



Troubleshooting of FILMTEC™ Membrane Plants

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Water & Process Solutions





Troubleshooting

means:

identify & correct performance issues

- ✓ Analyze symptoms
- ✓ Identify and localize causes
- ✓ Corrective measures
- ✓ Preventive measures





Troubleshooting in RO und NF Plants

Contents

1. Symptoms and causes
2. Effect on membrane performance if something goes wrong
3. Problem area: Feed water / pretreatment
4. Problem area: Plant operation
5. Problem area: System components
6. Troubleshooting Summary





Symptoms and Causes

Performance problems are recognized only when the symptoms are significant:

- Loss of normalized permeate flow rate
- Increase in normalized salt passage
- Increase in pressure drop





Symptoms and Causes

Performance problems are recognized only when the symptoms are significant:

- **Loss of normalized permeate flow rate**
 - Sudden or gradual change?
 - First or second stage?
 - Cleaning experience?





Symptoms and Causes

Performance problems are recognized only when the symptoms are significant:

- Loss of normalized permeate flow rate
- Increase in normalized salt passage
 - Sudden or gradual?
 - First or second stage?
 - Uniform or specific vessels?
 - Probing!





Symptoms and Causes

Performance problems are recognized only when the symptoms are significant:

- Loss of normalized permeate flow rate
- Increase in normalized salt passage
- Increase in pressure drop
 - First or second stage?





Symptoms and Causes

Early detection of potential problems requires:

- Instruments, sensors
- Calibration of instruments
- Record keeping
- Data normalization:

Translation of measured performance under prevailing conditions into performance under reference conditions





Symptoms and Causes

Direct causes of performance problems:

- **Fouling/Scaling**
 - Flux loss, salt passage increase, differential pressure increase
- **Mechanical damage**
 - Salt passage increase, differential pressure increase
- **Chemical damage**
 - Salt passage increase, Flux increase





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Effect on membrane performance if something goes wrong

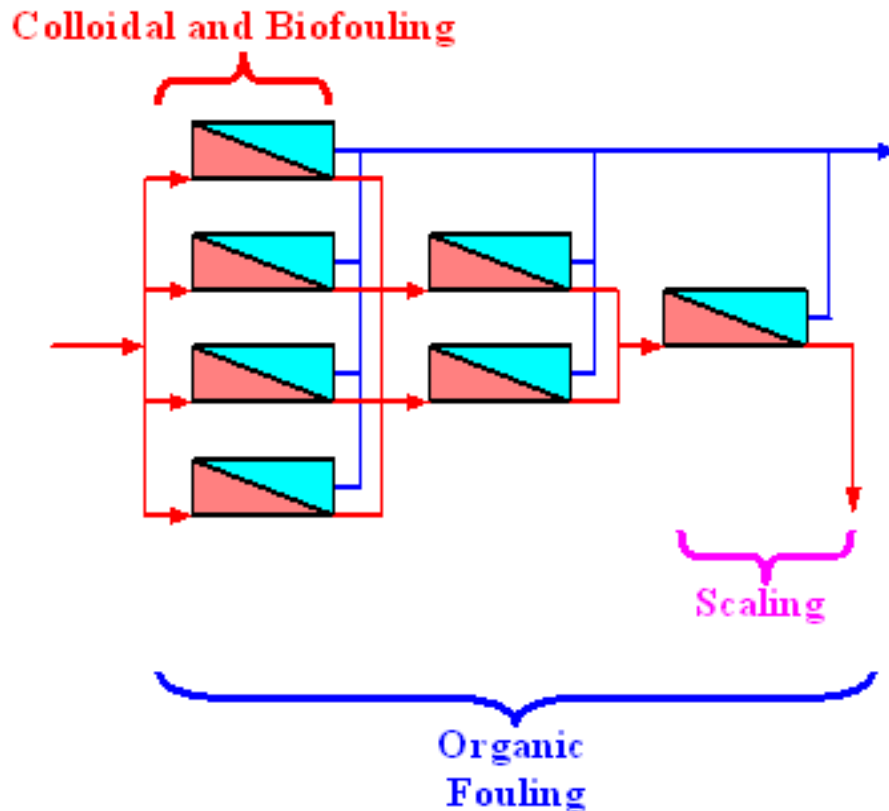
- **Fouling / Scaling**
- Mechanical damages
- Chemical damages





Fouling/Scaling

Fouling often originates in a specific part of the RO/NF system:





Fouling/Scaling

commonly caused by raw water characteristics and inappropriate pretreatment





Fouling

Colloidal and particle fouling
caused by solids from the pretreatment
entering the first stage elements





Colloidal and particle fouling



Extreme cases of fouling





Fouling

Colloidal and particle fouling
caused by solids from the pretreatment
entering the first stage elements

Correction: Alkaline/detergent cleaning, acid cleaning

Prevention: Pretreatment improvement
Membranes with wider feed spacer





Pretreatment methods to control particle fouling

- Filtration
 - Sand filter
 - Multimedia filter
 - Ultrafiltration
- Coagulation - filtration
- Coagulation/flocculation - filtration
- Coagulation/flocculation - clarification - filtration



Fouling

Biofouling

Occurs due to

- High biogrowth potential in feed water
- Improper operation and procedures
- Dead legs in system

typical: ΔP increase of front end elements





Biofouling





Fouling

Biofouling

Occurs due to

- High biogrowth potential in feed water
- Improper operation and procedures
- Dead legs in system

typical: ΔP increase of front end elements

Correction: Alkaline cleaning

Prevention: Pretreatment improvement
Fouling resistant membranes
Regular cleaning and sanitization
Sanitary design



Pretreatment methods to control biofouling

- Biofiltration
 - Slow sand filter
 - GAC filter
 - Pre-oxidation, e.g. by ozone
- Intermittent biocide dosage, e.g. DBNPA



Fouling

Organic Fouling

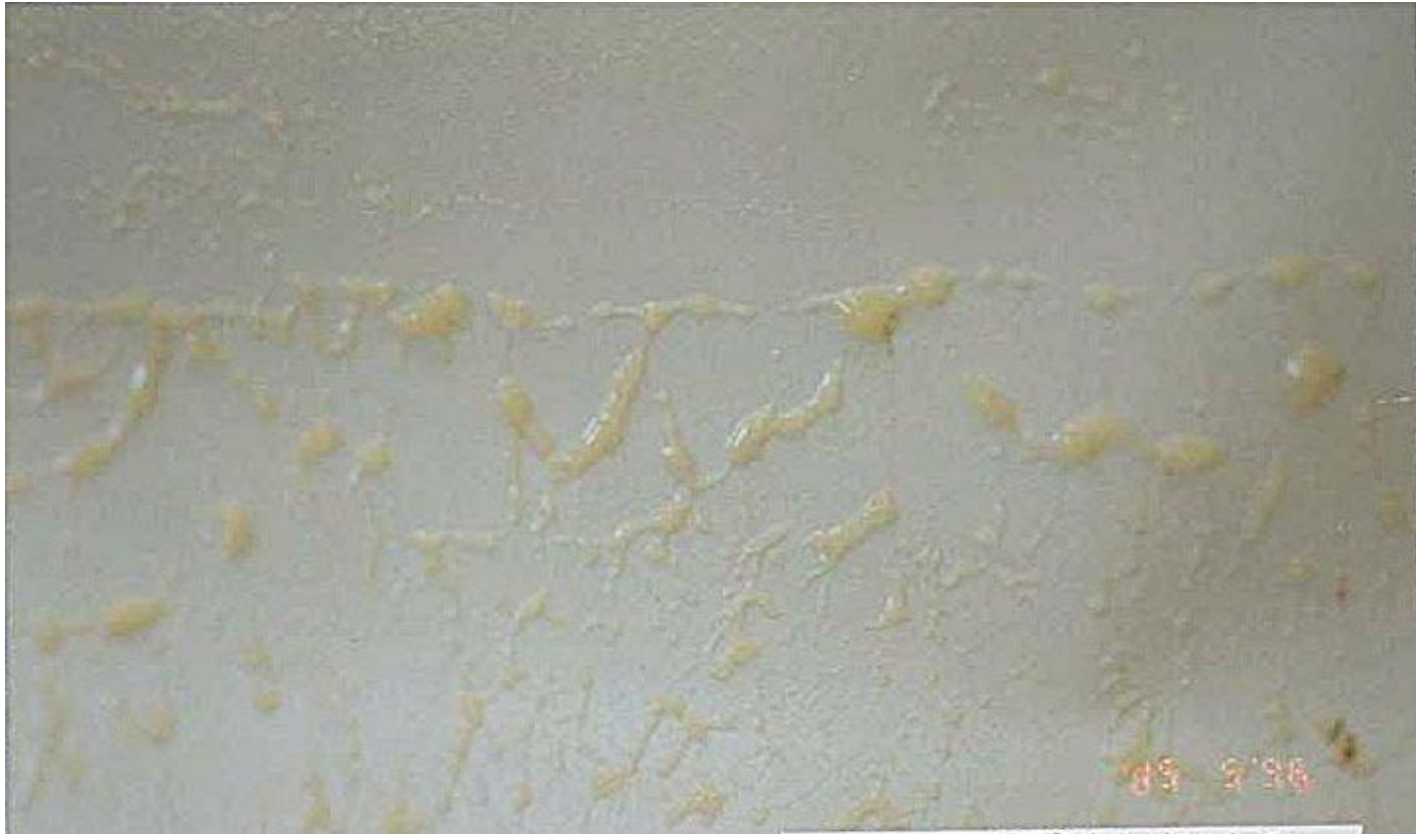
from

- Natural organic matter in the feed water
 - NOM, humic substances
- Polluted raw water
 - Oil, grease
- Polyelectrolytes in flocculation/coagulation pre-treatment
 - Scaling inhibitors
 - Coagulants





Precipitated scaling inhibitor





Fouling

Organic Fouling

from

- Natural organic matter in the feed water
 - NOM, humic substances
- Polluted raw water
 - Oil, grease
- Polyelectrolytes in flocculation/coagulation pre-treatment
 - Scaling inhibitors
 - Coagulants

Correction: alkaline cleaning

Prevention: pretreatment improvement, XFR membranes





Pretreatment methods to control organic fouling

- Lime softening
- GAC filtration
- GAC biofiltration
- Scavenger
- Inline coagulation
- Coagulation/flocculation
- Coagulation/flocculation - clarification



Fouling

Metal oxide fouling

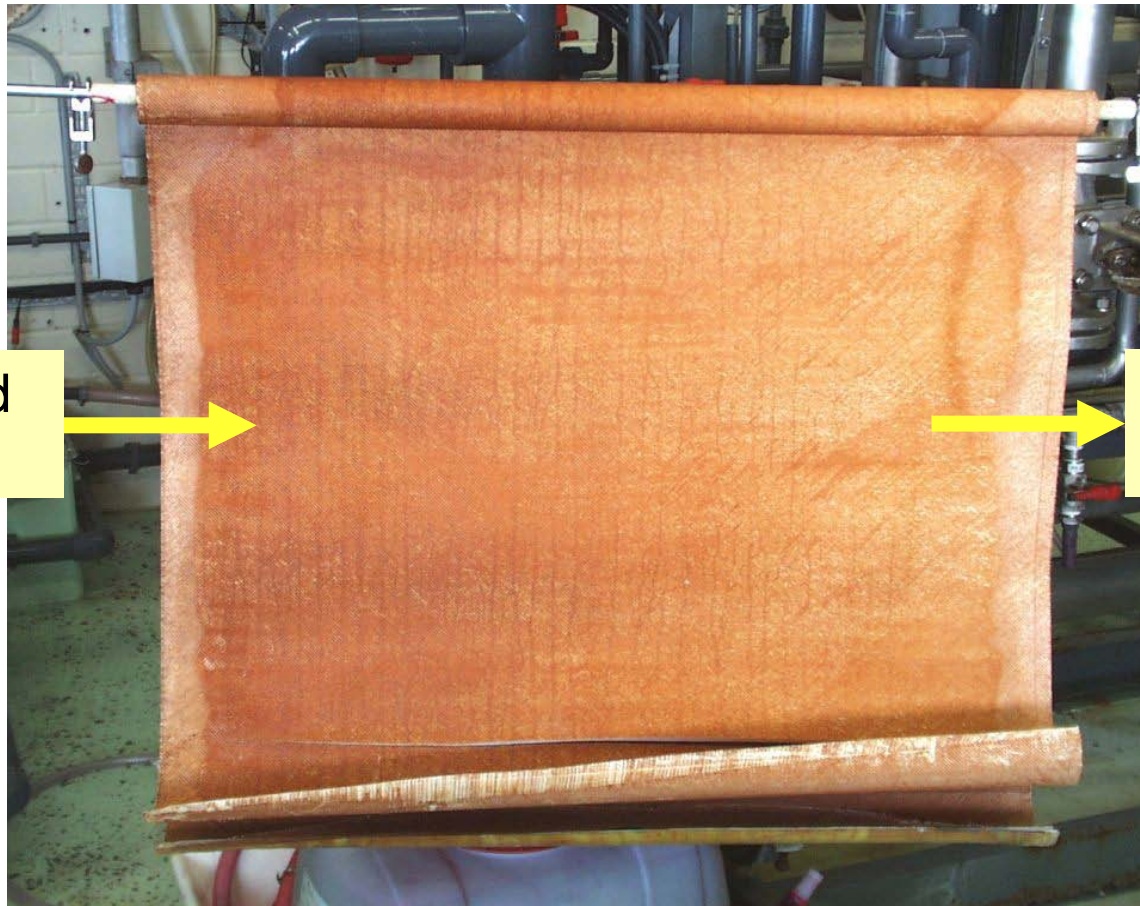
mainly occurs in the first stage

- from flocculation process
 - Iron
 - Aluminum
- from anoxic wells
 - Iron
 - Manganese
- from corroding system components
 - Iron
 - Copper





Iron fouling



Feed inlet

Concentrate outlet





Fouling

Metal oxide fouling

mainly occurs in the first stage

- from flocculation process
 - Iron
 - Aluminum
- from anoxic wells
 - Iron
 - Manganese
- from corroding system components
 - Iron
 - Copper

Correction: Acid cleaning

Prevention: Pretreatment improvement
Corrosion resistant materials
Membranes with wider feed spacer





Pretreatment methods to control metal oxide fouling

- Filtration
 - Sand filter
 - Multimedia filter
 - Ultrafiltration
- pH adjustment (Al^{3+})
- Anoxic process ($\text{Fe}^{2+}/\text{Mn}^{2+}$)
- Oxidation - filtration ($\text{Fe}^{2+}/\text{Mn}^{2+}$)



Fouling

Sulfur fouling

from

- Aeration or oxidation of hydrogen sulfide containing raw water
- Osmotic backflow of aerated permeate into a hydrogen sulfide containing anoxic system

Correction: Membrane replacement

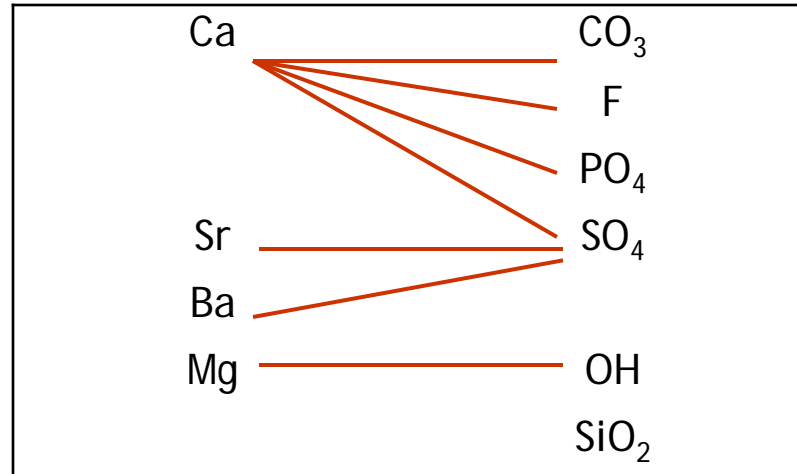
Prevention: Avoid contact with air or oxidants





Scaling

Precipitation and deposition of sparingly soluble salts

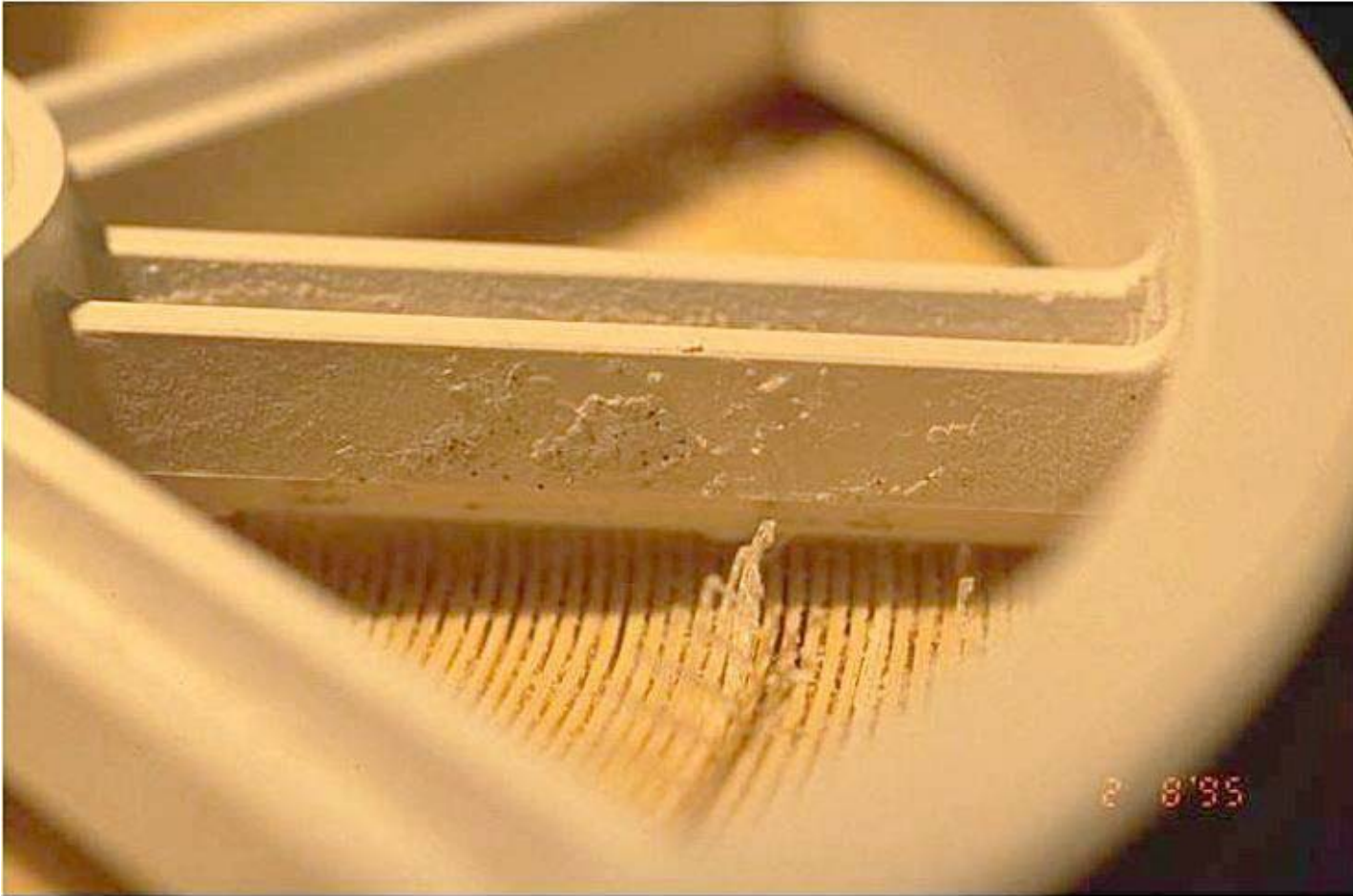


- Starts in tail end of the system
- Caused by:
 - Raw water changes
 - Improper dosage of scaling inhibitor
 - Too high recovery





Scaling



Extreme case of CaCO_3 scaling, concentrate side





Calcium carbonate scaling



Correction: Acid cleaning; extended acid contact time

Prevention: Pretreatment improvement





Scaling



CaCO₃ Scaling on Feed Spacer





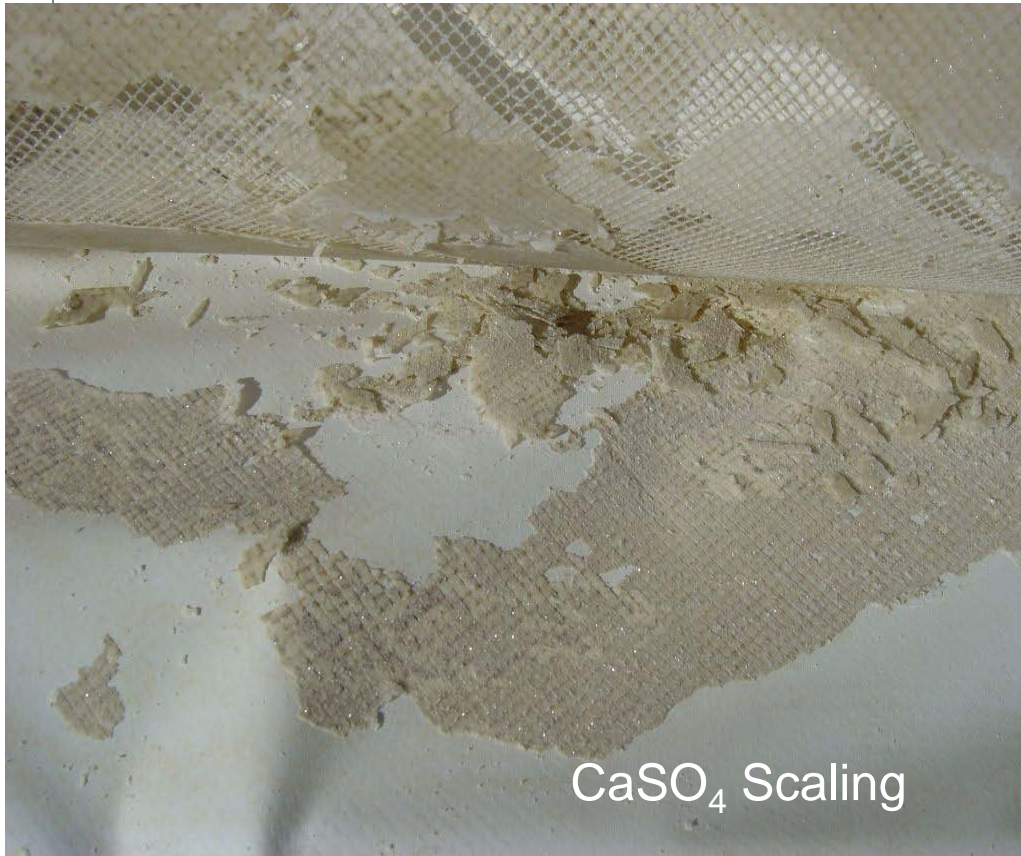
Scaling



CaCO₃ Scaling on Feed Spacer



Sulfate scaling



CaSO₄ Scaling

- | | |
|--------------------|--|
| Correction: | high pH EDTA cleaning (difficult!) |
| Prevention: | pretreatment improvement recovery reduction |





Pretreatment methods to control scaling

- Acid addition (Carbonate)
- Antiscalant
- Softening (strong cation resin)
- Dealkalization (weak cation resin)
- Lime softening



Effect on membrane performance if something goes wrong

- Fouling / Scaling
- Mechanical damages
- Chemical damages





Mechanical Damages

Abrasion

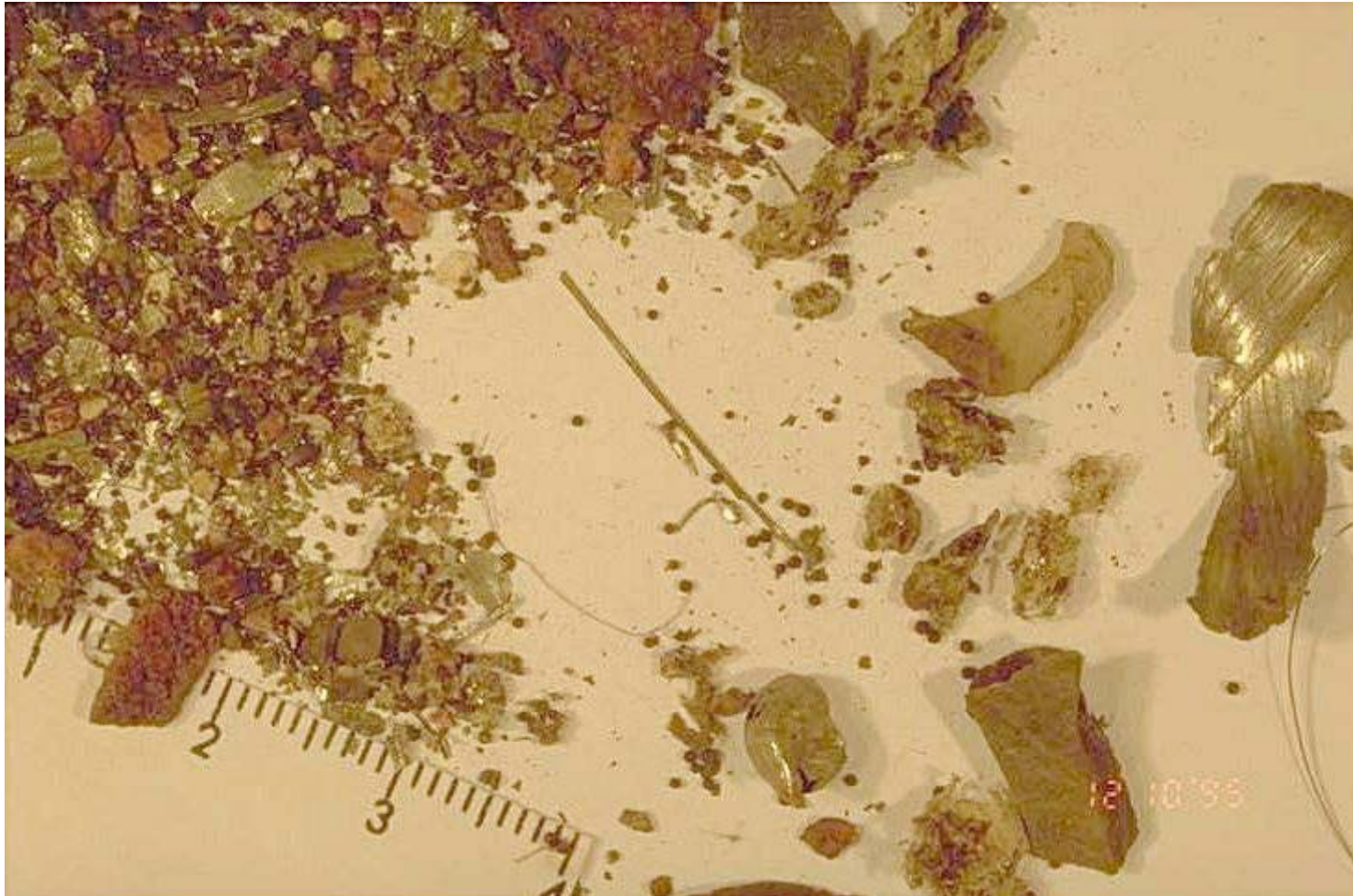
Increased salt passage

- Membrane scratched by crystalline or sharp-edged solids in the feed water
- Lead elements mostly affected





Abrasion by sharp-edged particles



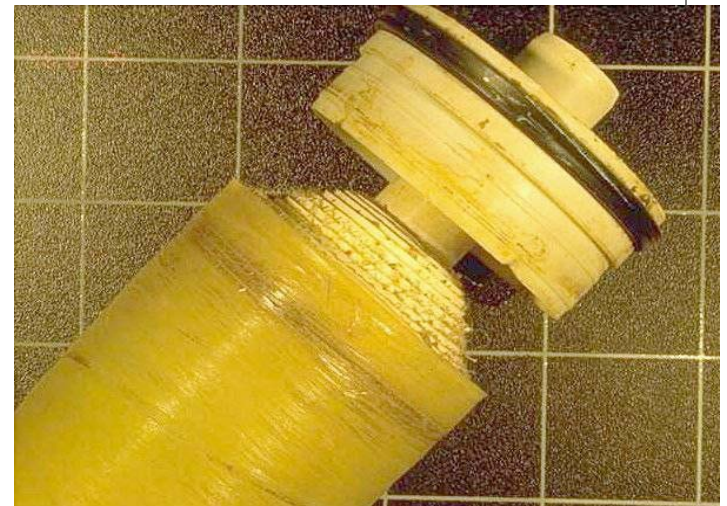


Mechanical Damages

Telescoping

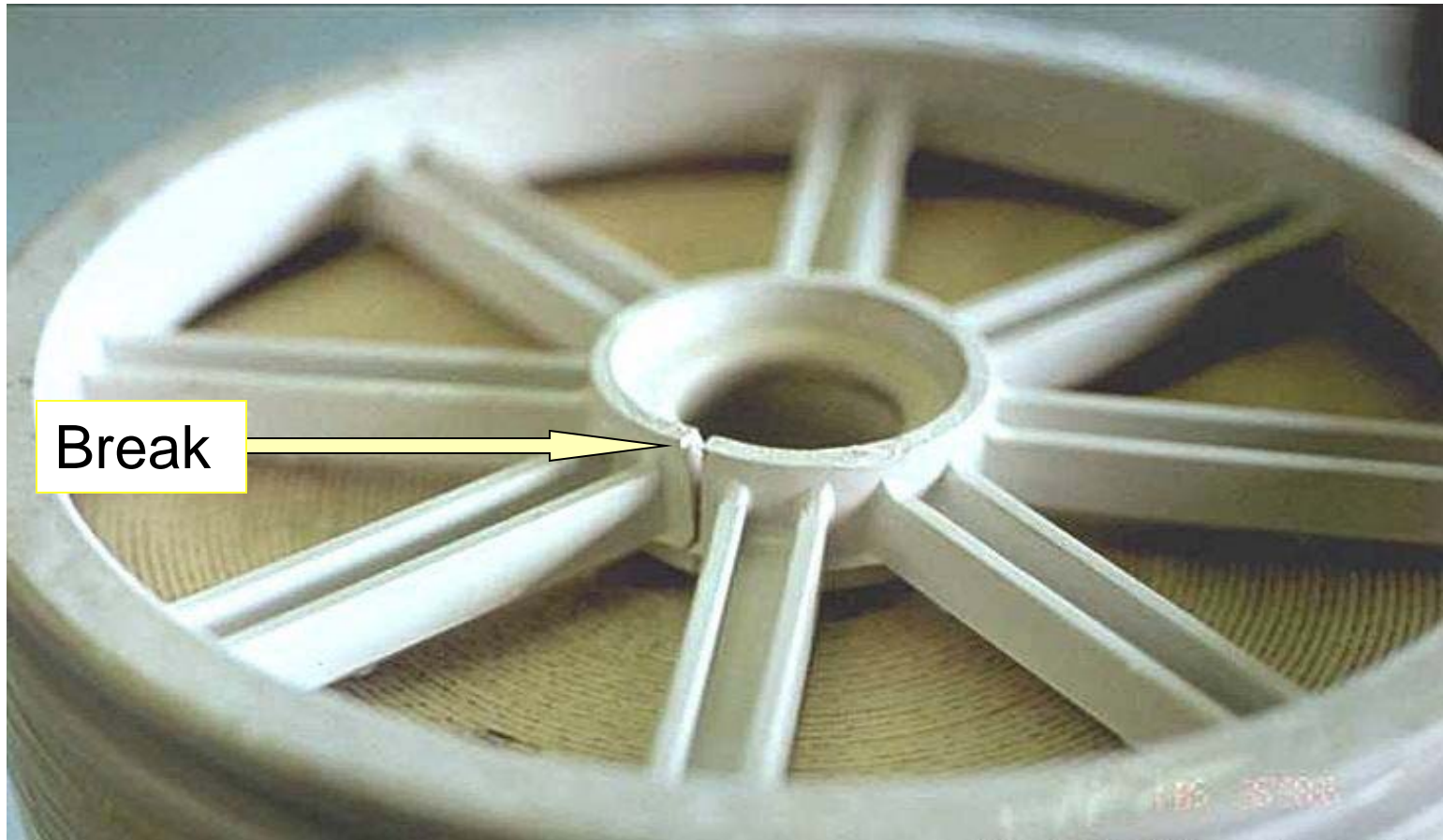
Axial displacement of the scroll by high pressure differential feed-concentrate caused by

- Water hammer
- High feed flow rate
- Feed channel plugging
- Missing thrust rings





Telescoping





Mechanical Damages

Intrusion of the membrane
/Collapsing in the permeate
carrier/Compaction ⇒ Flux loss

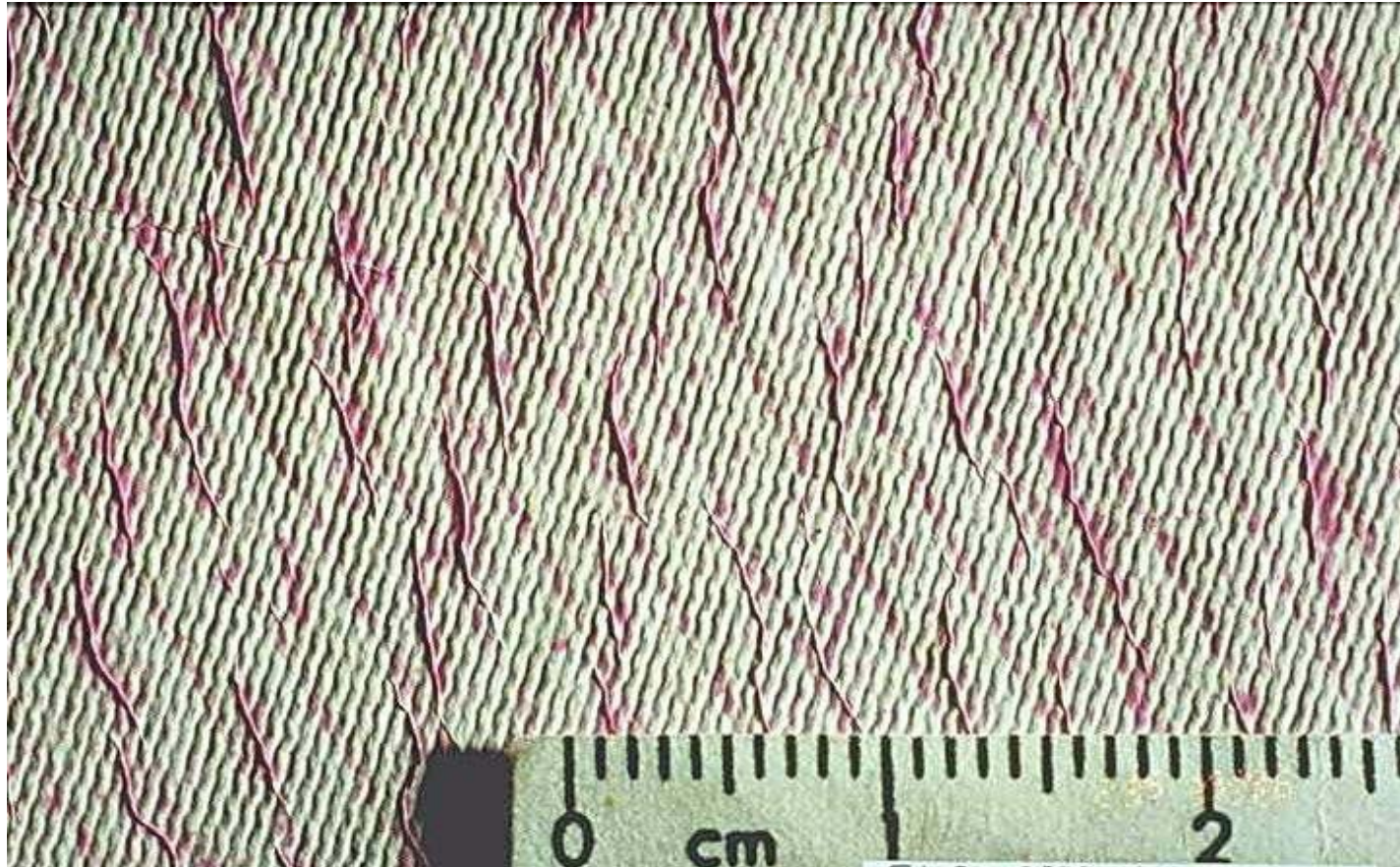
Can be originated by:

- Water hammer
- Too high pressure
- Too high temperature





Intrusion of the membrane





Mechanical Damages

Permeate backpressure damage

⇒ Increased salt passage

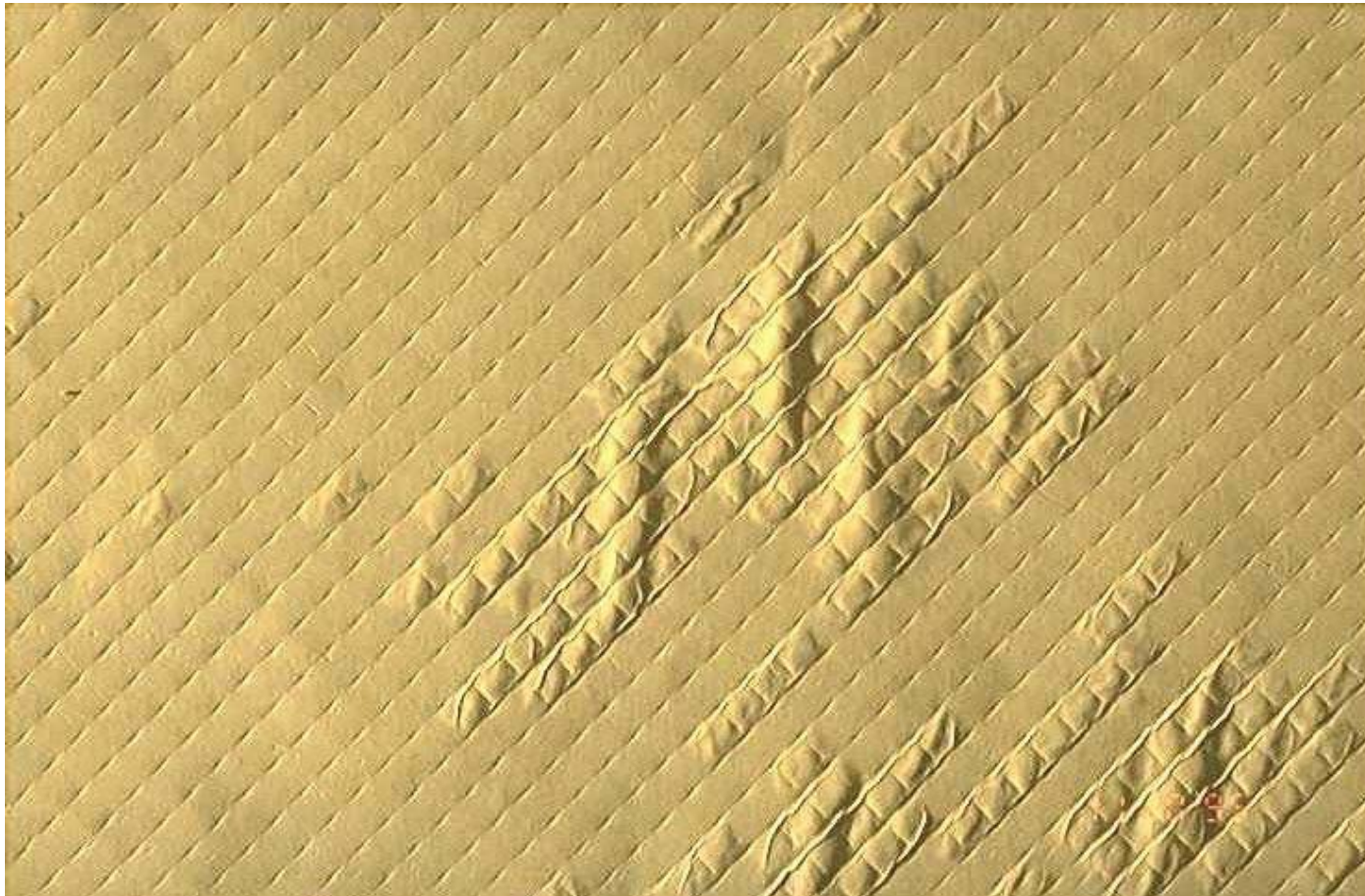
Delamination and tearing of the membrane

- if permeate pressure $>$ concentrate pressure
- typically during shut-down
- typically tail-end elements affected
- can be localized by probing
- positive leak test of element





Permeate backpressure damage





Effect on membrane performance if something goes wrong

- Fouling / Scaling
- Mechanical damages
- **Chemical damages**





Chemical Damages

■ From Chemicals

- in feed water
- in cleaning solutions
- in disinfecting solutions
- in preservation solutions

- Strong acids (pH<1)
- Strong alkalines (pH>13)
- Solvents

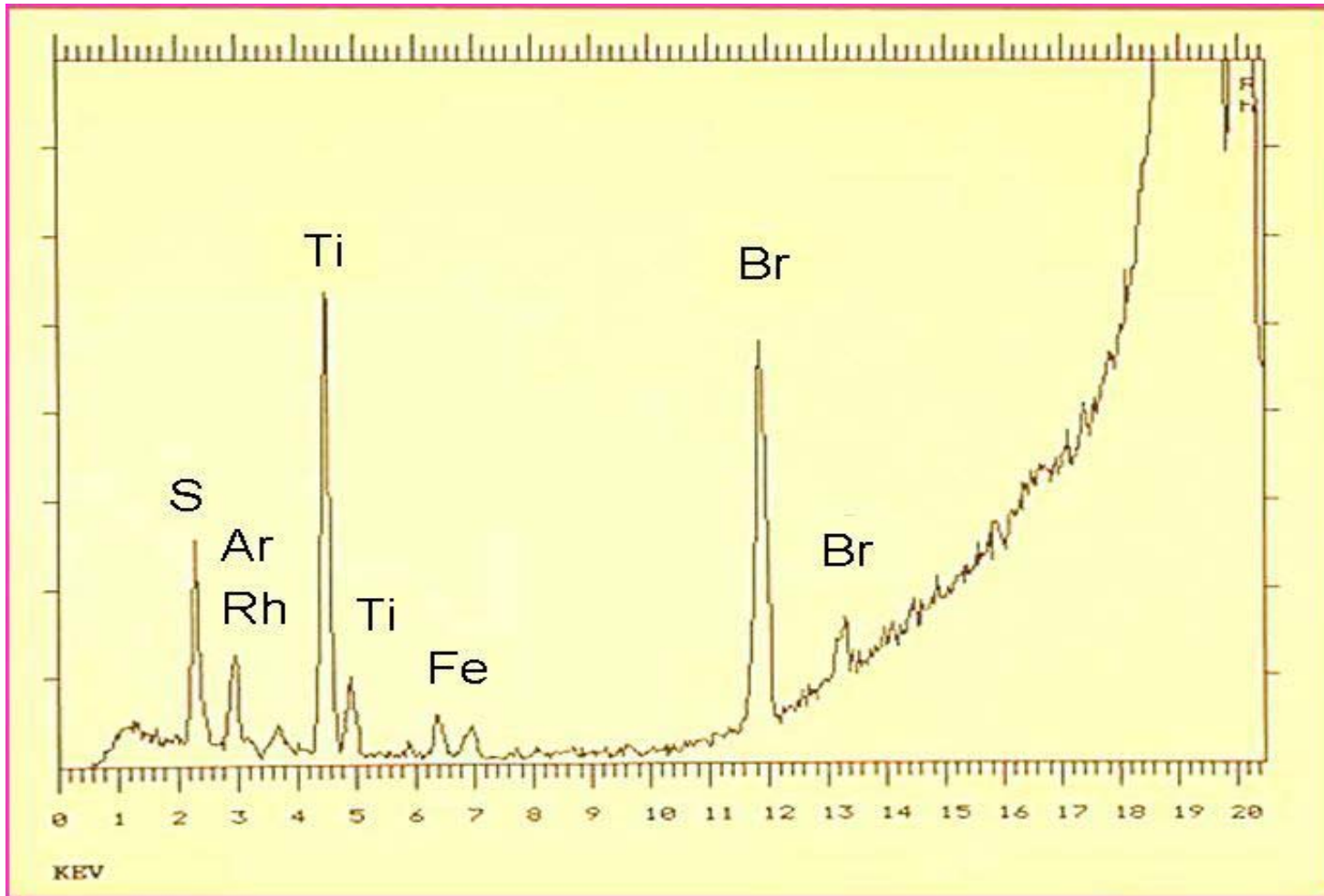
■ Oxidation of the barrier layer by

- free chlorine
- other oxidizing agents





Oxidation damage





Chemical Damages

■ From Chemicals

- in feed water
- in cleaning solutions
- in disinfecting solutions
- in preservation solutions

- Strong acids (pH<1)
- Strong alkalines (pH>13)
- Solvents

■ Oxidation of the barrier layer by

- free chlorine
- other oxidizing agents

Correction: Membrane replacement

Prevention: Dechlorination, ORP control, chemicals selection





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Problem area: Feed water/Pretreatment

- Feed water quality may change





Problem area: Feed water/Pretreatment

- Feed water quality may change
- Potential problems with dosing chemicals:
 - Dosing failure
 - No coupling of the dosing pump to the main plant
 - Over/under dosage
 - Missing / wrong / poor quality chemicals
 - Aged chemicals
 - Biological growth in stock solution
 - Insufficient mixing
 - Insufficient retention time





Problem area: Feed water/Pretreatment

- **Potential problems with flocculation:**
 - Too small flocs - carry over
 - Wrong type of flocculant / polymer
 - ◆ not efficient
 - ◆ not compatible with membrane, e.g. cationic polymers
 - Improper dosage of flocculant / polymer
 - ◆ Concentration
 - ◆ Dosing point: distribution, turbulence
 - ◆ Retention time
 - Improper pH control
 - Reaction of polymers with scaling inhibitors





Problem area: Feed water/Pretreatment

- **Potential problems with pre-filtration**
 - Breakthrough of particles due to
 - ◆ Wrong design
 - ◆ Discontinuous flow rate
 - ◆ Insufficient rinse-out
 - ◆ Too large pore size (cartridge filter)
 - ◆ Wrong filter media or size
 - ◆ Ineffective backwashing
 - ◆ Broken collectors





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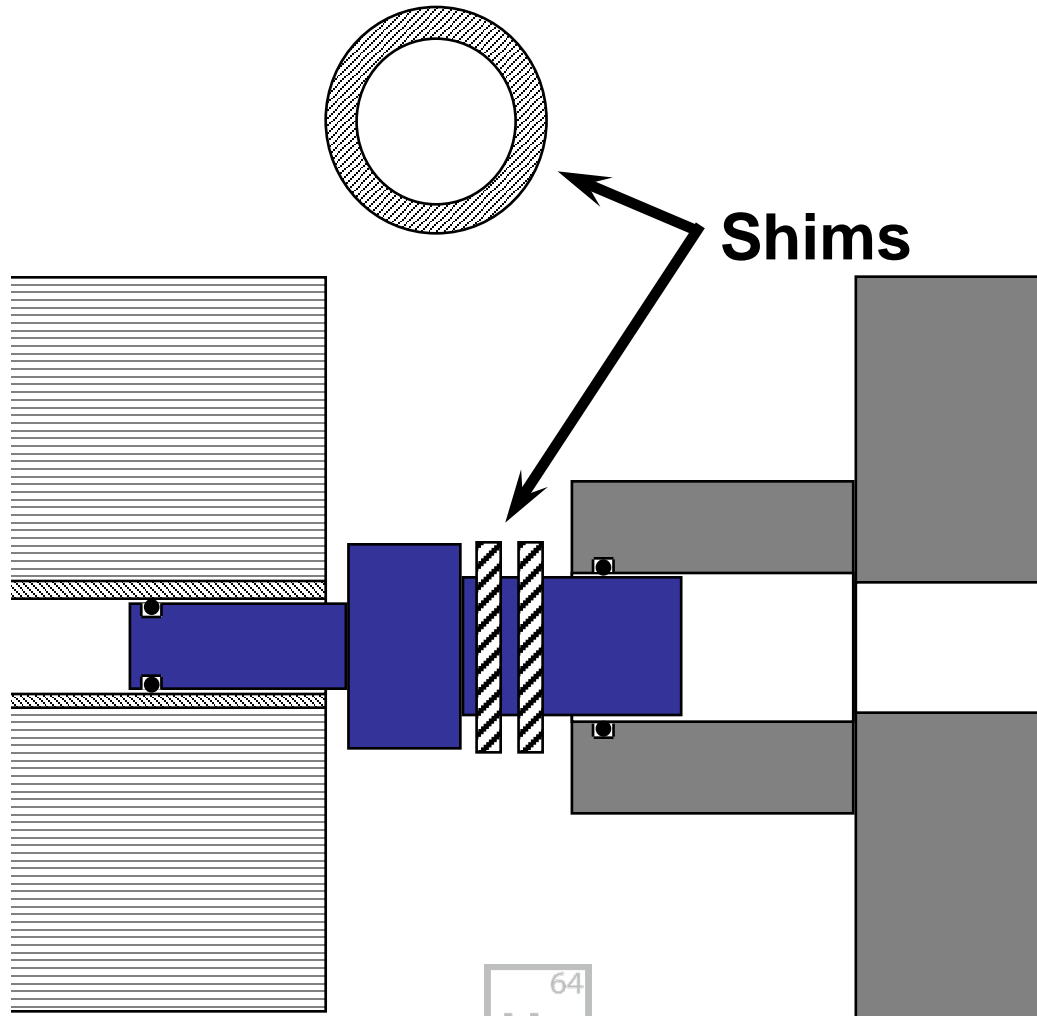
Problem area: plant operation

- **Storage and installation of membrane elements**
 - Improper storage leads to drying out or fouling of the membranes
 - Improper installation can result in mechanical damage to O-rings, interconnectors or permeate water tube
 - Lack of shimming can lead to leakage or membrane mechanical damage





Shimming





Problem area: plant operation

- Potential problems at start-up
 - Water hammer, when the high pressure pump is started with residual air in the system





Start-up with air in system





High pressure drop / water hammer





Problem area: plant operation

- **Potential problems at start-up**
 - Water hammer, when the high pressure pump is started with residual air in the system
 - Too high system recovery ⇒ Scaling
 - Unstable pre-treatment ⇒ leaking foulants or oxidants onto the membranes.





Problem area: plant operation

- **Potential problems during normal plant operation**
 - excessive feed pressure to compensate for reduced flux, results in membrane intrusion or fouling
 - frequent start/stop operation
 - too high recovery e.g. when the feed water changes, can result in scaling
 - irregular cleaning
 - insufficient pre-treatment
 - no performance evaluation





Problem area: plant operation

- **Potential problems during shut-down**
 - Residual pre-treatment chemicals (e.g. scale inhibitors) may precipitate in the system ⇒ flush with high quality water
 - Air entering the system can lead to a water hammer upon start-up ⇒ vacuum breaker
 - A pressurized permeate line may cause a permeate backpressure damage ⇒ check valve, pressure relief valve





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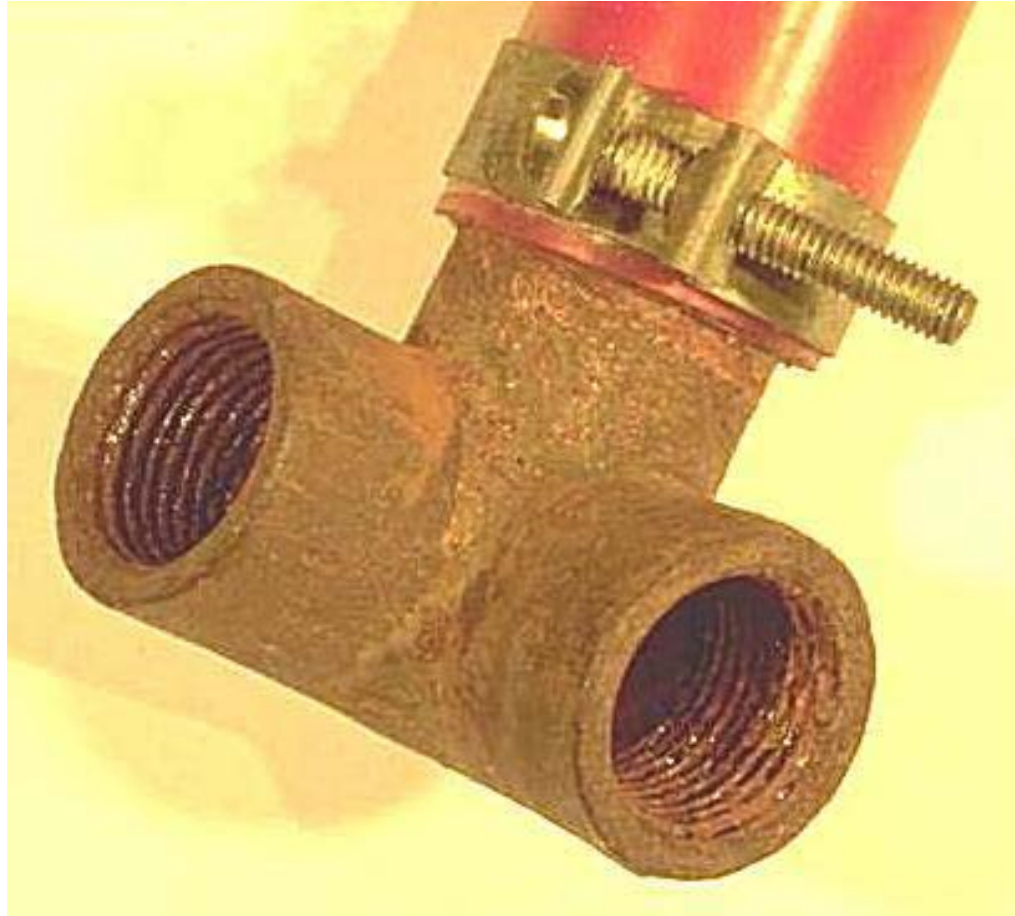
Problem area: system components

- **Pumps**
 - Impeller deterioration releases shavings onto the lead elements
 - Excessive pulsations can cause mechanical damage
- **Instrumentation**
 - Faulty, missing or wrongly calibrated
- **Pressure vessels**
 - Too small diameter double side ports ⇒ poor flow distribution
⇒ scaling / fouling
 - Incorrect end adaptors ⇒ leakage / membrane delamination
- **Corrosion**
 - Improper material selection ⇒ metal oxide fouling





Corrosion





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6. Troubleshooting Summary

| Source of problems | Effect on membranes | Symptoms observed | | | Corrective measures |
|---|--------------------------------|-------------------|---------------------|---------------|-------------------------------|
| | | Permeate Flow | Permeate Salt conc. | Pressure Drop | |
| Feed water | Scaling, fouling | ↓ | ↑ | ↑ | Clean |
| | Mechanical damage (compaction) | ↓ | ↓ | Normal | Replace elements |
| Pre-treatment: chemical dosing, Floc, lime, resin | Scaling, fouling | ↓ | ↑ | ↑ | Clean or replace elements |
| Pre-treatment: chemical dosing | Oxidative damage | ↑ | ↑ | Normal | Replace elements |
| Pre-treatment: pre-filtration | Colloid fouling | ↓ | ↑ | ↑ | Clean or replace elements |
| Plant operation: storage | Biofouling, incomplete wetting | ↓ | Normal | ↑ | Clean / re-wet |
| Plant operation: installation, start-up | Leaks, mechanical damage | Normal | ↑ | Normal or ↑ | Repair leaks/replace elements |
| Plant operation: control | Scaling, fouling | ↓ | ↑ | ↑ | Clean |
| Plant operation: shut-down | Biofouling, sulfur fouling | ↓ | Normal | ↑ | Clean |



Corrective Measures

- FILMTEC™ membranes and element components can be very effectively **cleaned** due to their pH and temperature resistance. However, if cleaning is delayed, it becomes increasingly difficult to remove foulants from the membrane surface. Cleaning will be more effective if it is tailored to the specific fouling problem.
- Oxidized or Mechanically Damaged Elements cannot be restored as the membrane has been irreversibly damaged. The elements need to be **replaced**. Elements with moderate telescoping may be still usable.





| Problem | Corrective measures | Prevention possibilities |
|-----------------|---------------------|---|
| Biofouling | Clean | <p>Renew old preservation solution for stored membranes.</p> <p>Check feed water for biofouling potential.</p> <p>Shock treat feed stream with non-oxidizing biocide or SBS during normal operation for limited time.</p> <p>Consider installing bioreactor upstream.</p> <p>Use micro/ultrafiltration to remove micro-organisms.</p> <p>Install fouling resistant (FR) elements.</p> |
| Scaling | Clean | <p>Check feed water for scaling potential at current system recovery.</p> <p>Analyze feed water, permeate and concentrate for potential scaling ions.</p> <p>Inspect concentrate side of system for scaling.</p> <p>Install or optimize acid or antiscalant pre-treatment.</p> <p>Add ion exchange or lime softener. Preventative regular cleaning/flushing.</p> <p>Lower recovery to eliminate precipitation risk.</p> |
| Organic fouling | Clean (difficult) | <p>Add pre-treatment if feed water TOC > 3 mg/L.</p> <p>Install/optimize coagulation, UF or active carbon.</p> <p>Coagulation / active carbon if oils & greases > 0.1mg/L.</p> <p>Consider oil/water separators as pretreatment.</p> |





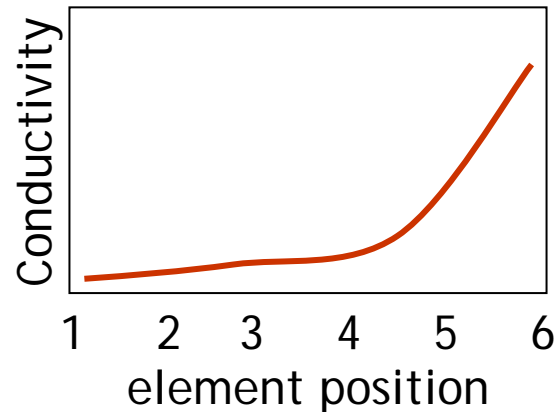
| Problem | Corrective Measures | Prevention possibilities |
|--------------------------|---------------------|--|
| Particle/Colloid fouling | Clean (difficult) | Replace corroded system components. Install or optimize pre-filtration pretreatment. Add coagulation/flocculation for Fe and colloids. Poor pre-treatment may be partly compensated by more frequent and/or harsher cleaning. |
| Mechanical Damage | Replace elements | Eliminate high pressure/water hammer (air in system) to avoid telescoping, compaction or product water tube damage. For surface abrasion: flush line and install cartridge filtration. For delaminated membranes, eliminate source of high static permeate backpressure. Develop protocol for correct element installation. |
| Oxidative damage | Replace elements | Remove oxidizing chemicals upstream of membranes e.g. SBS dosing. Add activated carbon filter. Replace corroded system components (metals act as oxidative catalyst). |
| Leaks | Repair or replace | Remove source of water hammer if appropriated. Develop program to inspect and replace old O-rings. Develop protocol for correct element installation. Profiling, probing. |





Example

- High permeate conductivity suddenly after the plant start up
- By probing high conductivity was localized at the rear elements of the second stage. (The plant has 2 stages.)



- Bubble test of rear elements gave a positive result (bubbles appeared from the scroll).





Example - Autopsy

| Element | Flow [m ³ /d] | Rejection [%] | ΔP [bar] |
|---------|--------------------------|---------------|------------------|
| Nominal | 47.8 | 99.3 | 0.3 |
| Example | 46 | 90 | 0.6 |

Problem: Too high back-pressure as a result of improper shut down procedure.

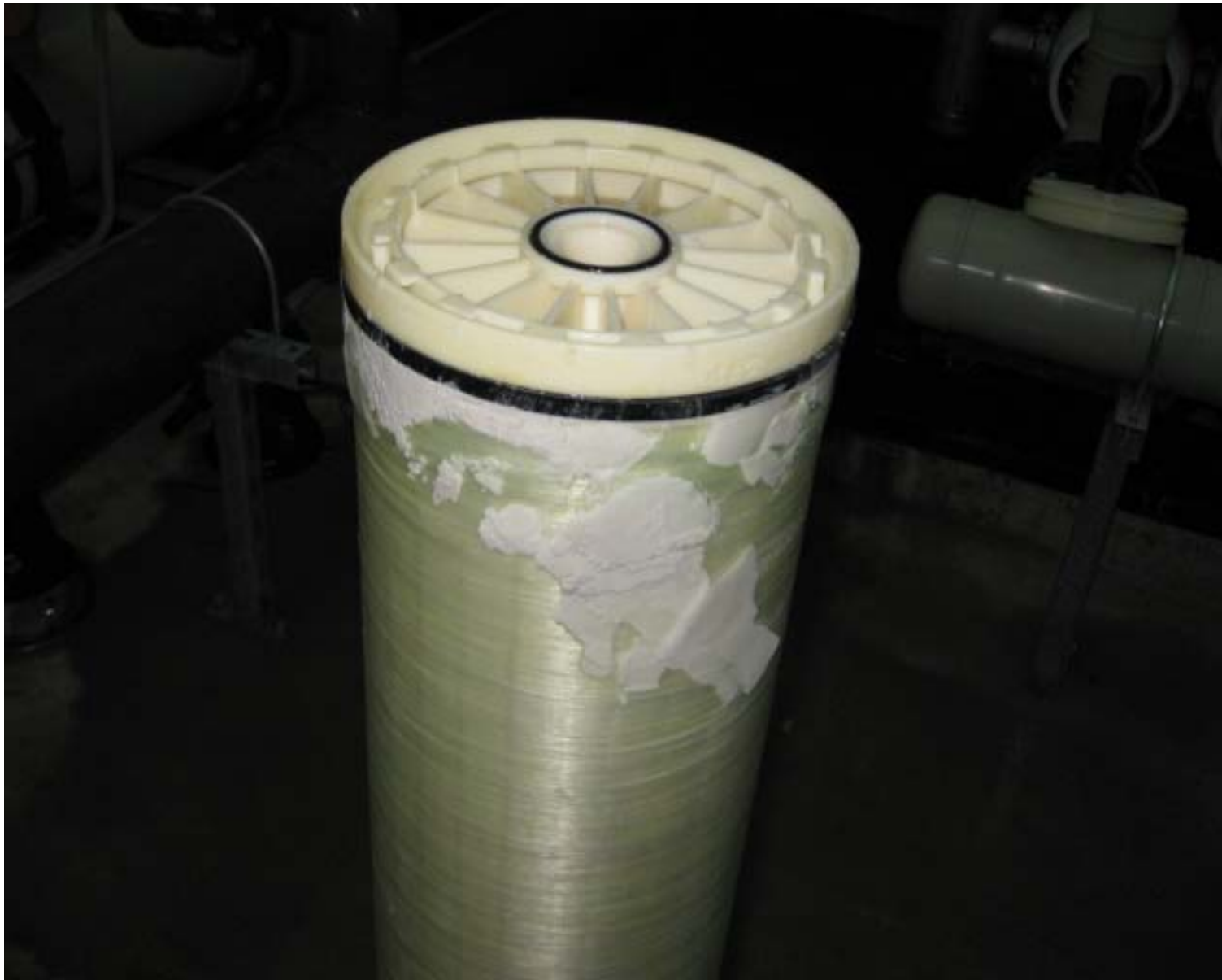




Example: Scaling

| Membrana | Peso (kg) |
|-----------------|------------------|
| F3013503 | 24 |
| F3013352 | 25.5 |
| F3013348 | 31 |
| F3013508 | 30.5 |
| F3151704 | 31 |
| F2915947 | 23 |
| Normal | 14-15 |





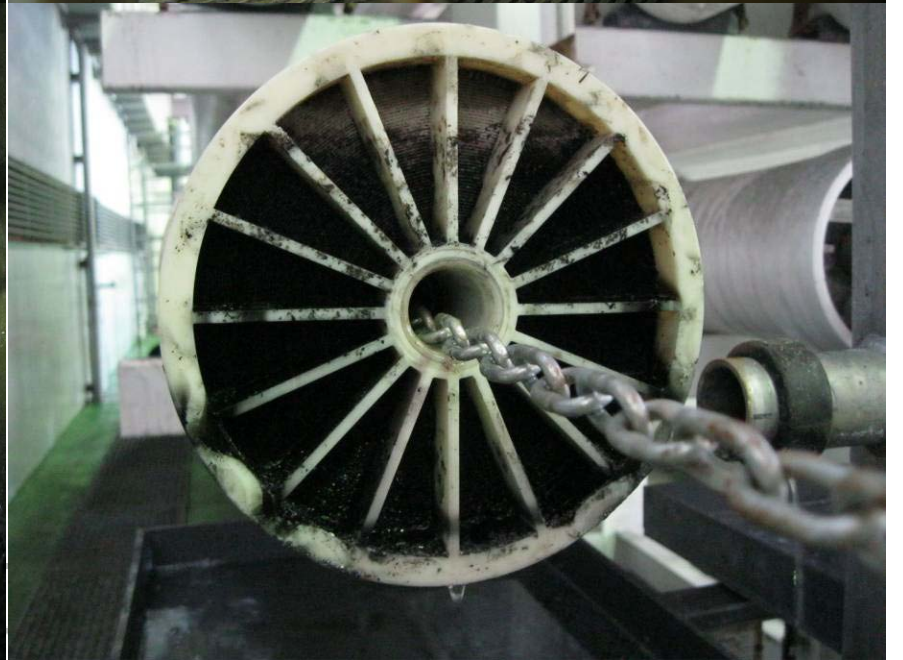


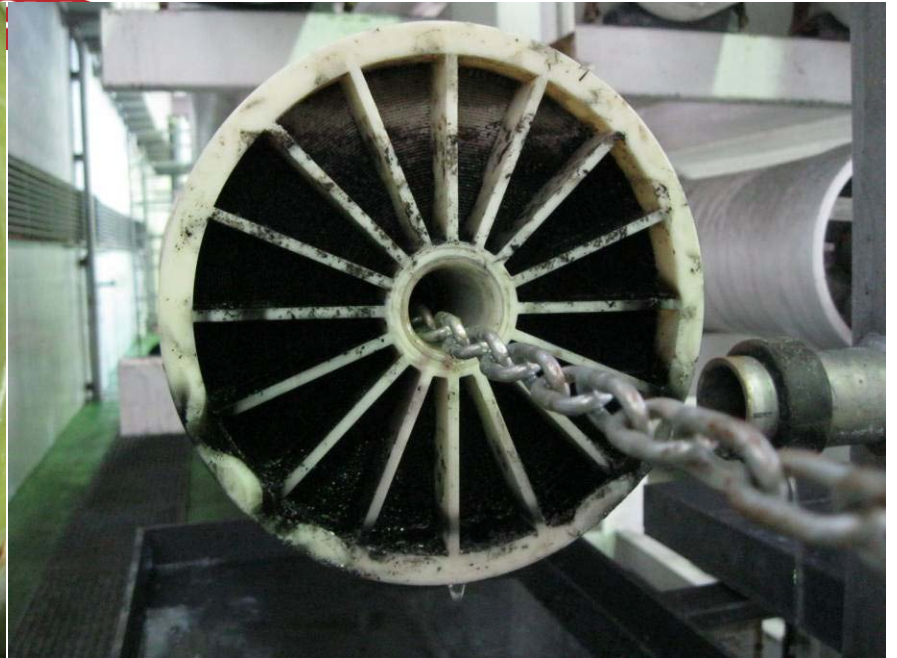


Example: Fouling / Scaling











Membranes in service 2003 -2010





We wish you a trouble free
operation of your membranes!



Water & Process Solutions

