



# BASIC PUMP FUNDAMENTALS

*When selecting centrifugal pumps*

## Brief History of KSB International

- 1871 KSB founded in Frankenthal, Germany by Klein, Schanzlin & Becker
- 1940 Operations in Argentina, Pakistan, Brazil, India
- 1980 Operations in France, Shanghai, USA
- 1991 Acquisition of Ajax (& Forrers) Pumps Australia

Major manufacturing plants in Germany, Italy, France, Netherlands, India, Pakistan, China, Brazil, USA, Mexico, Canada, Indonesia, South Africa

## Brief History of KSB in Australia

- 1939 Ajax Pumps Works established in Melbourne Victoria
- 1948 Ajax Pumps foundry opened in Kyneton, rural Victoria
- 1962 Forrers Pump Works Ipswich Qld begins producing submersible sewage pumps
- 1988 Ajax Pumps acquires the Forrers Pump Company in Ipswich Queensland
- 1991 KSB AG acquires Ajax Pumps, establishing KSB Ajax Pumps Pty Ltd
- 2007 Change name to KSB Australia
- 2011 Open new facility in Bundamba, QLD
- 2015 Open new facility in Hope Valley, WA

79 years in Australia and 147 years in Germany





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**Our Service and Sales facilities in QLD and WA**





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## Discover the world of KSB



- KSB Australia is the local subsidiary of Germany's number one pump manufacturer, KSB AG.
- We provide first-class products, excellent service and efficient, reliable solutions to the challenges of fluid transport.

[Company Film KSB Group.mp4](#)

MINING

WATER

WASTE WATER

ENERGY

BUILDING SERVICES

INDUSTRY





# BASIC PUMP FUNDAMENTALS

*When selecting centrifugal pumps*

**We will be talking about the basic criteria to keep in mind when selecting centrifugal pumps**



# BASIC PUMP FUNDAMENTALS

*When selecting centrifugal pumps*

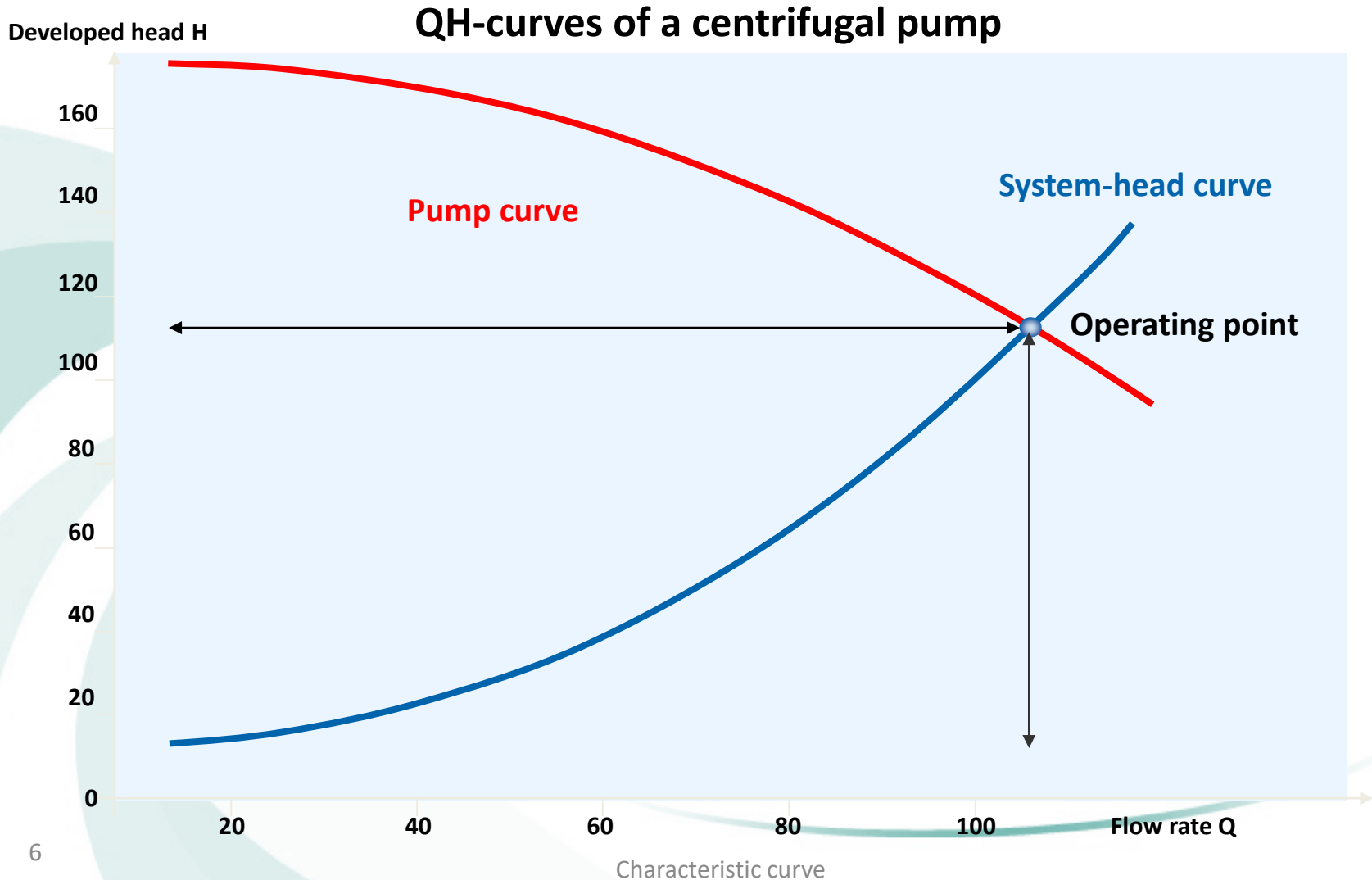
## When Selecting Pumps we **must** know:

- What we are pumping i.e. chemically aggressive, solids content etc.
- What is the temperature
- Is there any abrasive content
- What is the specific gravity
- The viscosity
- Required flow rate
- Total pump head



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## **Pump Duty:**

### Flow Rate (Q)

- The units typically used are  $\text{m}^3/\text{h}$ ,  $\text{m}^3/\text{s}$ ,  $\text{l}/\text{s}$ ,  $\text{l}/\text{h}$
- The flow rate of a centrifugal pump is independent of the **density** of the fluid being pumped
- The **viscosity** of the fluid being pumped affects the flow rate of the pump. The higher the viscosity, the lower the flow and the lower the viscosity the higher the flow
- Viscosity will change with temperature
- This will affect the power consumption of your pump
- 40 Centipoise is considered viscous



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## **Pump Duty:**

### Head (H) or (TDH)

- The unit is specified in meters head
- A centrifugal pump will deliver the same head to various fluids independent of its density
- If the viscosity of a fluid changes the developed head will also change



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## Pressure and developed head

$$H = \frac{p}{\rho \cdot g}$$

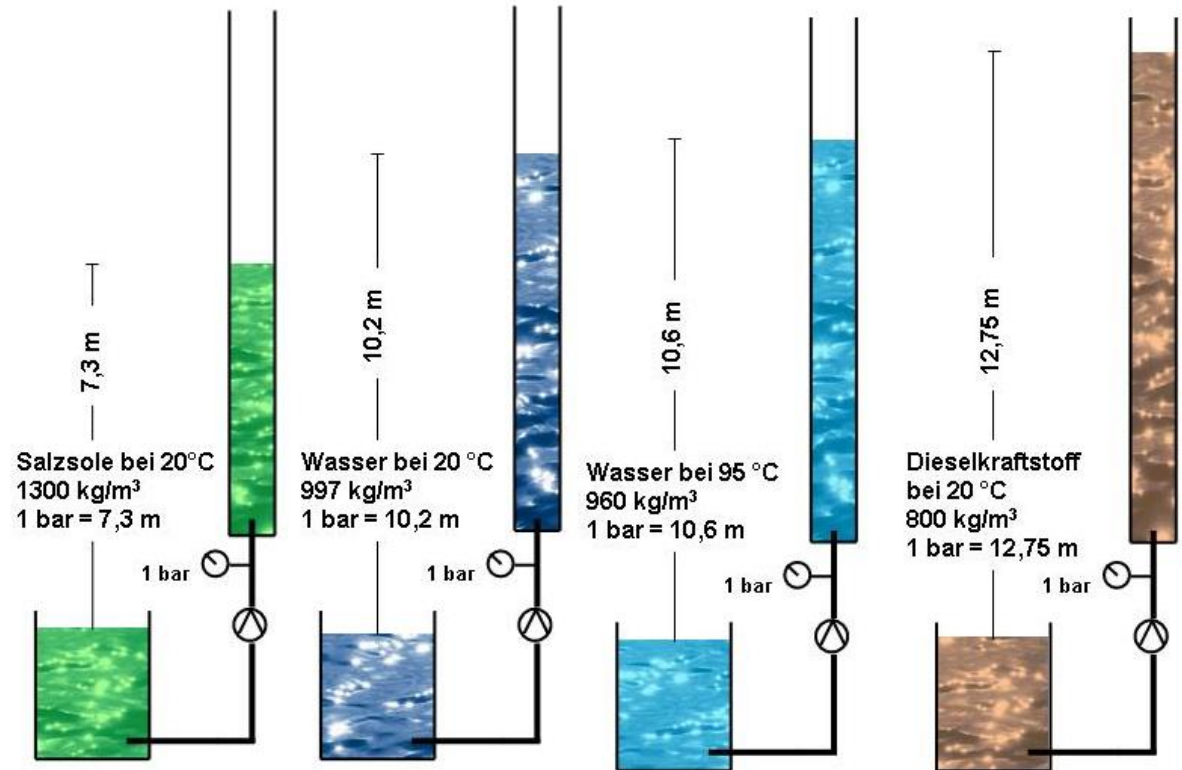
wobei:

H gleich Förderhöhe in [m]

p gleich Druck in [Pa = N/m<sup>2</sup>]

ρ gleich Flüssigkeitsdichte in [kg/m<sup>3</sup>]

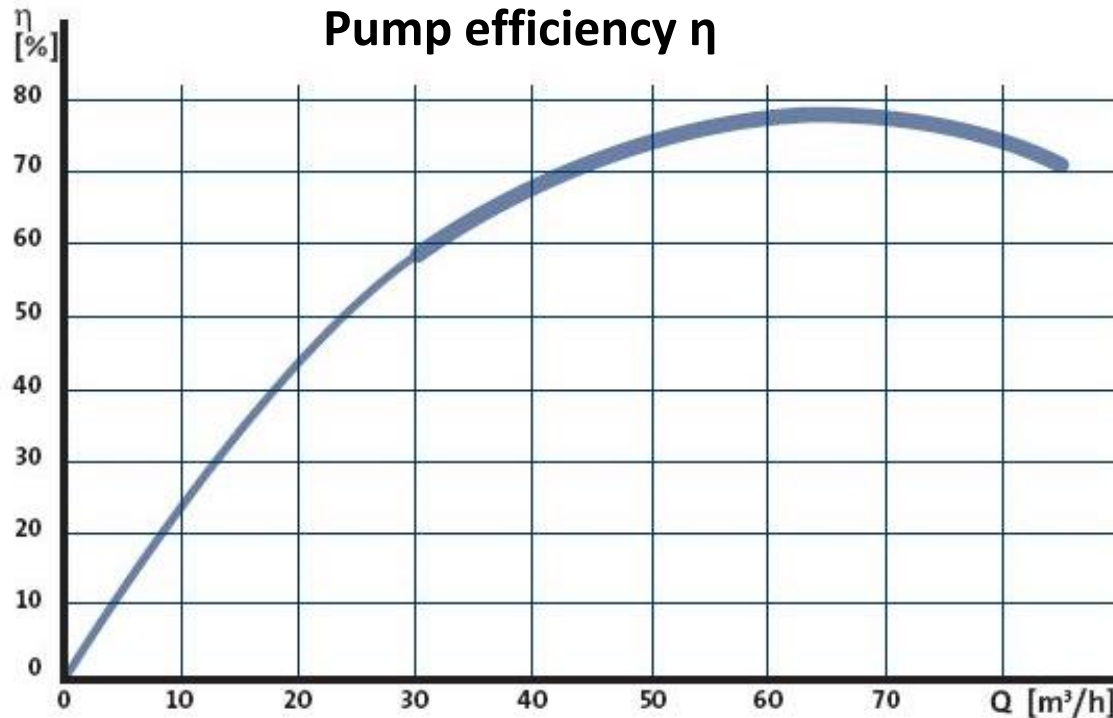
g gleich Erdbeschleunigung in [m/s<sup>2</sup>]





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$Q_{opt}$  is the point with the **best efficiency** of the pump, also common as **BEP** (= best efficiency point).

The **pump efficiency**  $\eta$  shows the proportion between the **flow rate**  $P_h$  of a pump and the **mechanical power**  $P_2$  of a pump shaft:

$$\eta = \frac{P_h}{P_2} = \frac{\rho \times Q \times g \times H}{P_2}$$

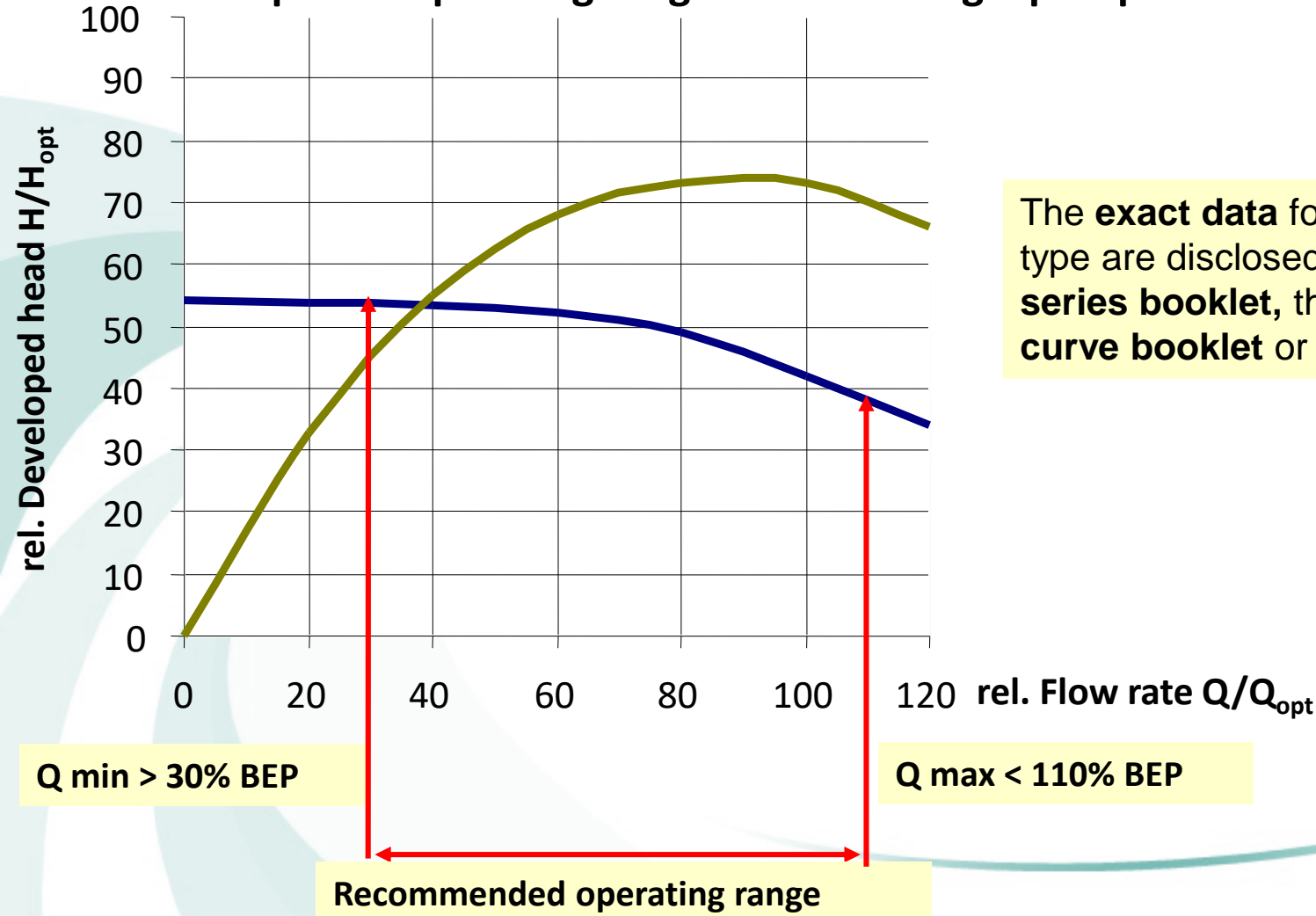
( $\rho$  in  $\text{kg}/\text{dm}^3$ ,  $Q$  in  $\text{m}^3/\text{s}$ ,  
 $g = 9,81 \text{ m}^2/\text{s}$ ,  $H$  in  $\text{m}$ ,  $P$  in  $\text{kW}$ )



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## Optimal operating range of a centrifugal pump



The **exact data** for each pump type are disclosed in the **type series booklet**, the **characteristic curve booklet** or in **EasySelect**.

**Q min > 30% BEP**

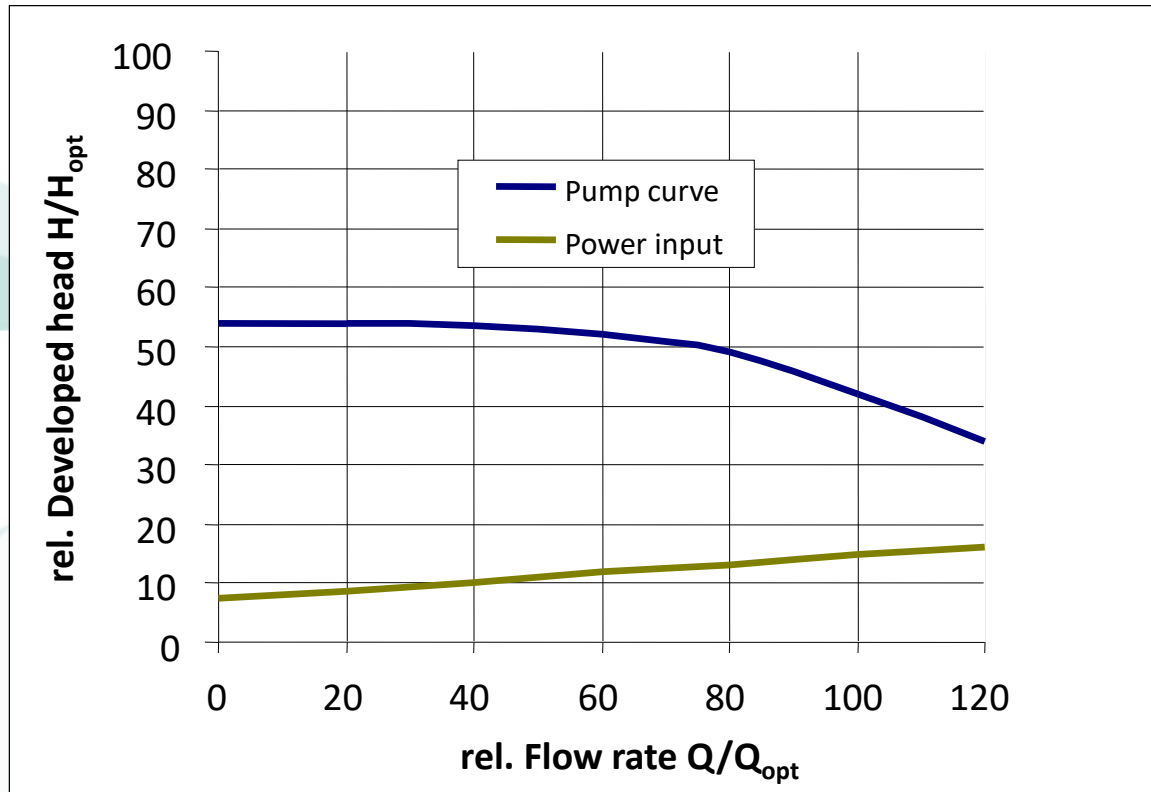
**Q max < 110% BEP**

**Recommended operating range**

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## Minimum flow rate



**Why minimum flow rate?** → protection of the pump against heating and unstable flow ratios (noise, vibrations etc.)

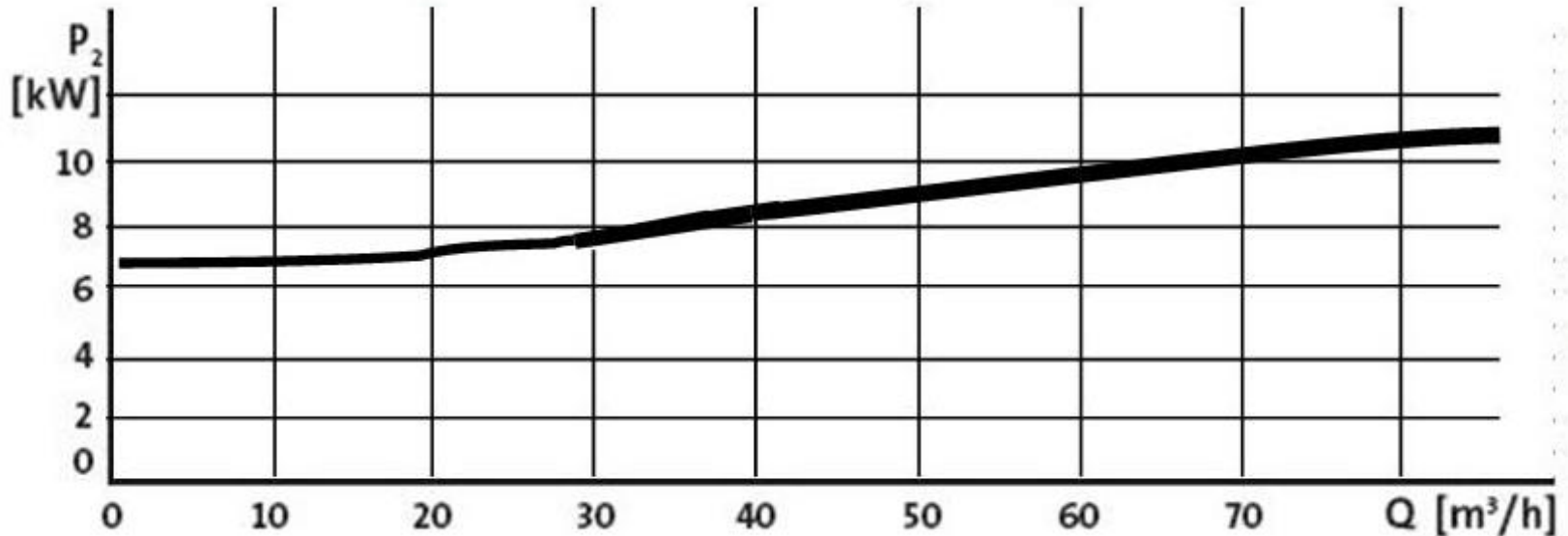
**The minimum flow rate of a centrifugal pump is ca. 15% of the  $Q_{opt}$**

The exact data of each pump type is disclosed in the type series booklet or in EasySelect

# BASIC PUMP FUNDAMENTALS

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**Characteristic curve of the power input  $P_2$**



The  **$P_2$  characteristic curve** shows the proportion between the mechanical power input of a centrifugal pump and the flow rate  $Q$ . If  $Q$  rises,  $P_2$  rises also.

**Important:** The characteristic curve shows the mechanical power input  $P_2$ . Electrical power input of the motor  **$P_1 = P_2 / \eta_{mot}$**  (motor efficiency)

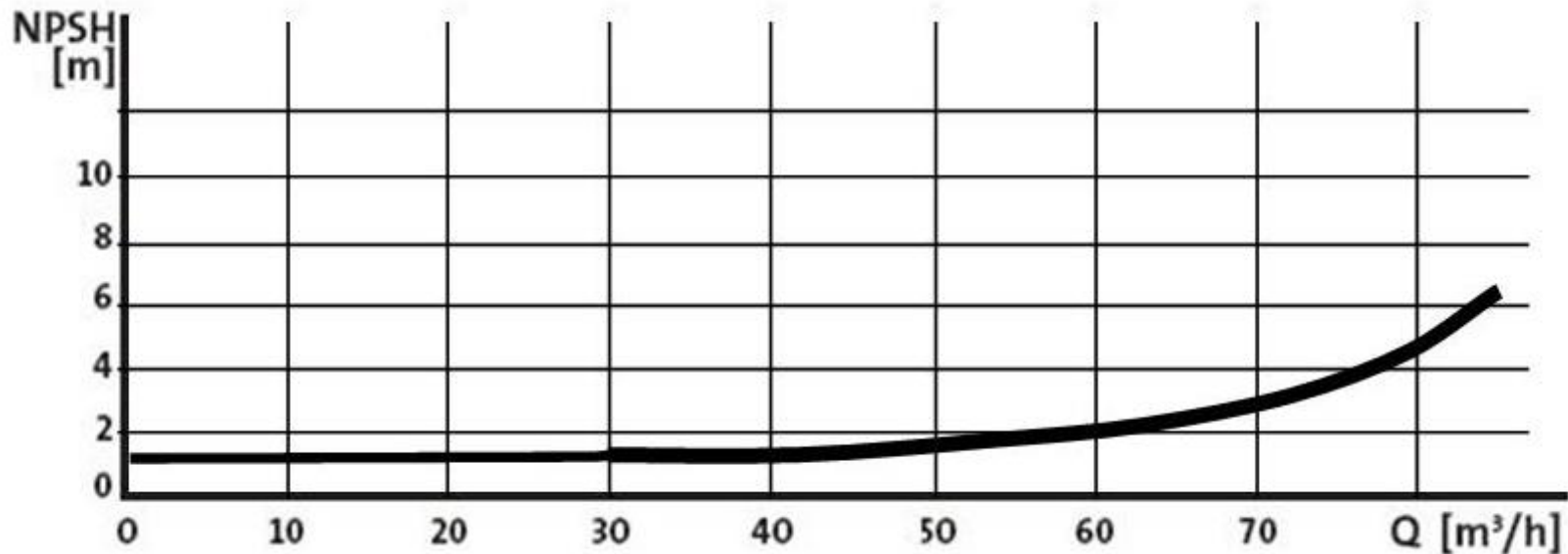
The  $P_2$  characteristic curve shows the power input of a stage at **multistage pumps!**



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## NPSH-characteristic curve of a centrifugal pump



The NPSH-value (**NetPositiveSuctionHead**) is the minimum pressure required at the suction side of the pump in order for it to work. The **NPSH-value is measured in [m]** and rises with the increase in flow (Q).

The NPSH-value is calculated by tests for each pump according to the ISO 9906 standards and on a approved testbed.

**Important:** The **NPSHa** of a installation has to be larger than the **NPSHr** by the pump to allow it to pump and to eliminate cavitation etc...



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## Pump Head:

Pressure : Head (H) or Total Dynamic Head (TDH)

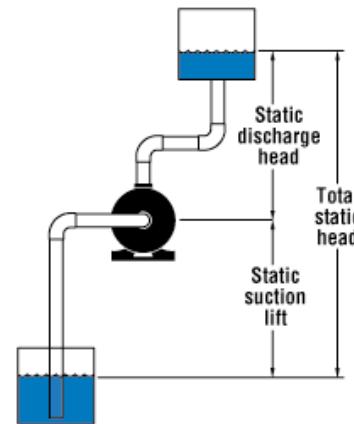
- When calculating Total Head the Suction Head should be listed separately to allow correct evaluation of the suction conditions
- Total Head (H) is made up of total Discharge Head (Hd) minus the Suction Head (+Hs) or plus the Suction Lift (-Hs)

$$H = H_d + / - H_s$$

## Calculating NPSHa for suction lift

For a suction lift, where the supply level is below the pump centreline, the **NPSHa** can be calculated using the following equation:

$$NPSHa = h_a - h_v - h_s - h_{fs}$$





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**NPSH:**

Where:

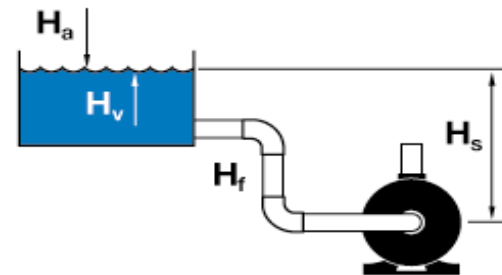
**ha** = the pressure on the surface of the supply vessel (m)

**hv** = velocity head or vapour pressure of the liquid at the operating temperature

**hs** = the suction lift or suction head to the pump centreline or impeller eye

**hfs** = all suction line losses

**For a flooded suction**



$$\text{NPSHa} = h_a - h_v + h_s - h_{fs}$$





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## Velocity Head (H<sub>v</sub>)

Velocity head of a liquid moving with a certain velocity is the equivalent static head through which it would have to fall in order to attain that velocity. It also is the amount of head generated when fluid velocity drops to zero.

$$\text{Velocity Head (H}_v\text{)} = V^2 / 2g$$

V = Velocity of fluid (m/sec)

g = Acceleration due to gravity (9.81 m/sec<sup>2</sup>)



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## Velocity Head (Hv)

Velocity may be calculated for a given flow in a known diameter pipe by employing the formula below:

$$V = 1273 Q / d^2$$

### **Where:**

Q = Quantity in l/s

d = Pipe diameter in mm

V = Fluid velocity in m/sec



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## Velocity Head (Hv)

For example we can now calculate the velocity head (Hv) in a 250mm diameter pipe in which there is a flow of 100 l/s

Calculate the velocity using

$$V = 1273 Q / d^2$$

$$V = 1273 \times 100 / 250^2$$

$$V = 2.04 \text{ m/sec}$$

Velocity Head

$$H_v = V^2 / 2g$$

$$H_v = 2.04^2 / 2 \times 9.81$$

$$H_v = 0.212 \text{ meters of fluid}$$

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## Suction Lift & Suction Head

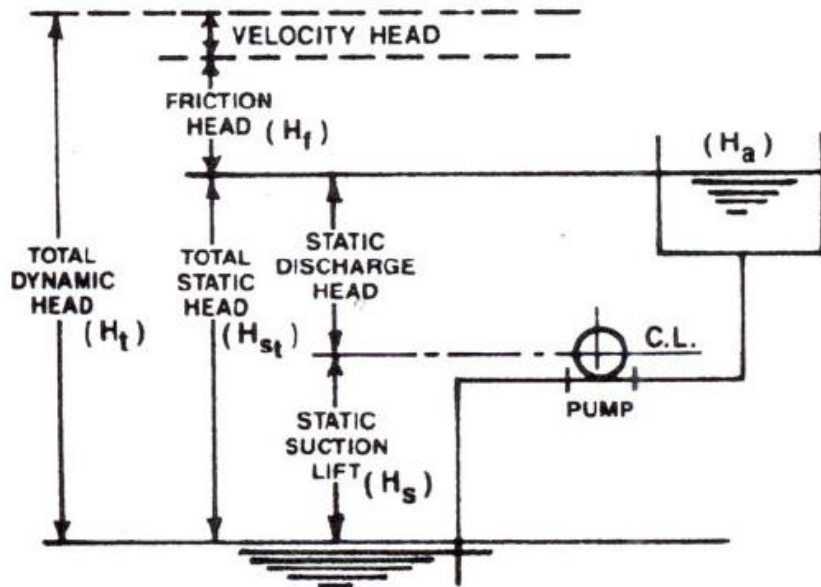


Fig. 1.3.1—Suction lift.

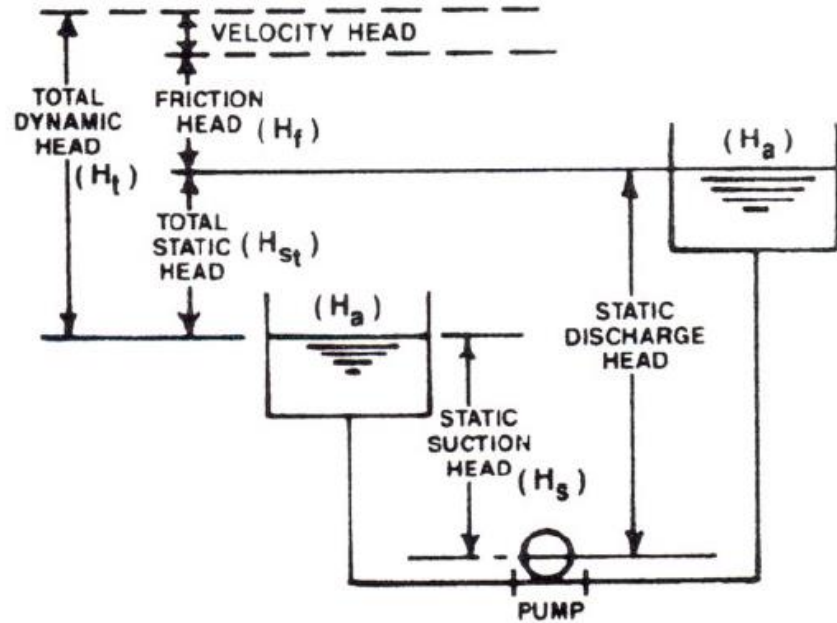


Fig. 1.3.2—Suction head.



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## Some tips to Keep in Mind:

The suction design of any pump system is key to a trouble free pumping operation

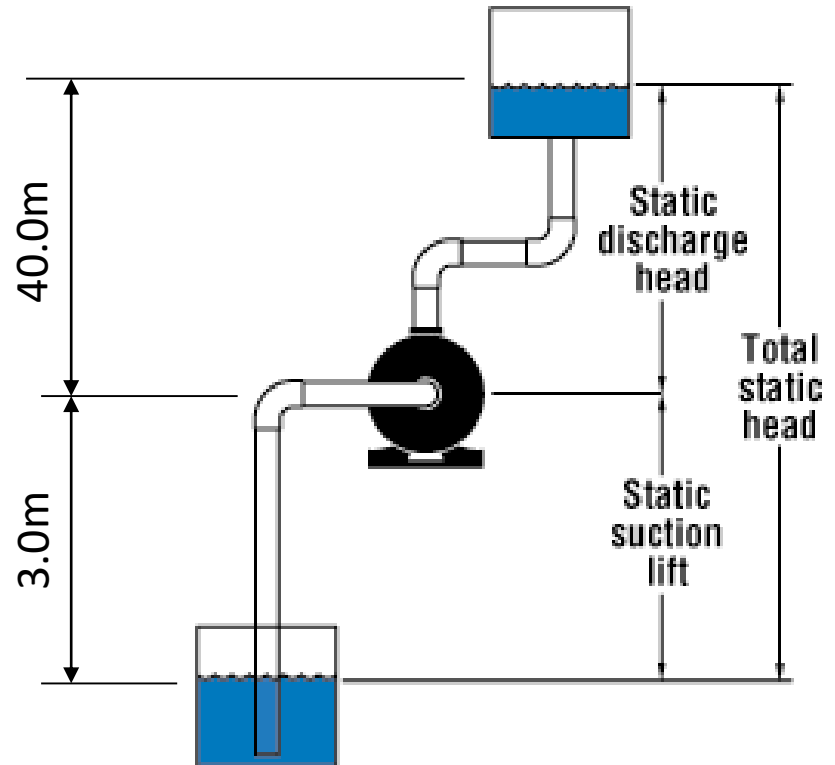
- Restricting the inlet port size and the inlet pipe ID will cause cavitation and damage the pump
- Rule of thumb is to have the suction pipes at least one size larger than the pump suction inlet
- Rule of thumb is to have a suction pipe velocity lower than 1.2 m/sec
- It is best to have a straight run of pipe leading into the pump inlet with an eccentric reducer
- The **NPSHa** must always be greater than **NPSHr** by the pump
- Use long radius bends on suction pipes
- Have suction slightly sloping upwards towards the pump suction nozzle
- Make sure there is no pipe stress on the pump nozzles after installation



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**Typical calculation of pump duty:**



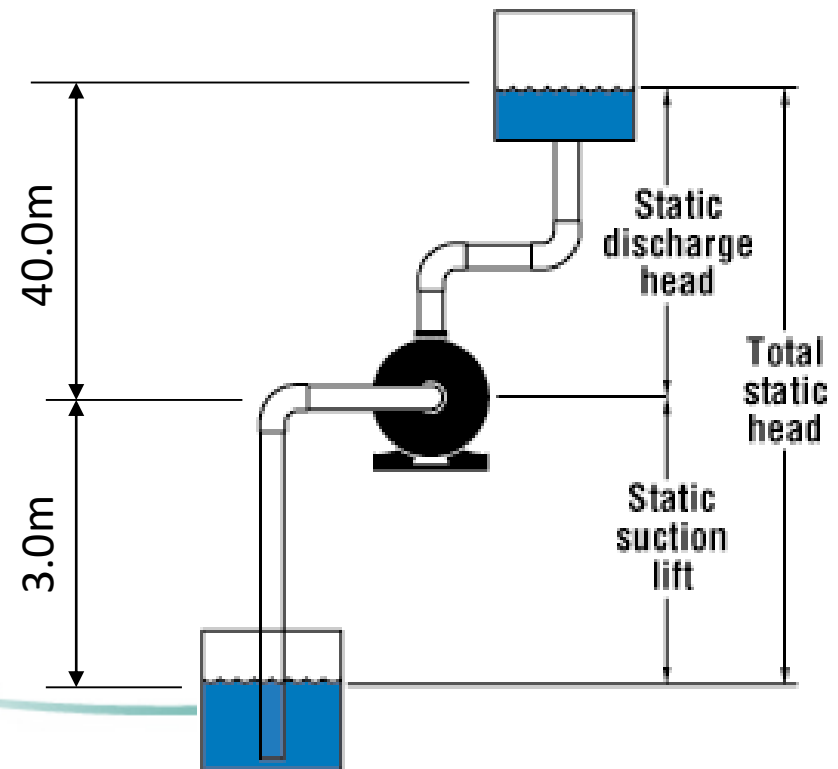


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## Calculation of pump duty:

Suction Lift	= 3.0m
Assumed friction losses	= 2.0m
<b>Total suction head</b>	<b>= 5.0m</b>
Discharge Static	= 40.0m
Assume friction losses	= 12.5m
Pressure required at discharge	= 17.5m
<b>Total discharge head</b>	<b>= 70.0m</b>
<b>Total dynamic head = <math>H_s + H_d</math></b>	<b>= 75.0m</b>





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## **Selection of suitable Pump:**

- We can now make a manual selection using our pump performance catalogue or we can use our computer aided selection program.





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## Computer Aided Pump Selection:

Many pump manufacturers provide computer programs to assist in pump selection.

KSB have developed a program called **Easy Select** and it is available on our website. This program will select the most suitable pumps for your particular application.

[https://www.ksb.com/ksb-au/?gclid=EAlaIQobChMIgv76hZnS2wIVEBSPCh1vigAfEAAAYASAAEgLA1\\_D\\_BwE](https://www.ksb.com/ksb-au/?gclid=EAlaIQobChMIgv76hZnS2wIVEBSPCh1vigAfEAAAYASAAEgLA1_D_BwE)