Design of Sewage Treatment Plants

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Acknowledgements

References:

- http://cpheeo.nic.in/Sewerage.aspx
- CPHEEO=Central Public Health and Environmental Engineering Organisation

Contents

- Wastewater quality parameters
- Wastewater treatment procedure
- Design of wastewater treatment
- Operation and maintenance

Sanitation

- Sanitary engineering starts at the point where water supply engineering ends.
- All the taps, fixtures and appurtenances that receive water for use, discharge into the waste-water systems.
- Sanitary engineering starts with the collecting system and ends after the streams or other bodies of receiving water have been returned to the condition of relative purity desired for them.

Sanitary works

- Collection works,
- Treatment works, and
- Disposal works

Philosophy of Wastewater treatment

• To remove various contaminants present in sewage so as to produce an effluent and sludge which can be disposed off in the environment without causing health hazards or nuisance.

Introduction

- The main contaminants in the domestic sewage that are to be removed are:
 - Biodegradable organics
 - Suspended solids
 - Pathogens and
 - Nutrients

Domestic Sewage

- The contaminants in the domestic sewage are present in the form of Suspended (settleable, Non-settelable); Colloidal and Dissolved solids.
- The objective of the treatment process involving various
 (i) operations/processes or (ii) combination of operations and processes; by which the contaminants are stabilised and removed.

Operations in Sewage Treatment

- Physical Unit Operations
 - Change is brought about by means of or through the application of physical forces
- Chemical Unit Processes
 - Change is brought about by means of or through chemical activities
- Biological Unit Processes
 - Change is brought about by means of or through biological activities

Physical Unit Operations

Applications of Physical Unit Operations in Sewage Treatment

Operation	Application
Screening Comminution	Removal of coarse and settleable solids by surface straining Grinding of coarse solids to a more or less uniform size
3. Flow equalization	Equalization of flow and mass loadings of BOD and suspended solids
4. Mixing 5. Flocculation	Mixing of chemicals and gases with sewage; and maintaining solids in suspension Promotes the aggregation of small particles into larger particles to enhance their removal by gravity sedimentation
6. Sedimentation	Removal of settleable solids and thickening of sludges
7. Floatation	Removal of finely divided suspended solids and particles with densities close to that of water. Also thickens biological sludges
8. Filtration	Removal of fine residual suspended solids remaining after biological or chemical treatment
9. Microscreening	Same as filtration. Also rémoval of algae from stabilization-pond effluents

Chemical Unit Processes

Applications of Chemical Unit Processes in Sewage Treatment

Process	Application
Chemical precipitation Gas transfer	Removal of phosphorus and enhancement of suspended solids removal in primary sedimentation facilities used for physical-chemical treatment. Addition and removal of gases.
3. Adsorption	Removal of organics not removed by conventional chemical and biological treatment methods; also used for dechlorination of sewage before final discharge of treated effluent.
4. Disinfection	Selective destruction of disease-causing organisms, usually with chlorine or ozone.
5. Dechlorination6. Others	Removal of chlorine residual that exists after chlorination. Various other chemicals can be used to achieve specific objectives in sewage treatment.

Biological Unit Processes

Major Biological Unit Processes used for Sewage Treatment

Туре	Common name	Use*
Aerobic processes: Suspended growth	Activated-sludge process Conventional (plug flow) Continuous-flow stirred-tank Step aeration	
	Pure oxygen Modified aeration Contact stabilization	Carbonaceous BOD removal (nitrification)
	Suspended-growth nitrification Aerated lagoons	Nitrification Carbonaceous BOD removal (nitrification)
	Aerobic digestion Conventional air Pure oxygen High-rate aerobic algal ponds	Stabilization, carbonaceous BOD removal Carbonaceous BOD removal

Biological Unit Processes

Attached growth

Major Biological Unit Processes used for Sewage Treatment

Trickling filters

Low-rate

High-rate

Roughing filters

Rotating biological contacters

Packed-bed reactors

Trickling filter, activated sludge

Activated sludge, trickling filter

Suspended-growth denitrification

Fixed-film denitrification

Anoxic processes:

Suspended growth

Combined processes

Attached growth

Carbonaceous BOD removal (nitrification)

Carbonaceous BOD removal Carbonaceous BOD removal (nitrification)

Nitrification

Carbonaceous BOD removal (nitrification)

Denitrification

Biological Unit Processes

Anaerobic processes: Suspended growth

Attached growth

Aerobic/anoxic or anaerobic processes: Suspended growth

Attached growth Combined process

Major Biological Unit Processes used for Sewage Treatment

Anaerobic digestion
Standard-rate, single-stage
High-rate, single-stage
Two-stage

Anaerobic contact process

Anaerobic filter

Anaerobic lagoons (ponds)

Single-stage
nitrification-denitrification
Nitrification-denitrification
Facultative lagoons (ponds)
Maturation or tertiary ponds

Anaerobic-facultative lagoons

Anaerobic -facultative-aerobic lagoons

Stabilization, carbonaceous BOD removal

Carbonaceous BOD removal Carbonaceous BOD removal, stabilization (denitrification) Carbonaceous BOD removal (stabilization)

Carbonaceous BOD removal, nitrification, denitrification
Nitrification, denitrification
Carbonaceous BOD removal
Carbonaceous BOD removal (nitrification)

Carbonaceous BOD removal

Reactors for Sewage Treatment

- Batch
- Plug flow
- CSTR (Continuous flow stirred tank)
- Arbitrary flow
- Fluidised bed
- Membrane bio reactor

Classification of Sewage Treatment

- Preliminary
 - To remove floating materials such as dead animals, wood pieces, tree branches, papers, heavy settleable inorganic solids, fats, oil, grease etc.
- Primary
 - To remove large suspended organic solids
- Secondary
 - Removal of residual organic matter and suspended material.
- Tertiary
 - To remove the contaminants that are not removed in conventional treatment

- Screens
- Grit chambers
- Comminutors
- Skimming tanks
- Floatation units
- Flow measuring units

Preliminary Treatment of Sewage Preliminary Treatment Units, their Functions and Expected Efficiencies

Purification Effected	Process or unit employed	BOD5 removal (% of original)	Removal of suspended solids (% of original)	Removal of Total coliforms (% of original)	Disposal of Residuals
Removal of floating materials such as dead animals, wood pieces, tree branches, rags, papers and other large sized floating materials	Coarse and fine screens of different designs	5-10	2-10	10-20	Screenings disposed of by burials or burnings
2. Removal of heavy settleable inorganic solids	Grit chambers or Detritus tanks.	10-20	20-40	10-20	Grits disposed of by burials or burnings or raising low lying area
3. Removal of fats and greases	Floatation units and skimming tanks	20-30	20-40	10-20	Skimmings being unstable volatile materials, are disposed of by first stabilizing them in digestion tanks by anaerobic process.

TABLE 10.5. Primary Treatment Units, their Functions and Expected Efficiencies

Purification Effected	Process or unit employed	BOD ₅ removal (% of original)	Removal of suspended solids (% of original)	Removal of Total coliforms (% of original)	Disposal of Residuals
Removal of large suspended	(i) Plain sedimentation tanks OR	30-35	60-65	25-75	Sludge, after stabilization in digestion tanks, is used as a manure or soil builder.
organic solids	(ii) Septic tanks OR (iii) Imhoff Tanks	20-30	40-60	25-75	These units combine sedimentation and sludge digestion. Sludge used as manure while effluents is either treated for secondary treatment or disposed of by land treatment.

Secondary Treatment of Sewage

TABLE 10.6. Secondary Treatment Units, their Functions and Expected Efficiencies

Purification Effected	Process or unit employed	BODs removal (% of original)	Removal of suspended solids (% of original)	Removal of Total coliforms (% of original)	Disposal of Residuals
Removal of fine suspended and	(i) Chemical flocculation and sedimentation OR	50-85	70-90	40-80	Sludge containing organic matter has to be stabilized in digestion tanks before use as manure or soil builder
dissolved organic matter	(ii) Intermittent sand filters followed and preceded by plain sedimentation OR	90-95	85-95	95-98	Same as above
	(iii) High rate trickling filters followed and preceded by plain sedimentation	60-95	65-92	80-85	Same as above

Secondary Treatment of Sewage

TABLE 10.6. Secondary Treatment Units, their Functions and Expected Efficiencies

Purification Effected	Process or unit employed	BOD ₅ removal (% of original)	Removal of suspended solids (% of original)	Removal of Total coliforms (% of original) 90-95	Disposal of Residuals Same as above
	(iv) Low rate trickling filters followed and preceded by plain	90-95	70-92	90-93	Same as doore
	sedimentation OR (v) Activated sludge	75-95	85-90	90-98	Same as above
	treatment process and secondary settling tanks OR				
	(vi) Oxidation ponds	85-90	85-90	90-98	Effluents are generally disposed of by using them for irrigation

Tertiary Treatment of Sewage

- Various processes that are used in the tertiary treatment of sewage are
 - Chemical clarification
 - Recarbonation
 - Filtration
 - Activated carbon adsorption
 - Disinfection
 - Nitrogen removal
 - Phosphorous removal
 - Demineralisation

Summary

Unit Operations, Unit Processes and Treatment Systems used to Remove Major Contaminants found in Sewage

Contaminant	Unit operation, unit process, or treatment system
Suspended solids	Sedimentation Screening and comminution Filtration (various types)
	Floatation Chemical-polymer addition Coagulation/sedimentation Land treatment systems
Biodegradable organics	Activated-sludge processes Fixed-film: trickling filters Fixed-film: rotating biological contactors
	Lagoon (various types) Intermittent sand filtration Land treatment systems Physical chemical systems
Pathogens	Physical-chemical systems Chlorination Hypochlorination Ozonation
	Land treatment systems

Summarv

Nitrogen

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Phosphorus

Refractory organics

Heavy metals

Dissolved inorganic solids

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Suspended-growth nitrification and denitrification (various types)

Fixed-film nitrification and denitrification (various types)

Ammonia stripping

Ion exchange

Breakpoint chlorination

Land treatment systems

Metal-salt addition

Lime coagulation/sedimentation

Biological-chemical phosphorus removal

Land treatment systems

Carbon adsorption

Tertiary ozonation

Land treatment systems

Chemical precipitation

Ion exchange

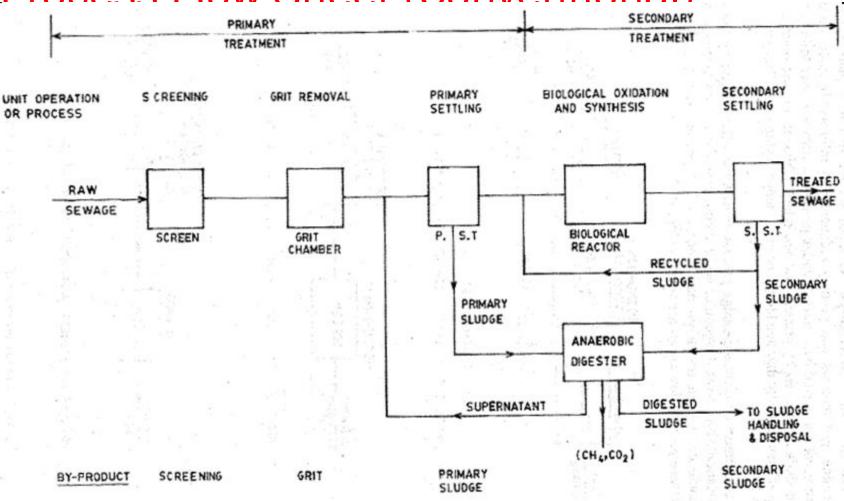
Land treatment systems

Ion exchange

Reverse osmosis

Electrodialysis

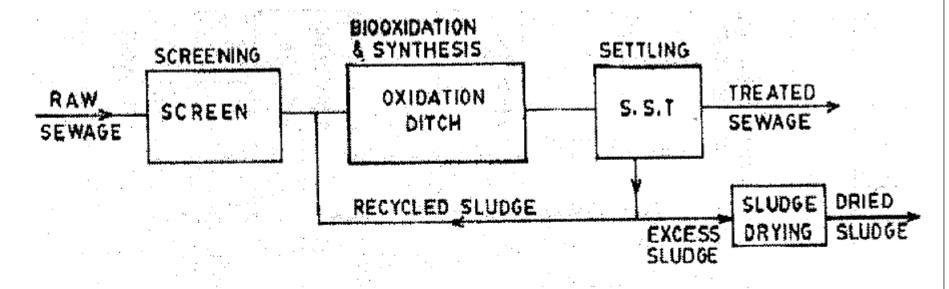
Process Flow Sheet (Conventional)



P. S. I = PRIMARY SETTLING TANK S.S. J = SECONDARY SETTLING TANK

Fig. 10.1 Process flow sheet of conventional Domestic sewage treatment.

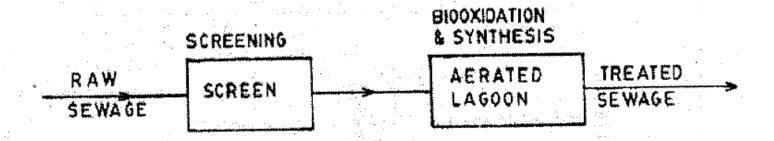
Process Flow Sheet (low cost)



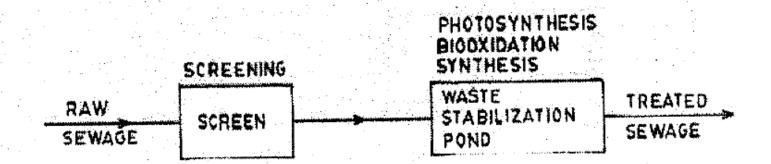
S.S. T= SECONDARY SETTLING TANK

(a) PROCESS FLOW SHEET INCORPORATING OXIDATION DITCH.

Process Flow Sheet (low cost)



(b) PROCESS FLOW SHEET EMPLOYING AERATED LAGOON.



(c) PROCESS FLOW SHEET USING WASTE STABILIZATION POND.

Process Flow Sheet (Anaerobic)

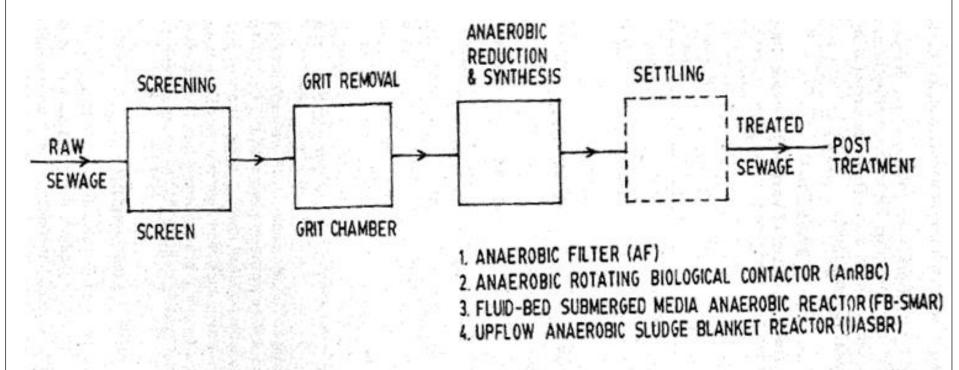


Fig. 10.3 Process flow sheet employing anaerobic treatment devices.

Expected Efficiencies of Various Treatment Units

	Pe	Percentage reduction				
Process	BOD_5	Suspended solids	Total coliform			
Primary Treatment (sedimentation)	30-45	45-60	40-60			
2. Chemical Treatment	45-65	60-80	60-90			
3. Secondary Treatment						
(i) Standard trickling filters	70-90	75-85	80-90			
(ii) High rate trickling filters						
(a) Single stage	75-80	75-85	80-90			
(b) Two stage	90-95	90-95	90-95			
(iii) Activated sludge plants	85-95	85-90	90-96			
(iv) Stabilization Ponds						
(a) Single cell	90-95	80-90	90-95			
(b) Two cells	95-97	90-95	95-98			

Design and Construction of S.T.Ps

Contribution of human wastes in grams per capita per day

	Parameters						
1	1 Biochemical oxygen demand, BOD						
2						nes BOD	
3	Total organic carbon,	тос			0.6-1.0 tin	nes BOD	
4	Total solids, TS				170-220		
5	Suspended solids, SS				70-145		
6	Grit (inorganic,0.2 mm	and above	e)		5-15		
7	Grease				10-30		
8	Alkalinity as calcium o	arbonate (0	CaCO₃)		20-30		
9	9 Chlorides				4-8		
10	Total nitrogen N				6-12		
11	Organic nitrogen				~0.4 total N		
12	Free ammonia				~0.6 total N		
13	Nitrate				~0.0-0.5 t	otal N	
14	Total phosphorus				~0.6-4.5		
15	Organic phosphorus				~0.3 total P		
16	Inorganic(ortho- and p	oly-phosph	ates)		~0.7 total	Р	
17	Potassium(as potassium)	um oxide K ₂	2O)		2.0-6.0		
	Mi	croorganisn	ns in 1	00 ml of sewage			
18	Total bacteria	10 ⁹ -10 ¹⁰	22	Protozoan cysts		Up to 10 ³	
19	Coliforms	10 ⁹ -10 ¹⁰	23	Helminthic eggs		Up to 10 ³	
20	Faecal streptococci	10 ⁵ -10 ⁶	24	Virus (plaque formi	ng units)	10 ² -10 ⁴	
21	Salmonella Typhosa	10 ¹ -10 ⁴					

Typical composition of Sewage (Concentration of various parameters)

Item	Per capita contribution (g / c /d)	water supply (L / c / d)	Sewage Generation 80 % of (3)	Concen- tration (mg/L)
(1)	(2)	(3)	(4)	(5)
BOD	27.0	135	108	250.0
COD	45.9	135	108	425.0
TSS	40.5	135	108	375.0
VSS	28.4	135	108	262.5
Total Nitrogen	5.4	135	108	50.0
Organic Nitrogen	1.4	135	108	12.5
Ammonia Nitrogen	3.5	135	108	32.5
Nitrate Nitrogen	0.5	135	108	5.0
Total Phosphorus	0.8	135	108	7.1
Ortho Phosphorous	0.5	135	108	5.0

Illustration BOD = 27 *1000 (mg) / 135 X 0.8 (litres) = 250 mg/L

General standards for Discharge of Environmental Pollutants

			Standar	ds	
No	Characteristics	Inland	Public	Land	Marine
110	Gridiadoriolog	Surface	Sewers,	for	Coastal
		Water	(A)	Irrigation	Areas
1	Colour and odour	(B)		(B)	(B)
2	SS	100	600	200	(C), (D)
3	Particle size of SS	(E)	-	-	(F), (G)
4	pH value	5.5 to 9.0			
5	Temperature	(H)	-	-	(H)
6	Oil and grease	10	20	10	10
7	Total residual chlorine	1.0	-	-	1.0
8	Ammoniacal nitrogen (as N)	50	50	-	50
9	Total Kjeldahl Nitrogen, (TKN) (as N)	100	-	-	100
10	Free ammonia (as NH ₃)	5.0	-	-	5.0
11	Biochemical Oxygen Demand	30	350	100	100
12	Chemical Oxygen Demand	250	-	-	250

General standards for Discharge of Environmental Pollutants

	Contract Clarina and Ton Dicona	900. —		110116	
13	Arsenic (as As)	0.2			
14	Mercury (as Hg)	0.01	0.01	-	0.01
15	Lead (as Pb)	0.1	1.0	-	2.0
16	Cadmium (as Cd)	2.0	1.0	-	2.0
17	Hexavalent Chromium (as Cr 6+)	0.1	2.0	-	1.0
18	Total Chromium (as Cr)	2.0	2.0	-	2.0
19	Copper (as Cu)	3.0	3.0	-	3.0
20	Zinc (as Zn)	5.0	15.0	-	15.0
21	Selenium (as Se)	0.05	0.05	-	0.05
22	Nickel (as Ni)	3.0	3.0	-	5.0
23	Cyanide (as CN)	0.2	2.0	0.2	0.2
24	Fluoride (as F)	2.0	15.0	-	15.0
25	Dissolved phosphates (as P)	5.0	-	-	-
26	Sulphide (as S)	2.0	-	-	5.0
27	Phenolic compounds (as C ₆ H ₅ OH)	1.0	5.0	-	5.0
	Radioactive materials				
28	Alpha emitters, micro curie/L	10 ⁻⁷	10 ⁻⁷	10 ⁻⁸	10 ⁻⁷
	Beta emitters, micro curie/L	10⁻6	10 ⁻⁶	10 ⁻⁷	10 ⁻⁶
29	Bio-assay test	(1)			
30	Manganese (as Mn),	2.0	2.0	-	2.0
31	Iron (as Fe),	3.0	3.0	-	3.0
32	Vanadium (as V),	0.2	0.2	-	0.2
33	Nitrate Nitrogen (as N),	10.0	-	-	20.0
34.	Faecal Coliform, MPN/100 ml for discharge	onto land		into water	
		(J)	(K)	(J)	(K)
		1,000	10,000	1,000	10,000

- Screening
- Screening is essential for removal of floating materials which are mainly sachets, plastic sheet bits, leaves, fibres, rags, etc.
- If these are not removed, they will get into the pumps and entangle in the impellers.
- They can also be drawn into suction pipes and choke them and it is difficult to locate their position in the pipeline.
- They can cause objectionable shoreline conditions where disposal into sea is practiced.
- Screens are used ahead of pumping stations, meters and as a first step in all STPs.
- A screen is a device with openings generally of uniform size.

- Screening
- Types of Screens
 - Coarse Screens (with openings >25 mm)
 - Medium Screens (with openings of ≈ 12 mm)
 - Fine Screens (with openings of ≈ 5 mm)

Screening





Screening

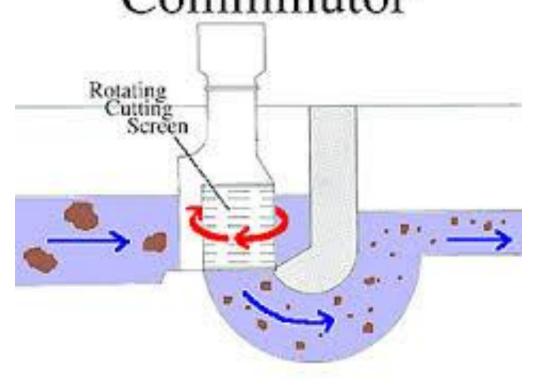


- Screening
- Design Considerations
 - Velocity of flow
 - 0.6-1.2 m/s
 - Loss of head
 - Normally 0.15 m, should not exceed 0.3 m
 - Materials
 - Coarse screens
 - Steel bars
 - Fine screens
 - o Steel bars, Bronze plates or wire mesh
 - Angle of inclination
 - 45-60 with horizontal for manually cleaned and 60-90 for mechanically cleaned
 - Free board
 - 0.3 m
 - Max width
 - 1.5 m

- Screening
- Design Procedure for Screens
 - Calculate the projected area of screens using the peak sewage flow
 - Calculate the number of bars
 - Calculate the width and length of screen channel
 - Calculate the height of screen
 - Calculate the velocity of flow in screen channel
 - Calculate the head loss through the screens
 - Calculate the hydraulic loading for peak flow

- Comminuting Devices
- a mechanically cleaned screen which incorporates a cutting mechanism that shreds the retained material and enabling it to pass along with the sewage
- recommended for smaller sized STPs of up to 1 MLD.

Preliminary Treatment of Sewage Comminutor



- Grit Removal
- Grit removal is necessary to protect the moving mechanical equipment and pump elements from abrasion and accompanying abnormal wear and tear.
- Removal of grit also reduces the frequency of cleaning of digesters and settling tanks.

- Grit Removal
- Design considerations
 - Settling velocity
 - Surface overflow rate
 - Detention period
 - 45 to 90 sec
 - Bottom scour velocity
 - Velocity control device
 - Proportional flow weir
 - Parshall flume
 - Number of units
 - Loss of Head

- Grit Removal
- Design Procedure for GRIT chamber
 - Compute the settling velocity
 - Compute the surface overflow rate
 - Determine the dimensions of the chamber
 - Design the velocity control facility

Preliminary Treatment of Sewage • Velocity control devices





Proportional flow weir

Preliminary Treatment of Sewage • Velocity control devices



Parshall Flume

- Flow Equalization
- when the peak factor exceeds 3 by a wide margin, it is advisable to equalize the sewage flow before feeding to the STP units.

- SETTLING
- The primary clarifier is located after screens and grit chambers and reduces the organic load on secondary treatment units.

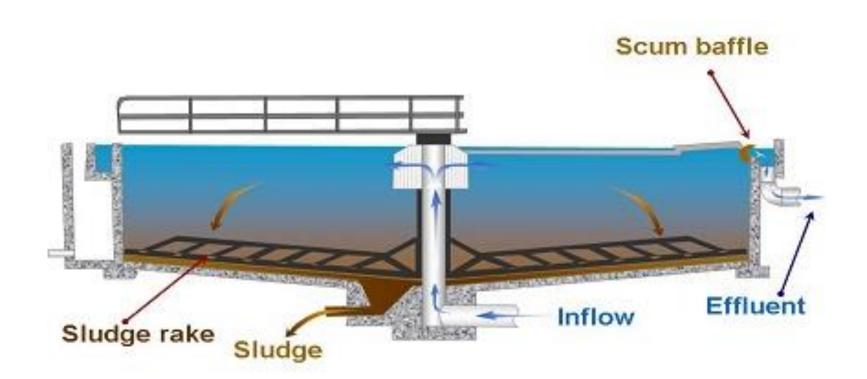
- SETTLING
- Design considerations
 - Velocity of flow
 - Surface overflow rate
 - Detention period
 - 2-2.5 hours
 - Tank dimensions
 - Rectangular or circular
 - Inlet and outlet
 - Weir loading

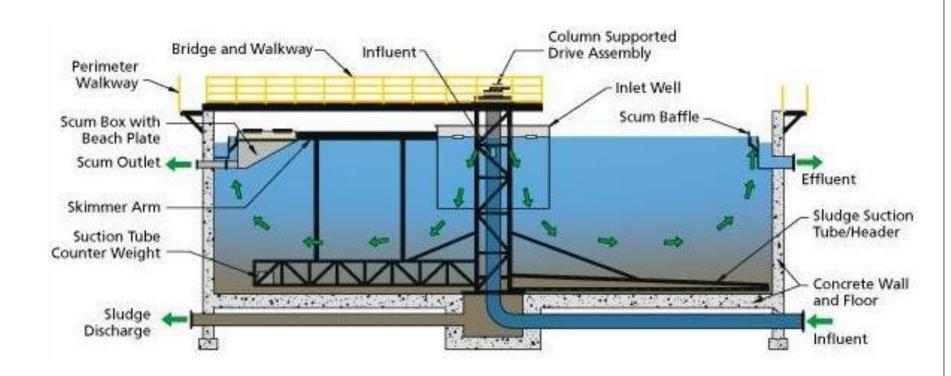
• SETTLING

Table 5.8 Design Parameters for Clarifiers

Type of Settling	Overflow rate, cum/sqm/day		Solid loading, kg/day/sqm		Side Water Depth, m	Weir loading, cum/m/day			
	Average	Peak	Average	Peak	Average	Average			
Primary Clarifiers									
Primary Settling only	25 - 30	50 - 60	Not applicable		≥ 2.5 - 3.5	125			
Followed by secondary treatment	35 - 50	80 - 120	Not applicable		≥ 2.5 - 3.5	125			
With excess sludge return	25 - 35	50 - 60	Not applicable		≥ 3.5 - 4.5	125			
Secondary Clarifiers									
Secondary settling for activated sludge	15 - 35	40 - 50	70 - 140	210	≥ 3.0 - 3.5	185			
Secondary settling for extended aeration	8 - 15	25 - 35	25 - 120	170	≥ 3.0 - 4.0	185			

- SETTLING
- Design procedure
 - Compute the capacity of the tank by assuming the detention period.
 - Adopt the required depth of the tank
 - Calculate the surface area required
 - Perform cross check for the dimensions obtained





Activities in Aerobic Digestion

Oxidation

 $Organic matter + O_2 + bacteria \rightarrow CO_2 + H_2O + NH_3 + other$ end products + energy

Synthesis

Organic matter + O_2 + bacteria+ energy \rightarrow New microbial cell tisue

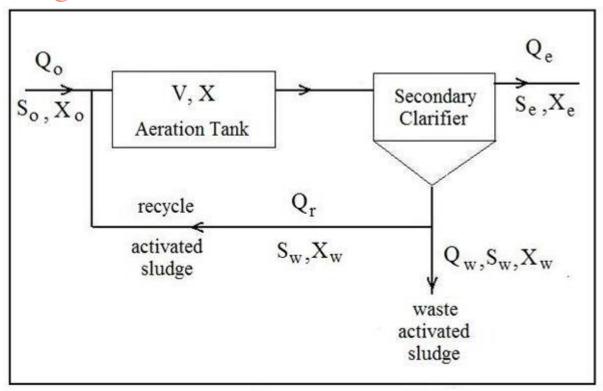
Endogeneous respiration

New microbial cell tissue $+5O_2 \rightarrow 5CO_2 + NH_3 + 2H_2O + energy$

• Activated Sludge Process



Activated Sludge Process



Activated Sludge Flow Diagram & Parameters

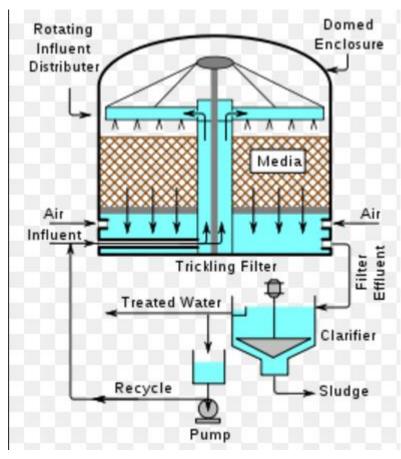
- Activated Sludge Process
- Activated sludge plant involves:
 - wastewater aeration in the presence of a microbial suspension,
 - solid-liquid separation following aeration,
 - discharge of clarified effluent,
 - wasting of excess biomass, and
 - return of remaining biomass to the aeration tank.

- Activated Sludge Process
- Design elements:
 - Design of Aeration tank
 - Design of clarifier
 - Return sludge rate
 - Sludge wasting

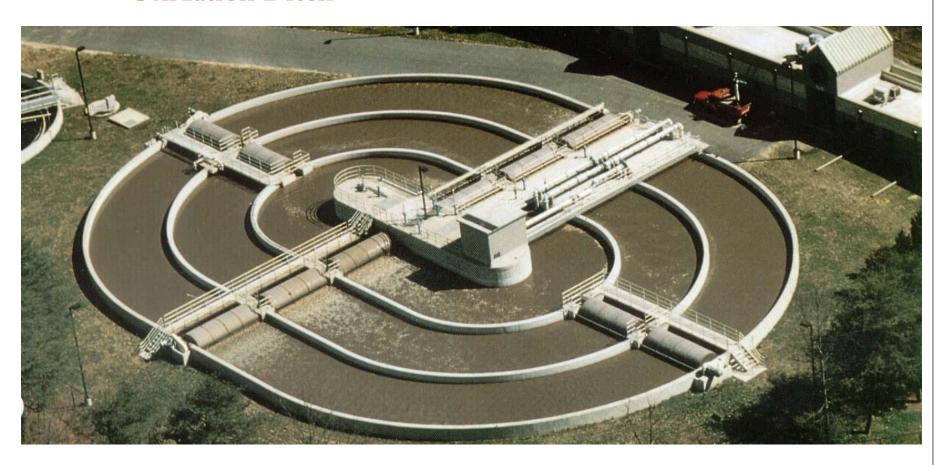
- Activated Sludge Process
- Key considerations in ASP design:
 - MLSS (mixed liquor suspended solids)
 - F/M Ratio
 - Oxygen transfer rate
 - Rate of sludge production
 - Aeration tank volume
 - Sludge recycle rate

- Activated Sludge Process
- Modifications to the conventional ASP
 - Tapered aeration
 - Step aeration
 - Contact stabilisation
 - Extended aeration
 - Complete mix

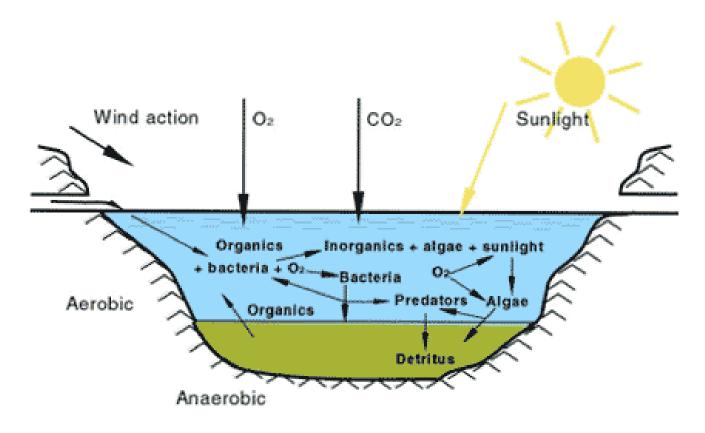
• Trickling filters



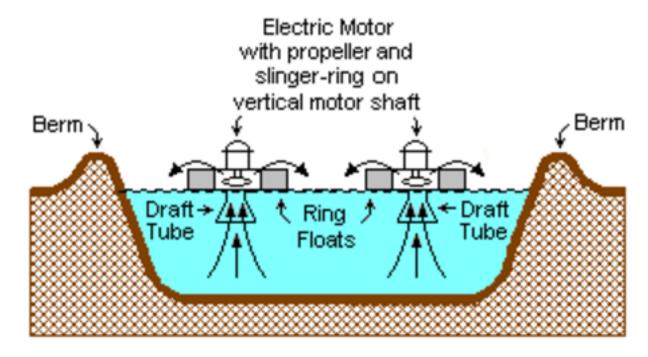
• Oxidation Ditch



• Oxidation Ponds (Stabilisation Ponds)



Aerated Lagoons



A TYPICAL SURFACE – AERATED BASIN

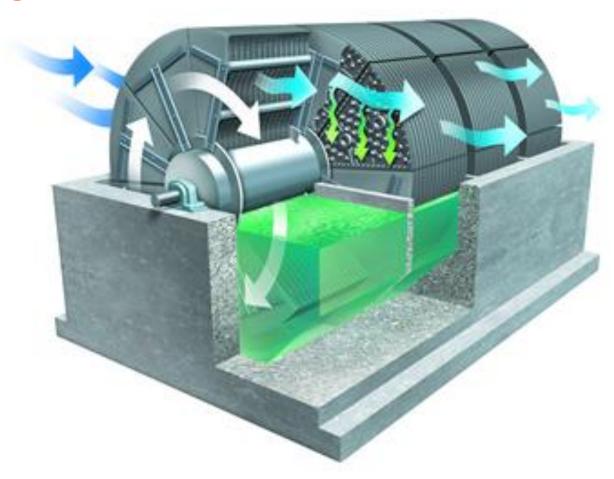
Note: The ring floats are tethered to posts on the berms.

Aerated lagoons

Table 5.12 Some Characteristics of Aerated Lagoons

No.	Characteristics	Facultative Aerated Lagoons	Fully Aerobic	Extended Aeration System (for comparison)
1.	Detention time, days	3 - 5	2 - 3	0.5 - 1.0
2.	Depth, m	2.5 – 5.0	2.5 - 4.0	2.5 - 4.0
3.	Land required, m²/person	0.15 - 0.30	0.10 - 0.20	
4.	BOO removal efficiency %	80 - 90	50 - 60	95 - 98
5.	Overall BOD removal rate, K (A)	0.6 – 0.8	1-1.5	20 - 30
6.	Suspended solids in lagoon, mg/l	40 - 150	150 - 350	3,000 - 5,000
7.	VSS/SS	0.6	0.8	0.6
8.	Desirable power level (B)	0.75	2.75 - 6.0	15 - 18
9	Power requirement, kWh/person/year	12 - 15	12 - 14	16 - 20

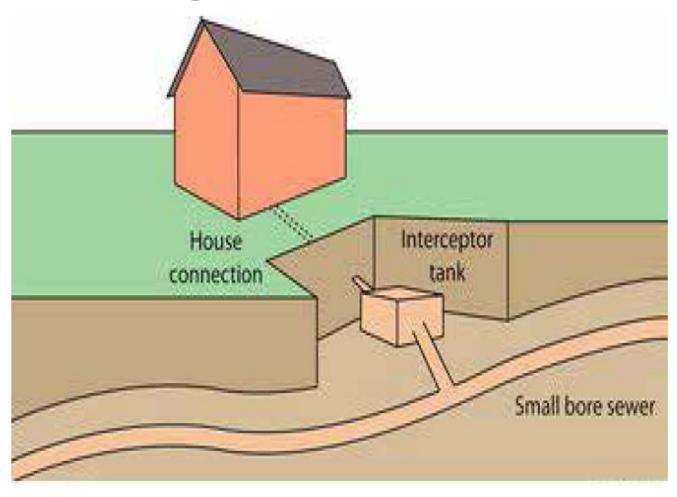
• Rotating biological Contactors



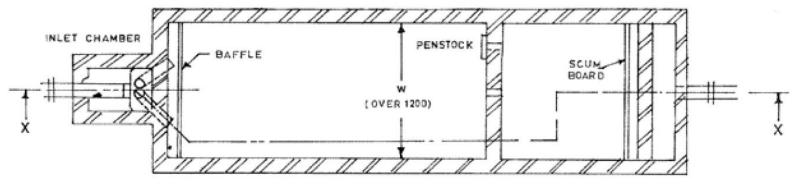
Rural Wastewater treatment systems

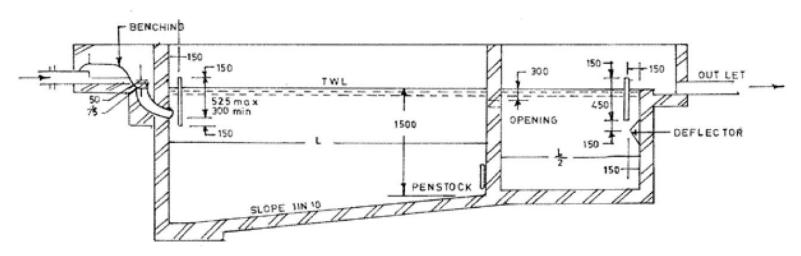
- Septic tank
- Constructed wetlands
- Lagoons
- Waste stabilisation ponds

A schematic diagram of Small bore sewer



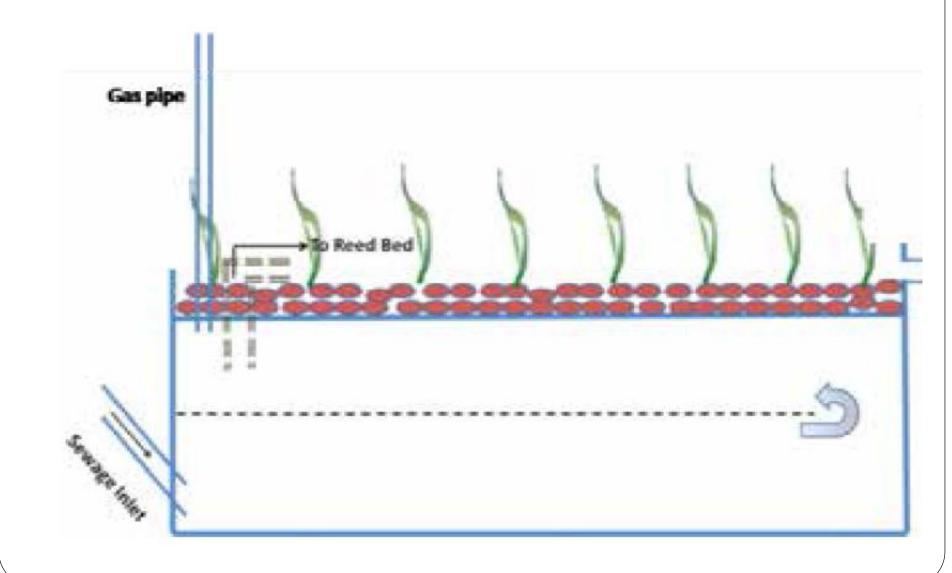
Septic Tank





SECTION XX

Wetland/Reed bed systems



Wasta stabilisation nond



Thank you