ENV H 440/ENV H 541

Wastewater treatment processes (II)

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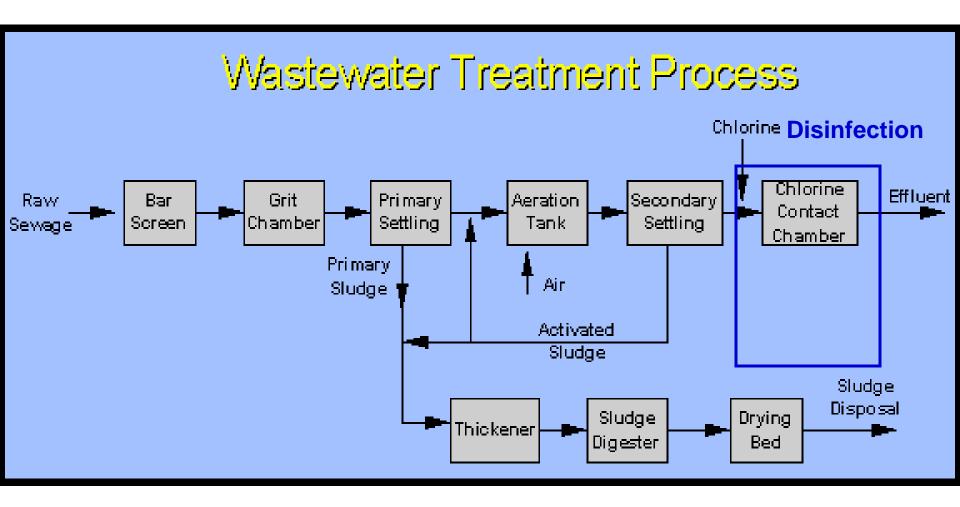
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Wastewater Disinfection



Wastewater disinfection

- To inactivate pathogens in wastewater
- Several choices
 - Free chlorine and combined chlorine
 - UV
 - Ozone
 - Chlorine dioxide

Chlorination

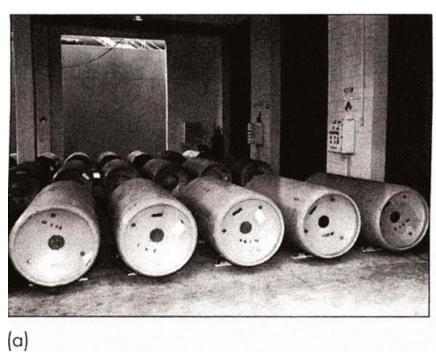
Free chlorine - Chemistry

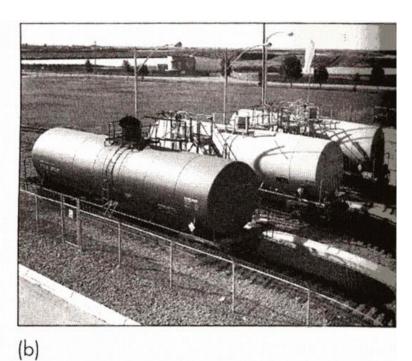
- Three different methods of application
 - $-Cl_2$ (gas)
 - NaOCl (liquid)
 - Ca(OCl)₂ (solid)
- Reactions for free chlorine formation:

$$Cl_2(g) + H_2O <=> HOCl + Cl^- + H^+$$

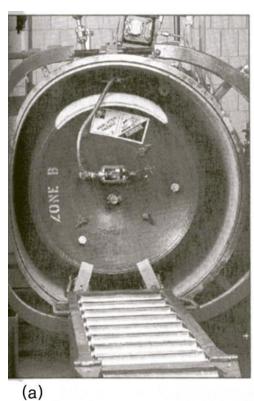
HOCl <=> OCl^- + H^+ (at pH >7.6)

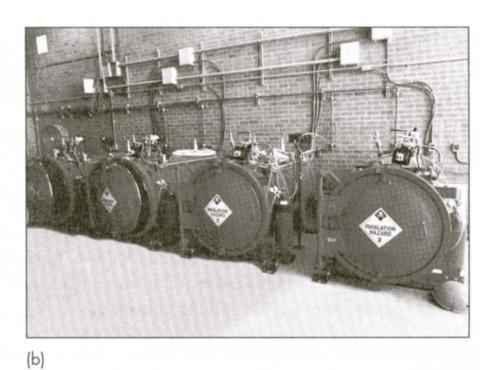
Chlorine application (I)



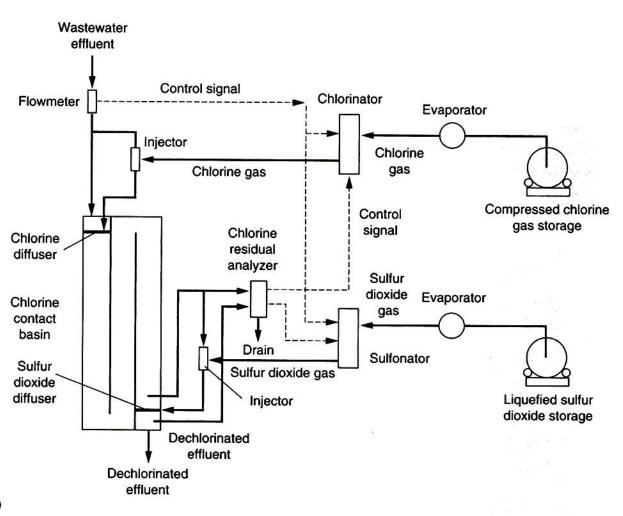


Chlorine application (II)





Chlorine application (III): Gas



Chlorine application (IV): Mixing

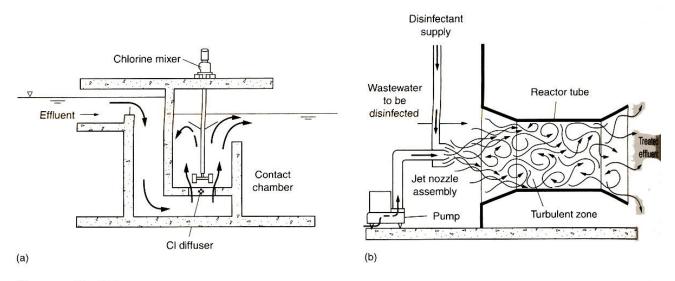


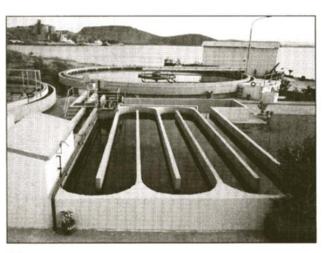
Figure 12-22

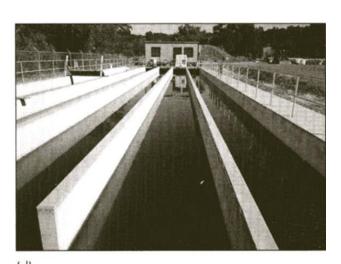
Typical mixers for the addition of chlorine: (a) in-line turbine mixer and (b) injector pump type. (From Pentech-Houdaille.) for additional types of chlorine mixers see Fig. 5–14 in Chap. 5.

Chlorine application (V): Contact chambers (I)

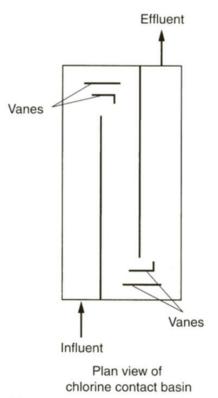


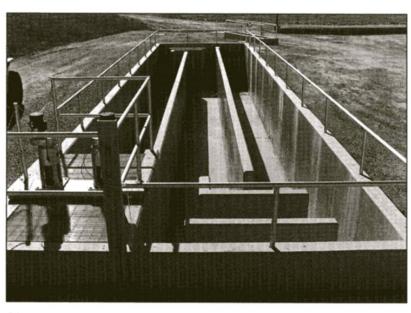






Chlorine application (VI): Contact chambers (II)





(b)

(a)

Chlorination in drinking water

• Reactions for free chlorine formation:

$$Cl_2(g) + H_2O <=> HOCl + Cl^- + H^+$$

HOCl <=> OCl^- + H^+ (at pH >7.6)

Chlorination in wastewater

- Dynamic chloramination
 - Reaction of free chlorine and ammonia in situ
- Chloramine formation
 - $HOCl + NH_3 <=> NH_2Cl + H_2O$
 - $-NH_2Cl + HOCl <=> NHCl_2 + H_2O$
 - $-NHCl_2 + HOCl <=> NCl_3 + H_2O$
 - $-\frac{1}{2}$ NHCl₂ + $\frac{1}{2}$ H₂O <=> $\frac{1}{2}$ NOH + H⁺ + Cl⁻
 - $-\frac{1}{2}$ NHCl₂ + $\frac{1}{2}$ NOH <=> $\frac{1}{2}$ N₂ + $\frac{1}{2}$ HOCl + $\frac{1}{2}$ H⁺ + $\frac{1}{2}$ Cl⁻

Breakpoint Reaction for Chlorine

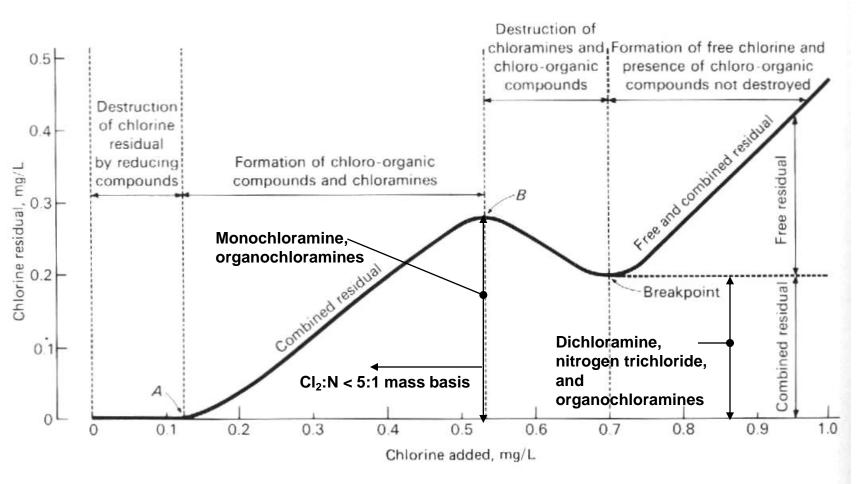


Figure 7-14 Generalized curve obtained during breakpoint chlorination. Note: $mg/L = g/m^3$.

Ref: Metcalf & Eddy, Inc., 1979. Wastewater Engineering, Treatment and Disposal. McGraw-Hill, New York.

Total and combined chlorine

- Total chlorine = free chlorine + combined chlorine
- Combined chlorine = inorganic chloramines (monochloramine, dichloramine, nitrogen trichloride) + organic chloramines

Wastewater chlorination

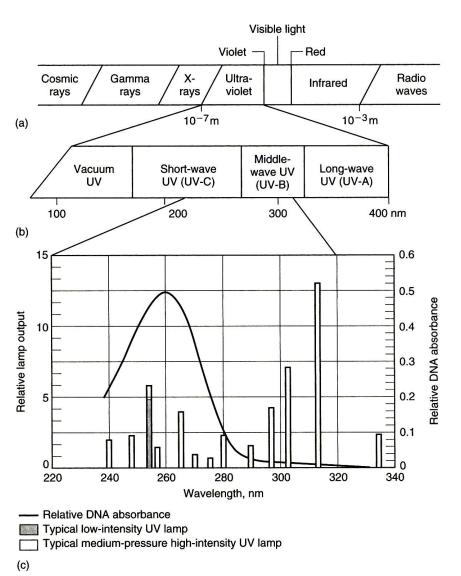
- To inactivate pathogens in wastewater
- Dynamic chloramination and breakpoint chlorination
- 5 20 mg/L for 30 minutes
- > 99.99 % reduction of total and fecal coliforms, ~90 % reduction of enteric viruses, ~50% reduction of *Giardia lamblia* cysts, but <10 % reduction of *Cryptosporidium parvum* oocysts

Dechlorination

- Chlorine and monochloramine are very toxic to aquatic life in the receiving stream.
- Neutralization of chlorine
 - Sulfur dioxide (gas)
 - Sodium metabisulfite (liquid)
 - UV irradiation

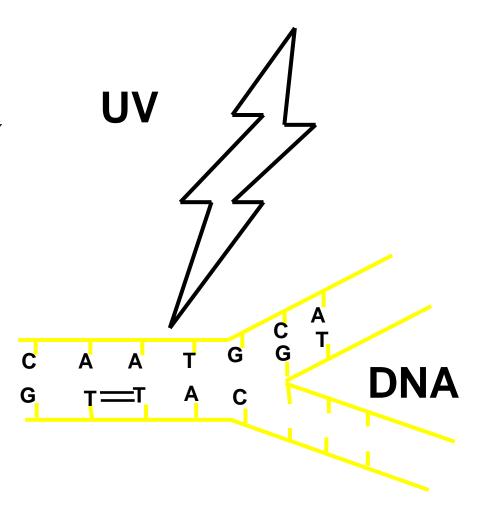
UV irradiation

Spectrum of radiations



Ultraviolet irradiation

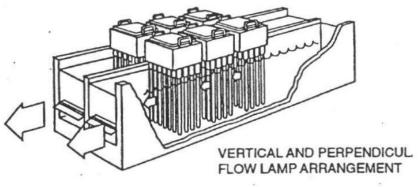
- Physical process
- Energy absorbed by DNA
 - pyrimidine dimers,strand breaks, otherdamages
 - inhibits replication



UV disinfection – UV lamps

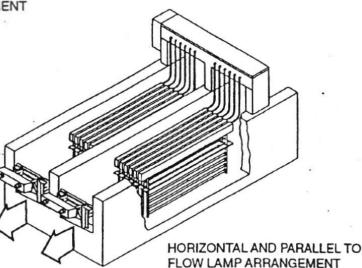
- Low pressure (LP) UV lamps
 - Wavelength at 254 nm
 - Low intensity
- Medium pressure (MP) UV lamps
 - Wavelengths between 100-1000 nm
 - High intensity
- Pulsed UV lamps
 - Intermittent emission
 - High intensity

UV application (I): configuration

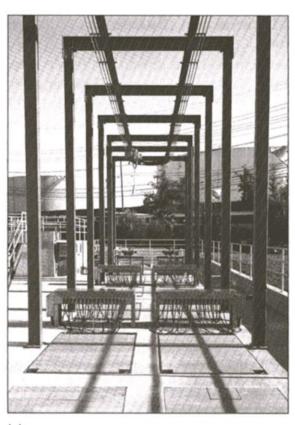


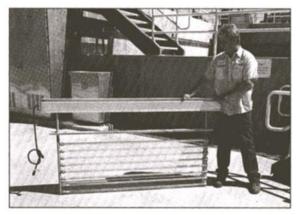
See next few slides for pictures of UV units

Typical Contactor Configurations



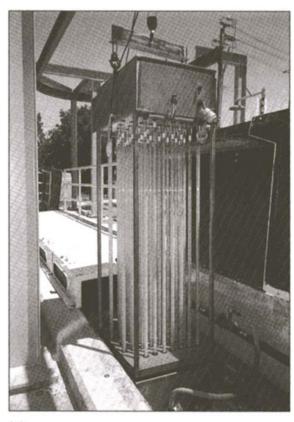
UV application (II): LP UV with vertical arrangement





(a) (b)

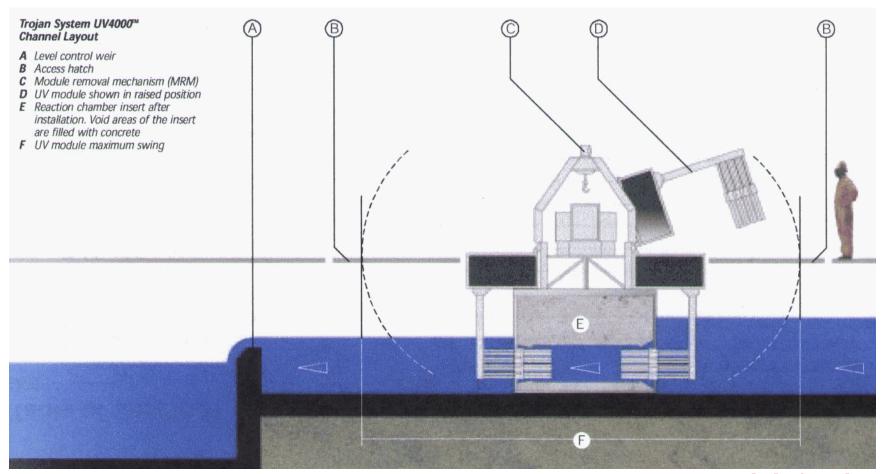
UV application (III): LP UV with horizontal arrangement





UV application (**IV**): **MP UV** (**I**)

Closed-channel, horizontal, parallel to flow Medium pressure, high-intensity lamps Automatic cleaning



UV application (V): MP UV(II)



Closed-channel, horizontal, parallel to flow (Trojan)

Raised UV Lamp Unit



Disinfection

UV disinfection in wastewater

- To inactivate pathogens in wastewater
- LP, LPHO, or MP UV lamps
- 40 mJ/cm²
- Similar level of reduction for total and fecal coliforms, and enteric viruses, but a lot higher level of reduction for Giardia lamblia cysts and Cryptosporidium parvum oocysts

Advanced treatment

(Minimum) Goals of wastewater treatment processes

- $<30 \text{ mg/L of BOD}_5$
- <30 mg/L of suspended solids
- <200 CFU/100ml of fecal coliforms

Limitation of conventional wastewater treatment

- Low reduction of phosphorus and nitrogen (ammonia)
- No removal of soluble nonbiodegradable chemicals
- Variable removal rate of heavy metals, and toxins

The effect of contaminants

- Phosphorus and nitrogen: eutrophication
 - Excessive growth of algae
 - Depletion of dissolved oxygen
 - Release of foul smell
 - Death of fish species
- Soluble organic and inorganic chemicals
 - Aesthetic problems (foam and colors)
 - Harmful to aquatic life and human (bioaccumulation)

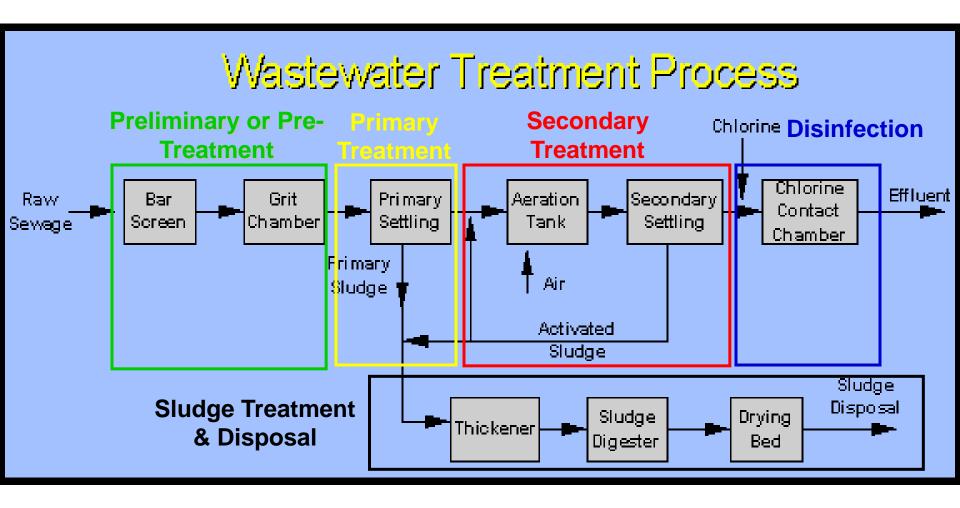
Removal of phosphorus

- The common forms of phosphorus in wastewater
 - Orthophosphates (PO₄³⁻)
 - Polyphosphates
 - Organically bound phosphates
- Phosphorus removal in conventional wastewater treatment
 - Incorporation into the biomass for bacterial growth
 - Overall 20-40% removal of influent phosphorus

Chemical-biological phosphorus removal

- Chemical precipitation (w/ aluminum and iron coagulants)
 - Orthophosphates (PO₄³⁻)
 - $Al_2(SO_4)_314.3H_2O + 2 PO_4^{3-} = 2 AIPO_4 \downarrow + 3 SO_4^{2-} + 14.3H_2O$
 - $FeCl_3 6H_2O + PO_4^{3-} = FePO_4 \downarrow + 3 Cl^{-} + 6 H_2 O_3$
 - Polyphosphates and organically bound phosphates (entrapped or adsorbed in flocs)
- Variable reduction of phosphorus depending on the alum-phosphorus weight ratio
 - 13: 1 (75%), 16: 1 (85%), and 22:1 (95%)
- Point of application
 - Prior to primary clarification
 - Directly to biological process
 - Prior to final clarification

Typical Municipal Wastewater Treatment System



Removal of nitrogen

- The common forms of nitrogen in wastewater
 - Ammonia
 - Nitrate
 - Nitrite
 - Gaseous nitrogen
 - Organic nitrogen
- Nitrogen removal in conventional wastewater treatment
 - Sedimentation: 15%
 - Uptake in subsequent biological process: 10%
 - Overall 25% removal of influent nitrogen

Biological nitrification and denitrification

- Organic nitrogen compound → NH₃ (in sewer)
- $NH_3 + O_2 \rightarrow NO_3^-$: aerobic nitrification
- $NO_3^- + AH_2 \rightarrow A + H_2O + N_2$: denitrification

Nitrification Process

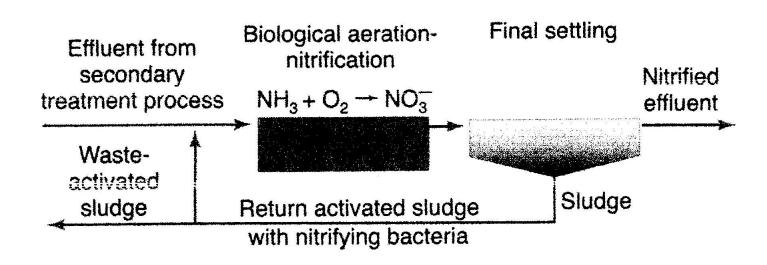


Figure 13-14

Flow diagram for nitrification by suspended-growth aeration following conventional biological treatment.

Operating conditions for nitrification

- Temperature: > 8°C
- Optimum pH: 8.4
- Dissolved oxygen level: >1.0 mg/L
- Ammonia nitrogen loading: 160-320 g/m³/day
- Aeration period: 4-6 hours

Nitrification plant

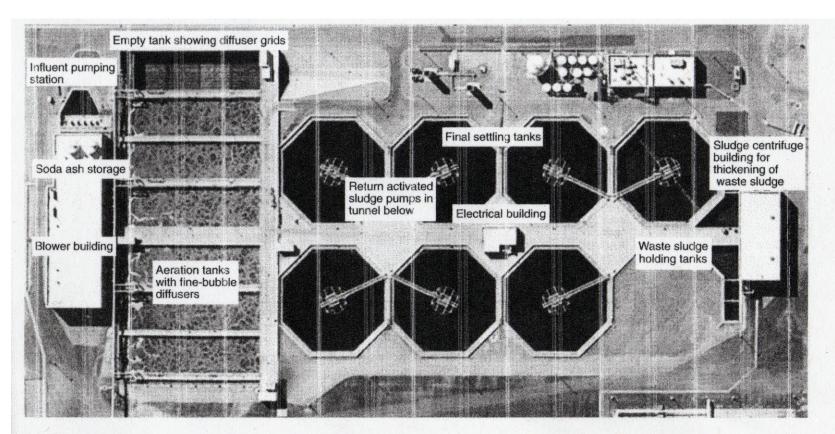


Figure 13-15

Processing arrangement for nitrification by suspended-growth aeration. City of Las Vegas Water Pollution Control Facility, Nevada.

(Courtesy of the C ty of Las Vegas, NV.)

Denitrification reaction

- Methanol is used as a carbon source
- $5CH_3OH + 6NO_3^- = 3 N_2 \uparrow + 5 CO_2 \uparrow + 7H_2O + 6OH^-$
- Mechanically mixed anoxic chambers
- Nitrogen stripping in the last chamber
- Detention time 2-4 hours

Denitrification process

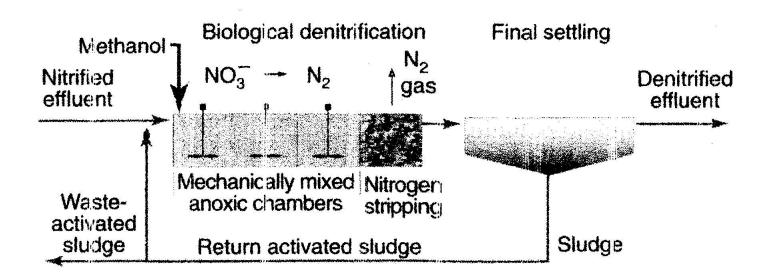


Figure 13-17

Flow diagram for denitrification by anoxic suspended growth following nitrification.

Soluble organic and inorganic chemicals

- Best removed at the source of origin
- Partially removed by entrapment and adsorption onto settable solids and biological flocs
- In water reclamation plants, these materials are removed by highly advanced processes such as membrane filtration and advanced oxygenic processes (O₃, UV and so on)