



Technical Seminar Wastewater Technology

Innovative solutions to achieve sustainable goals

Riyadh, 19 June 2023

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Witteveen+Bos Consulting Engineers

Company Introduction

Top expertise with a worldwide experience and a strong regional footprint



STP Manfouha IV, Saudi Arabia



Ajman Sewage Treatment Plant, UAE



Sharq Crossing, Qatar



Duqm Liquid Bulk Berth Terminal, Oman



The need for access to good-quality water is recognized as one of the major contemporary challenges in the Middle East.

What we do:

- Sanitation and water supply
- Water and wastewater treatment
- Water re-use and recycling
- Renewable energy and energy efficiency
- Bio-energy and resource recovery



Reference Amsterdam WWTP

- 1,000,000 p.e.
- 180.000 m³ wastewater/day
- 8.400 m³/h max DWF, 33.000 m³/h max SWF
- 4 primary sedimentation tanks (8,400 m³/tank)
- 7 aeration tanks (17,000 m³/tank), 8 m water depth
- 14 final sedimentation tanks (9,200 m³/tank)
- 3 sludge digestion tanks (11,100 m³/tank)
- 4 CHP's each 1,110 kW_e





Water Refinery, Innovative Wastewater Treatment

June 2023

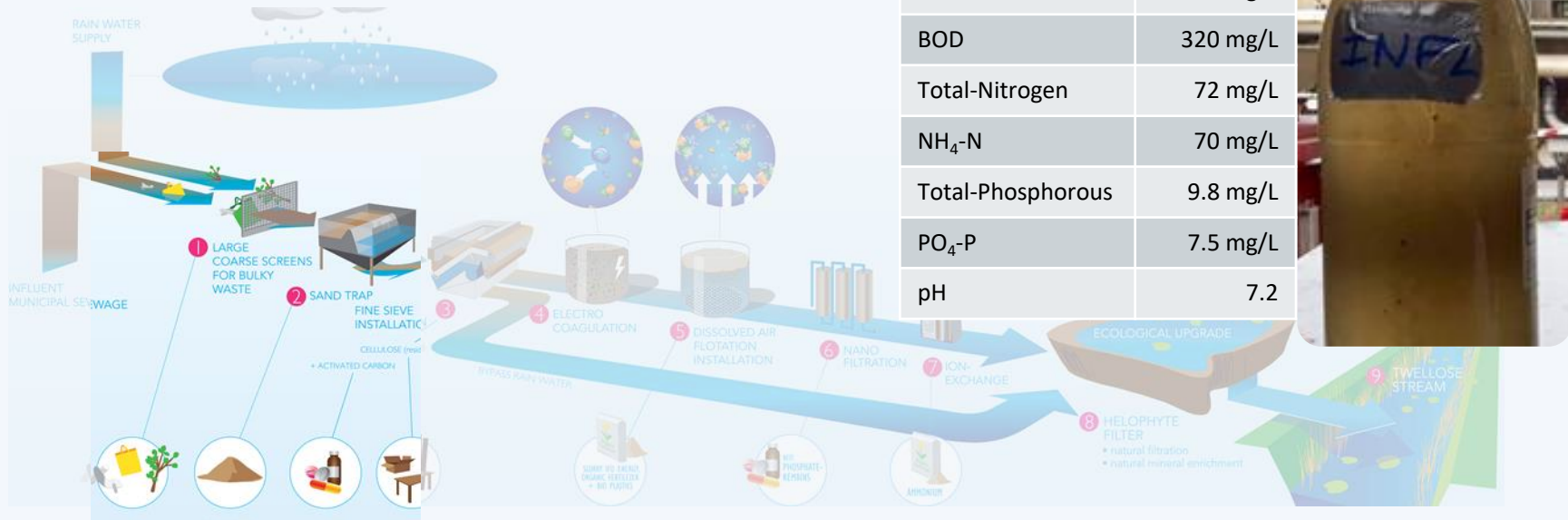
Carbon Zero Wastewater Treatment and Resources Recovery



- Complete **innovative physical-chemical treatment** concept for water reuse + resource recovery
- **No oxidation nor biological conversion** of potentially valuable materials
- **Zero carbon process emissions** (No Green House Gases: CO_2 , CH_4 , N_2O)
- **High Quality Water** production (applicable as process water / irrigation water / feed to NEWater)
- Removal of **Micropollutants / Pharmaceutical Residues and Microplastics**
- Extraction and Refinery of **Circular Resources and Materials** (cellulose, organics, phosphorous, ammonia)



1. Screening and Sand Recovery



parameter	Feedwater
TSS	350 mg/L
COD	820 mg/L
BOD	320 mg/L
Total-Nitrogen	72 mg/L
NH ₄ -N	70 mg/L
Total-Phosphorous	9.8 mg/L
PO ₄ -P	7.5 mg/L
pH	7.2

Aims: - protection of installations
- grid and sand removal

Products: - screening material
- sand

2. Fine Sieving (350 μm)



Aims:

- protection of installations

Product:

- production of cellulose (for upcycling into bio-composite, green activated carbon, bio char)

3. (Electro) Coagulation – Flocculation - Dissolved Air Flotation

400 Ampere / 6 V

0,5 ppm PE

20 m³/m²h



Aims:

- coagulation + flocculation and floc separation as pre-treatment for nanofiltration
- precipitation of phosphorous, metals and complex organics

Products:

- organic concentrate for biogas or fatty acids, bio-flocculants, bioplastics + phosphate precipitate

4. Direct hollow fiber Nanofiltration (400 Dalton)



Aims:

- removal of TSS, COD, flocs, colloids, $\text{NO}_3\text{-N}$, N_{org} , P_{org} , P_{total}
 - removal of di-valent ions (and larger)
 - removal of micropollutants and microplastics to up to 95% removal
- Product:**
- high quality water with ammonia and mono valent salts



5. Ion Exchange (2x)



Parameter	Product water
TSS	< 0.1 mg/L
COD	~ 30 mg/L
BOD	~ 5 mg/L
Total-Nitrogen	< 1.0 mg/L
NH ₄ -N	< 0.8 mg/L
Total-Phosphorous	< 0,05 mg/L
PO ₄ -P	< 0,03 mg/L
pH	~ 3.5

Aims:

- removal of mono valent hardness
- removal of ammonium to < 1 mg/L

Product:

- produce a concentrated ammonium stream (5 g/L NH₄SO₄)
- high quality water for irrigation, green houses, industry and process water



6. Optional: Ecology wetland filter (Biocascade® water purification)

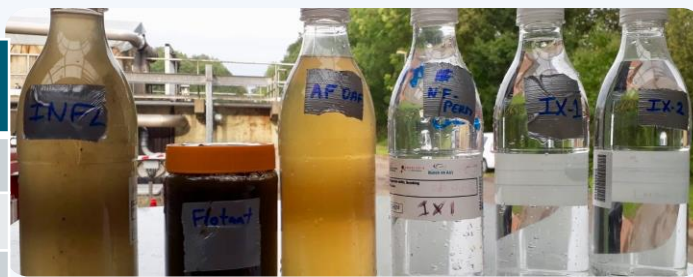


Aims:

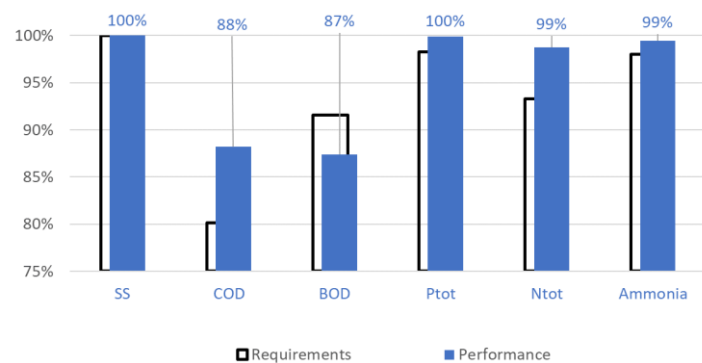
Product:

- remineralisation and revival of produced water + storm water treatment
- ecological water and groundwater recharge feed
- biomass for bio-composite, renewable bio-energy

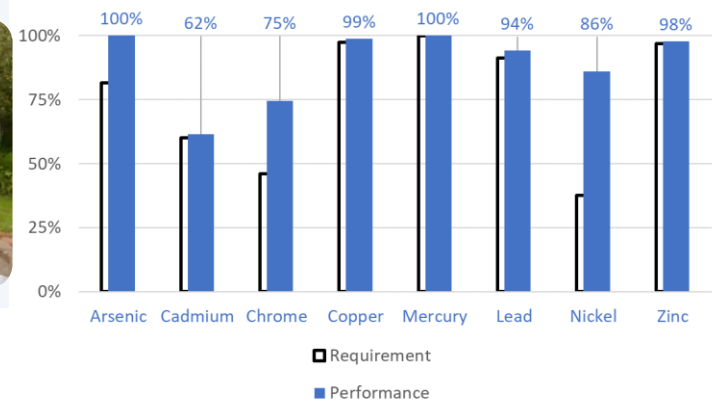
Parameter	Product water
TSS	< 0.05 mg/L
COD	~ 30 mg/L
BOD	~ 5 mg/L
Total-Nitrogen	< 1.0 mg/L
NH ₄ -N	< 0.8 mg/L
Total-Phosphorous	< 0,05 mg/L
PO ₄ -P	< 0,03 mg/L
pH	~ 6-7



Macro parameters



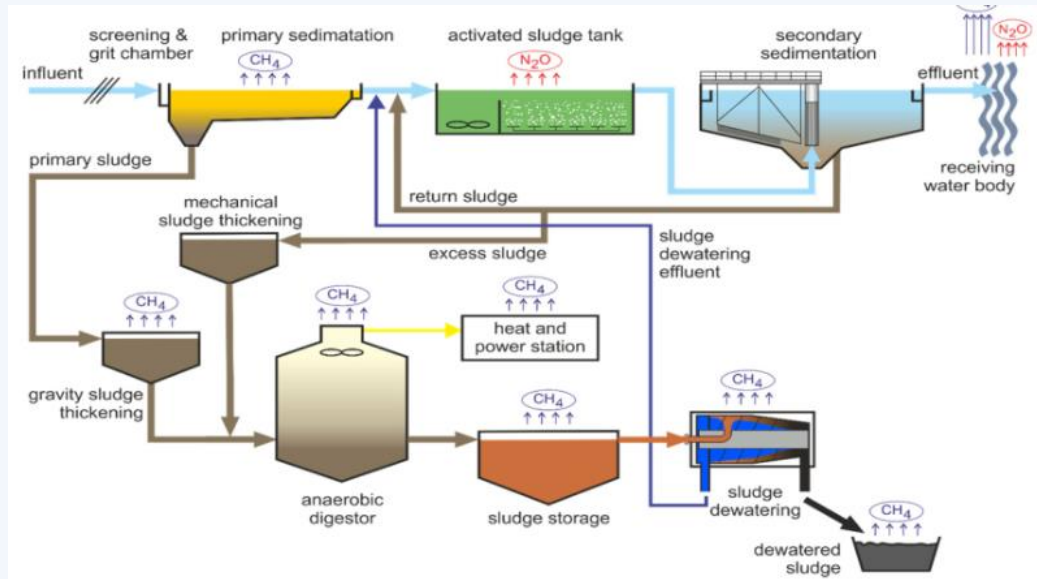
Heavy metals



Micro pollutants
removal efficiency



- **Process-related CO₂ emissions** (Green House Gases: CO₂, CH₄, N₂O)
- **Electricity** related CO₂ emissions
- CO₂ emission due to consumption of **chemicals** and production of **residuals**



CO₂ emissions

Conventional Activated Sludge: = 100%

Water Refinery + Sludge Digestion & Incineration: 50% CO₂-emission reduction

Water Refinery + Resources Valorisation: 100% CO₂-emission reduction

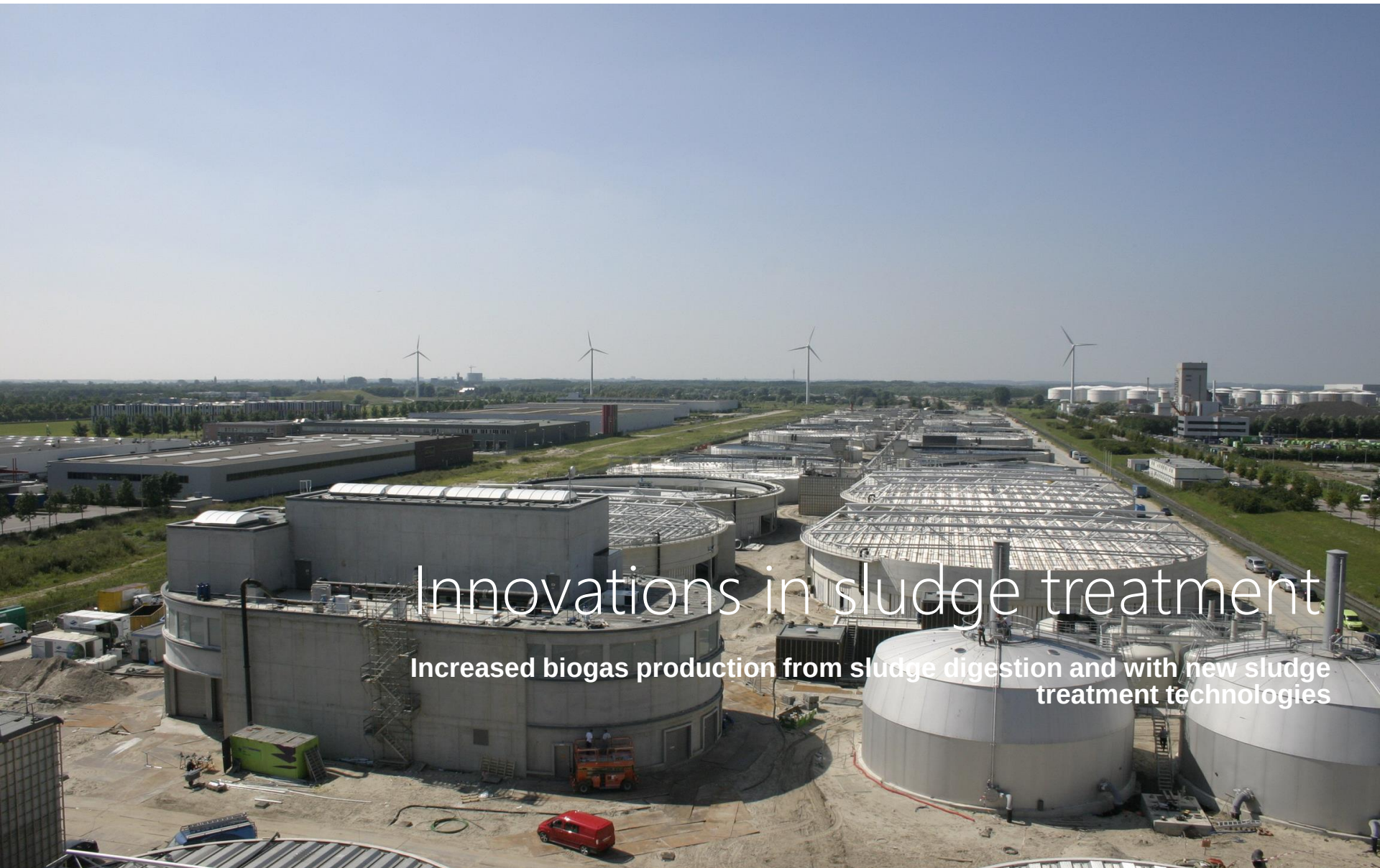


Think Future Proof
Act Circular and Carbon Zero

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Innovations in sludge treatment

Increased biogas production from sludge digestion and with new sludge treatment technologies



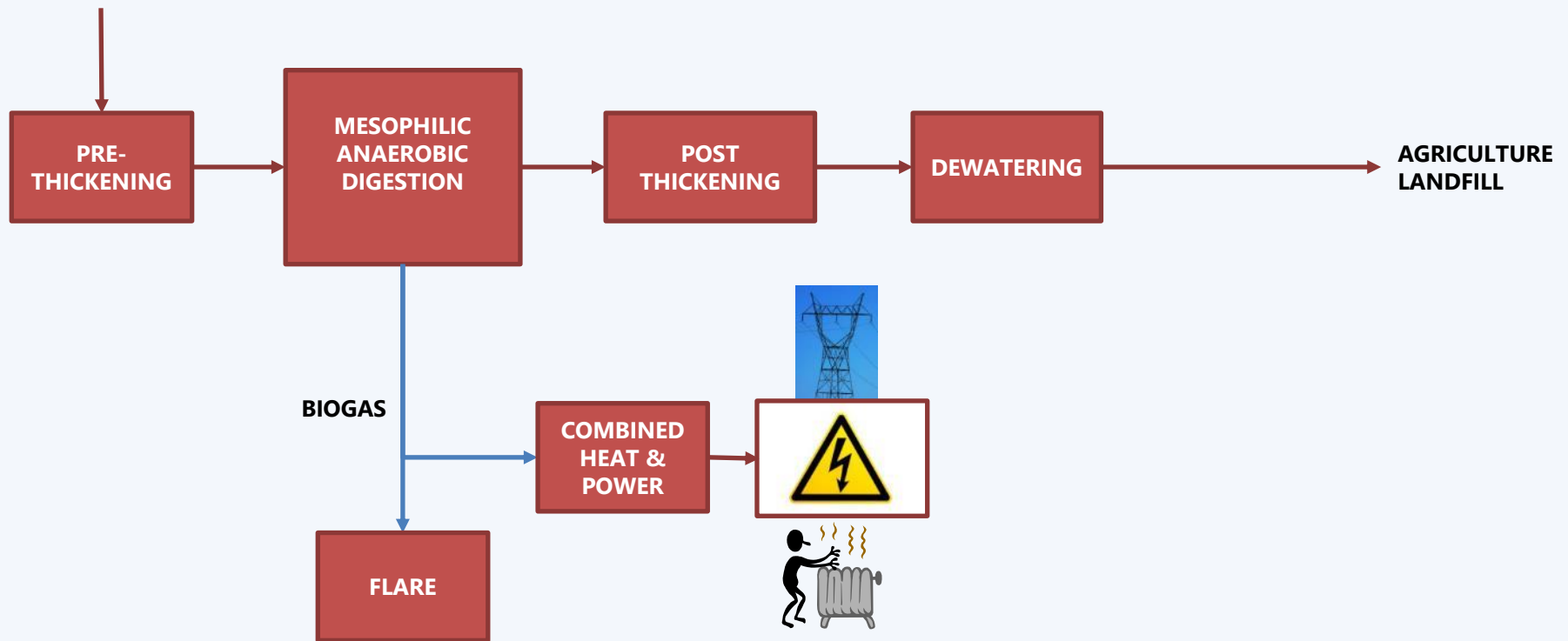
Overview sludge treatment in the Netherlands :

- >75% of total sludge production from municipal WWTPs is digested anaerobically
- Mainly Mesophilic (35°C) digestion, 1 Thermophilic (55°C) digester operational
- Total sludge production increasing
- No new sludge digestion plants build over the last 10 years
- More sludge is digested and biogas production increased through higher dry solids content and thermal pre-treatment of sludge

Grounds to choose anaerobic sludge digestion:

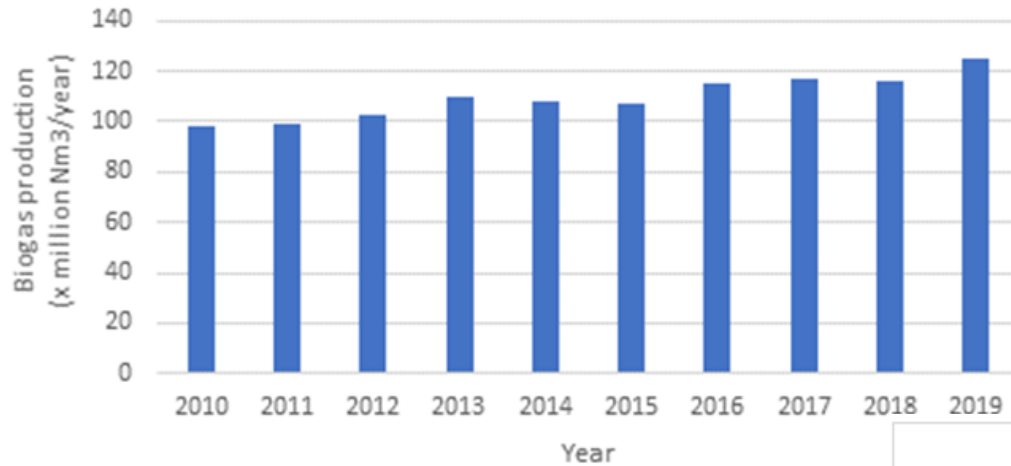
- (further) Stabilization
- Volume reduction
- Improvement of dewaterability
- Energy production

Primary & Secondary
Sludge WWTP

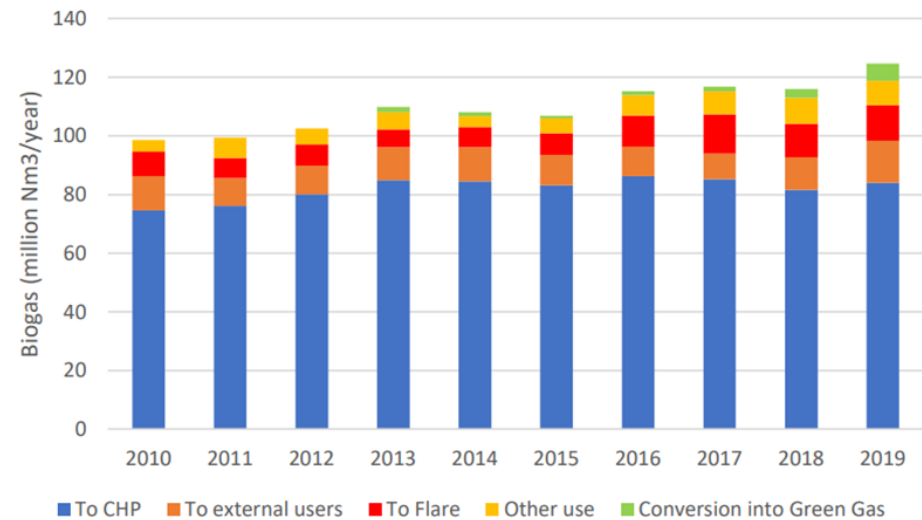


- Pre-thickening by gravity till 3-4% DS
- Mechanical pre-thickening till 5-6% DS
- Biogas production mesophilic digesters able to supply 60-65 % power consumption of WWTP
- SRT Mesophilic digestion (35 oC) > 20 days, Thermophilic digestion (55 oC) ~ 12 days

Biogas production sludge digestion in Netherlands



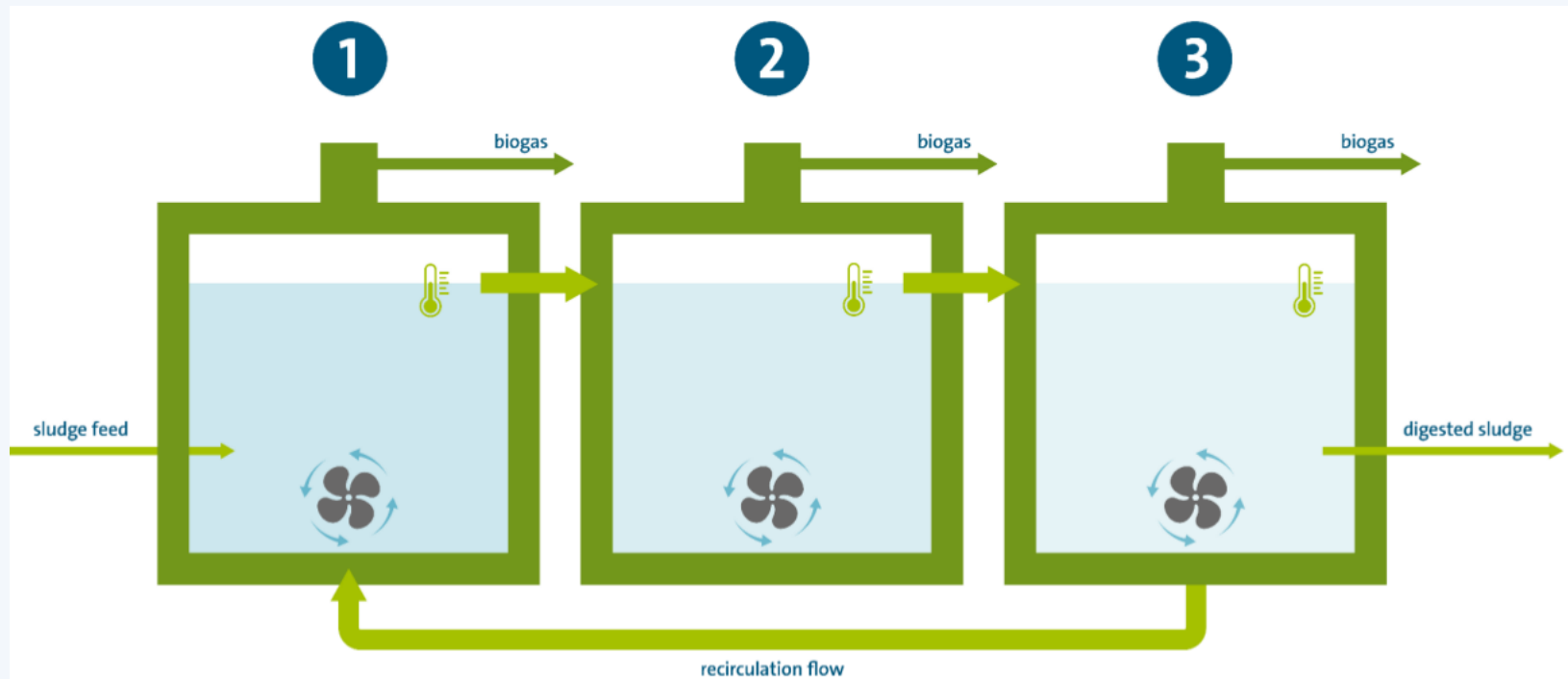
Annual Biogas usage from WWTP's in NL





- Thermophilic sludge digestion
- Sludge digestion at higher dry solids content
- Multiple (2-4) digesters in series with recirculation
- Thermal Pressure Hydrolysis as pre-treatment for sludge digestion
- Hydrothermolysis after sludge digestion or direct on secondary sludge

Multiple digesters in series with recirculation



- Plug flow regime (2-4 reactors)
- No short-circuiting
- Higher biogas production compared to single reactor with same SRT
- Reduced GHG emissions due to optimized digestion
- Design operating window SRT 8 – 15 days

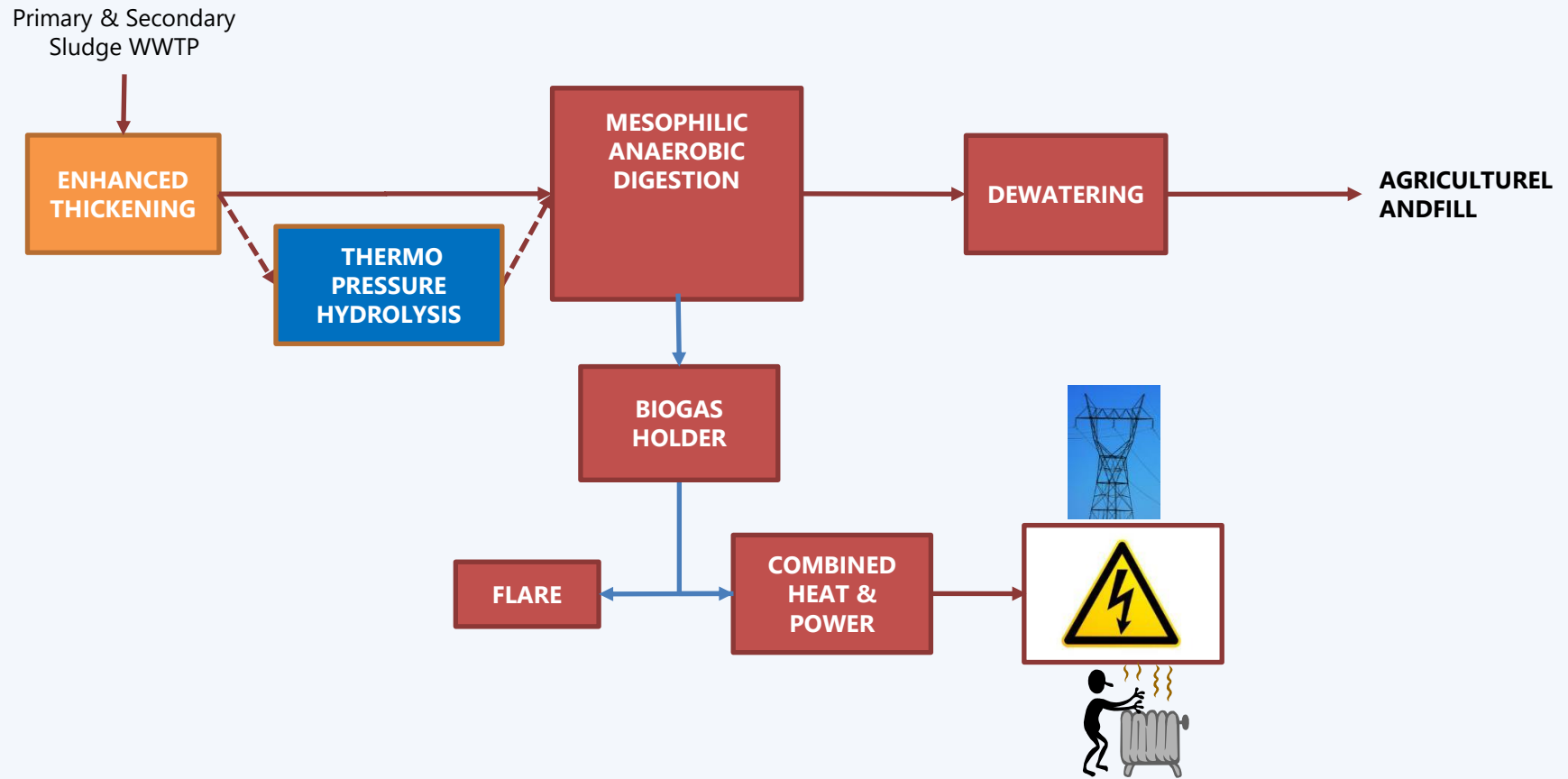
TPH hydrolyses organic material at high temperature (130 – 150 °C) and pressure (5 bar) by steam injection during approx. 1 hour

After hydrolysis the material can be digested easily

Benefits

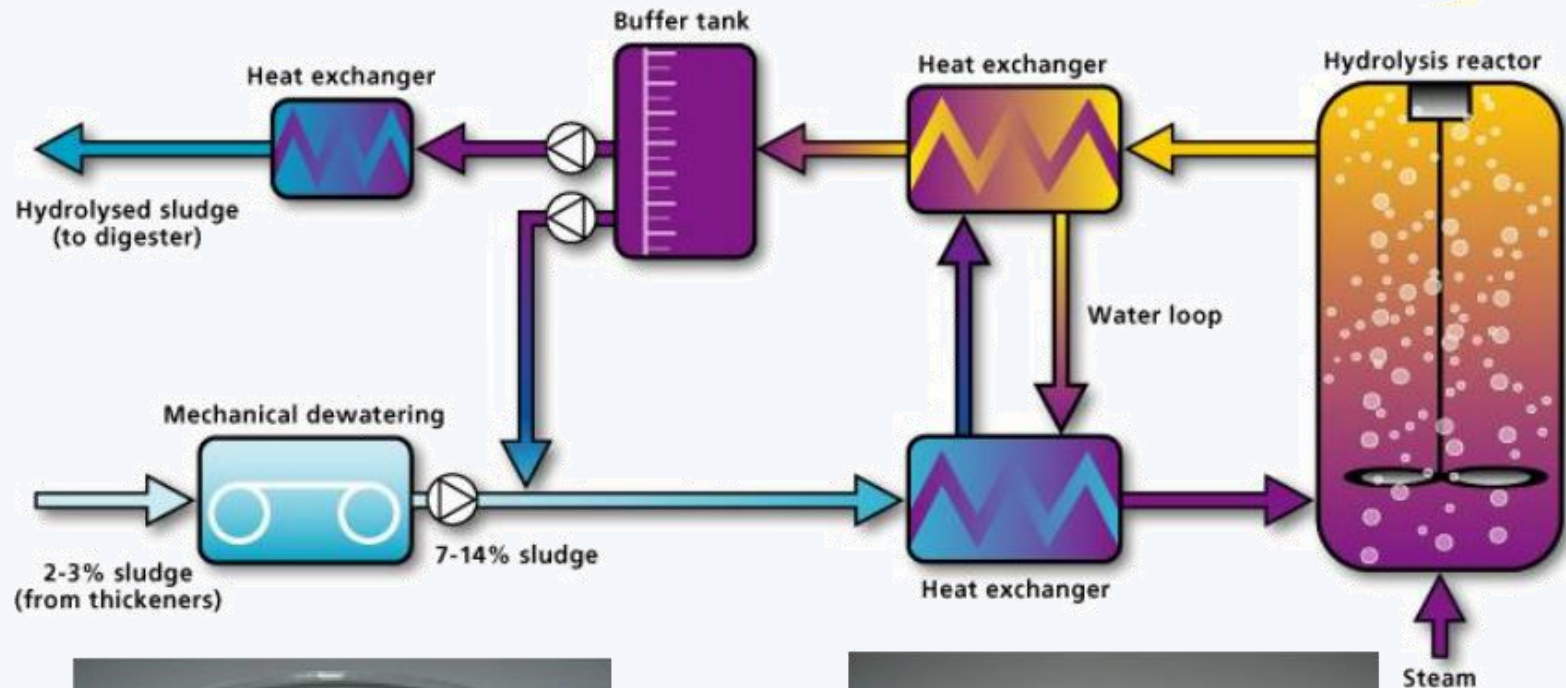
- higher fermentation efficiency (20 – 45% more)
- higher biogas yields (15 - 40% more)
- reduced retention time (so smaller digesters)
- lowering viscosity of sludge (easily pumping and mixing)
- improved dewaterability (sewage sludge > 30% DS)
- TPH delivers similar result as thermophilic digestion at same digestion tank volume



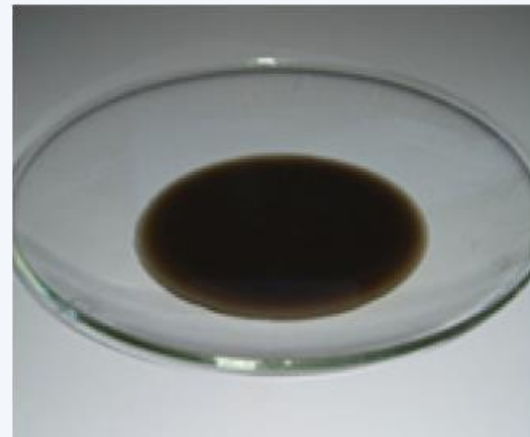


- Enhanced thickening till 7-14% DS. Smaller digestion tank volume and no post-thickening required
- Pre-treatment by thermal pressure hydrolysis to increase dry solid removal
- Biogas holder to maximize energy production, no flaring at peak production

Thermal Pressure Hydrolysis (TPH)



Thickened sludge before TPH



Thickened sludge after TPH



Amsterdam WWTP:

- Sludge production 32,000 tons DS/year
- 3 sludge digestion tanks each 11,000 m³
- 11.8 Mln m³/year biogas production
- 4 CHP's each 1,100 kWe
- Conversion biogas to Green gas

Apeldoorn WWTP:

- Sludge production 20,000 tons DS/year
- 8 Mln m³/year biogas production
- 4 CHP's each 750 kWe and 1x 880kWe

Sludge is a global problem and opportunity

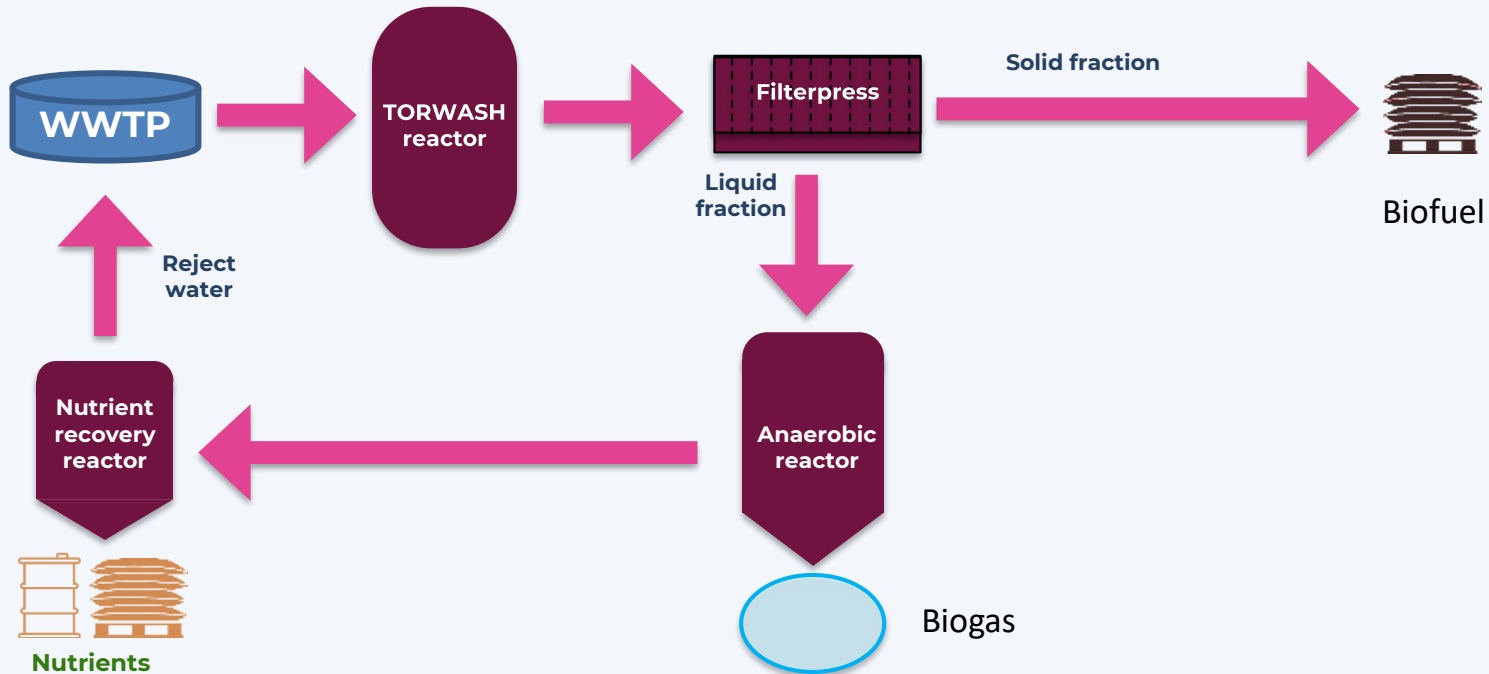


Sludge = (a lot of) waste ...

- Wet and contaminated: landfill or incineration
- Worldwide insufficient treatment capacity
- No circular products
- Use of fossil chemicals and extensive road transport

Increasing demand for circular products

- Green gas
- Feedstock for biochemistry and biofuel
- Fertilizers
- Clean water



- Conditions TORWASH: 150-250 oC, max pressure 25 bar, retention time 20-30 minutes
- Dewatering in filterpress without dosing polymer, dry solid content 50-60% in sludge cake
- Organic matter is converted into fatty acids, effluent is treated anaerobically at 35 oC to produce biogas
- Nitrogen and phosphorus are recovered as fertilizers



50% lower costs
for sludge
treatment



energy
neutral
process



60% phosphate
recovery



solid biofuel
approved for
power plants



no chemicals (PE)
consumption



90% less transport



50% lower
CO₂- emission

Applications:

- After sludge digestion of primary and secondary sludge
- After digestion of secondary sludge
- Direct on secondary sludge

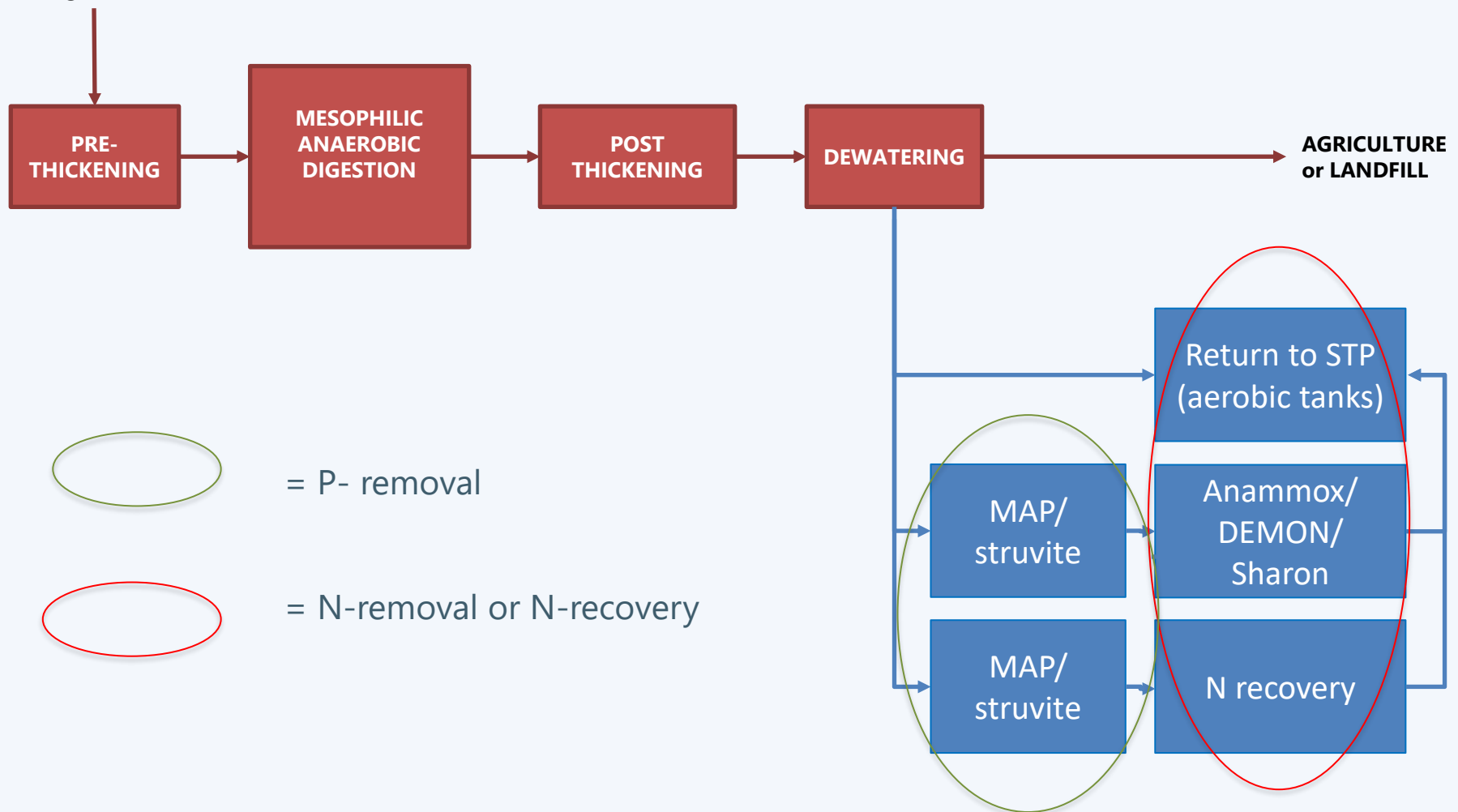




Resource Recovery from Sludge Dewatering

Treatment of liquid phase of digested sludge: phosphorous (P) and nitrogen (N)

Primary & Secondary
Sludge WWTP



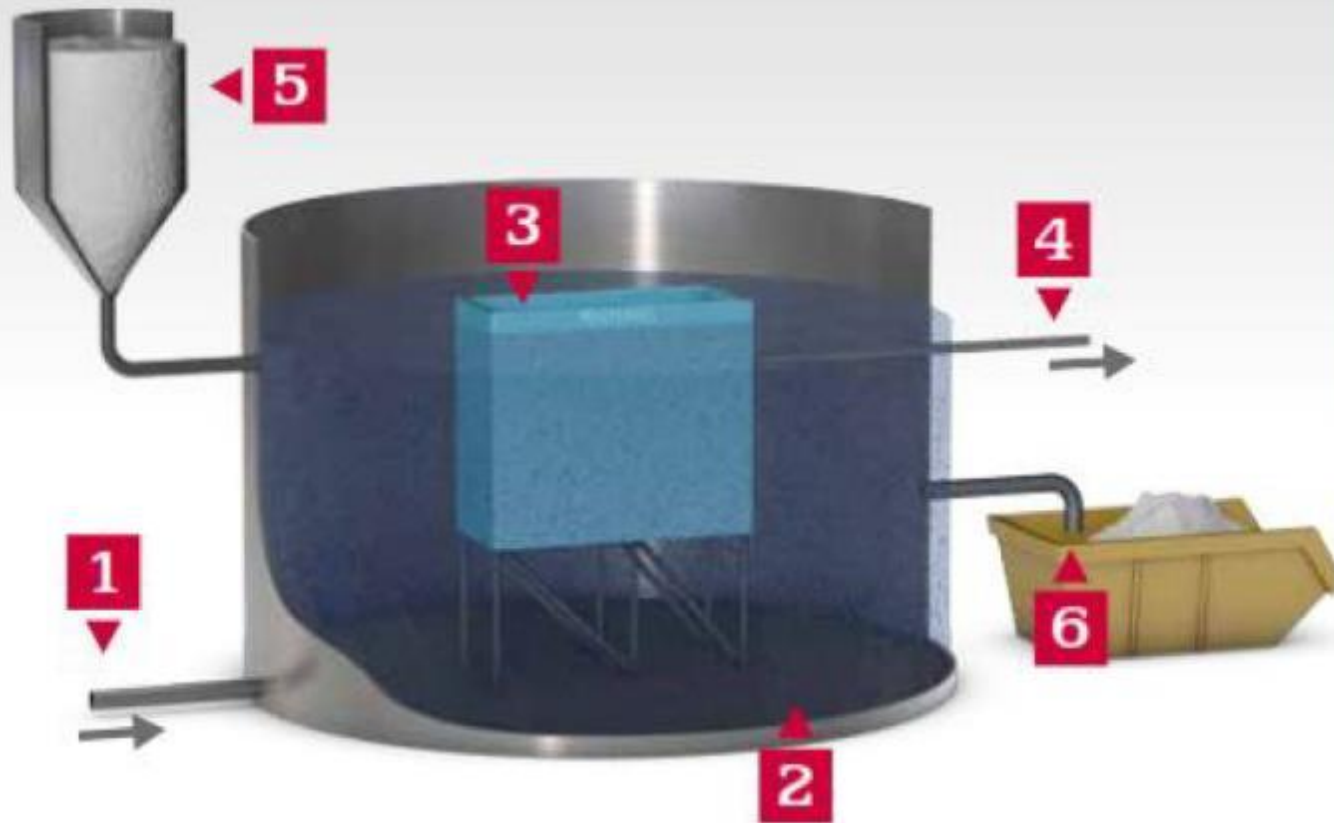
Dosing of MgO , $\text{Mg}(\text{OH})_2$ or MgCl_2

- Source of Mg
- Increase pH to 8.3

Struvite precipitate (MgNH_4PO_4)

- Struvite is anorganic and doesn't contain organic material
- Dewatering by screw press till > 90 %DS
- It has no smell and can be stored for long time

P-recovery via MAP/struvite technology



PHOSPAQ™ process

- 1 Phosphate rich Influent
- 2 Aerators grid for mixing
- 3 PHOSPAQ™ separator for struvite retention
- 4 Effluent from reactor
- 5 MgO dosing
- 6 Struvite harvesting

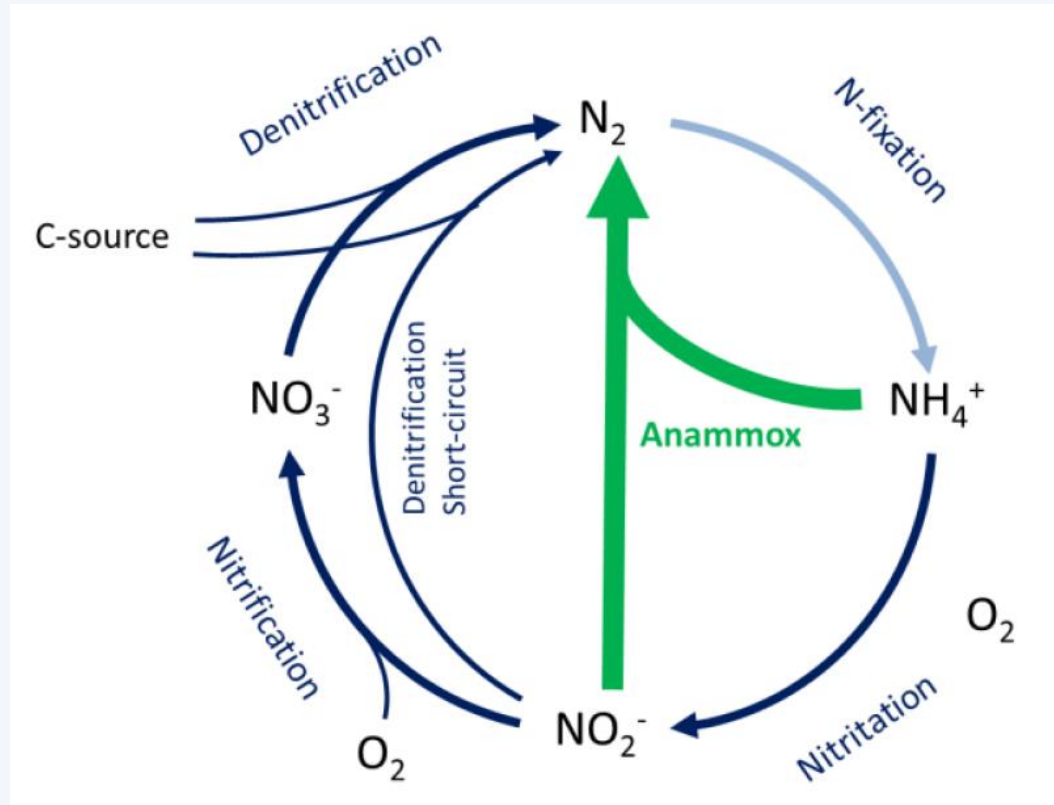


Struvite reactor (average for 2016-2020):

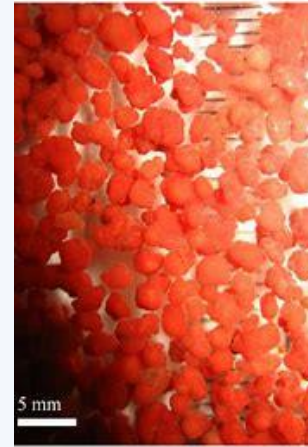
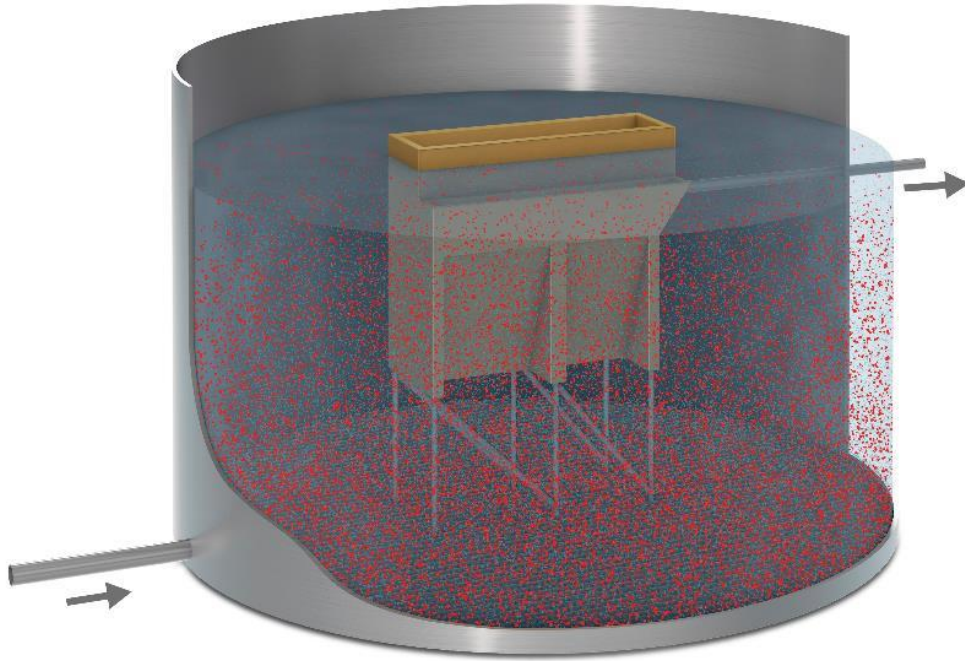
- Inlet: 400 mg P/L
- Outlet: 94 mg P/L
- Removal efficiency: 76%

Anammox/DEMON N-removal process

Anaerobic Ammonium Oxidation



Anammox/DEMOn technology



Anammox bacteria

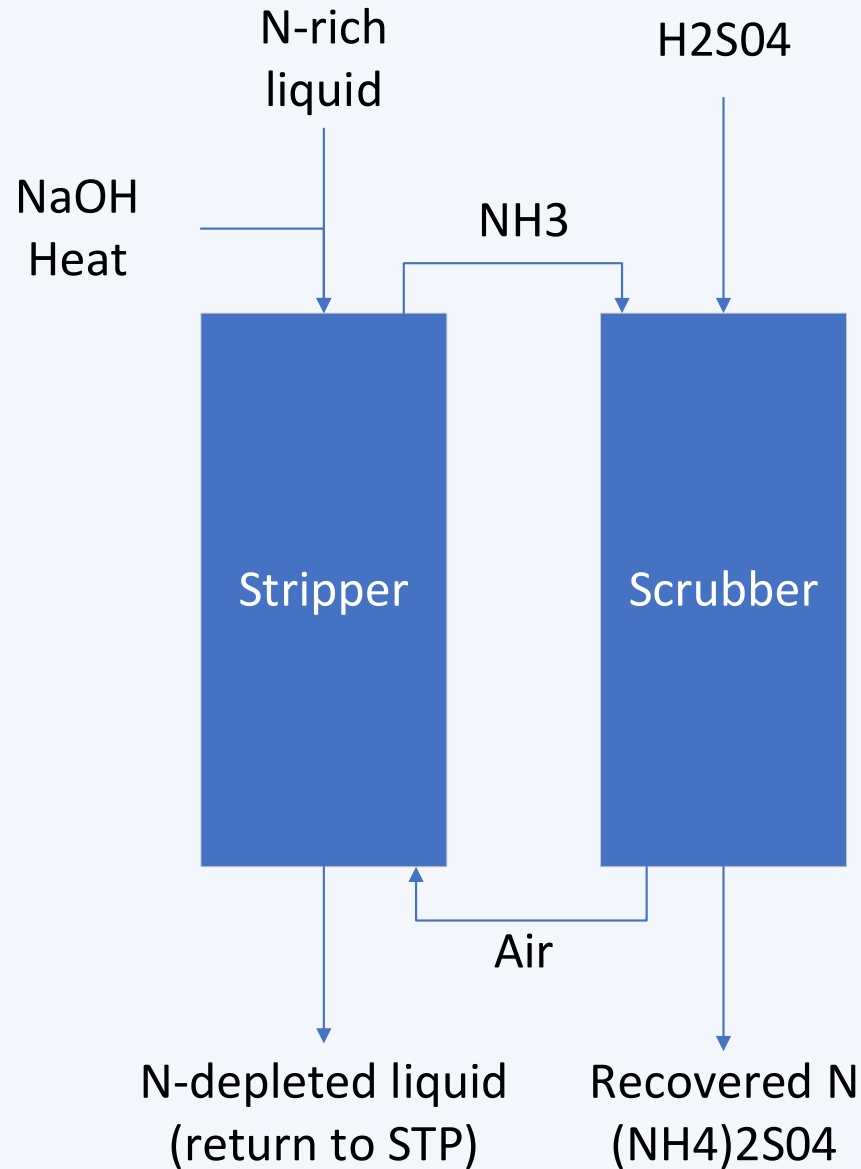


	Unit	Conventional treatment	Anammox
Power	kWh/kg N	2.8	1
Methanol	kg/kg N	3	0
Sludge production	kg VSS/kg N	0.5 – 1.0	0.1
CO ₂ emission	kg/kg N	> 4.7	0.7

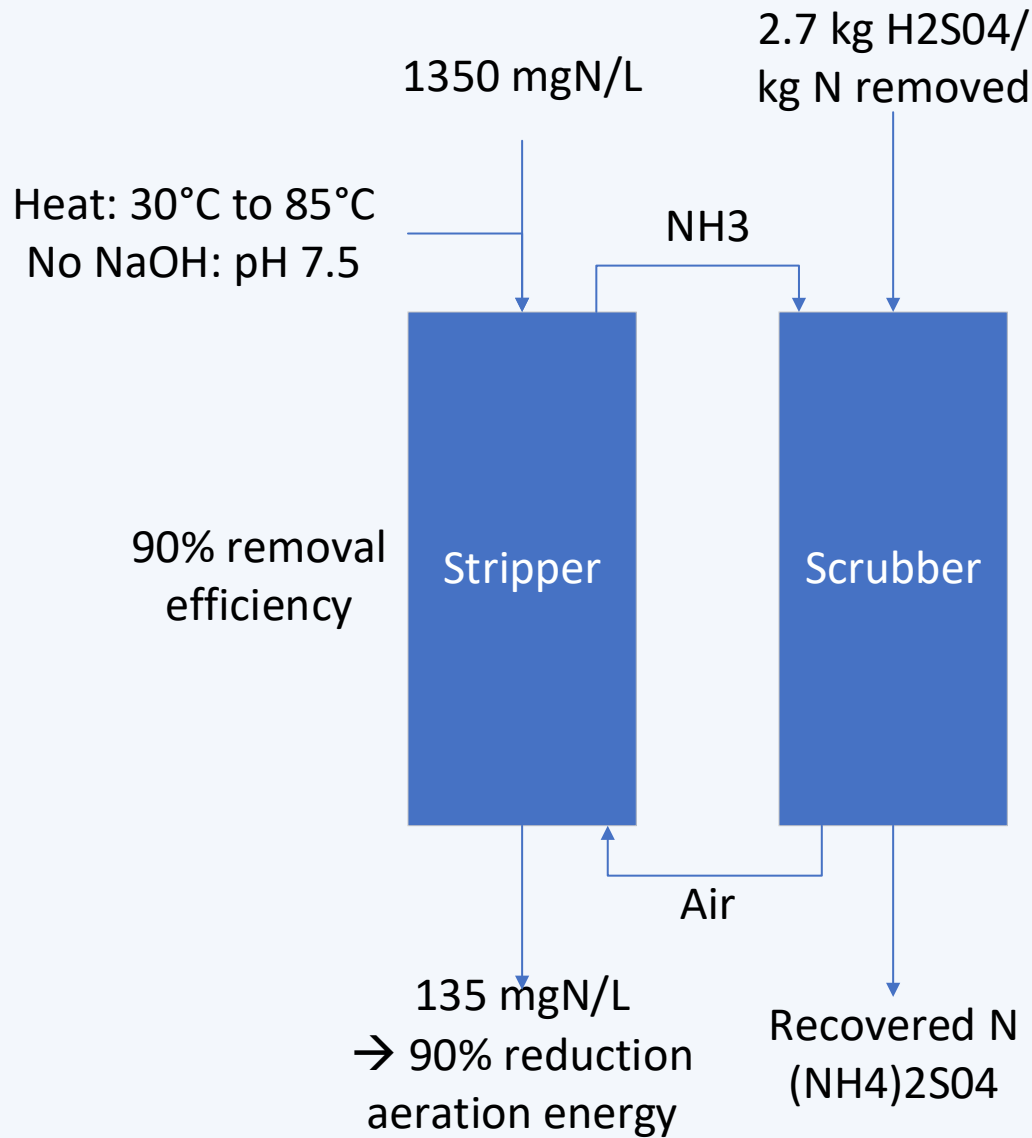
- 60% less power required (aeration)
- No carbon source required
- 5-10x lower sludge production

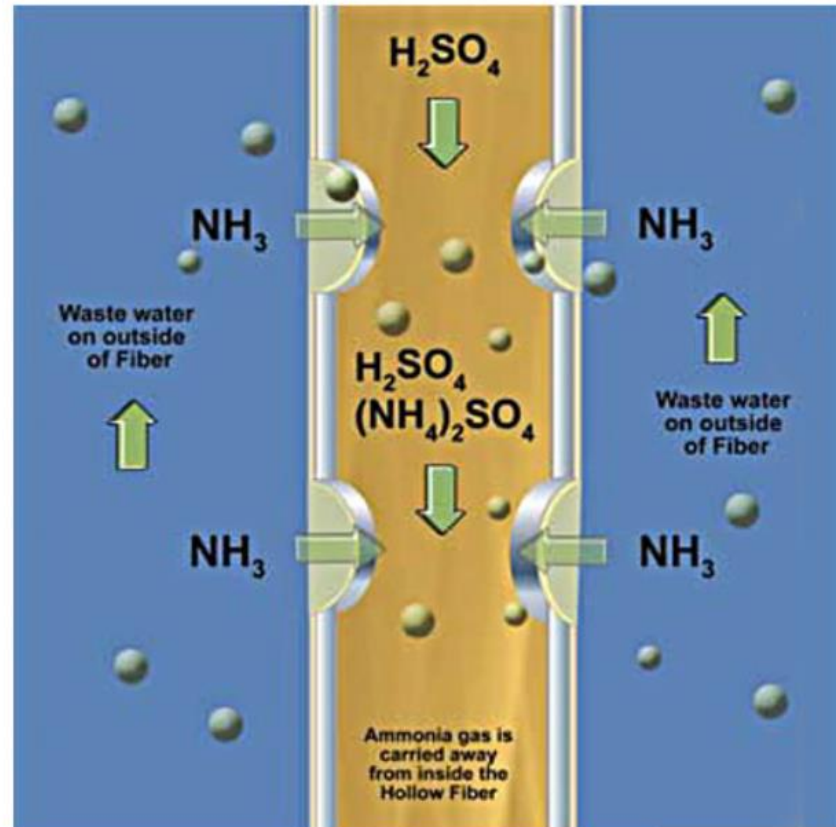
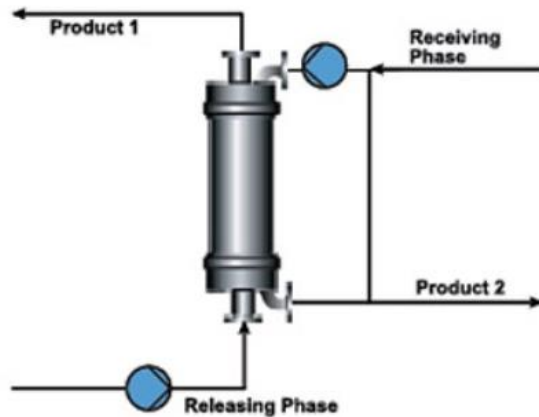
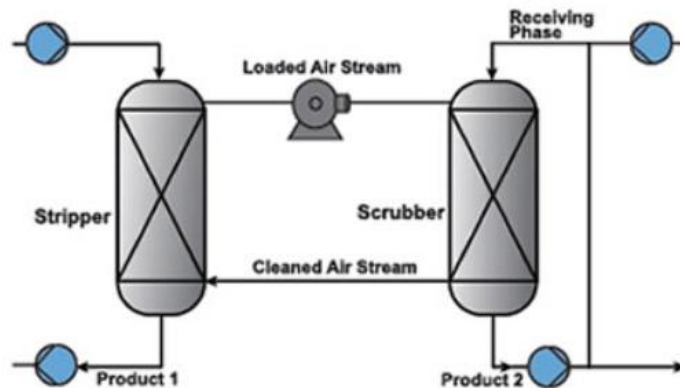
But: N₂O emission. N₂O is a Greenhouse Gas (265 times CO₂)

N-recovery technology – air stripping



STP Echten, the Netherlands



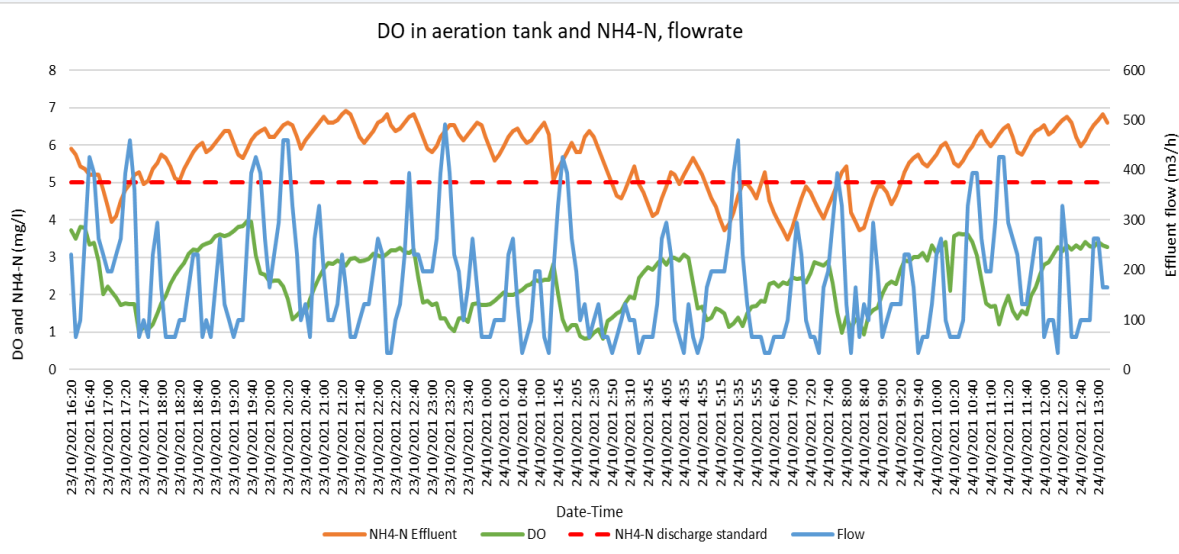




Advanced Process Control for optimal operation of Wastewater Treatment Plants

Current practice:

- Many WWTP's have limited and not optimal monitoring control system, sometime only O₂
- Aeration consumes 50-65% of total energy at a WWTP



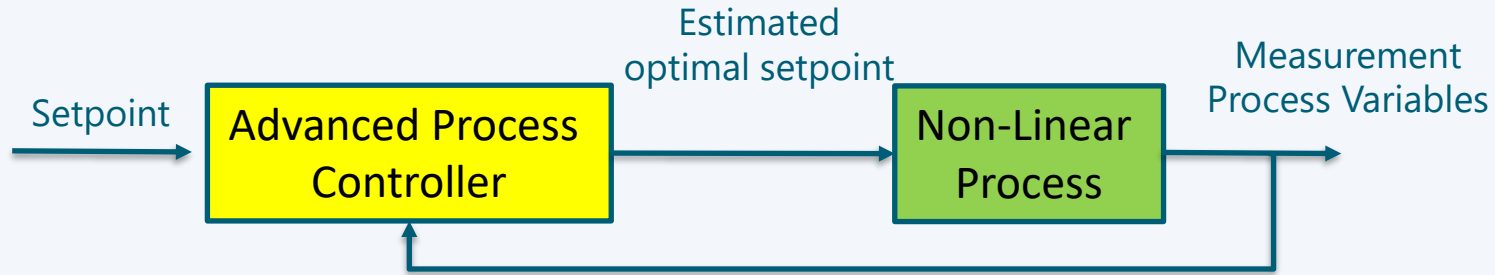
Disadvantages:

- Long delay time leads to overshoot or undershoot
- Missing interaction control among parameters

Problems:

- Large effluent quality fluctuation
- High energy and chemical consumption

WOMBAT – W+B Advanced Process Control



Predictive control enables efficient processes based on what will happen rather than what has happened

Features:

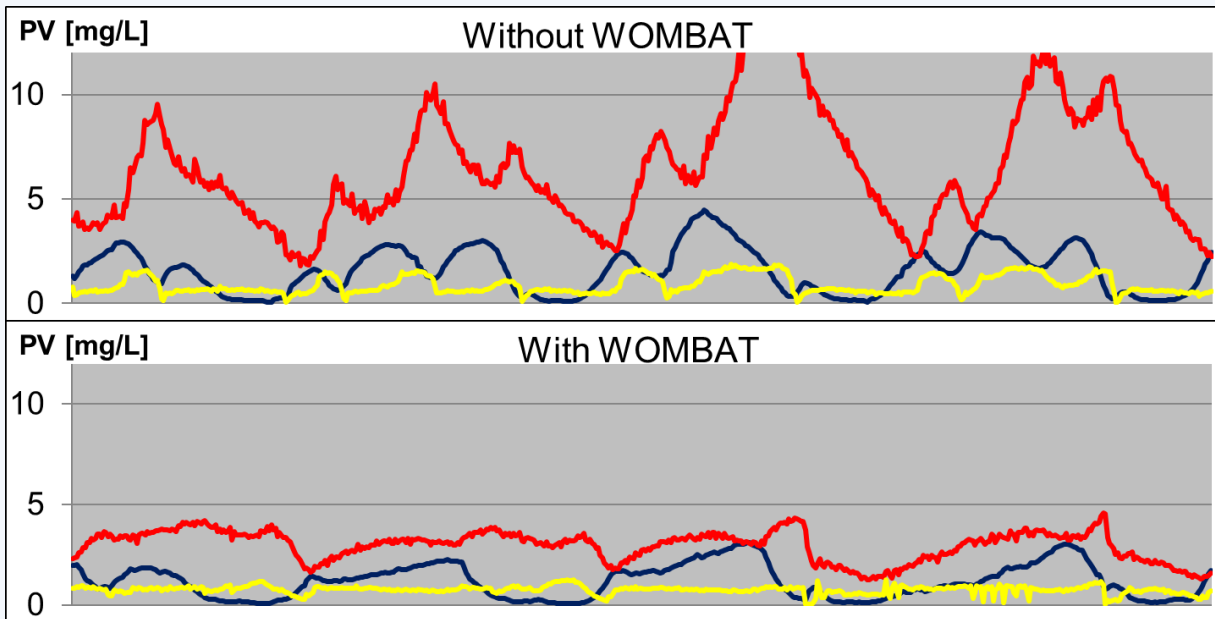
- Model predictive control
- Feed forward and Feedback control
- Self learning and adaptive control

Advantages:

- More stable effluent quality
- Higher energy efficiency
- Lower chemical consumption for denitrification

Benefits of WOMBAT in practise

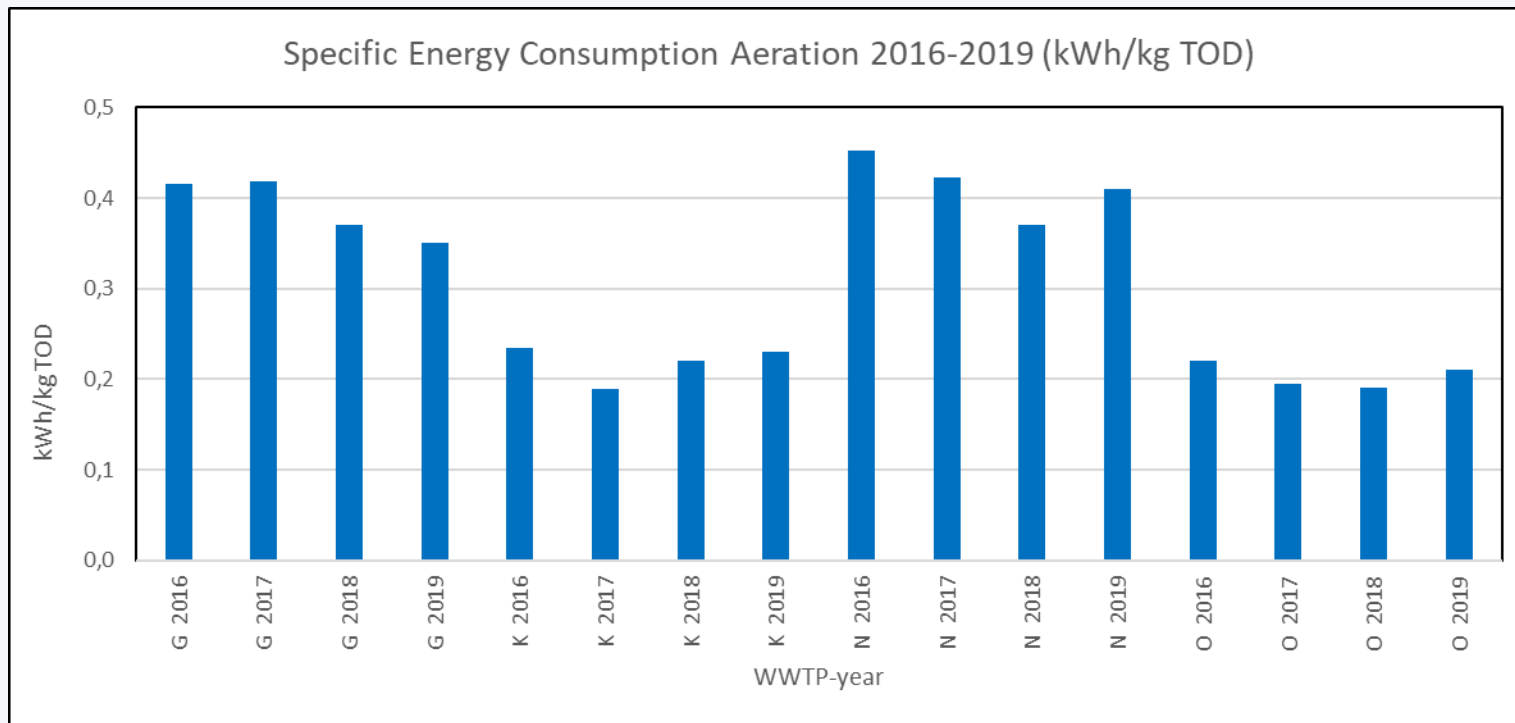
Nitrogen, Ammonium, Oxygen



Benefits

- Stable process and tighter process control also at fluctuating influent quality
- Lower $\text{NH}_4\text{-N}$, $\text{NO}_3\text{-N}$ concentrations in effluent
- 5 - 25% reduction of energy consumption in aeration
- 5 - 10% lower sludge waste
- 5 - 30% reduction of chemicals used

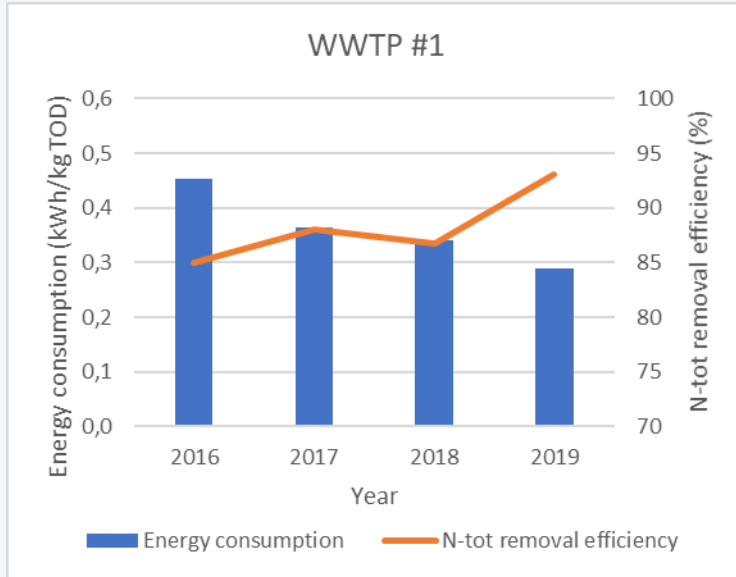
Benchmark energy consumption aeration WWTP's



- Energy consumption of 4 WWTP's (G, K, N, O) with different aeration systems (2016-2019)
- Improvement of monitoring, control and setpoints

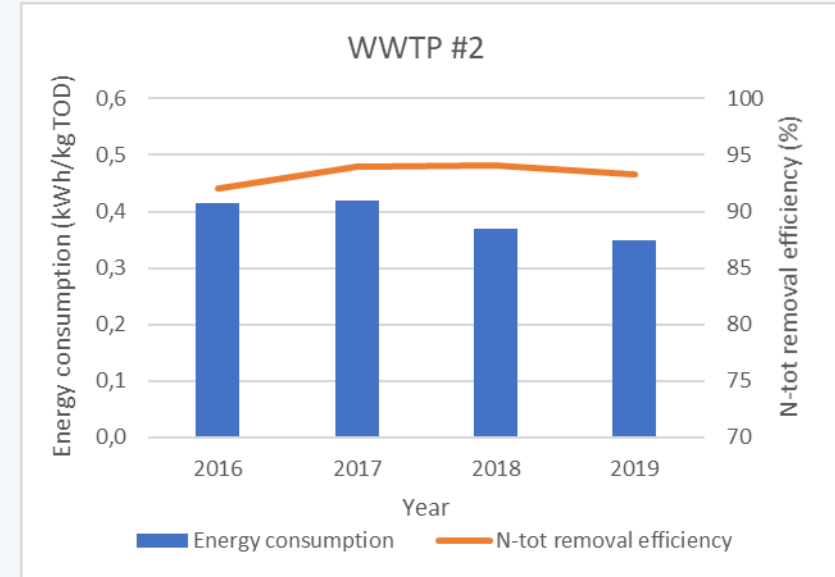
Note: $TOD = COD + 4,57 \cdot TKN$

Energy consumption and improved effluent quality



WWTP #1

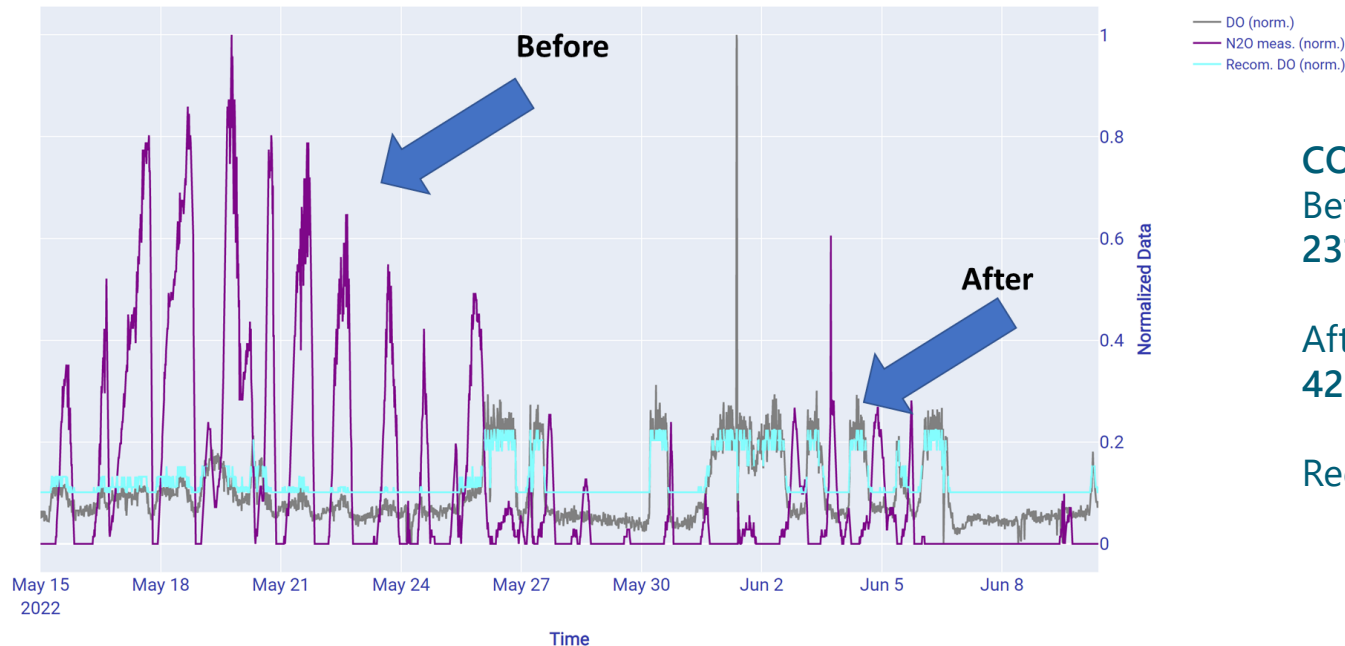
- Energy consumption decreased from 0.46 to 0.29 kWh/kg TOD, energy saving 37%
- N-tot removal efficiency increased from 85 to 93%



WWTP #2

- Energy consumption decreased from 0.41 to 0.35 kWh/kg TOD, energy saving 15%
- N-tot removal efficiency increased from 91 to 93%

- N₂O is emitted from aeration tanks during nitrification and denitrification
- N₂O is 265 time more harmful than CO₂
- Advanced process control reduces the N₂O emission. Implemented 25 May



CO₂ emission:
Before (May 5 – May 25)
231 tons CO₂e/year

After (May 25 – June 10)
42 tons CO₂e/year

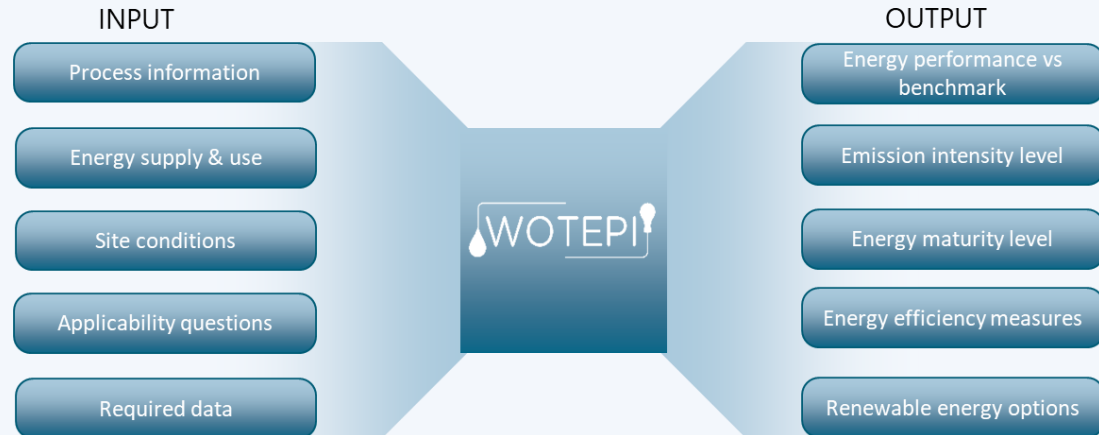
Reduction 82%

Water Operators Tool for Energy Performance and Improvement

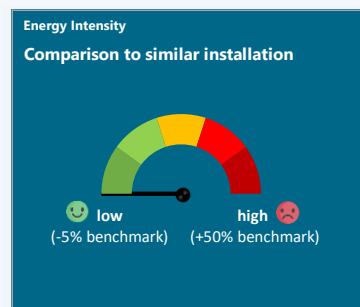
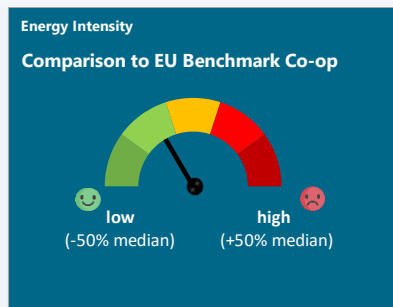
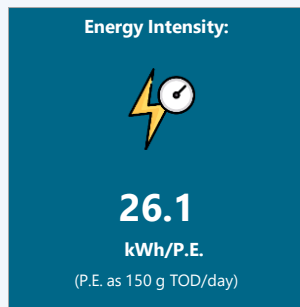
WOTEPI: Water Operators Tool for Energy Performance and Improvement

For the European Bank for Reconstruction and Development (EBRD), Witteveen+Bos developed a toolkit that enables **water-** and **wastewater** treatment operators to **save energy** and **become future and climate proof**.

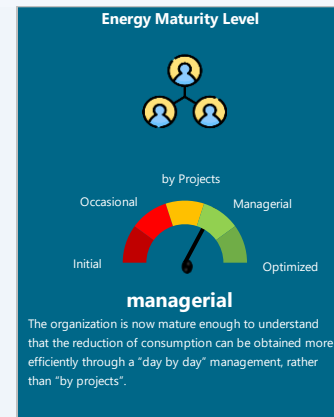
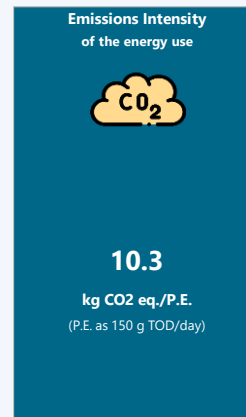
Promo film: <https://vimeo.com/702920875/19f35bbff3>



With WOTEPI, you get insight into your energy intensity comparison to benchmarks...



WOTEPI provides a list of potential energy efficiency measures





Re-use of treated wastewater for
production of boiler feed water

Quality WWTP Effluent

Parameter	Average	UoM
Turbidity	8	NTU
TSS	30	mg/l
EC	65	mS/cm
Chloride	90	mg/l
Sulphate	60	mg/l
TDS	500	mg/l
SiO ₂	17	mg/l
DOC	15	mg C/l
COD	60	mg/l
BOD	<10	mg/l
NH ₄ -N	< 10	mg/l
NO ₃ -N	< 10	mg/l



- 350 m³/h boiler feed water production from WWTP effluent. Start up in 2010.
- Requirements to recycled water:
 - Conductivity < 0,1 $\mu\text{S}/\text{cm}$
 - Ca, Mg, Si, Cu, Fe, Mn < detection limits
 - Low use of chemicals for biofouling and anti scalant

Treatment technologies:

- Ultrafiltration: submerged membranes (ZeeWeed 500)
- Biological Activated Carbon Filtration (BACF) with oxygen supply.
- Desalination by double pass Reverse Osmosis (RO)
- Electro-De-Ionisation (EDI)



Effects BACF with oxygen supply:

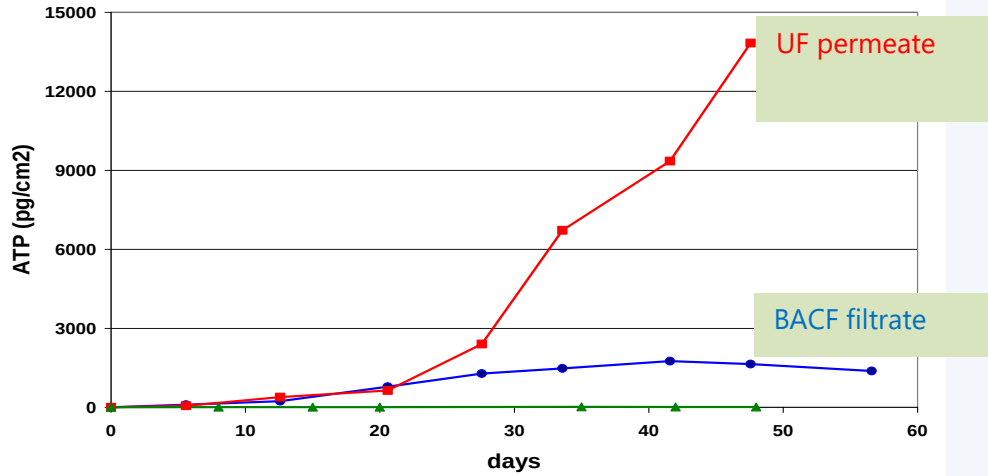
- Biofilm growth on activated carbon, decrease of BOD and oxidise NH_4 present in WWTP effluent and not removed by UF
- Low concentration of growth limiting substrates in the RO feed water and preventing biofouling on RO membranes
- pH decrease due to nitrification
- Lower dosing of anti scalant dose in feed RO

Backwash BACF	1 or 2 times a week
---------------	---------------------

Nitrification	100%
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Turbidity	< 0,1 FTU
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Effect of BACF on biofilm forming rate



Biofilm Forming Rate



Effect of BACF on cartridge filter

RO-1 performance

Recovery	75%
EC feed	400 - 1700 $\mu\text{S}/\text{cm}$
EC product	5 - 15 $\mu\text{S}/\text{cm}$
Anti scalant dosing	2 ppm
CIP frequency	2-3 times a year
CIP chemicals	NaOH / HCl
Lifetime RO membranes	currently 13 years, projection >15 years



1-STEP® filter
Ultimate One Step Total Effluent Polishing filter

June 2023

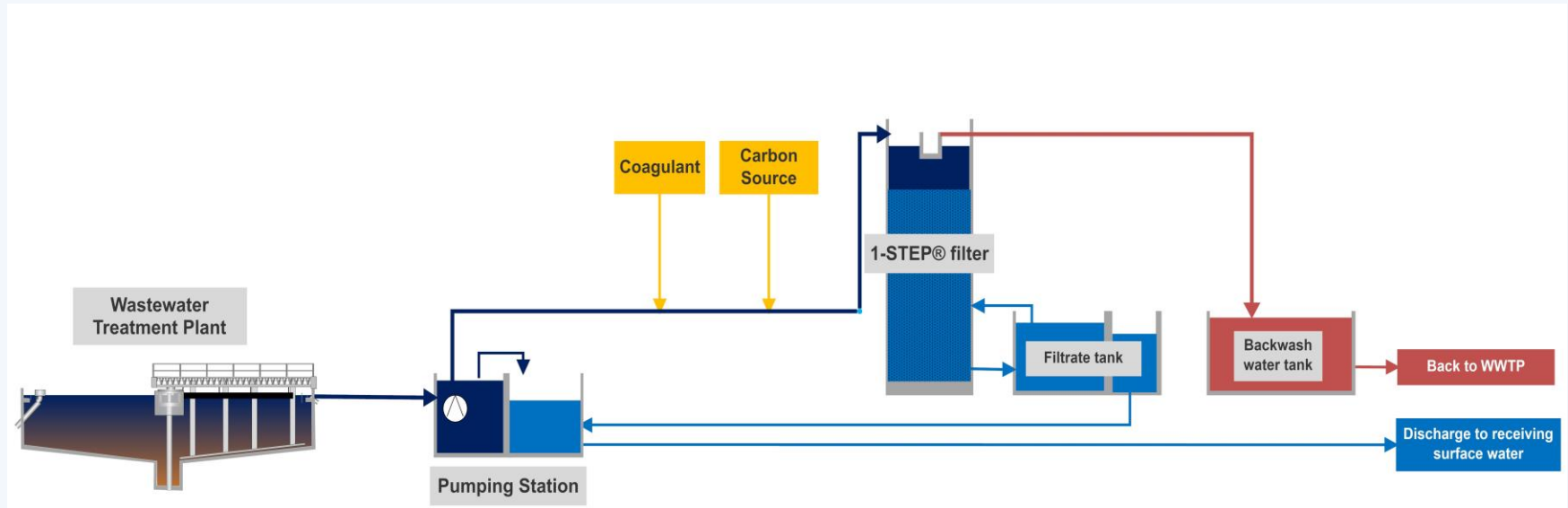
Drivers for innovation and implementation 1-STEP[®] filter

- A cleaner and protected environment; least-cost of compliance with stringent discharge limits (i.e. EU WFD) to protect water resources
 - Advanced nitrogen removal
 - Phosphorous removal to a standard < 0.25 mg P/l
 - Priority substances removal
 - Final effluent polishing
- Significant OPEX savings and limiting CAPEX in treated effluent recycling schemes

STP Horstermeer, the Netherlands (165,000 p.e.)

1-STEP® filter fully operational from 2013 onwards, capacity 1,500 m³/h

Flow diagram 1-STEP[®] filter



Our 1-STEP[®] filter solution

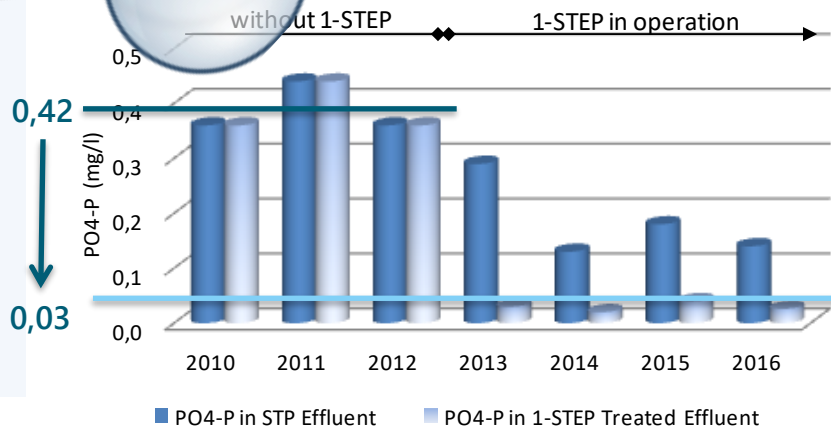
- 1 Step Total Effluent Polishing filter



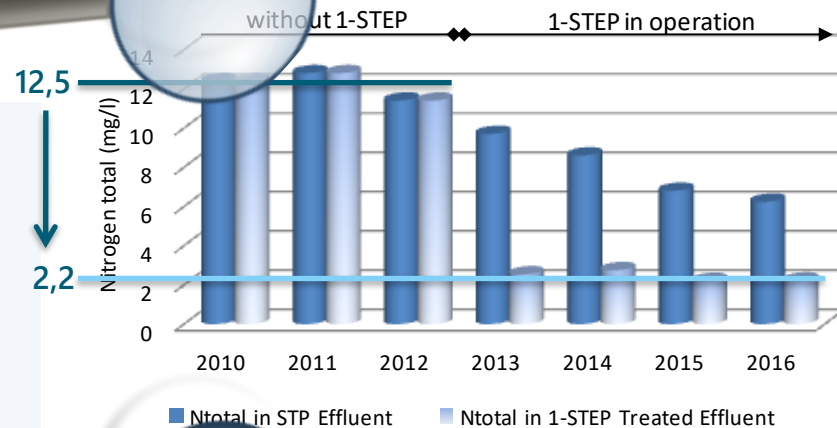
Performance: nutrients

- High removal efficiency
- Stable effluent quality

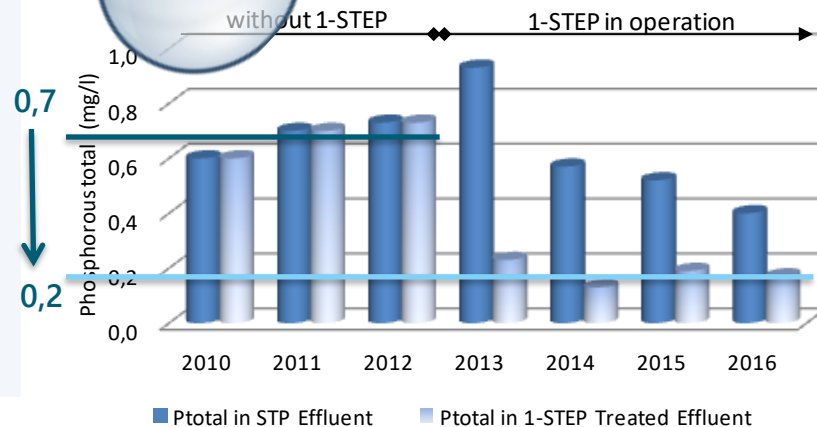
PO4-P Removal 1-STEP® filter Horstermeer



Nitrogen Removal 1-STEP® Filter Horstermeer



Ptotal Removal 1-STEP® filter Horstermeer



Innovations resulting in excellent operational performance

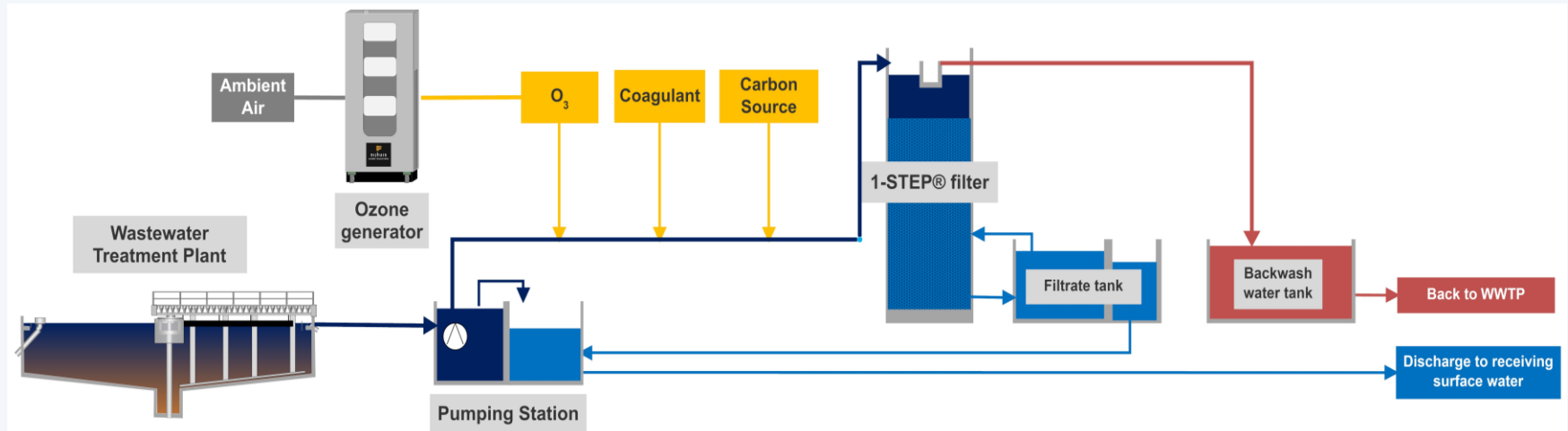
- Intelligent dosage and control of chemicals
 - Efficient PAC consumption for P-removal
 - Efficient MeOH dosage (N removal up to 4 kg N/m³ filter bed volume)
- Intelligent filtration and backwash control
 - Selected type of activated carbon
 - High filtration rates: up to 15 m³/m²h
 - Backwashing down time: ~5%
- Low energy usage (0.04 kWh/m³ treated)

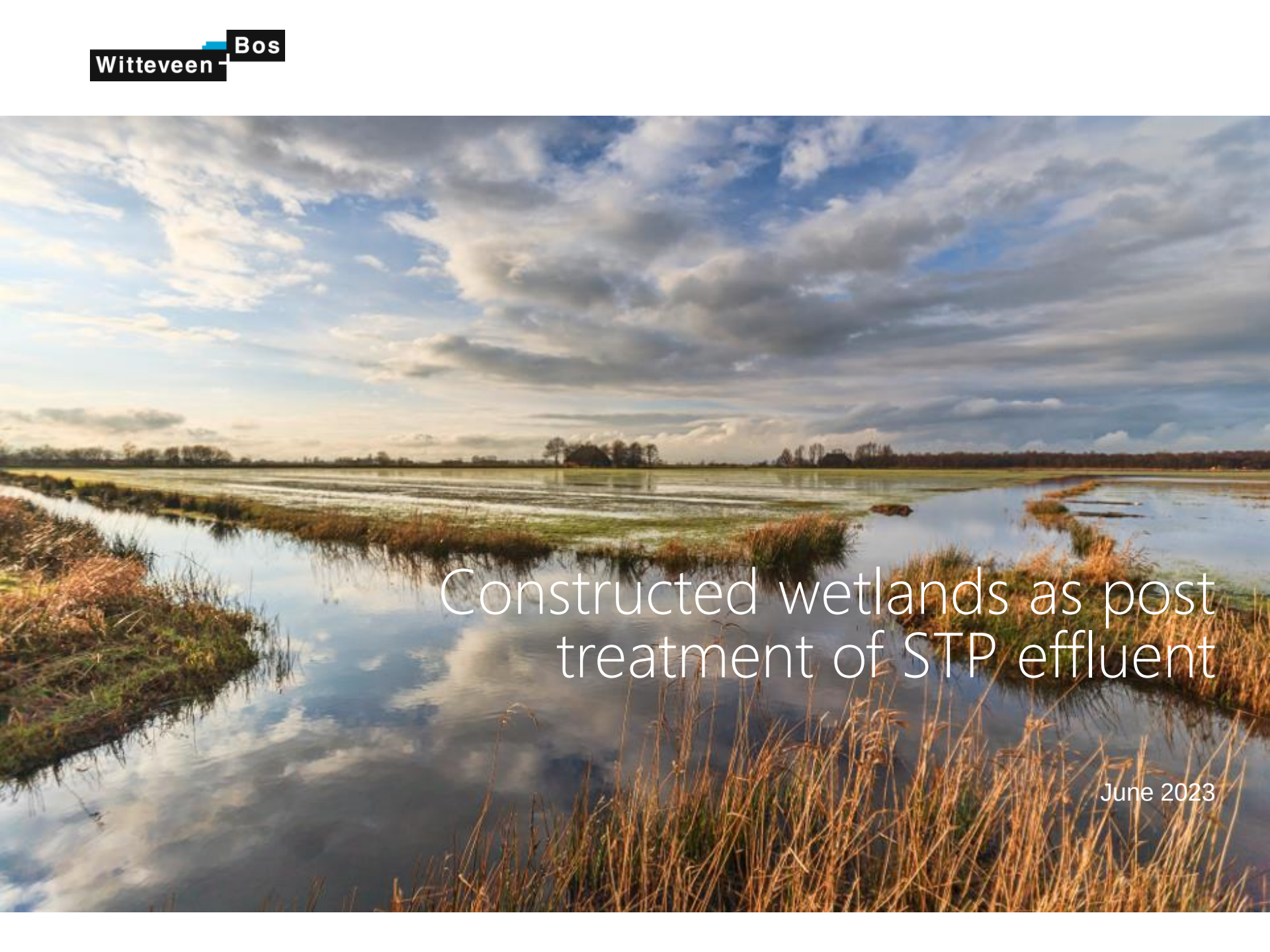
Implementation for least-cost high quality treated effluent

- Easy to implement; small footprint; easy to integrate
- Lowest phosphorous level so far in practice, low nitrogen level
 - Best suited to applications where phosphorous and another polishing requirement is necessary
 - Future proof for pharmaceuticals and organic micro pollutants
- 30-50% saving in CAPEX and OPEX compared to conventional successive processes
 - 1-STEP[®] filter solution versus denitrification, sand filtration and GAC filtration

O₃-STEP® filter

- Oxidation of organic (micro)pollutants for improved biological degradation
- Further disinfection





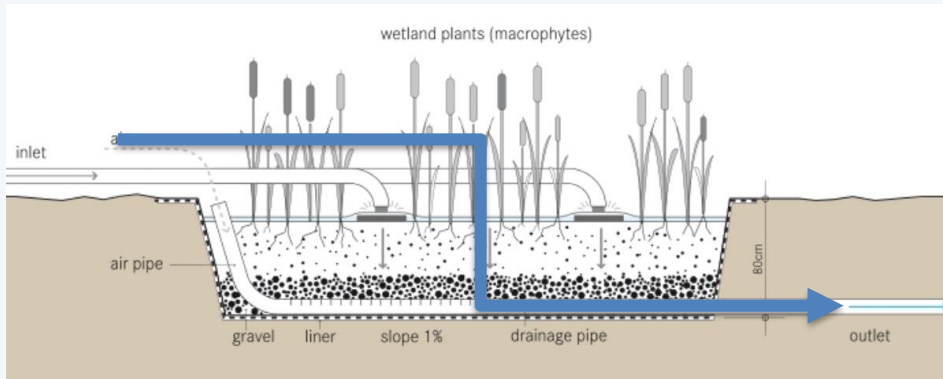
Constructed wetlands as post treatment of STP effluent

June 2023

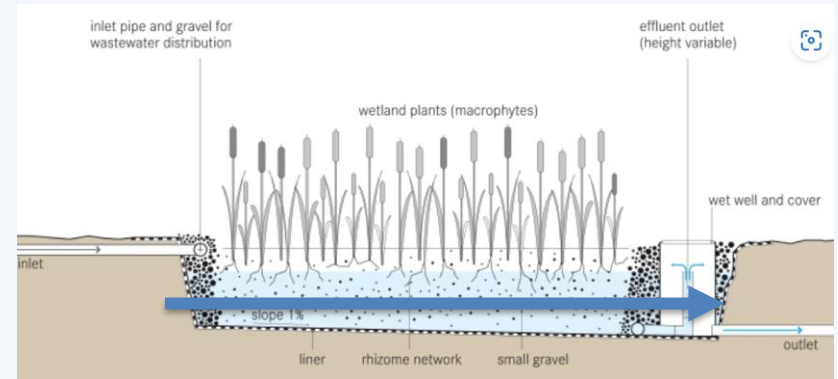
What are constructed wetlands?

- Engineered systems that use the natural functions of vegetation, soil and organisms to provide secondary treatment to wastewater
- Vertical and horizontal systems, based on direction of waterflow. Vertical systems have a soil passage.

Vertical system



Horizontal system



- Natural reduction of remaining organic pollution (BOD/COD), mostly by sedimentation and partly by conversion of bacteria, algae etc.
- Create a natural oxygen ritme before discharging
- Natural disinfection capacity: removal of pathogens mainly related to retention time
- Buffering of peak flow, and peaks in pollution concentrations
- Further reduction of nutrients

PRO

- Natural systems, no need for chemicals
- Operation and maintenance is cheap and straight forward
- Very good in buffering peak loads
- Create “natural” water that can be discharged to surface water without problems
- No need for disinfection of STE if treated by constructed wetlands

CON

- Demand large areas (especially the horizontal systems)
- Natural systems, so more uncontrolled natural fluctuations
- Evaporation

Wetlands Kristalbad, the Netherlands



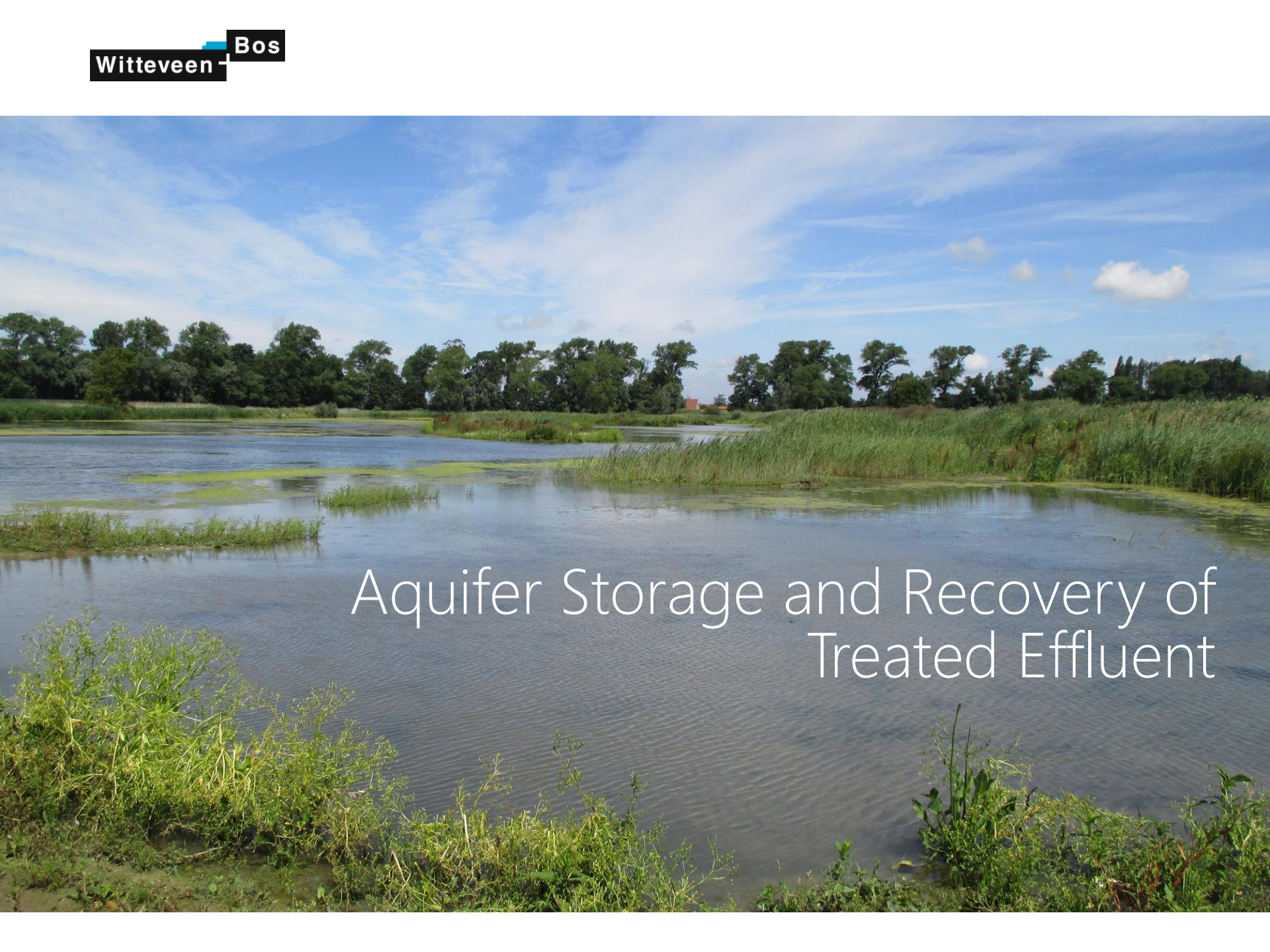
- Functions: buffering storm water, biological treatment of STE of STP Enschede, nature development, recreation
- 400,000 m²



5.1 million m²

Wastewater of oil processing:

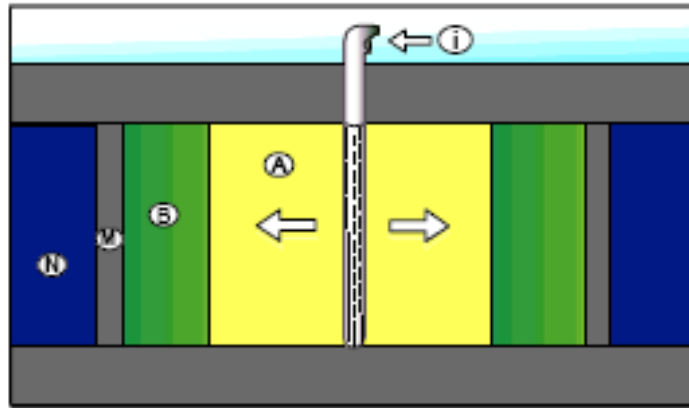
- 175,000 m³/d
- up to 8,000 mg TDS/L (brackish)
- 500 mg oil/L (oil water separator)



Aquifer Storage and Recovery of Treated Effluent

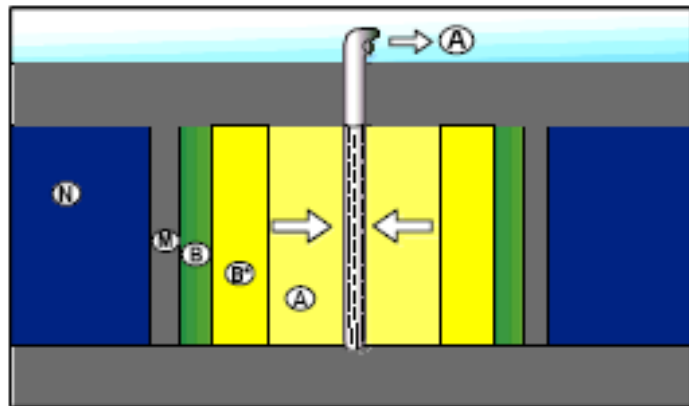
Aquifer Storage and Recovery (ASR)

STORAGE



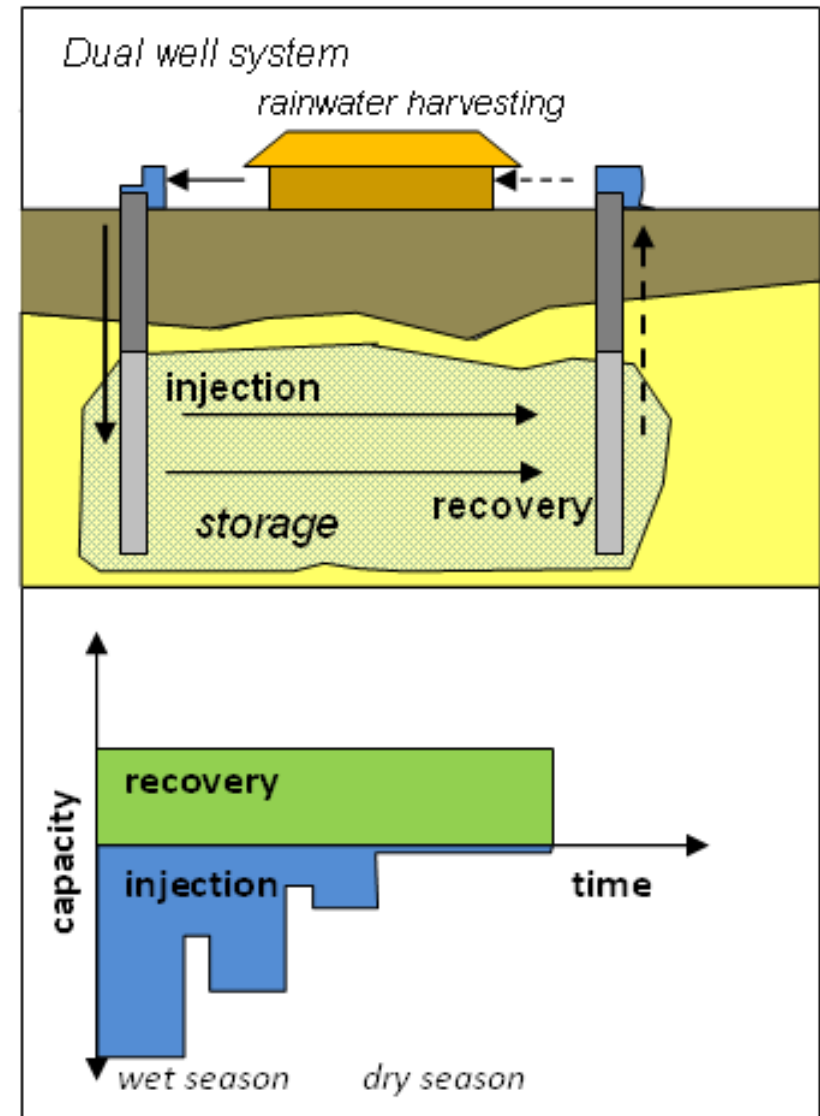
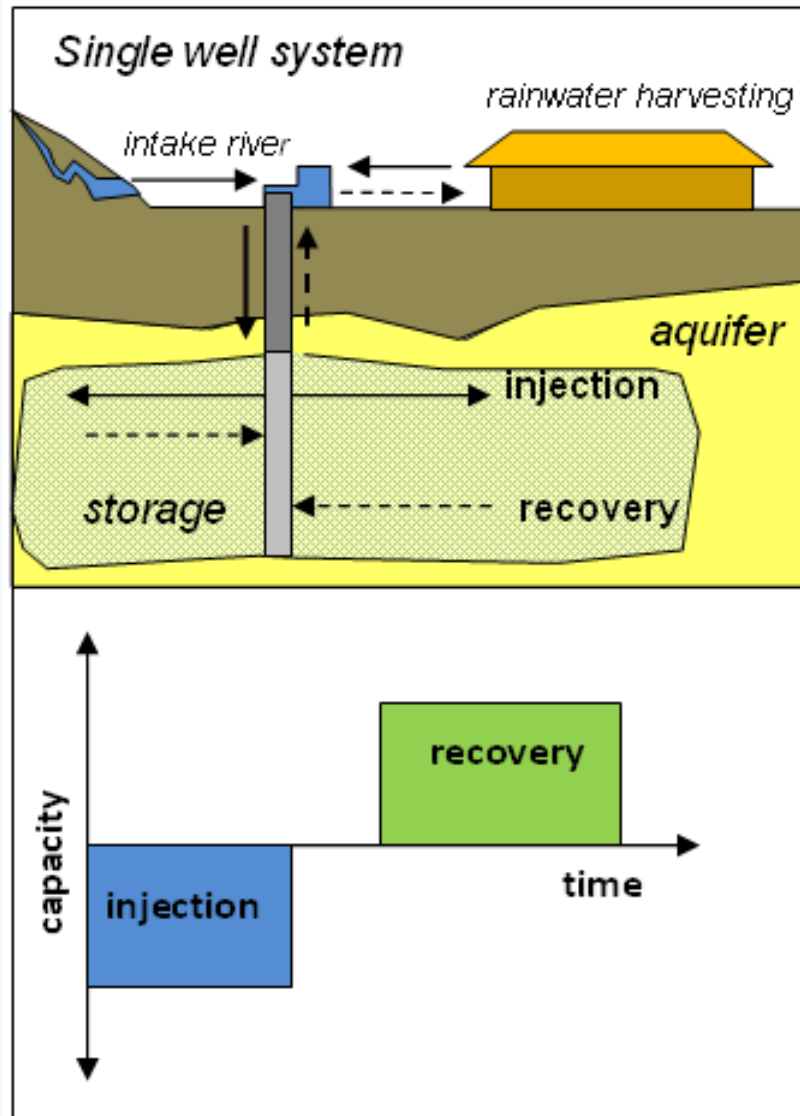
Injection of water via a (deep) well in an aquifer

RECOVERY



Extract water later, when needed, via the (deep) well

Aquifer Storage and Recovery (ASR)



- How large is the aquifer capacity?
- What is the constitution of the soil? ASR can have impact on geochemical processes such as precipitation of minerals, degradation of organic material, redox reactions, potential algae growth.
- How is the rearrangement of the particles in the aquifer?
- Clogging of the well is the biggest risk/problem.



- Growth of cities in the West of the Netherlands caused depletion of aquifers and drop in ground water levels.
- Prevent intrusion of salt sea water via underground
- ASR is applied in sand dunes (unconfined) since 1940
- Water recovery from aquifers: 180 million m³/yr



Discharge treated effluent of STP Al Kharj after tertiary treatment into aquifer:

- Current discharge of 200,000 m³/d via lagoons (Darkal) and percolation into the ground
- If phase III will be operational: 400,000 m³/d discharge required. Lagoons cannot cope with this. Saudi legislation requires secondary treatment + nutrient removal for aquifer discharge
- Design deep well system to recharge aquifer for this large capacity