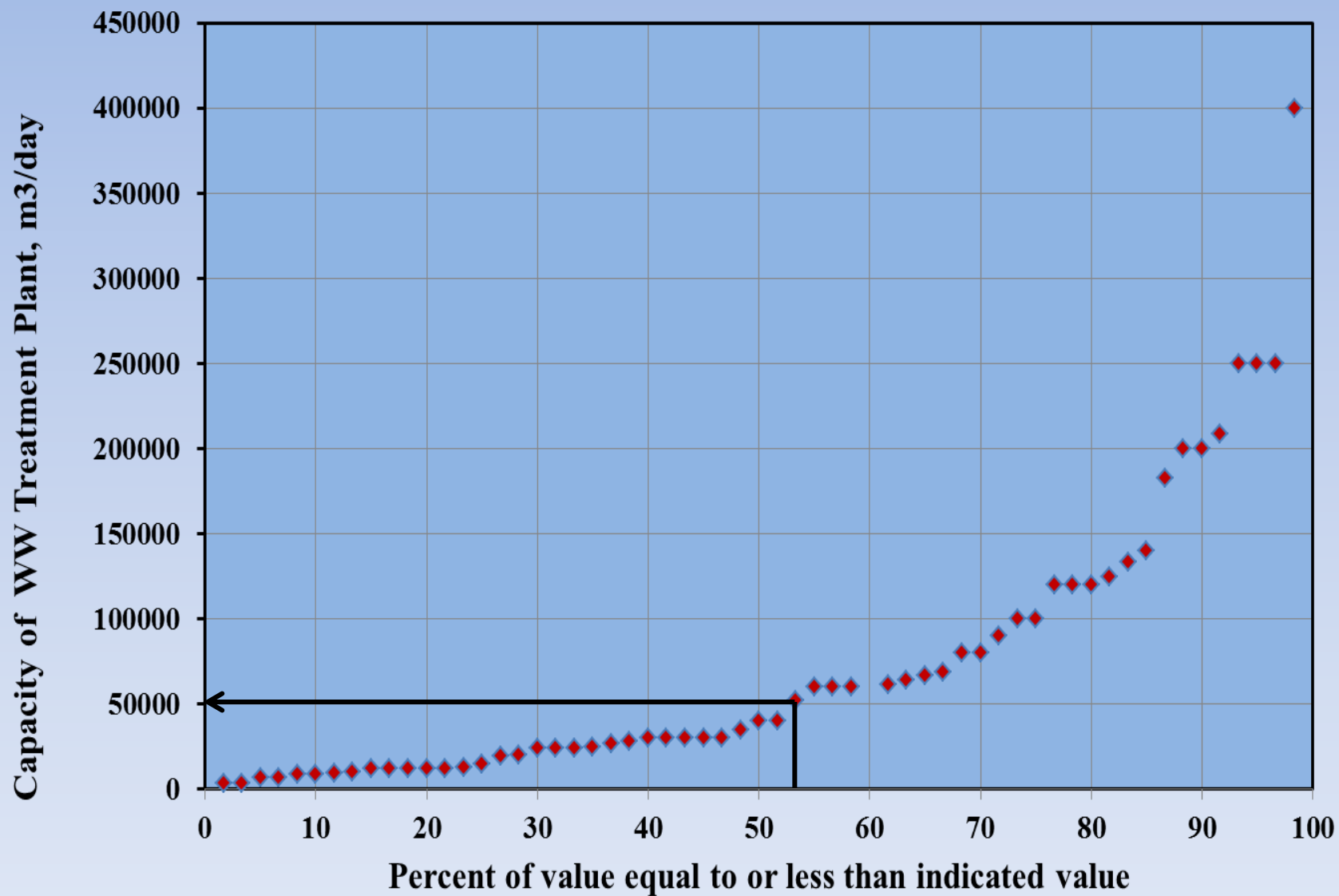


A Plant in Khateef

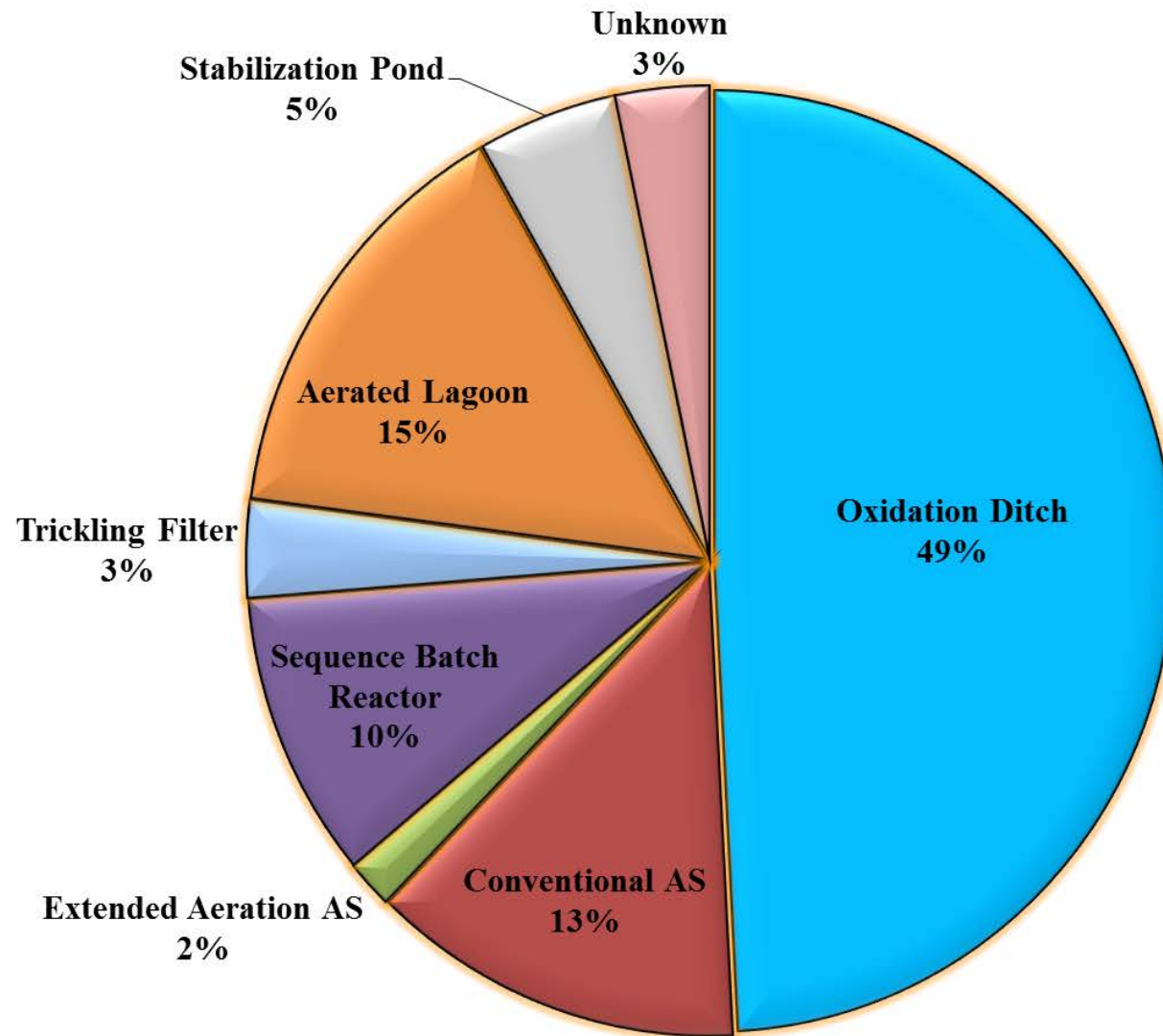


A Plant in Hafouf

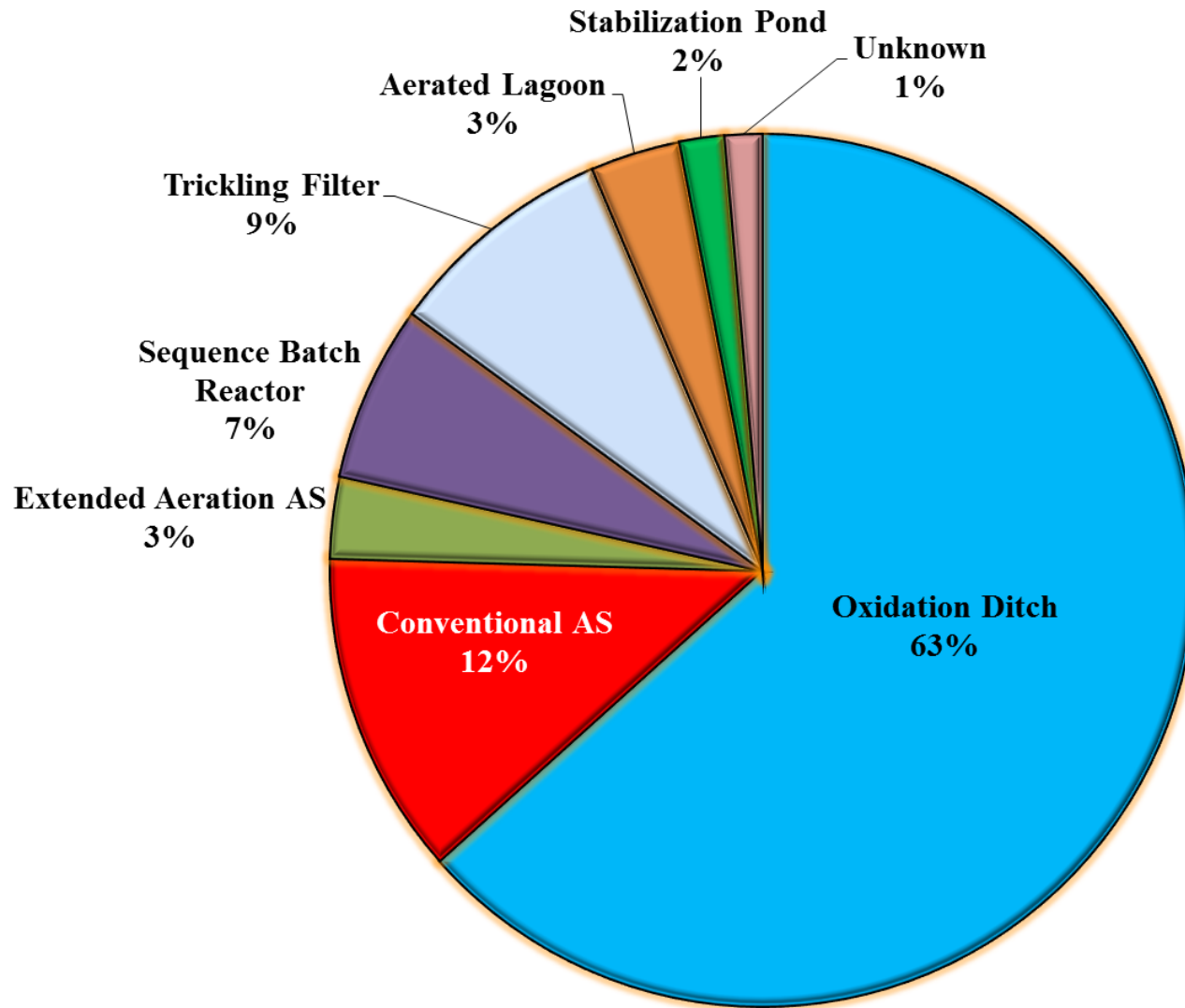
Cumulated Capacity of Wastewater Treatment Plants in SA



Types of Wastewater treatment Plants



Percent of Wastewater Treated by Different Systems



Evaluation of the Oxidation Ditch Process for the Biological Treatment of Municipal Wastewater in Saudi Arabia

**Research Project Sponsored by the Science & Technology Program –
King Saud University**

Objectives

- **Evaluate the treatment efficiency of the main oxidation-ditch wastewater treatment plants in Saudi Arabia**
- **Assess major operation concerns associated with oxidation ditch process**
- **Compare the OD with other biological treatment processes in terms of cost effectiveness**

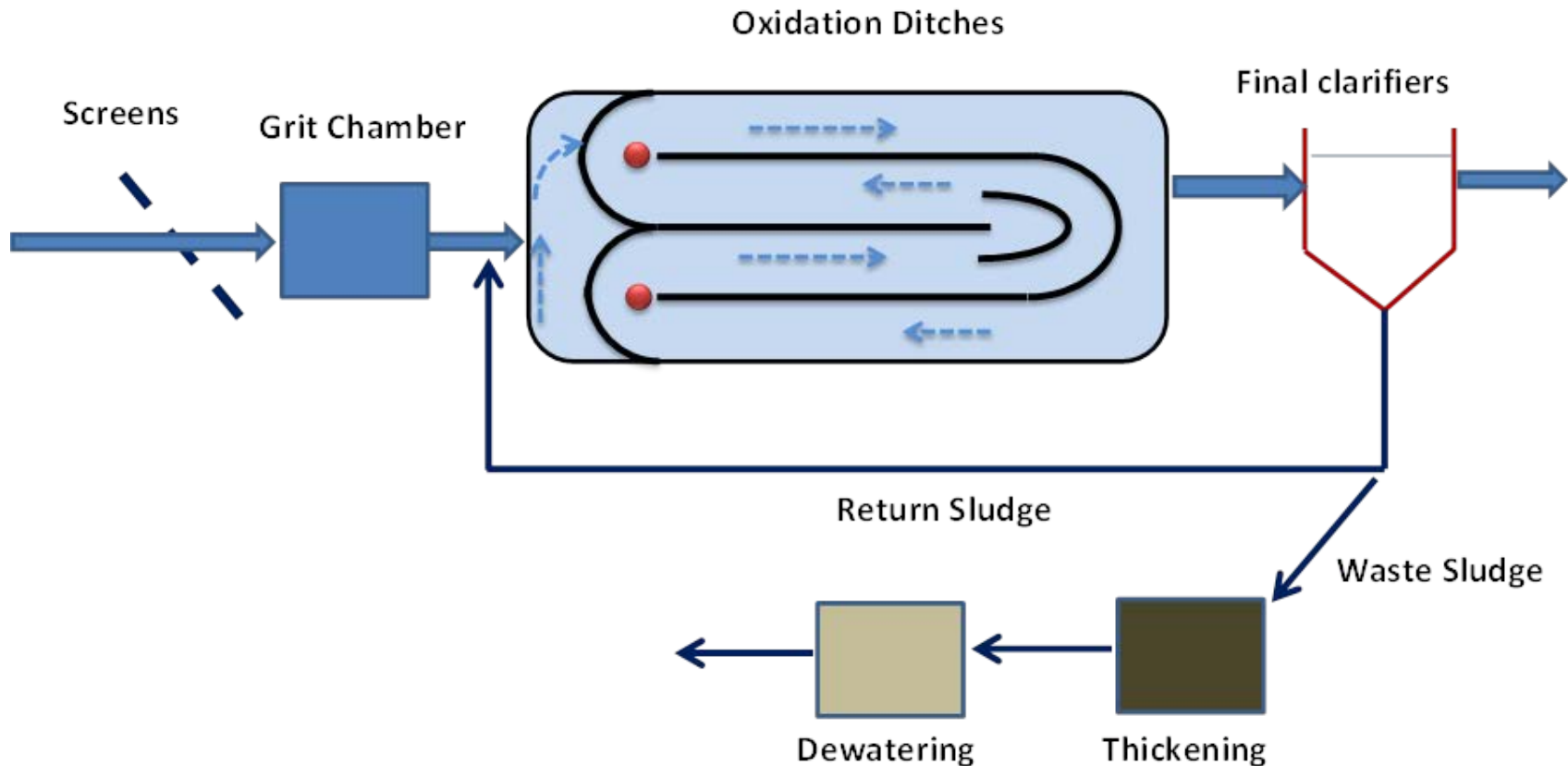
Oxidation Ditch Process



Solids Retention Time: up to 48 days



Typical Oxidation Ditch Plant



Nitrification

De-Nitrification

Advantages

- **Less Sludge due to Extended Solids Retention Time**
- **Resistance to Shock Loads & Hydraulic Surges Due to Long Hydraulic Detention Time**

Disadvantages

- **Requires a Large Land Area (Costly)**
- **Effluent SS Concentrations are Relatively High**

The First Oxidation Ditch

**Pasveer Ditch – 1954
in Netherland**



Modifications to Oxidation Ditch

Jet Aeration Channel



Orbal Process

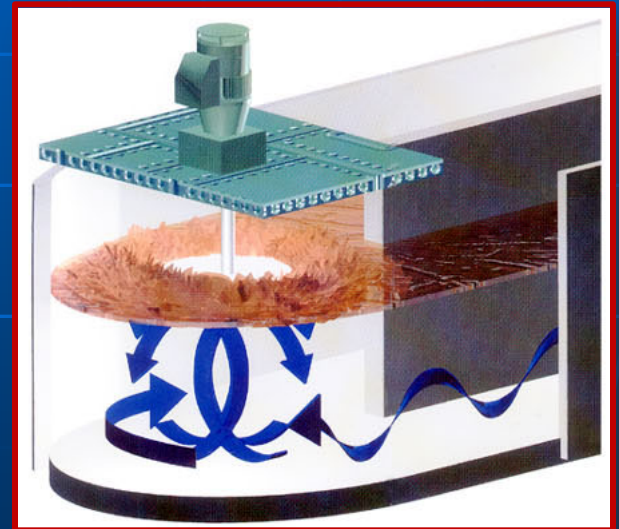


Modifications to Oxidation Ditch

Carrousel System



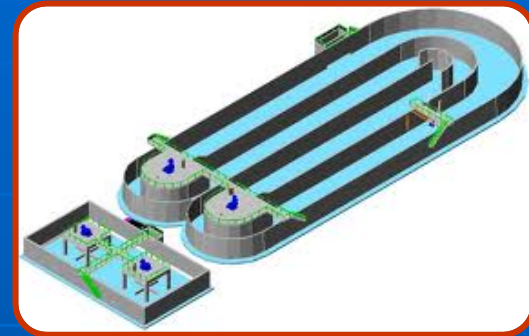
Vertical Shaft Surface Aerator



Modifications to Oxidation Ditch

Carrousel 1000

- Compact System for Small-Scale WWTPs



Carrousel 2000

- Standard Carrousel System + Pre-Denitrification Tank
- + Anaerobic Tank for Phosphorus Removal



Carrousel 3000

- Deep Unit (up to 8 m)



History of Oxidation Ditch in SA

- **Khamees-Meshait** **1981** **Oxidation Ditch**
- **Dammam phase-1** **1982** **Carrousel** **DHV**
- **Al-khobar phase-1** **1982** **Carrousel** **DHV**
- **Al-Jarodiah** **1988** **Carrousel** **DHV+Other**
- .
- .
- .
- **Dammam phase-2** **2008** **Carrousel 2000** **DHV**
- **Al-khobar phase-2** **2008** **Carrousel 2000** **DHV**
- .
- .

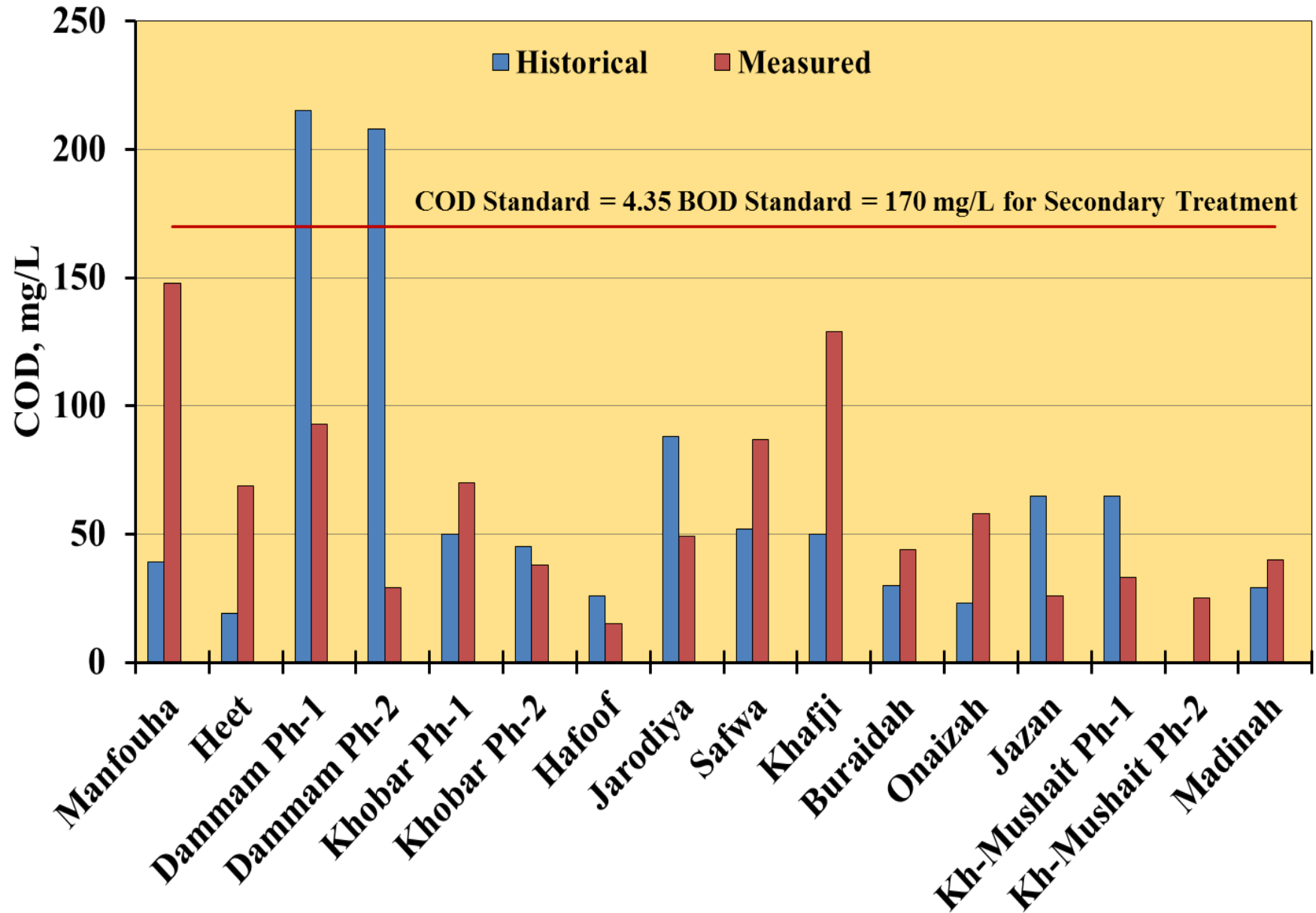
Old Oxidation Ditch in Khamees-Meshait (built 1981)



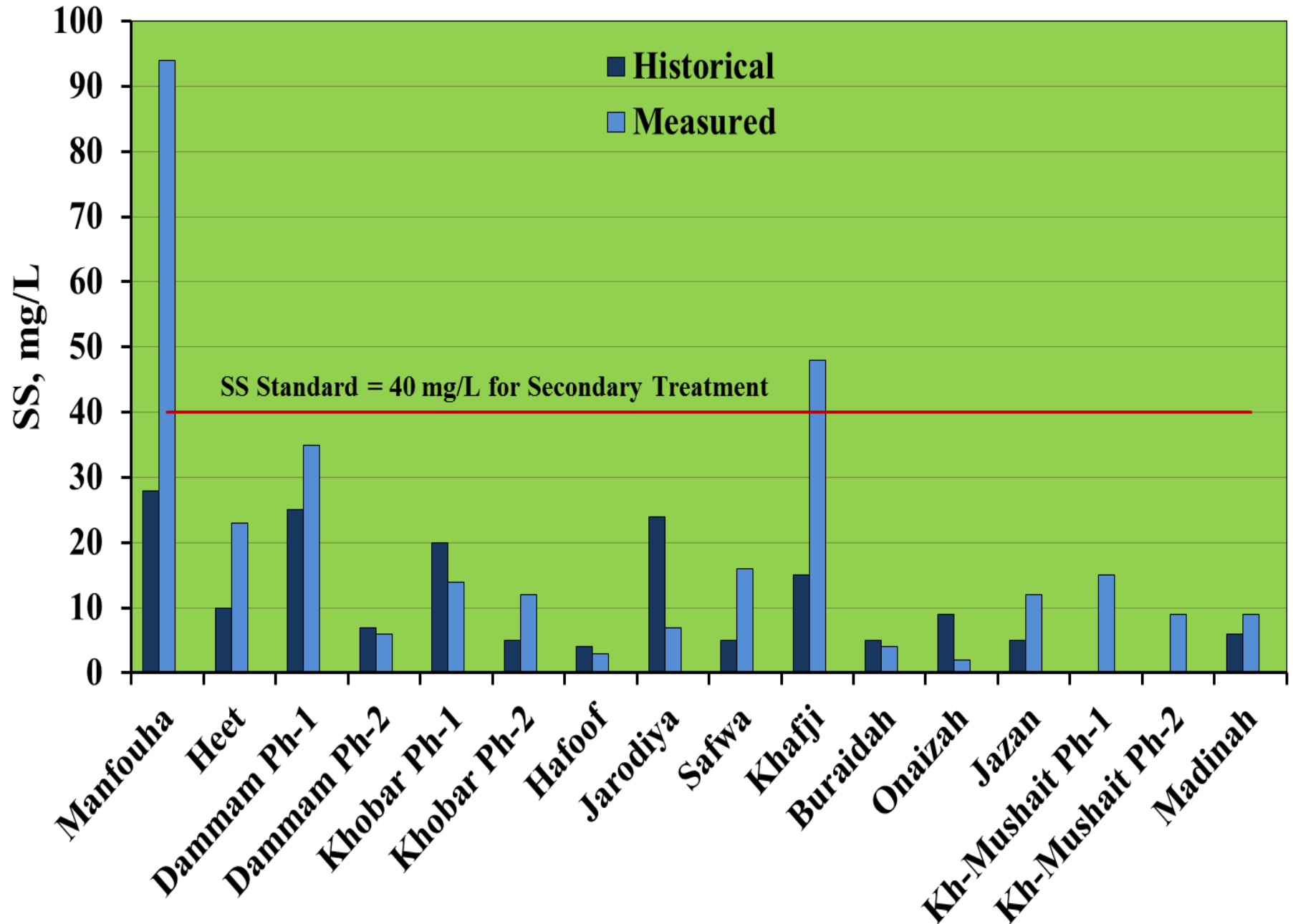
Oxidation Ditch WWTPs Studied

Region	Plant	Capacity, m ³ /day	Oxidation Ditch Type	System Configuration
Riyadh (2)	Manfoha East	200,000	Carousel	Pre-anoxic
	Heet	200,000	Carousel	Pre-anoxic
Al-Qaseem (2)	Buraidah	69,000	Carousel	Post-anoxic
	Onayzah	35,500	Carousel	
Al-Sharqiyah (8)	Dammam Ph-1	208,810	Carousel	Post-anoxic
	Dammam Ph-2	61,500	Carousel 2000	Pre-anaerobic & anoxic
	Khobar Ph-1	133,330	Carousel	Post-anoxic
	Khobar Ph-2	60,000	Carousel 2000	Pre-anaerobic & anoxic
	Hafoof	183,000	Carousel	Post-anoxic
	Jarodiya	90,000	Carousel	Post-anoxic
	Safwa	15,000	Carousel	
	Khafji	15,600	Carousel	
Madinah (1)	Madinah	120,000	Carousel + EA	Pre-anaerobic
Aseer (2)	Kh-Mushait Ph-1	9,000	Oxidation Ditch	
	Kh-Mushait Ph-2	30,000	Carousel	
Jazan (1)	Jazan	20,000	Carousel	

Effluent COD - Historical vs Measured Values

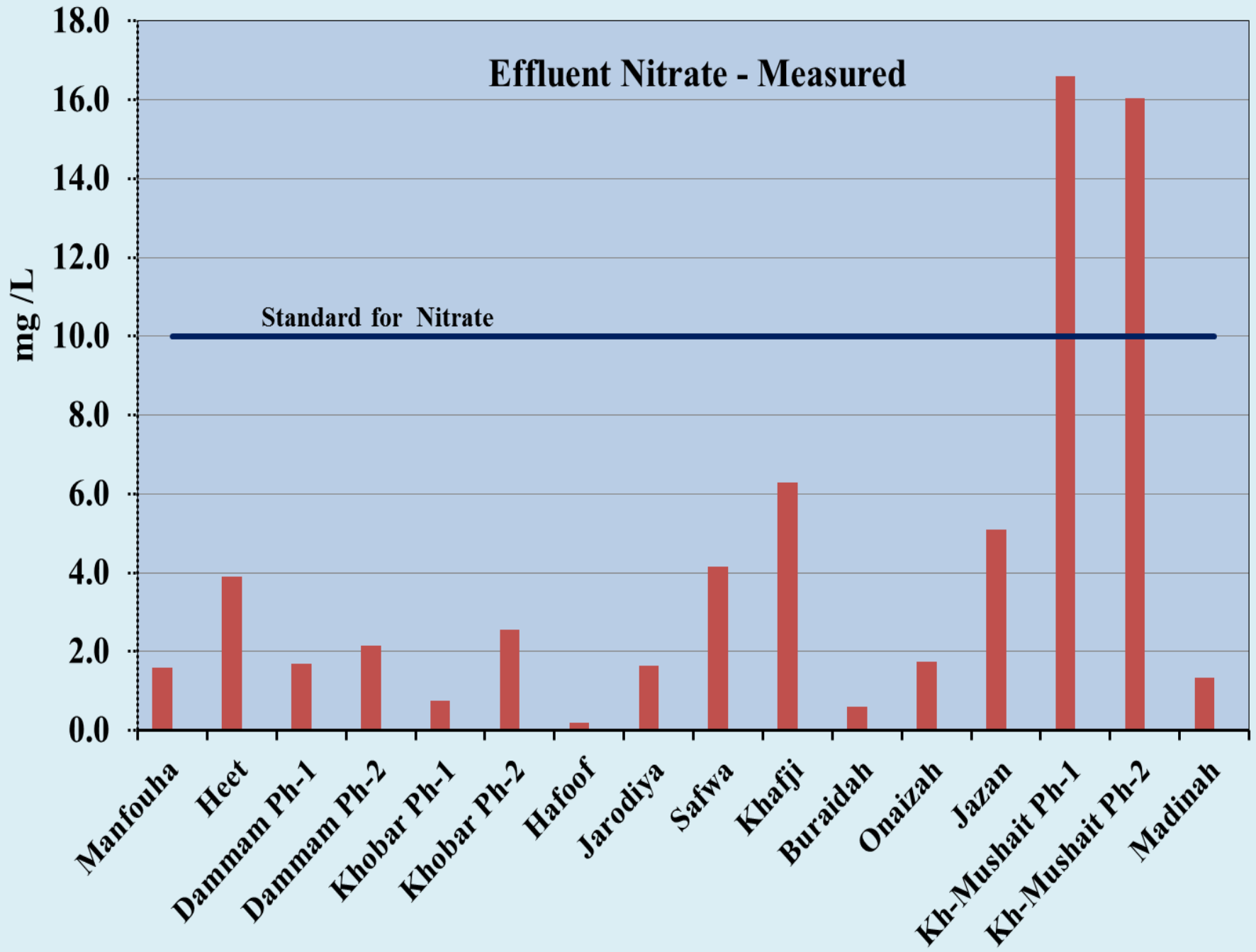


Effluent SS - Historical vs Measured Values



Effluent Nitrate - Measured

Standard for Nitrate



Common Features of Oxidation Ditch Plants in Saudi Arabia

- No primary Sedimentation except in Madinah Plant
- Surface aerators with fixed speed (some are manufactured locally) > difficulty in controlling oxygen requirements for variable organic loading



Common OD plants Operational Problems

Sand deposition in OD If not properly removed in preliminary treatment. (at dead ends of aeration tanks)



Operational Problems

Splashing around surface aerators (endanger health of workers)



Operational Problems

Foam & Floating Scum (oil and grease, & others) in Ditches



Operational Problems

If the Surface Aerator is Broken Down!!, or If the Operator Decides to Safe the Mechanical Aerator



Operational Problems

Sludge & Scum Floating in Final Clarifiers

(Insufficient time for de-nitrification in oxidation ditches)



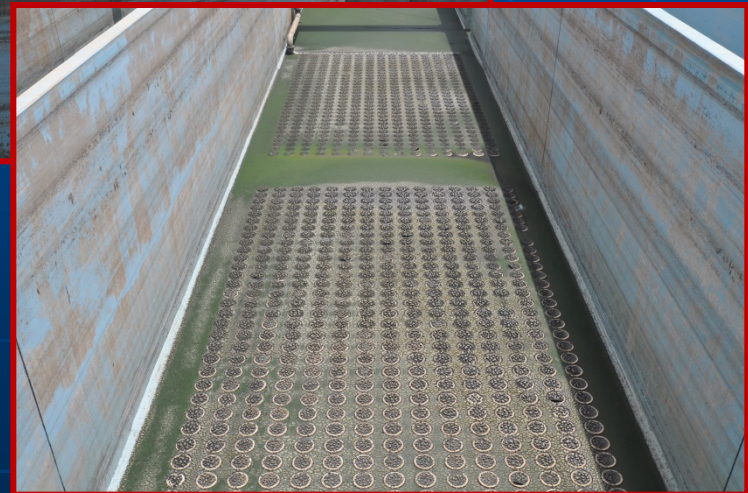
Operational Problems

Design Error!,, Aerators are Fully Covered!



Operational Problems

Regular Maintenance of Diffused Aeration Systems



Other Operational Problems

Excessive and variable organic loadings due to discharge of industrial wastewater and septage into some plants



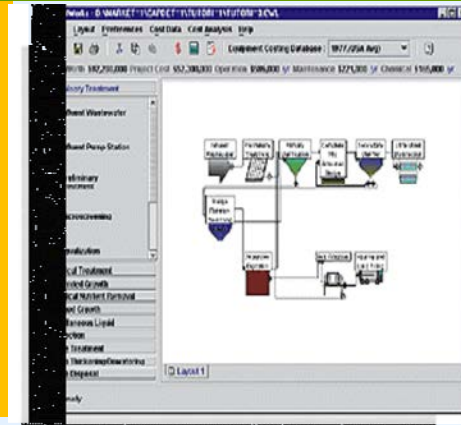
Insufficient capacity of scum collection systems in final clarifiers



Cost Estimation and Analysis

The CapdetWorks (A cost-estimating program for wastewater-treatment construction projects)

- **Calculates the design of each unit process based on the process influent and then cost that design**
- **It estimates costs using the U.S July 2000 data base, and uses “*Cost Indices*” to adjust costs to the present**



- **The Marshall & Swift Equipment Cost Index**
- **The Pipe, Valve, & Fitting Cost Index**
- **The Engineering News Record Construction Cost Index**

2010 values

1302

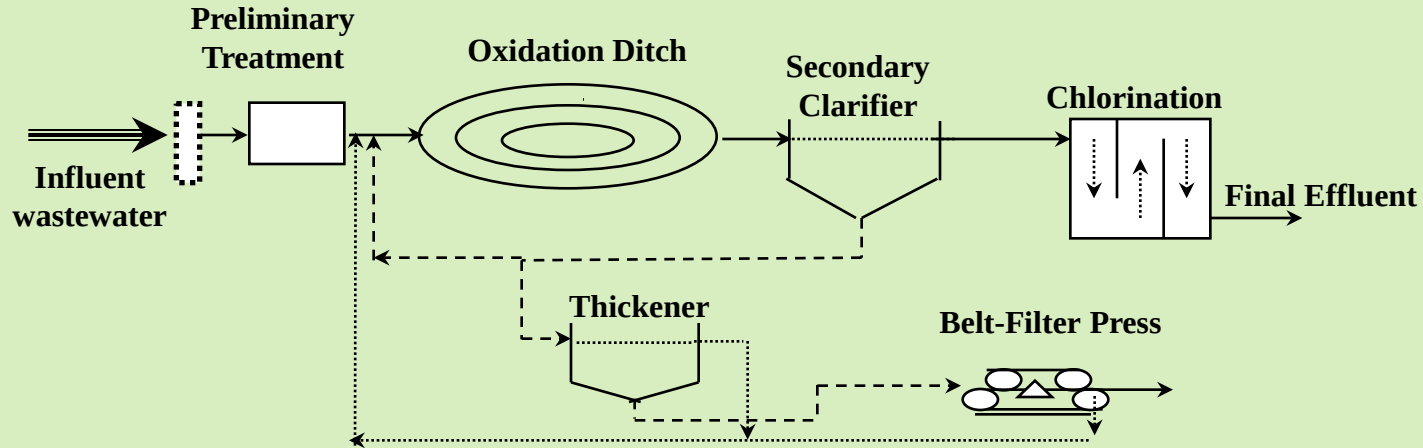
656

7751

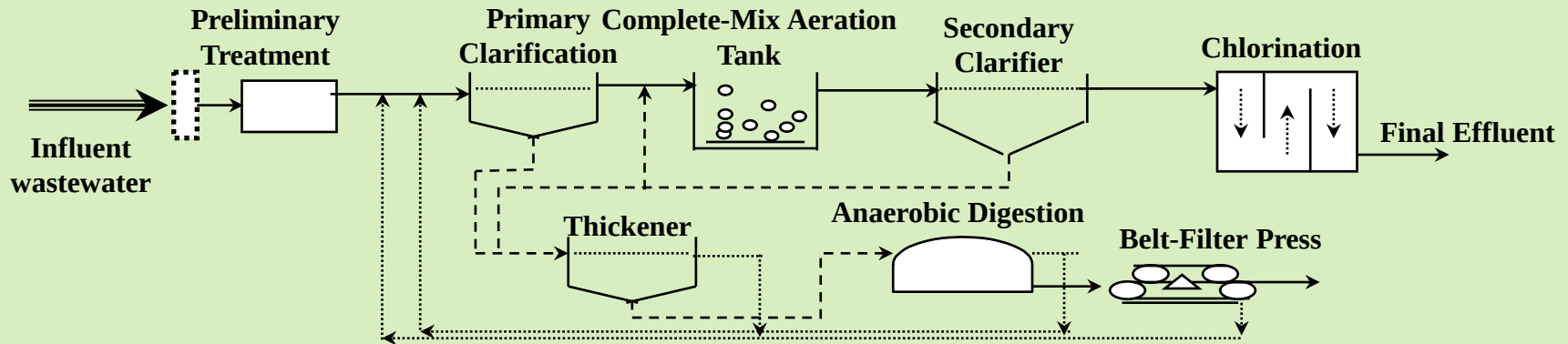
Unit costs for some construction activities & materials, chemicals, and supplies were acquired from local markets

Cost Estimation and Analysis

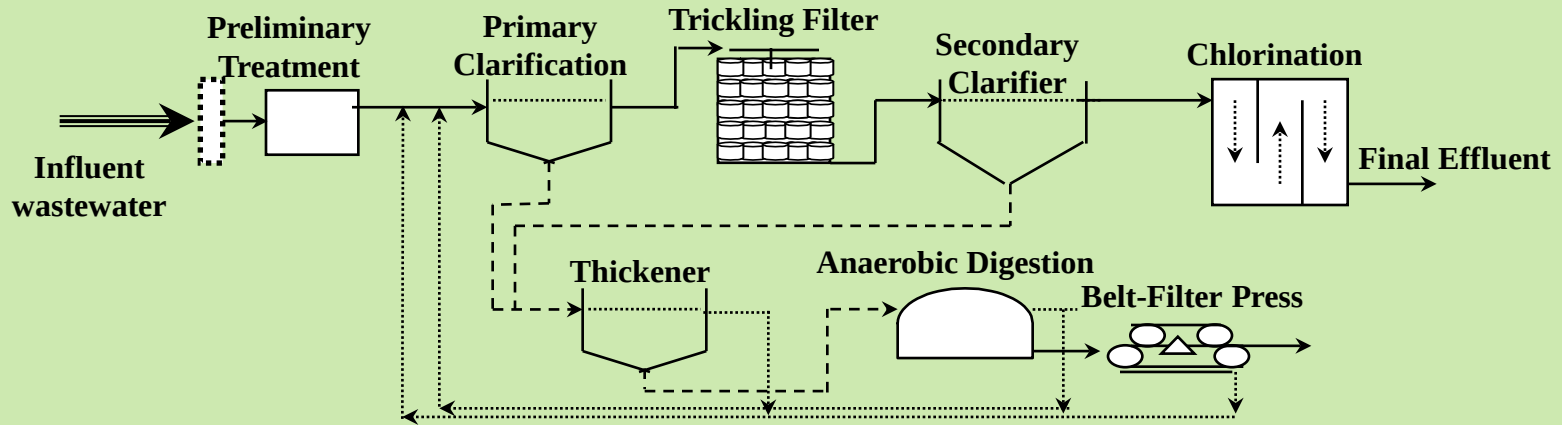
Treatment Schemes



(a) Oxidation Ditch Activated Sludge Plant



(b) Complete-Mix Activated Sludge Plant



(c) Trickling Filtration Plant

Data for design and Cost

✓ Wastewater flows & Characteristics

Manfuha WW Treatment Plant (Riyadh)

Average flow = 200,000 m³/d, Peak flow = 320,000 m³/day

BOD₅ = 300 mg/L, COD = 500 mg/L, SS = 400 mg/L, TKN = 50 mg/L

✓ Desired effluent quality

Reclaimed water quality criteria for un-restricted irrigation (Ministry of Water & Electricity)

✓ Design Period = 30 years

To determine the most cost-effective treatment scheme

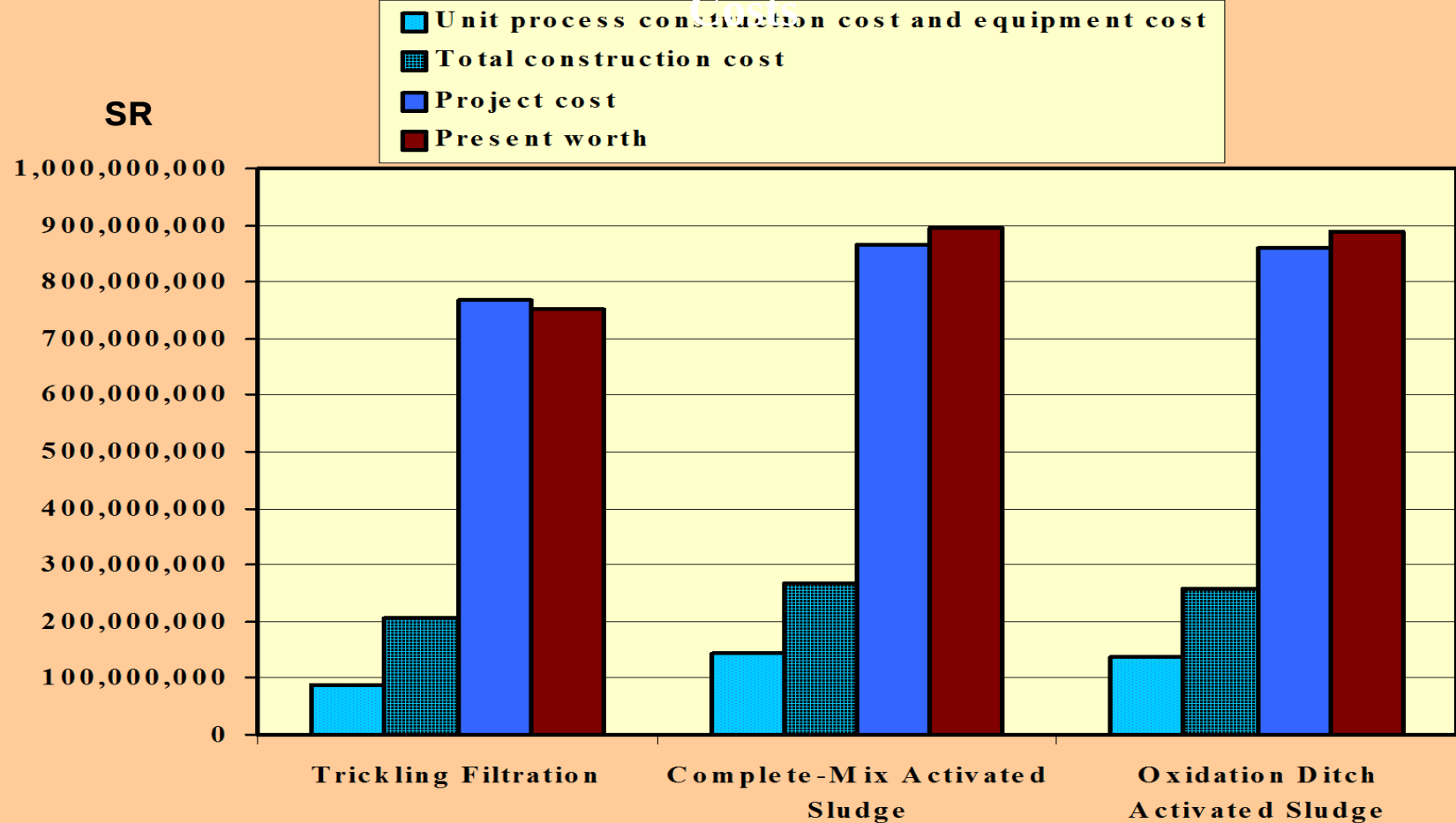
- ✓ The Present Worth Cost
- ✓ The Unit Cost per m³ of wastewater treated

➤ **The Present Worth Cost**

The amount of money required at the beginning of the planning period to pay the project cost immediately *and* the present worth of the annual O & M costs for the entire planning period

Comparison of Construction, Capital & Present Worth

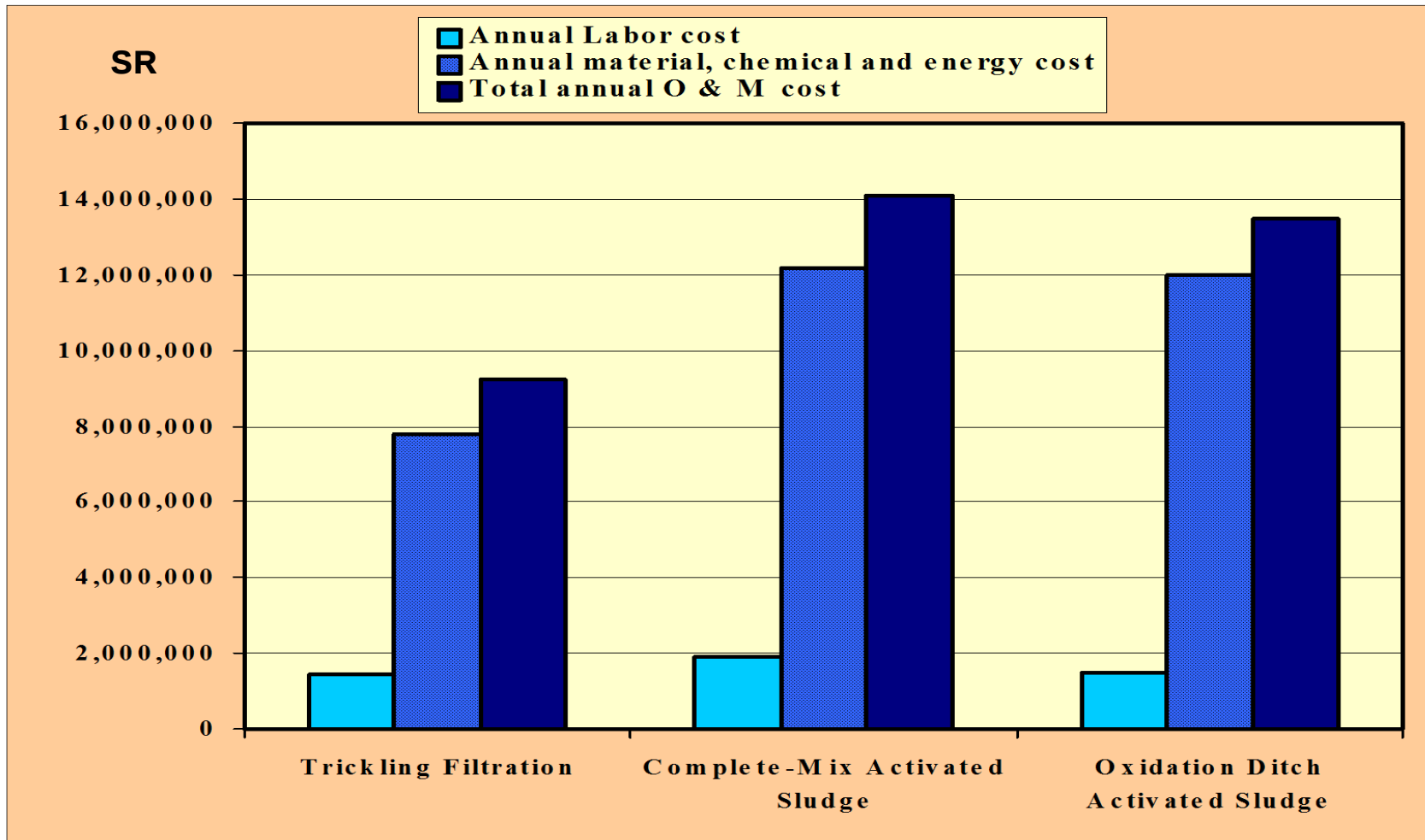
Costs



The capital and present worth costs for the complete-mix and oxidation-ditch AS plants are higher than those of TF

- Total construction cost (27% - 31%)
- Project cost (12%)
- Present Worth Cost (18%)

Comparison of Operation & Maintenance Costs



The O & M costs for the *complete-mix* and *oxidation ditch AS plants* are higher than those of *Tricking filter plant*

- ✓ The annual material, chemical and energy cost (54% - 57%)
- ✓ The total annual O & M cost (46% - 52%)

The per unit cost:

❑ Complete-mix AS: **SR 1.55/m³**

❑ Oxidation-ditch AS: **SR 1.53/m³**

❑ Trickling Filter: **SR 1.36/m³**

Main Findings & Conclusions

- ★ Most Oxidation Ditch Plants Satisfy Effluent Standards for Restricted Irrigation in terms of SS, COD and Nitrate**
- ★ Tertiary Treatment is Needed to Satisfy Effluent Standards for Unrestricted Irrigation**
- ★ Some plants Experience Some Operational Problems and Need More Attention & Qualified Operators**
- ★ The Oxidation Ditch is Not the Most-Cost Effective Treatment Plant**
(Does not satisfies effluent requirements with the lowest cost)

Main Findings & Conclusions

- ✱ There are no typical best type and design for WW treatment plants that can be generalized for all rural and urban cities, and every case need to be studied separately according to the local conditions and circumstances

Thanks