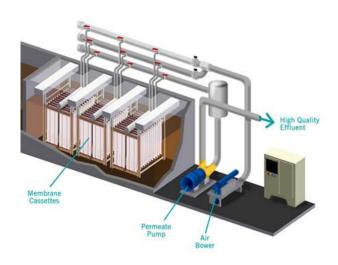
Advanced Water Treatment

Course # 3110





Fleming Training Center March 4 – 8, 2013

http://www.tn.gov/environment/fleming/



Fleming Training Center

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Fleming Training Center



Your Partner in Clean Water http://tn.gov/environment/fleming

Advanced Water Treatment

Course # 3110

March 4-8, 2013

| Monday | <u>, March 4:</u> |
|--------|-------------------|
| | |

| 8:30 Filters - C | Optimization and Performance | Amanda Carter |
|------------------|------------------------------|---------------|
|------------------|------------------------------|---------------|

11:00 LUNCH

12:15 Filters - Troubleshooting and Math Amanda

Tuesday, March 5: 0.20

| 8:30 | Pumps | Amanda |
|-------|--------------------------|--------|
| 9:00 | Part Identification | Amanda |
| 10:30 | Preventative Maintenance | Amanda |
| 12:00 | LUNCH | |

1:15 **Bacteriological Sampling and Plans** Amanda 2:30 Algae Identification Amanda

Wednesday, March 6:

| 8:30 Membrane Filtration | Amanda |
|--------------------------|--------|
|--------------------------|--------|

11:00 LUNCH

1:30 Tour- Duck River WTP

Thursday, March 7:

| 8:30 | Fluoridation | Amanda |
|-------|--------------|--------|
| 12:00 | Lunch | |
| 1:15 | EOP | Amanda |

Friday, March 8:

| 8:30 | Safety | Amanda |
|-------|----------------------------|--------|
| 9:45 | Review for Exam | Amanda |
| 11:00 | LUNCH | |
| 12:15 | Exam and Course Evaluation | Amanda |

Advanced Water Treatment

| Section 1 | Pumps Part Identification Preventive Maintenance Predictive Maintenance | Page 3 |
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| Section 2 | Filters Optimizing and Performance Troubleshooting Math | Page 31 |
| Section 3 | Membrane Filtration Science and Theory Operations Pilot Studies Regulations | Page 117 |
| Section 4 | Bacteriological Sampling & Plans | Page 141 |
| Section 5 | Fluoride Health Benefits Regulations Additives Lab Analysis Equipment | Page 149 |
| Section 6 | Emergency Operation Plans | Page 189 |
| Section 7 | Algae Identification | Page 205 |
| Section 8 | Safety General Safety Personal Protective Equipment Chlorine Safety | Page 215 |

Section 1

Pumps
Part Identification **Preventive Maintenance Predictive Maintenance**

Pump Review

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Pump Types

- There are two main types used in water treatment:
 - Positive displacement
 - Used for small volumes
 - More accurate
 - Chemical feeders
 - Centrifugal
 - Used for big flows

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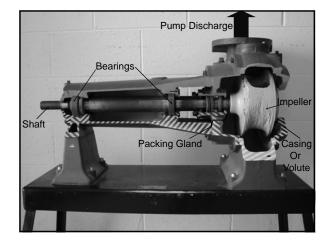
Centrifugal Pumps

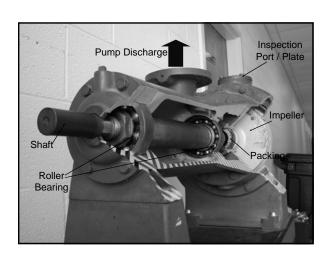
- Centrifugal pumps are velocity type pumps
- Most common type of pump found in water utilities
- Vary in size, shape and width of impeller
- Vary in a wide range of flows and pressures

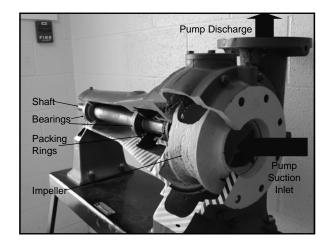
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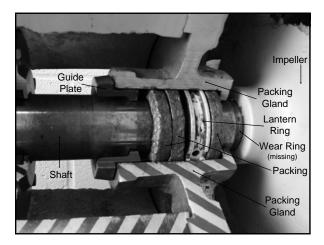
Centrifugal Pump Parts

- Centrifugal pumps consist of many rotating parts
- Three designs for impellers
 - Axial
 - Radial
 - Mixed



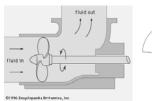






Axial Flow Design

• Propeller shaped impeller and adds head by lifting action on vanes







Radial Flow Design

- Flow from impeller is thrown outward
- Water enters from eye or center of impeller





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Mixed Flow Design

Impeller has both axial and radial flow design features combined

Mechanical Parts of Centrifugal Pumps

- Volute: the case or housing holding the impeller
 - Usually made of cast iron and spiral shape

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Mechanical Parts of Centrifugal Pumps

 Foot valve: a check valve placed in the bottom of the suction pipe which allows water to enter the casing to hold prime

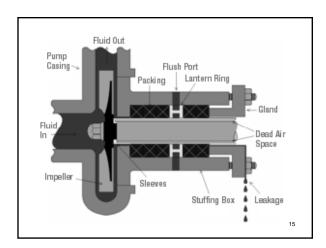


13

Mechanical Parts

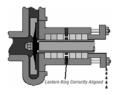
- Bearings: roller bearings support the pump shaft to guide rotation
- Packing: rings of graphite materials used to control leakage along the shaft
- Wear Rings: rings made of brass place on the impeller to control leakage of water from the the sides of the impeller

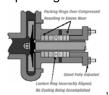
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Mechanicals Parts

 Lantern Ring: a small perforated ring placed around the shaft to form a liquid seal that lubricates the packing





Mechanicals Parts

- Mechanical Seal: a seal placed on the pump shaft to prevent leakage along the shaft and leak proof
 - Also prevent air from entering the pump





Pump Operation

- Cavitation: a condition where a partial vacuum forms near the impeller blade and the pump case causing a pinging sound to implode against the impeller
 - Will damage the impeller causing the pitting condition of the metal





Pump Conditions

- Water Hammer: the potential damage occurred from closing water valves to quickly
 - The sudden change in water direction or water velocity creates great water pressure

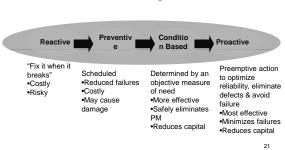
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Pump Maintenance

Preventive and Predictive Maintenance

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Operating Equipment Lifetime Management



Lifetime Maintenance Costs



Over 60% of equipment lifetime maintenance cost were caused by preventable errors during design, procurement, installation, operation and maintenance.

__

Definitions

- Preventive maintenance is a schedule of maintenance activities aimed at the preventing of pump breakdowns and failures.
 - It is designed to preserve and enhance equipment operations by equipment checks, system overhauls, oil checks and other detailed maintenance checks on equipment.

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Long Term Benefits of P/M

- Improved equipment reliability and longevity.
- Decrease in cost and replacement of parts.
- Decrease in down time of equipment.

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Breakdown Maintenance

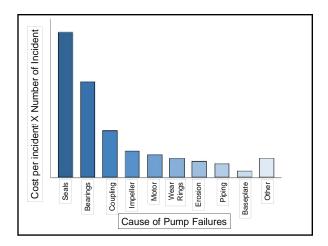
- Definition: includes the failure of equipment due to no Preventive maintenance measures
- Reasons for failures:
 - No planning of servicing equipment
 - No preventive measures, checks, service and monitors

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Breakdown Maintenance

- Cost of breakdowns
 - Loss time of the equipment
 - Dollar cost of parts repair or replacement
 - Customer service

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Breakdown Maintenance

Avoid the breakdown failure mode

- Bad operation habits
- Run to fail
- No P/M inspections
- No equipment checks by operators

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Goals of Preventive Maintenance

- Define P/M maintenance in your plant and establish some set goals of performance of equipment
- · Locate equipment needs
 - Look at a workable goal, start with something that can be achieved

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Goals of Preventive Maintenance

- Describe and assign P/M functions
 - Activities by operators
 - Activities by maintenance personnel
- Describe the P/M function of equipment
 - Perform P/M or SOP's
 - frequency of checks goals: week, month, year

Goals of P/M

- Define the scope of work and define the needs of maintenance or electrical work
- Establish the operations check on equipment operation
- Establish clear work goals. Focus on the frequency of equipment checks and historical trends of equipment
- Look at cost savings, increase run times
- · Savings on parts and energy cost

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Establish P/M Program

- Define the inspection check plan on equipment
- Define the frequency of inspection to a weekly or monthly inspection
- Define all the equipment involved or types of pumps, chlorine, feeders, chemicals, clarifiers, valves, water tanks, hydrants, meters

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Establish P/M



Locate
 equipment
 info on
 pump
 labels and
 tags

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Establish P/M

- Locate OEM (Original Equipment Manuals), catalogs and web sites
- Locate operations SOP's on equipment
- Establish preventive maintenance SOP on each equipment or pump
- Train personnel, operators and staff on P/M schedules

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P/M

- Record all P/m data, records on equipment and CMMS (Computer Management Maintenance Systems) files
- Create parts inventory listing
- Start a monthly list of P/M work orders to check equipment
- Start a weekly out of service inventory sheet for equipment, list causes and date to return to service

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Check List

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Preventive Maintenance Inspections

- Plan and schedule the work orders and seek your data on equipment
- Establish data recording levels of equipment settings, such as temperature and pressure settings
- · Set equipment parameters for data
- Establish parameters for oil measures and temperatures and other settings

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Inspections

- · Establish run times of equipment
- Decide weekly or monthly check and frequency
- Record data and historic trends of equipment
- After 6 months establish less breakdowns
- Last phase, trend equipment toward predictive maintenance and consult with vibration analysis, oils analysis or thermal inspection

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Predictive Maintenance

 Predictive maintenance will analyze equipment operations with a proactive predictive analysis of real time data of equipment operations and assessing the measurement technology available on equipment operations

> Not to be done by operator. Trained professionals are needed.

> > 39

Predictive Maintenance

- Predictive processes include:
 - Vibration analysis
 - Laser alignment
 - Ultrasonic test
 - Heat thermography
 - Oil analysis
- Predictive maintenance uses technology to predict equipment operations and maintenance schedules.

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Predictive Processes

- All pump and motors are tested for wear and run times of equipment for bearing wear
 - Laser alignment of pumps and motors for vibration analysis
 - Lubrication wear is tested for mineral deposits of bearing failure

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Predictive Processes

- · Down time failures are predicted and avoided
- Equipment conditioning to record on time telemetry of equipment run times and on line monitors
- Cost benefits of predictive maintenance to improve plant maintenance reduced failures and no downtimes
- Predictive processes can save money

Vibration Analysis



- Vibration analysis can identify defects such as:
 - Rotor unbalance,
 - Coupling misalignment,
 - Identify bearing frequency,
 - Mechanical looseness
- Vibration looks at frequency and severity of defects along with data trials.

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Laser Alignment

- The balance of rotating assemblies with laser alignment and shaft balance.
- Shaft balance is measured at every 90 degree intervals.
- Also a post and return balance of equipment is required along with P/M records of equipment balance and wear indicators.



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Heat Thermography

- Thermography is a predictive tool in electrical insulation of wear and damage
- · On pumps, thermal indicators can predict:
 - Bearing heat and wear as an increase in shaft temps
 - And can predict failures or leakage
- More thermal testing of equipment is vital for needed predictive testing and base-lines of pumps and electrical equipment

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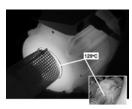
Heat Thermography

- Heat is one of the greatest wear indications of equipment and bearings and seals.
- Heat and temperature sensors on equipment are essential for proper operations.
- The use of thermal imaging on equipment is a key factor in location of hot spots on equipment.



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Heat Thermography

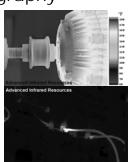


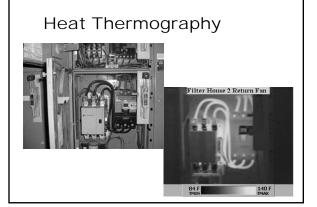
- Thermography uses a camera which produces an image of temperature variations on equipment with color intensity.
- Hot spots glow in yellow and red colors on the camera.

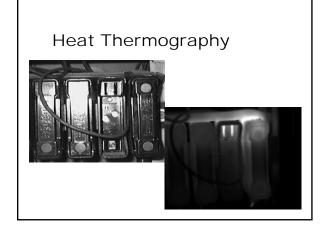
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Heat Thermography

- Heat thermography is used to locate:
 - Loose electrical connections
 - Friable electrical insulation on wiring
 - Hot spots on electrical panels
 - Worn equipment and circuits







Shock Pulse and Ultrasonic Testing

 Shock Pulse and Ultrasonic testing of equipment continue to test the vibration frequency patterns of roller bearings and establish a base line of shaft operation to base a defective bearing against.

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Ultrasonic Testing

 Ultrasonic testing can register audible sounds on headphones such as lifters on cams or valve actions and closings.



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Oil Analysis

- Establish an need for an oil analysis of plant motors and pumps
- Locate current lubrication needs and types of oils and grease
- Schedule of lubrication inspect weekly or monthly



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Oil Analysis

- What kinds of wear indicators are showing
- Used oil indicators and inspect for contamination
- Oil consumption indicators of seal failures

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Oil Analysis

- · Lubrication system rating of extended oil life
- · Oil viscosity and rating
- Quality of my oils and grease or the cheapest grades
- Chemical oil testing of breakdowns due to heat,metals,sulfurs or moisture
- Oil filters include better filtration of impurities and clean equipment
- · Keep records of oil schedules and results

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Oil Analysis

- Establish the need for adequate lubrication of equipment
- Lubrication of equipment covers the selection of lubricants related to oil, grease, filters, rating viscosity, oil analysis and the handling or storage of oils

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Lubricants

- Oil selection is based on OEM (Original Equipment Manufacturer) recommendations and design.
- Lube schedules and frequency establish along with system checks.
- Oil analysis of oils can use data of wear times and breakdown of oils and factors.

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Oil Breakdowns

- Lubricants can be the cause to equipment failures
- Equipment or bearing wear due to fatigue
- Oil breakdown due to excessive heat on equipment
- Water or moisture leakage or contaminants in the oil such as dust or metals contamination

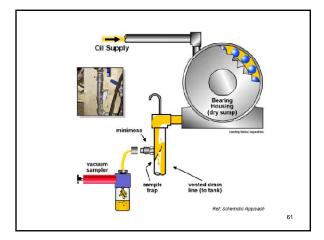
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Oil Testing

- Oil inspection and proper sampling of equipment is needed
- Lab testing of oils inspect for:
 - Water
 - Dust
 - Metal content
 - Viscosity
 - Other contaminants and wear factors
- · Oil temperature is key to life of oil usage

Metal shavings found in oil testing

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Oil Longevity

- Wear indicators of oil require inspecting all equipment for moisture, leaks, leaking oil seals and filter replacements.
- Several P/M maintenance checks can locate oil leaks of pumps, seals and other maintenance needs.

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Oil Schedules

- · Plan oil schedules and lube records
- Plan all oil checks and changes
- Use index cards on oiling schedules
 Use data cards and sheets for each pump
- · Indicate oil locations and types of oils

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Oil Schedule - Recycle

- A good environmental response is always recycle spent oils
- Have a plan with local recycler and vendor



Oil Schedule - Recycle



- Have a spill protection plan
- Store all used oils to be recycle
- Use berms and soil dry
- · Always recycle oil

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Oil Schedule - Recycle



 Never pollute water ways or land areas

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Cost Savings

- Providing results and proof of cost savings of predictive maintenance
- · Less down time of equipment
- Operations of equipment are improved and less failures

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CMMS

- Computer Maintenance Management System
 - CMMS is a computer driven maintenance management system of planned and work order driven maintenance reports and inspections.

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CMMS

- · Computer program of workorders
 - Predict time schedules and trend work maintenance of equipment
- Able to keep cost work times, parts and overtime
- · Can keep parts inventory of all equipment
- Provide monthly summary reports of cost and work
- · Also can contract out work service contracts

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CMMS

- CMMS will generate a planned maintenance schedule of equipment services and work orders of scheduled work.
- CMMS will generate planned work schedules and inventory of work orders and data.

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CMMS

- Produce cost summary and work time generation for maintenance cost.
- Produce yearly cost projections of maintenance cost and projections for failures
- · Keep inventory of parts and service contracts
- Also complete inventory of tools and equipment or track chemical cost and usage.

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End Results

- · Complete process improvement of P/M
- · Improved operations and less downtime
- · Less equipment failures and reduced cost
- Conditioned equipment for complete life cycle
- A complete road map for plant maintenance.
- Start with training plant operators toward preventive maintenance.

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Lasting Thoughts

- Plant maintenance has to be planned to operate and service equipment.Preventive measures have to be provided in timely schedules to prevent equipment failures.
- A planned preventative and predictive maintenance program will save you money and downtime of equipment and make plant operations more efficient.

DAILY ITEMS

| FACILITY NAME: | MACHINE TYPE: | DATE (MM/DD/YY) |
|----------------|---------------|------------------------------|
| FACILITY ID: | MACHINE ID: | (first working day of week): |

OPERATIONS AND MAINTENANCE CHECKLIST

CHECK THE FOLLOWING ITEMS DAILY

Check button trap and button trap screen AT LEAST once a day (more often if necessary). Place debris in sealed container.

Clean lint trap as often as required to avoid clogging fans and condensers. Place lint in sealed container.

Clean strainer in pre-lint filter (if applicable). Clean pump strainer. Place debris in sealed container.

Check all pressure gauges. Ensure proper operation pressures (refer to equipment operation manuals for specific requirements).

Empty wastewater collector into closed containers or wastewater processor (atomizer or evaporator).

Perform a visual leak inspection. This is a quick inspection – a thorough inspection should be accomplished weekly using the leak inspection checklist and a leak detector.

Check back pressure on cartridge filters, replace when manufacturer's recommended back pressure is reached. Drain filters for 24 hours (standard) or 48 hours (adsorptive), then place cartridges in sealed containers.

Check the still to ensure it does not exceed 75 percent of capacity (N/A for continuous stills).

CHECK THE FOLLOWING ITEMS WEEKLY. CHECK-OFF AND INITIAL THE APPROPRIATE BOXES. WEEK 2 3 4 5 WEEKLY CHECKLIST ITEMS USE THE FIVE BOXES TO THE RIGHT TO ANNOTATE INSPECTION DATES INSPECTOR INITIALS Check pump for proper lubrication, flow rate and operation (refer to equipment owner's manual). Check air relief and diverter valves to ensure proper operation and closure. Check water separator for debris: empty into still and clean if necessary. Inspect and clean the still. Check the operation of waste eater treatment unit (if applicable). Replace carbon according to manufacturer's recommended frequency. Check to ensure the air-vapor stream downstream of the condenser is \leq 45 deg F (7.2 deg C). Monitor carbon adsorber (if applicable) according to AQMD specifications.

| CHECK THESE ITEMS USING THE SUGGESTED FREQUENCY BELOW | DATE | INITIAL |
|--|------|---------|
| Check the drive belts for proper tension and condition (Semi-Annually). | | |
| Clean evaporative water towers to remove dirt and scale (Semi-Annually). | | |
| Inspect cooling coils (condenser) for lint buildup and proper operating temperatures (Annually). | | |
| Inspect cooling coils (still) for leaks, corrosion, and buildup (Annually). | | |
| Check steam coils (heating) for lint buildup and proper drying temperatures (Annually). | | |
| Check and clean all other machine areas (e.g., steam traps, fan blades, and air ducts).that may collect lint and affect proper operation (Annually). | | |
| Check disk filters for damage and dry clean them (Annually). | | |
| Change inductive door fan carbon (if applicable) (per manufacturer's recommendation). | | |
| Lubricate (grease) fittings (per manufacturer's recommendation). | | |
| Clean and inspect base solvent tanks (per manufacturer's recommendation). | | |

^{*}This is a suggested frequency. Follow manufacturer's operating manual in cases where more frequent schedules are recommended.

Revised 4/17/96.



PREVENEU-VIEW MANNOTOENNANCE FORM - VACUUM PUMP

| CUSTOMER SAMPLE REPORT | | PM SCHEDULE | [] Annual | [] Semi | Do | cument - PMF_VP2.2 | |
|---|-------------------------|---------------------------|---------------|-------------|------------|--------------------|--|
| ADDRESS | | | [X] Quarterly | [] Monthly | [] Other | | Page 1 of 1 |
| EQUIPMENT S/N | Vacuum Pump | MFG ID | DATE DUE DATE | | | PM STATUS | C - Completed CA - Completed - Add'l parts/labor req'd I - Incomplete - Add'l parts/labor req'd X - Not Applicable |
| | Ch | eck List | | | Status | | Comments |
| Drain oil fror | m reservoir, place into | o oil drain bucket. | | | С | Oil was lov | V. |
| Remove oil f | filter & replace. | | | | С | | |
| Remove oil | sight glass & clean as | s needed. | | | С | | |
| Add approxi | mately 7 quarts of va | cuum oil. | | | С | | |
| Remove exh | aust filter cover plate | s & remove filter. | | | С | | |
| Inspect exha | aust chamber for exce | ess oil, wipe out if need | ded. | | С | | |
| Check exhaust chamber; oil return line for clogging; clean if needed. | | | С | Cleaned re | turn line. | | |
| Reinstall ext | naust filter. | | | | С | | |
| Replace exh | aust filter. | | | | С | Next PM. | |
| Re-install ex | haust chamber cover | | | | С | | |
| Inspect vacu | ıum inlet filter. | | | | С | | |
| Wipe out interior of filter housing. | | | | С | | | |
| Wipe exterior surfaces of pump free of debris & oil. | | | С | | | | |
| Clean exces | s oil from floor. | | | | С | | |
| Remove & clean vacuum diverter valve, replace with new if needed. | | С | | | | | |
| Reconnect vacuum pump to press. | | | | С | | | |
| | | | | | | | |

Pump Maintenance Checklist

| Description | Comment | Maintenance Frequency | | | |
|-----------------------------|---|-----------------------|--------|---------|----------|
| | | | Weekly | Monthly | Annually |
| Pump use and sequencing | Turn off or sequence unnecessary motors. | Х | | | |
| Overall visual inspection | Complete overall visual inspection to be sure all equipment is operating and safety systems are in place. | X | | | |
| Check lubrication | Assure that all bearings are lubricated per the manufacturer's recommendation. | | | Х | |
| Check packing | Check packing for wear and repack as necessary. Consider replacing packing with mechanical seals. | | | Х | |
| Motor and pump alignment | Align the pump/motor coupling to allow for efficient torque transfer to the pump. | | | Х | |
| Check mountings | Check and secure all pump mountings. | | | Х | |
| Check bearings | Inspect bearings and drive belts for wear. Adjust, repair, or replace as necessary. | | | | Х |
| Motor condition | Check the condition of the motor through temperature or vibration analysis to assure long life. | | | | Х |

http://www1.eere.energy.gov/femp/operations_maintenance/printable_versions/om_pumpchecklist.html

Pump Vocabulary

- 1. <u>Axial-Flow Pump</u> a pump in which a propeller-like impeller forces water out in the direction parallel to the shaft. Also called a propeller pump.
- 2. <u>Bearing</u> anti-friction device used to support and guide a pump and motor shafts.
- 3. <u>Casing</u> the enclosure surrounding a pump impeller, into which the suction and discharge ports are machined.
- 4. <u>Cavitation</u> a condition that can occur when pumps are run too fast or water is forced to change direction quickly. A partial vacuum forms near the pipe wall or impeller blade causing potentially rapid pitting of the metal.
- 5. <u>Centrifugal Pumps</u> a pump consisting of an impeller on a rotating shaft enclosed by a casing having suction and discharge connections. The spinning impeller throws water outward at high velocity, and the casing shape converts this velocity to pressure.
- 6. <u>Closed-Coupled Pump</u> a pump assembly where the impeller is mounted on the shaft of the motor that drives the pump.
- 7. <u>Diffuser Vanes</u> vanes installed within a pump casing on diffuser centrifugal pumps to change velocity head to pressure head.
- 8. <u>Double-Suction Pump</u> a centrifugal pump in which the water enters from both sides of the impeller. Also called a split-case pump.
- 9. <u>Foot Valve</u> a check valve placed in the bottom of the suction pipe of a pump, which opens to allow water to enter the suction pipe but closes to prevent water from passing out of it at the bottom end. Keeps prime.
- 10. <u>Frame-Mounted Pump</u> a centrifugal pump in which the pump shaft is connected to the motor shaft with a coupling.
- 11. <u>Impeller</u> the rotating set of vanes that forces water through the pump.
- 12. <u>Jet Pump</u> a device that pumps fluid by converting the energy of a high-pressure fluid into that of a high-velocity fluid.
- 13. <u>Lantern Ring</u> a perforated ring placed around the pump shaft in the stuffing box. Water from the pump discharge is piped to this ring. The water forms a liquid seal around the shaft and lubricates the packing.
- 14. <u>Mechanical Seal</u> a seal placed on the pump shaft to prevent water from leaking from the pump along the shaft; the seal also prevents air from entering the pump.
- 15. <u>Mixed-Flow Pump</u> a pump that imparts both radial and axial flow to the water.
- 16. <u>Packing</u> rings of graphite-impregnated cotton, flax, or synthetic materials, used to control leakage along a valve stem or a pump shaft.
- 17. Packing Gland a follower ring that compressed the packing in the stuffing box.
- 18. <u>Positive Displacement Pump</u> a pump that delivers a precise volume of liquid for each stroke of the piston or rotation of the shaft.
- 19. <u>Prime Mover</u> a source of power, such as an internal combustion engine or an electric motor, designed to supply force and motion to drive machinery, such as a pump.

- 20. <u>Radial-Flow Pump</u> a pump that moves water by centrifugal force, spinning the water radially outward from the center of the impeller.
- 21. <u>Reciprocating Pump</u> a type of positive-displacement pump consisting of a closed cylinder containing a piston or plunger to draw liquid into the cylinder through an inlet valve and forces it out through an outlet valve.
- 22. <u>Rotary Pump</u> a type of positive-displacement pump consisting of elements resembling gears that rotate in a close-fitting pump case. The rotation of these elements alternately draws in and discharges the water being pumped.
- 23. <u>Single-Suction Pump</u> a centrifugal pump in which the water enters from only one side of the impeller. Also called an end-suction pump.
- 24. <u>Stuffing Box</u> a portion of the pump casing through which the shaft extends and in which packing or a mechanical seal is placed to prevent leakage.
- 25. <u>Submersible Pump</u> a vertical-turbine pump with the motor placed below the impellers. The motor is designed to be submersed in water.
- 26. <u>Suction Lift</u> the condition existing when the source of water supply is below the centerline of the pump.
- 27. <u>Velocity Pump</u> the general class of pumps that use a rapidly turning impeller to impart kinetic energy or velocity to fluids. The pump casing then converts this velocity head, in part, to pressure head. Also known as kinetic pumps.
- 28. <u>Vertical Turbine Pump</u> a centrifugal pump, commonly of the multistage, diffuser type, in which the pump shaft is mounted vertically.
- 29. <u>Volute</u> the expanding section of pump casing (in a volute centrifugal pump), which converts velocity head to pressure head..
- 30. <u>Water Hammer</u> the potentially damaging slam that occurs in a pipe when a sudden change in water velocity (usually as a result of too-rapidly starting a pump or operating a valve) creates a great increase in water pressure.
- 31. Wear Rings rings made of brass or bronze placed on the impeller and/or casing of a centrifugal pump to control the amount of water that is allowed to leak from the discharge to the suction side of the pump.

Pump and Motor Facts

Pump Facts

High-service pump – discharges water under pressure to the distribution system.

Booster pump – used to increase pressure in the distribution system and to fill elevated storage tanks.

Impeller or centrifugal pump used to move water.

Likely causes of vibration in an existing pump/motor installation:

- 1. bad bearings
- 2. imbalance of rotating elements
- 3. misalignment from shifts in underlying foundation

Pump and motor should be tested and complete test results recorded as a baseline for the measurement of performance within the first 30 days of operations.

Calipers and thickness gauges can be used to check alignment on flexible couplings.

Packing/Seals Facts

If new packing leaks, stop the motor and repack the pump.

Pumps need new packing when the gland or follower is pulled all the way down.

The packing around the shaft should be tightened just enough to allow an occasional drop of liquid.

Joints of packing should be staggered at least 90°.

Mechanical seals consist of a rotating ring and stationary element.

The operating temperature on a mechanical seal should never exceed 160°F.

Motor Facts

Motors pull the most current on start up.

In order to prevent damage, turn the circuit off immediately if the fuse on one of the legs of a three-phase circuit blows.

An electric motor changes electrical energy into mechanical energy.

Power factors on motors can be improved by:

- 1. changing the motor loading
- 2. changing the motor type
- 3. using capacitors

Routing cleaning of pump motors includes:

- 1. checking alignment and balance
- 2. checking brushes
- 3. removing dirt and moisture
- 4. removal of obstructions that prevent air circulation

Cool air extends the useful life of motors.

A motor (electrical or internal combustion) used to drive a pump is called a prime mover.

The speed at which the magnetic field rotates is called the motor synchronous speed and is expressed in rpm.

If a variable speed belt drive is not to be used for 30 days or more, shift the unit to minimum speed setting.

Emory cloth should not be used on electric motor components because it is electrically conductive and may contaminate parts.

Ohmmeters used to test a fuse in a motor starter circuit.

The most likely cause of a three-phase motor not coming to speed after starting – the motor has lost power to one or more phases.

Transformer Facts

Transformers are used to convert high voltage to low voltage.

High voltage is 440 volts or higher.

Standby engines should be run weekly to ensure that it is working properly.

Relays are used to protect electric motors.

Pump and Motor Review Questions

- 1. Leakage of water around the packing on a centrifugal pump is important because it acts as a (n):
 - a. Adhesive
 - b. Lubricant
 - c. Absorbent
 - d. Backflow preventer
- 2. What is the purpose of wear rings in a pump?
 - a. Hold the shaft in place
 - b. Hold the impeller in place
 - c. Control amount of water leaking from discharge to suction side
 - d. Prevent oil from getting into the casing of the pump
- 3. Which of the following does a lantern ring accomplish?
 - a. Lubricates the packing
 - b. Helps keep air from entering the pump
 - c. Both (a.) and (b.)
- 4. Closed, open and semi-open are types of what pump part?
 - a. Impeller
 - b. Shaft sleeve
 - c. Casing
 - d. Coupling
- 5. When tightening the packing on a centrifugal pump, which of the following applies?
 - a. Tighten hand tight, never use a wrench
 - b. Tighten to 20 foot pounds of pressure
 - c. Tighten slowly, over a period of several hours
 - d. Tighten until no leakage can be seen from the shaft
- 6. Excessive vibrations in a pump can be caused by:
 - a. Bearing failure
 - b. Damage to the impeller
 - c. Misalignment of the pump shaft and motor
 - d. All of the above
- 7. What component can be installed on a pump to hold the prime?
 - a. Toe valve
 - b. Foot valve
 - c. Prime valve
 - d. Casing valve

- 8. The operating temperature of a mechanical seal should not exceed:
 - a. 60°C
 - b. 150°F
 - c. 160°F
 - d. 71°C
 - e. c and d
- 9. What is the term for the condition where small bubbles of vapor form and explode against the impeller, causing a pinging sound?
 - a. Corrosion
 - b. Cavitation
 - c. Aeration
 - d. Combustion
- 10. The first thing that should be done before any work is begun on a pump or electrical motor is:
 - a. Notify the state
 - b. Put on safety goggles
 - c. Lock out the power source and tag it
 - d. Have a competent person to supervise the work
- 11. Under what operating condition do electric motors pull the most current?
 - a. At start up
 - b. At full operating speed
 - c. At shut down
 - d. When locked out
- 12. Positive displacement pumps are rarely used for water distribution because:
 - a. They require too much maintenance
 - b. They are no longer manufactured
 - c. They require constant observation
 - d. Centrifugal pumps are much more efficient
- 13. Another name for double-suction pump is
 - a. Double-jet pump
 - b. Reciprocating pump
 - c. Horizontal split-case pump
 - d. Double-displacement pump
- 14. As the impeller on a pump becomes worn, the pump efficiency will:
 - a. Decrease
 - b. Increase
 - c. Stay the same
- 15. How do the two basic parts of a velocity pump operate?

| 10. | what are two designs used to change high velocity to high pressure in a pump? |
|-----|---|
| 17. | In what type of pump are centrifugal force and the lifting action of the impeller vanes combined to develop the total dynamic head? |
| 18. | Identify one unique safety advantage that velocity pumps have over positive-displacement pumps. |
| 19. | What is the multistage centrifugal pump? What effects does the design have on discharge pressure and flow volume? |
| 20. | What are two types of vertical turbine pump, as distinguished by pump and motor arrangement, which are commonly used to pump ground water from wells? |
| 21. | What type of vertical turbine pump is commonly used as an inline booster pump? |
| 22. | Describe the two main parts of a jet pump. |
| 23. | What is the most common used of positive-displacement pumps in water plants today? |
| 24. | What is the purpose of the foot valve on a centrifugal pump? |

| 26. What is the function of wear rings in centrifugal pumps of the closed-impeller design? We is the function of the lantern rings? | /hat |
|---|------|
| 27. Describe the two common types of seals used to control leakage between the pump shaft the casing. | and |
| 28. What feature distinguishes a close-coupled pump and motor? | |
| 29. What is the value of listening to a pump or laying a hand on the unit as it operates? | |
| 30. Define the term "racking" as applied to pump and motor control. | |
| 31. When do most electric motors take the most current? | |
| 32. What are three major ways of reducing power costs where electric motors are used? | |
| 33. What effect could over lubrication of motor bearings have? | |

34. Why should emery cloth not be used around electrical machines?
35. What are the most likely causes of vibration in an existing pump installation?
36. What can happen when a fuse blows on a single leg of a three-phase circuit?
37. Name at least three common fuels for internal-combustion engines.
38. List the type of information that should be recorded on a basic data card for pumping equipment.

39. What is the first rule of safety when repairing electrical devices?

Answers:

| 1. | В | 6. D | 11. A |
|----|---|-------|-------|
| 2. | C | 7. B | 12. D |
| 3. | C | 8. E | 13. C |
| 4. | A | 9. B | 14. A |
| 5. | C | 10. C | |

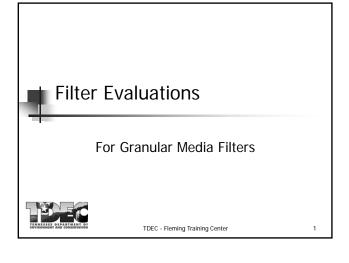
- 15. A spinning impeller accelerates water to a high velocity within a casing, which changes the high-velocity, low-pressure water to a low-velocity, high-pressure discharge.
- 16. Volute casing and diffuser vanes.
- 17. Mixed-flow pump (the design used for most vertical turbine pumps)
- 18. If a valve is closed in the discharge line, the pump impeller can continue to rotate for a time without pumping water or damaging the pump.
- 19. A multistage centrifugal pump is made up of a series of impellers and casings (housings) arranged in layers, or stages. This increases the pressure at the discharge outlet, but does not increase flow volume.
- 20. Shaft-type and submersible-type vertical turbines.
- 21. A close-coupled vertical turbine with an integral sump or pot.
- 22. The jet pump consists of a centrifugal pump at the ground surface and an ejector nozzle below the water level.
- 23. Positive-displacement pumps are generally used in water plants to feed chemical into the water supply.
- 24. The foot valve prevents water from draining when the pump is stopped, so the pump will be primed when restarted.
- 25. The bolts holding the two halves of the casing together are removed and the top half is lifted off.
- 26. Wear rings prevent excessive circulation of water between the impeller discharge and suction area. Lantern rings allow sealing water to be fed into the stuffing box.
- 27. (1) Packing rings are made of graphite-impregnated cotton, flax, or synthetic materials. They are inserted in the stuffing box and held snuggly against the shaft by an adjustable packing gland. (2) Mechanical seals consist of two machined and polished surfaces. One is attached to the shaft, the other to the casing. Spring pressure maintains contact between the two surfaces.
- 28. The pump impeller is mounted directly on the shaft of the motor.
- 29. An experienced operator can often detect unusual vibration by simply listening or touching. Vibration, especially changes in vibration level, are viewed as symptoms or indicators of other underlying problems in foundation, alignment and/or pump wear.
- 30. Racking refers to erratic operation that may result from pressure surges when the pump starts; it is often a problem when the pressure sensor for the pump control is located too close to the pump station.
- 31. During start-up.
- **32.** (1) Increase system efficiency; (2) spread the pumping load more evenly throughout the day; (3) reduce power-factor charges
- 33. The bearings may run hot, and excess grease or oil could run out and reach the motor windings, causing the insulation to deteriorate.
- **34.** The abrasive material on emery cloth is electrically conductive and could contaminate electrical components.
- 35. Imbalance of the rotating elements, bad bearings and misalignment
- **36.** A condition called single-phasing can occur, causing the motor windings to overheat and eventually fail.

- 37. gasoline, propane, methane, natural gas and diesel oil (diesel fuel)
- 38. make, model, capacity, type, date and location installed, and other information for both the driver (motor) and the driven unit (pump)
- 39. Make sure the power to the device is disconnected. This is critical since rubber gloves, insulated tools and other protective gear are not guarantees against electrical shock.

Section 2

Filters

Optimizing and Performance Troubleshooting Math





Preventive Maintenance

- Think of filter evaluation as preventive maintenance for your filters
 - Unfortunately filters have been evaluated due to a problem or "run to fail" attitude

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Review Filter Design

- Before you begin, you need to know:
 - Type of media used
 - Different media depths for each grain size
 - Designed backflow rates
 - Effective size and uniformity coefficients of media
 - Appropriate backwash bed expansion

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Review Water Quality

- Don't just look at the water quality being produced by the filter
- Look at the water quality leaving the sedimentation basins too

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32 Filters



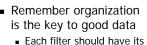
Water from Sed Basins

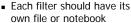
- Good rule of thumb
 - If your raw water turbidity is less than 10 NTU most of the time, then you should have about 1 NTU coming in from sedimentation basins
 - If your raw water turbidity is greater than 10 NTU most of the time, then you should have about 2 NTU coming in from sedimentation basins

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Organization





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Safety

- Remember, a filter bay is a considered a confined space, please take all necessary precautions before entering into filter bay
 - Use a ladder to enter the filter
 - Allow no more than one team member on the ladder at a time
 - Provide a source of forced air to the team members in the filter
 - Troughs can be walked down but not used to jump into the filter
 - No team member should enter the filter alone, practice the buddy system

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Safety cont.

- Never walk directly on filter media
 - Use 2'x2' plywood boards
- Make sure filter is completely drained before entering

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Safety cont.

- While fluidizing the media AND a person HAS to be in the filter bay, it is recommended that they should be attached to an emergency extraction harness and rope
 - NEVER fluidize the media while a person is standing on the surface of the media; they will disappear quickly into the filter media

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Scheduling the Evaluation

- Inspections should be performed on a frequent basis
 - Annual is sufficient
- However, if a problem arises, then an evaluation should be performed more frequently
- Remember, filter will be out of service for at least a day, if not more

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Review of Filtration Rules

Chapter 0400-45-01 Public Water System Rules

http://www.tn.gov/sos/rules_all/2012/0400-45-01.20121030.pdf

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0400-45-1-.31(4)(c)

- The turbidity in the combined filter effluent must:
 - Be less than or equal to 0.3 NTU in at least 95% of measurements taken each month
 - And at no time exceed 1 NTU

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Notes from Field Office

- Having a filter exceedance is not a violation
- The violation occurs when the water system fails to submit the filter exceedance report of denote a filter exceedance on the Filter Performance Report
 - It would be in the water system's best interest to go ahead and submit a filter exceedance report when in doubt rather than not submit a report at all

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Notes from Field Office continued

It may also be helpful for water systems to have a flow meter and be able to chart the flow of the effluent water going to the clear well against the turbidity

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Notes from Field Office continued

- Also, the way the rules is written any measured turbidity level greater than 0.5 NTU in two consecutive readings 15 minutes apart requires a filter profile or obvious reason
 - This means if someone knocks the turbidimeter and the reading is elevated above 0.5 NTU for fifteen minutes or longer, they would technically need to report the filter exceedance
 - The obvious reason being someone bumped the turbidimeter

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Notes from Field Office continued

- One example from the Field Office is that one water system had an elevated turbidity reading because a water system personnel sprayed the pipe gallery while cleaning
 - This would be an obvious reason as well

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Notes from Field Office continued

- It may also be helpful for water systems to know that they use the filter data recorded on the back of the MOR to check plant operations, such as turbidity readings
- So it would be in their best interest to ensure the filter data section accurately reflects the daily operations of the filters

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Notes from Field Office continued

- An example is if a system has eight filters and they know that two of the filters are out of service for two weeks
 - Then they would expect that the filter data would reflect this and not show that all eight filters were being used the entire month
 - This goes for the filter run time and could even be the amount of backwash water used

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Levels Exceeded

- Depending on the exceedance level, the system must:
 - Produce a filter profile
 - Conduct a self-assessment and/or
 - Must arrange for the conduct of a comprehensive performance evaluation by the State or a 3rd party approved by the State

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Filter Profile

Is defined as a graphical representation of individual filter performance, based on continuous turbidity measurements or total particle counts versus time for an entire filter run, from startup to backwash inclusively, that includes an assessment of filter performance while another filter is being backwashed

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Filter Profile continued

 A filter profile is basically a strip chart of the problem filter with the time of the filter backwashes for the filter and other filters denoted on the chart

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Filter Profile continued

- For any individual filter that has a measured turbidity level of greater than 1.0 NTU in two consecutive measurements taken 15 minutes apart
- For any individual filter that has a measured turbidity level of greater than 0.5 NTU in two consecutive measurements taken 15 minutes apart at the end of the first four hours of continuous filter operation after the filter has been backwashed or otherwise taken offline

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Filter Profile continued

- The system must either:
 - Produce a filter profile for the filter within 7 days of the exceedance
 - if the system is not able to identify an obvious reason for the abnormal filter performance
 - and report that the profile has been produced
 - Or report the obvious reason for the exceedance

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FILTER PROFILE REPORT FOR INDIVIDUAL FILTERS

FOR PUBLIC WATER SYSTEMS THAT ARE USING SURFACE WATER SOURCES OR GROUND WATER SOURCES UNDER THE INFLUENCE OF SURFACE WATER THAT ARE REQUIRED TO CONDUCT ADDITIONAL INDIVIDUAL FILTER MONITORING

| PUBLIC WATER SYSTEM NAME: TCEQ WSC | | LANT NAME R NUMBER: PDWS Water Trea | itment Plant |
|---|--|--|---|
| PWS ID No.: 1234567 | | onth: February | Year: 2002 |
| | | | |
| | OBVIOUS REASONS | | |
| OBVIOUS REASONS (Check all that apply) | FILTER NO.: 1 DATE: 02-04-02 TIME: 10:00 AM DURATION: 45.00 TURBIDITY: 1.32 | FILTER NO.: 1 DATE: 02-04-02 TIME: 4:15 PM DURATION: 15.00 TURBIDITY: 0.57 | FILTER NO.: 5 DATE: 02-04-02 TIME: 11:45 AM DURATION: 15.00 TURBIDITY: 1.05 |
| NONE IDENTIFIED - A Filter Profile must be submitted | (See Profile No. | (See Profile No.) | (See Profile No. |
| Filter Problems Post-Backwash Turbidity Spike Prolonged Filter Run Time Excessive Filter-Loading Rate Rate-of-Flow Control Valve Failure Media Defects (insufficient depth, mudballs, etc.) Inadequate Surface Wash or Backwash Facilities Backwash Artifact Turbidimeter Errors | | | |
| Incorrect Calibration Air Bubble Debris | | | |
| Chemical Feed Equipment Failure Coagulant Coagulant Aid Filter Aid Poor Raw Water Quality | | | |
| Other Major Unit Process Failures/Maintenance Activities Specify: | <u> </u> | <u> </u> | Backwash Filter No. 1 |
| | | | |
| | OBVIOUS REASONS | | |
| | OBVIOUS REASONS FILTER NO.: 5 DATE: 02-13-02 TIME: 2:15 PM DURATION: 15.00 TURBIDITY: 1.24 | FILTER NO.: DATE: TIME: DURATION: TURBIDITY: | FILTER NO.: DATE: TIME: DURATION: TURBIDITY: |
| OBVIOUS REASONS (Check all that apply) NONE IDENTIFIED - A Filter Profile must be submitted | FILTER NO.: 5 DATE: 02-13-02 TIME: 2:15 PM DURATION: 15.00 | DATE: TIME: DURATION: | DATE: TIME: DURATION: |
| NONE IDENTIFIED - A Filter Profile must be submitted Filter Problems Post-Backwash Turbidity Spike Prolonged Filter Run Time Excessive Filter-Loading Rate Rate-of-Flow Control Valve Failure Media Defects (insufficient depth, mudballs, etc.) Inadequate Surface Wash or Backwash Facilities Backwash Artifact Turbidimeter Errors | FILTER NO.: 5 DATE: 02-13-02 TIME: 2:15 PM DURATION: 15.00 TURBIDITY: 1.24 | DATE: TIME: DURATION: TURBIDITY: | DATE: TIME: DURATION: TURBIDITY: |
| NONE IDENTIFIED - A Filter Profile must be submitted Filter Problems Post-Backwash Turbidity Spike Prolonged Filter Run Time Excessive Filter-Loading Rate Rate-of-Flow Control Valve Failure Media Defects (insufficient depth, mudballs, etc.) Inadequate Surface Wash or Backwash Facilities Backwash Artifact Turbidimeter Errors Incorrect Calibration Air Bubble Debris | FILTER NO.: 5 DATE: 02-13-02 TIME: 2:15 PM DURATION: 15.00 TURBIDITY: 1.24 | DATE: TIME: DURATION: TURBIDITY: | DATE: TIME: DURATION: TURBIDITY: |
| NONE IDENTIFIED - A Filter Profile must be submitted Filter Problems Post-Backwash Turbidity Spike Prolonged Filter Run Time Excessive Filter-Loading Rate Rate-of-Flow Control Valve Failure Media Defects (insufficient depth, mudballs, etc.) Inadequate Surface Wash or Backwash Facilities Backwash Artifact Turbidimeter Errors Incorrect Calibration Air Bubble | FILTER NO.: 5 DATE: 02-13-02 TIME: 2:15 PM DURATION: 15.00 TURBIDITY: 1.24 | DATE: TIME: DURATION: TURBIDITY: | DATE: TIME: DURATION: TURBIDITY: (See Profile No) |

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Filter Self-Assessment

■ For any individual filter that has a measured turbidity level of greater than 1.0 NTU in two consecutive measurements taken 15 minutes apart at any time in each of three consecutive months

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Filter Self-Assessment continued

- Self-assessment must be conducted within 14 days of the exceedance
- Report that the self-assessment was conducted

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Filter Self-Assessment continued

- Must consist of at least the following components:
 - Assessment of filter performance
 - Development of a filter profile
 - Identification and prioritization of factors limiting filter performance
 - Assessment of the applicability of corrections
 - Preparation of a filter self-assessment report

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PUBLIC WATER

FILTER ASSESSMENT REPORT FOR INDIVIDUAL FILTERS

FOR PUBLIC WATER SYSTEMS THAT ARE USING SURFACE WATER SOURCES OR GROUND WATER SOURCES UNDER THE INFLUENCE OF SURFACE WATER THAT ARE REQUIRED TO CONDUCT AN INDIVIDUAL FILTER ASSSESSMENT

PLANT NAME

| SYSTEM NAME: | | | | OR NUMBER: | | |
|--|-----------------------------|------------------------|------------------------|---------------------------------|----------------------|--------------------|
| | | | | FILTER | | |
| PWS ID No.: | | | | NUMBER: | | |
| | | DESIGN SPE | ECIFICATIONS | | | |
| FILTER TYPE | | | OPERATING MOD | DE | | |
| | Diameter (ft) | Length (ft) | Width (ft) | Surface Area (ft ²) | Freeboard (ft) | Max Head Loss (ft) |
| MEDIA BED DIMENSIONS | | | | . , | | |
| MEDIA TYPE | | | 1 | | | |
| MEDIA SPECS | Material | Depth (inches) | Min. Size (mm) | Max. Size (mm) | UC | Specific Gravity |
| Layer 1 Material Layer 2 Material | | | | | | |
| Layer 3 Material | | | | | | |
| Layer 4 Material | | | | | | |
| TOTAL DEPTH (inches) | | | | | | |
| L/D RATIO | | | | | | |
| UNDERDRAIN TYPE | No. of Grades | Min. Size (in) | May Cina (in) | Total Depth (in) | 1 | |
| SUPPORT GRAVEL | No. or Grades | wiii. Size (iii) | Max. Size (in) | Total Depth (III) | | |
| TROUGHS | | SUPPL. BACKWA | SH | | ı | 1 |
| Number. | | OOI I E. BAOKWA | 011 | | | 1 |
| Separation (inches) | | FILTER-TO-WAST | E | | | |
| | Regulatory Std | Design | Typical | During Backwash | Maximum | App'd Exception |
| FILTER FLOW RATE (gpm) | | | | | | |
| LOADING RATE (gpm/ft²) | | | | | | |
| BW FLOW RATE (gpm) | | | | | | - |
| BW LOADING RATE (gpm/ft ²) | | | | | | |
| FILTER INFLUENT | Source | Controller | Meter | Turbid | imeter | LOHG |
| FILTER EFFLUENT | | | | | | |
| BACKWASH WATER | | | | | | |
| | | | | | | |
| | | OPERATING | PROCEDURES | | | |
| CALIBRATION | Flow Meter | Backwash Meter | Mech. ROFC | NTU (Primary) | NTU (Secondary) | 1 |
| Method | | | | | | |
| Frequency Date of Last | | | | | | _ |
| | Total Con (ALTID) | 1011 (6) | D T (1) | | Elication Bata | <u>]</u> 7 |
| BACKWASH Criteria | Turbidity (NTU) | LOH (ft) | Run Time (hr) | Run Volume (gal) | Filtration Rate | 1 |
| Monitoring Interval | | | | | | 1 |
| WRITTEN SOPs | | ADDITIONAL REM | ARKS: | • | • | _ |
| Plant Start-up | | | | | | |
| Filter Start-up | | | | | | |
| Plant Shutdown Filter Shutdown | | | | | | |
| Filter Backwash | | | | | | |
| Filter Inspection | | | | | | |
| L certify that | t I am familiar with the in | oformation contained i | n this report and that | to the best of my knowle | dge the information | |
| <u>.</u> | plete, and accurate. | normation contained i | ir and report and and, | to the boot of my fallowing | ago, aro imorridadir | |
| Operator's Signature: | • | | | | | |
| Operator's Name (printed): | | | | | | |
| Certificate No. and Class: | | | | Date: | | |
| Submit Report to TCFO/ | MP&RM Division/Public | n Drinking Water Sect | ion(MC-155) ATTN | Monthly Reports P.O. Ro | ov 13087 Austin TY | 78711-3087 |

The report is due the 10th of the following month

FILTER ASSESSMENT REPORT FOR INDIVIDUAL FILTERS

FOR PUBLIC WATER SYSTEMS THAT ARE USING SURFACE WATER SOURCES OR GROUND WATER SOURCES UNDER THE INFLUENCE OF SURFACE WATER THAT ARE REQUIRED TO CONDUCT AN INDIVIDUAL FILTER ASSSESSMENT

| | PUBLIC WATER SYSTEM NAME: | | | | PLANT NAME OR NUMBER: | | |
|--------------|---|-----------|------------------|--------------------------------|--------------------------|---------------|------------------|
| STSTEM NAME: | | | | FILTER | | | |
| | PWS ID No.: | | | | NUMBER: | | |
| | | | CURRENT | CONDITIONS | | | |
| | 2.75 | 71145 | | | | | I= |
| | DATE | TIME | TURBIDITY (NTU) | LOH (ft) | FLOW RATE (gpm) | RUN TIME (hr) | RUN VOLUME (gal) |
| | PHYSICAL CONDITION | 1 | ADDITIONAL REM | APKS: | <u> </u> | | |
| | Walls | | ADDITIONAL ILLIM | AITTO. | | | |
| | Troughs | | | | | | |
| | Suppl. Backwash Flow Meter | | | | | | |
| | ROFC | | | | | | |
| | Flow Control Valve | | | | | | |
| | Turbidimeter | | | | | | |
| | LOHG | | | | | | |
| | | | MEDIA SURFAC | CE CONDITIONS | | | |
| | | Before BW | After BW | | Before BW | After BW | 7 |
| | MOUNDS | | | RETRACTION | | | |
| | Number | | | Number | | | |
| | Length (inches) Width (inches) | | | Length (inches) Width (inches) | | | _ |
| | Height (inches) | | | Depth (inches) | | | - |
| | DEPRESSIONS | | | CRACKS | | | |
| | Number | | | Number | | | |
| | Length (inches) | | | Length (inches) Width (inches) | | | _ |
| | Width (inches) Depth (inches) | | | Depth (inches) | | | - |
| | ACCUMULATED FLOC | | | MUDBALLS | | | |
| | Thickness (inches) | | | No. per ft ² | | | |
| | Distribution | | | Size (inches) | | | |
| | | | | Distribution | | | |
| | ADDITIONAL REMARKS: | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | | | | | |
| | | | BACKWASH | CONDITIONS | | | |
| | BW FLOW RATE (gpm) | | ADDITIONAL REM | ARKS: | | | |
| | RISE RATE (inches/minute) LOADING RATE (gpm/ft²) | | | | | | |
| | DURATION (minutes) | | | | | | |
| | TOTAL VOLUME (gallons) | | | | | | |
| | TROUGHS | | | | | | |
| | Levelness | | | | | | |
| | Flooding SUPPL. BACKWASH | | | | | | |
| | Duration (minutes) | | | | | | |
| | Effectiveness | | | | | | |
| | JETTING | | | | | | |
| | No. of Sites | | | | | | |
| | Severity BW WATER DISTRIBUTION | | | | | | |
| | SPENT BWW TURBIDITY | | | | | | |
| | EXPANSION (inches) | | | | | | |
| | EXPANSION (Inches) | | | | | | |
| | YIELD (percent) | | | | | | |
| | | | | | | | |
| | Submitted by: | | | | Date: | | |

TCEQ - 10277 (10-02-00) PAGE 2 Filter Assessment Report

FILTER ASSESSMENT REPORT FOR INDIVIDUAL FILTERS

FOR PUBLIC WATER SYSTEMS THAT ARE USING SURFACE WATER SOURCES OR GROUND WATER SOURCES UNDER THE INFLUENCE OF SURFACE WATER THAT ARE REQUIRED TO CONDUCT AN INDIVIDUAL FILTER ASSSESSMENT

| PUBLIC WATER | | | | PLANT NAME | | |
|---|---------------------|-----------------|------------|-------------------|------------------|----------------------|
| SYSTEM NAME: | | | | OR NUMBER: FILTER | | |
| PWS ID No.: | | | | NUMBER: | | |
| | | | RPROBE | | | |
| NUMBER OF SITES | | ADDITIONAL REM | ARKS: | | | |
| MEDIA | | | | | | |
| Max. Thickness (inches) Min. Thickness (inches) | | | | | | |
| Typ. Thickness (inches) | | | | | | |
| SUPPORT MATERIAL | | | | | | |
| Max. Elevation | | | | | | |
| Min. Elevation | | | | | | |
| Typ. Elevation | | | | | | |
| | | FILTER EX | KCAVATION | | | |
| | REFERENCE | SITE 2 | SITE 3 | SITE 4 | SITE 5 | SITE 6 |
| SITE CHARACTERISTIC | Normal | | | | | |
| LAYER 1 (Top Layer) | | | | | | |
| INTERFACE 1 | | | | | | |
| LAYER 2 INTERFACE 2 | | | | | | |
| LAYER 3 | | | | | | |
| INTERFACE 3 | | | | | | |
| LAYER 4 | | | | | | |
| MUDBALLS | | | | | | |
| Max. Size (inches) | | | | | | |
| Min. Size (inches) Max. Depth (inches) | | | | | | |
| max. Deptil (iliches) | AITE - | 0.77 | 0.75 | 0.75 40 | 0:== 44 | 0.77 |
| SITE CHARACTERISTIC | SITE 7 | SITE 8 | SITE 9 | SITE 10 | SITE 11 | SITE 12 |
| LAYER 1 (Top Layer) | | | | | | |
| INTERFACE 1 | | | | | | |
| LAYER 2 | | | | | | |
| INTERFACE 2 | | | | | | |
| LAYER 3 | | | | | | |
| INTERFACE 3 LAYER 4 | | | | | | |
| MUDBALLS | | | | | | |
| Max. Size (inches) | | | | | | |
| Min. Size (inches) | | | | | | |
| Max. Depth (inches) | | | | | | |
| MEDIA CONDITION | | ADDITIONAL REM | ARKS: | | | |
| Sharpness | | | | | | |
| Encrustation Uniformity | | | | | | |
| Officiality | | | | | | |
| | | ADDITION | AL STUDIES | | | |
| FILTER PROFILE ATTACHED? | | ADDITIONAL REMA | RKS: | | | |
| Note: A Filter Profile must be attack | hed to this report. | | | | | |
| DEDOENT MUDEAU C | | | | | | |
| PERCENT MUDBALLS Media Volume (ml) | | | | | | |
| Mudball Volume (ml) | | | | | | |
| % Mudballs | | | | | | |
| | | | | | | |
| | | CONCI | LUSIONS | | Ioonnessure : :: | NI BI AN |
| CONCLUSIONS: | | | | | CORRECTIVE ACTIO | ON PLAN ATTACHED? |
| | | | | | | |
| | | | | | WOULD YOU LIKE | SOME TECHNICAL |
| | | | | | | ROM THE TCEQ? |
| | | | | | | |
| | | | | | | |
| Submitted by: | | | | Date | | |
| TCEQ - 10277 (10-02-00) | | | PAGE 3 | | Filte | er Assessment Report |

FILTER ASSESSMENT REPORT FOR INDIVIDUAL FILTERS

FOR PUBLIC WATER SYSTEMS THAT ARE USING SURFACE WATER SOURCES OR GROUND WATER SOURCES UNDER THE INFLUENCE OF SURFACE WATER THAT ARE REQUIRED TO CONDUCT AN INDIVIDUAL FILTER ASSSESSMENT

| PUBLIC WATER SYSTEM NAME: | PLANT NAME OR NUMBER: |
|--|--------------------------|
| PWS ID No.: | FILTER NUMBER: |
| FILTER SCHEM. | |
| PREPARE A SIMPLE FILTER SCHEMATIC SHOWING THE LOCATION OF BACKWA | |
| | |
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| Submitted by: | Date: |

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Comprehensive Performance Evaluation

- For any individual filter that has a measured turbidity level of greater than 2.0 NTU in two consecutive measurements taken 15 minutes apart at any time in each of two consecutive months
- Must be conducted by the State or a third party approved by the State

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Comprehensive Performance Evaluation continued

- System has to arrange for this to be done no later than 30 days following exceedance
- The evaluation completed and submitted to the State no later than 90 days following the exceedance

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Factors affecting filtration

- Physical condition of filter bed
- Physical condition of filter media
 - Depends on how frequently filter is backwashed
 - Media rubs together and eventually wears down
- Filtration rate
- Backwash procedures
 - Need SOP, everyone needs to backwash the same
- Backwash conditions and/or rates

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Filtration Rate

■ Filtration = (Filtration) (Area Available for Flow)



Q = Filtration Rate, is constant

V = Filtration Velocity

A = Area Available for Flow between Media Grains

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Filtration Rate

As Particles are Stored in a Filter Bed,
 "A" becomes Smaller



Q = Filtration Rate, is constant

V = Filtration Velocity

A = Area Available for Flow between Media Grains

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Filtration Rate

As "A" becomes Smaller, "V" becomes Larger



Q = Filtration Rate, is constant V = Filtration Velocity

A = Area Available for Flow between Media Grains

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- And, if "V" becomes too Large
 - Particles stored in a filter bed by:
 - Strained particles can be driven deeper into the filter bed
 - Particles stuck to the filter media can be detached from the media surface
 - Then both types of particles will go through the bottom of the filter resulting in turbidity breakthrough

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Filter Run Hour Analysis

- Compares filters to each other throughout the facility
 - Allows the operator to see how many hours the filters are operated through the year, which determines if one is used more than others

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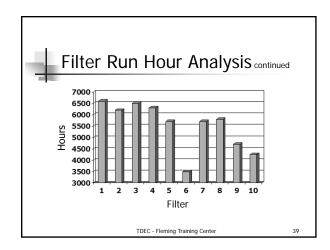
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Filter Run Hour Analysis continued

- Procedure
 - Count the number of hours each filter is in service monthly
 - Put together an annual total filter run hours in a graph format

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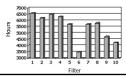


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Filter Run Hour Analysis continued

- Filter 6 may have been out of service for maintenance for most of the year
- Filter 9 and 10 were not used as much as the others either, what would be the explanation for this?



Physical Condition of Bed

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Physical Condition of Filter Bed

- Mounding
- Craters
- Mud/silt on top of filter
- Cracks in filter bed
- Sand separating from walls
- Algae

- Structural defects in filter
 - Blown tiles and/or grout
- Media in troughs
 - Backwash rate too high?
- Levelness of troughs
 - Length and width
 - Between troughs

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Visual Observations

- This is your first line of defense in filter monitoring and evaluation
- Look for easy to recognize issues:
 - Media boils
 - Uneven wash distribution
 - Uneven overflow into backwash water troughs
 - Craters
 - Mudballs
- Create a map of any issues found

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Media Depth

- Single-media filter
 - Must be 30 inches of sand
- Dual-media filter
 - Must be 30 inches of dual media
 - 10-12 inches of sand
 - 18-20 inches of anthracite
- Take 10-12 core samples and measure
 - Near wall and near center
 - Random

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Media Depth continued

- Determine average media depth
 - First, backwash filter and then drain
 - You will be standing in the filter, have plywood down so you are not standing on the media

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Media Depth continued

- Determine average media depth continued
 - Poke 5-ft ruler or steel rod into filter media at random spots until you reach support gravel or underdrains
 - Determined by feel or the sound of a "crunch" once you hit gravel
 - If you are using a steel rod, pinch at surface and carefully pull it out, tape at that point then measure distance
 - Determine average media depth by repeating about 10 times randomly around filter bed

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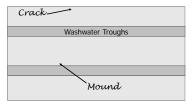
46



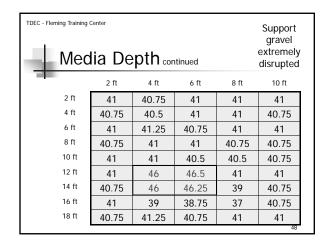


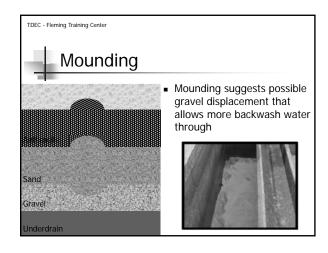
Media Depth continued

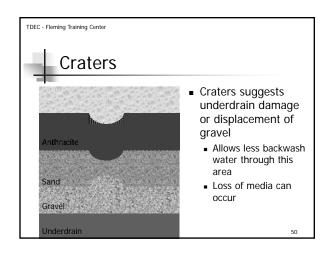
 Draw picture of filter and write down depths where the measurement was taken along with other physical observations

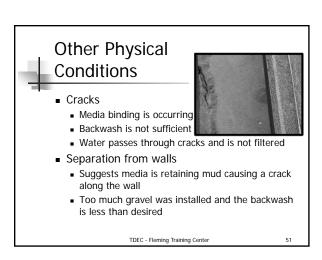


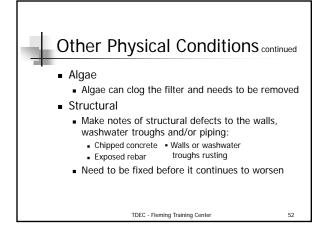
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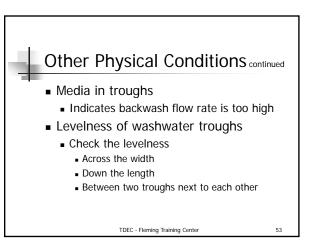










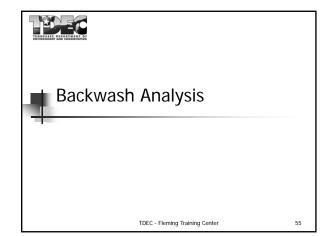




Other Physical Conditions continued

- Freeboard measurement
 - This is the measurement between the top of the washwater troughs and the top of the media surface
 - Take measurements when and where level readings were taken

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Backwash Procedure

- Every plant needs an SOP
 - Everyone needs to backwash the same way every time
 - Variable rate of backwashing
 - Wide open and shut is not good
 - Ramp up: 25%, 50%, 75% then 100% and back down when finished
 - Rewash
 - Time
 - Not too clean nor left too dirty
 - How often
 - Hours run, effluent turbidity, head loss

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Conditions of Backwash

- Intensity
- Time
- Efficiency

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Backwash Intensity

- Measured by:
 - Backwash flow rate
 - ~15-20 gpm/ft²
 - Design Criteria requires a minimum rate of 18.75 gpm/ft² for sand filter
 - Filter bed expansion
 - ~20-30%
 - Design Criteria recommends 50%
 - 4.2.1 K(1)

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Length of Backwash

- Do not wash the filter too much
- Wash until water coming through the bed is about 10 NTU

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Backwash Observations

- Media boils
 - Look for these toward the end of the backwash, you must be able to see the media
- Uneven backwash water distribution
 - Check for areas that are not moving, these areas are not being sufficiently washed and normally have mudballs in that area

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Backwash Observations continued

- Media carryover
 - Can be several issues going on for media carryover
 - Backwash water jetting under trough
 - Too much media expansion near the bottom of the trough
 - Too high a backwash rate

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Backwash Bed Expansion

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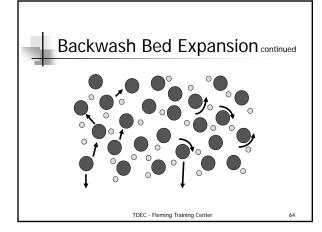


Backwash Bed Expansion

- Backwash rate needs to be high enough to completely suspend the filter media in the water
 - To clean the filter bed, the media grains need to be moved and bumped into each other.
 - This creates a scrubbing action that releases the floc from the media

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Backwash Bed Expansion continued

- Inadequate bed expansion may lead an operator to believe filter is clean due to backwash water looking "clean"
 - If media is not expanded enough to rub together and knock loose the dirt, backwash water will look clean

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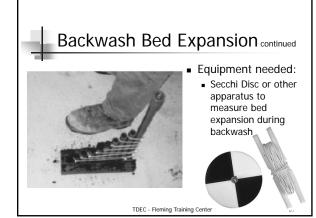
65



Backwash Bed Expansion continued

- If the filter is not sufficiently expanded during backwash, it will not be sufficiently cleaned
- This can lead to numerous problems:
 - Poor post-backwash recovery
 - Sensitivity to hydraulic surges during flow changes
 - Shortened filter run times
 - Mudball formation

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Backwash Bed Expansion continued

- Steps
 - Determine average media depth
 - Poke 5-ft ruler or steel rod into filter media at random spots until you reach support gravel or
 - Determined by feel or the sound of a "crunch" once you hit gravel
 - If you are using a steel rod, pinch at surface and carefully pull it out, tape at that point then measure distance
 - Determine average media depth

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Backwash Bed Expansion continued

- Steps
 - Determine bed expansion using a Secchi disk
 - Using a Secchi disk on a rope, lower the disk into the water until you reach the top of the filter
 - Place piece of tape on rope at handrail level
 - Remove the Secchi disk
 - Start backwash

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Backwash Bed Expansion continued

- Steps
 - Determine bed expansion using a Secchi disk
 - Once water clears, lower Secchi disk back down into filter until small amounts of filter cover the disc
 - If it becomes completely submerged, raise and slowly lower again
 - Place piece of tape on rope at handrail level
 - Measure distance between two pieces of tape

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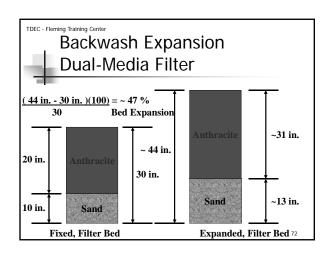
Backwash Bed Expansion continued

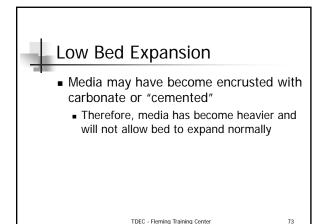
- Steps
 - Determine bed expansion using a Secchi disk
 - The distance between the two pieces of tape is your bed expansion in inches

Bed expansion, $\% = \frac{\text{(Bed expansion, in)}(100)}{\text{Media depth, in}}$

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Water Temp vs. Backwash Rates

- Changes in water temperature will affect your backwash rates
- Cold water is more viscous than warm water
- Imagine dropping filter media into cold maple syrup and warm maple syrup
 - Media will stay suspended for a longer period of time in the cold maple syrup
 - Same goes for filter media in cold water versus warm water

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Water Temp vs. Backwash Rates cont.

- If backwash flow rates stay the same, yearround, you will get a higher bed expansion during colder water temps than warmer water temps
 - If rates are not changed during summer and winter months
 - Mudballs may occur during the summer
 - Media loss may occur during the winter
 - Colder water temps need lower backwash rates
 - Warmer water temps need higher backwash rates

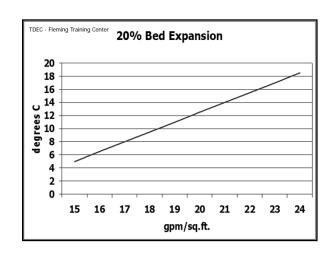
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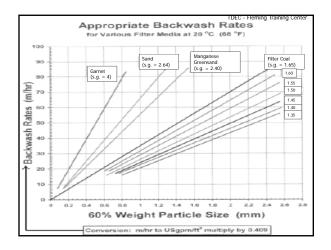
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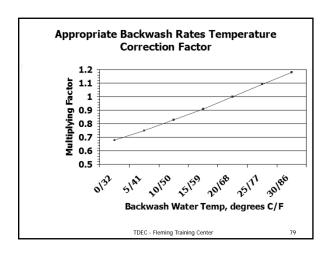
Water Temp vs. Backwash Rates cont.

- Check bed expansion seasonally
 - Chart water temperature and backwash rate that allows a 20% bed expansion throughout the year
 - If you have different filter designs, do one for each design

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Filter Bed Expansion Worksheet

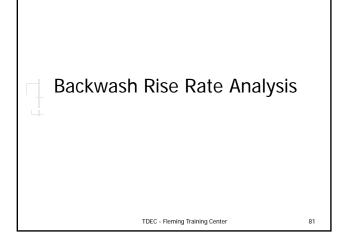
| Filter Media Depth Measurements | | | |
|---|-----------------|--------------|-----------------|
| Measurements | Media | Measurements | Media Depth, in |
| | Depth, in | | |
| 1 | | 11 | |
| 2 | | 12 | |
| 3 | | 13 | |
| 4 | | 14 | |
| 5 | | 15 | |
| 6 | | 16 | |
| 7 | | 17 | |
| 8 | | 18 | |
| 9 | | 19 | |
| 10 | | 20 | |
| Sum of | | Sum of | |
| Measurements | | Measurements | |
| Total Depth = Add the sums of the two columns of | | | |
| | measurements | | |
| Average Depth = Divide the total depth by the number of | | | |
| measurements | | | |
| Bed Expansion, in | | | |
| Bed Expansion, $\% = (Bed Expansion, in)(100)$ | | | |
| Average Media Depth, in | | | |
| Wate | er Temperature | e, °C | |
| Backwash | n Control Valve | , % Open | |
| Is this | the desirable 2 | 0-30% | |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |

Bed Expansion Math

| 1. | While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 4 ¼ inches. The average media depth was 30 inches. Calculate the bed expansion in percent. |
|----|---|
| 2. | While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 6 $\frac{1}{2}$ inches. The average media depth was 31 inches. Calculate the bed expansion in percent. |
| 3. | While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 8 inches. The average media depth was 36 inches. Calculate the bed expansion in percent. |
| 4. | Filter 5 at a water plant has an average media depth of 29 inches. The bed expanded by 8 inches during backwash. What is the bed expansion in percent? |
| 5. | Filter 2 at a water plant has an average media depth of 28 inches. The bed expanded by 4 inches during backwash. What is the bed expansion in percent? |
| 6. | Filter 16 at a water plant has an average media depth of 32 inches. The bed expanded by 10 inches during backwash. What is the bed expansion in percent? |

7. Calculate the filter bed expansion if the average media depth is 33 inches and the bed expansion is 5.5 inches. 8. Calculate the filter bed expansion if the average media depth is 34 ½ inches and the bed expansion is 7 inches. 9. Calculate the filter bed expansion if the average media depth is 28 inches and the bed expansion is 9 inches. 10. Calculate the filter bed expansion if the average media depth is 31 inches and the bed expansion is 5 inches. Answers: 6. 31% 1. 14% 7. 17% 2. 21% 3. 22% 8. 20% 4. 28% 9. 32% 5. 14% 10. 16%





Backwash Flow Rate Analysis

- Also known as rise test
- Determines actual backwash rate in gpm/ft² and gpm
- Backwash flow meters can become inaccurate and may need calibration
 - Determines meter accuracy

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Backwash Flow Rate Analysis

- Equipment needed:
 - Hook gauge two hooks 6 inches apart
 - Stop watch
 - Tape measure
 - Calculator

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Backwash Flow Rate Analysis

continued

- Recommended backwash rates:
 - Single media filters = 18.75 gpm/ft²
 - Dual media filters = 20 gpm/ft²

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Backwash Flow Rate Analysis

continue

- Steps
 - Measure the length and width of the filter bed and basin
 - Place hook gauge in filter with the top hook well below the washwater troughs
 - Make sure the hook gauge is level front to back and side to side
 - Drain the filter

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Backwash Flow Rate Analysis

continue

- Steps
 - Begin backwash
 - Start the timer when the water reaches the top of the bottom hook
 - Stop the timer when the water reaches the top of the top hook
 - Record time
 - Drop water below bottom nail and repeat two more times

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Backwash Flow Rate Analysis

continued

- Number Crunch
 - Calculate the volume of the water that rose in the filter

 $volume, gal = (filter\ bed\ length,\ ft)(filter\ bed\ width,\ ft)(0.5\ ft\ depth)(7.48\ gal/\ ft^3)$

■ Calculate the average time in minutes

avg. time, min =
$$\frac{(Time_1 + Time_2 + Time_3)}{(3)(60 \text{ sec/ min})}$$

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Backwash Flow Rate Analysis

continued

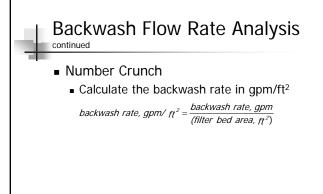
- Number Crunch
 - Calculate the filter bed area

filter bed area, ft2 = (bed length, ft)(bed width, ft)

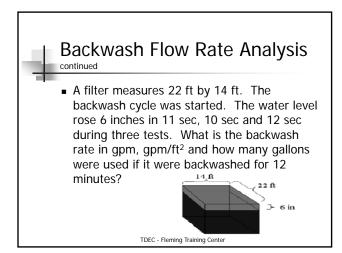
Calculate backwash rate in gpm

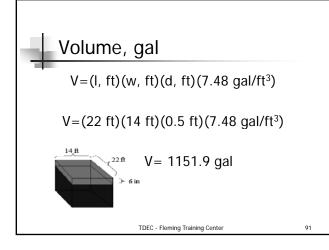
$$backwash\ rate,\ gpm = \frac{volume,\ gal}{(avg.\ time,\ min)}$$

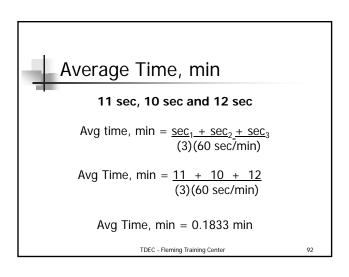
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Sand Bed Area

A filter measures 22 ft by 14 ft.

Sand Area, $ft^2 = (length, ft)(width, ft)$

Sand Area, $ft^2 = (22 \text{ ft})(14 \text{ ft})$

Sand Area, $ft^2 = 308 ft^2$

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Backwash Rate, gpm/ft2

Filter rate, gpm= volume, gal average time, min

Filter rate, gpm = 1151.9 gal0.1833 min

Filter rate, gpm = 6284 gpm

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0.4

Volume, gal = 1151.9 gal Time, min = 0.1833 min Area, ft² = 308 ft²

Backwash Rate, gpm = 6284 gpm Volume, gal = 1151.9 gal Time, min = 0.1833 min Area, ft² = 308 ft² Backwash Rate, gpm/ft²

Filter rate gpm/ft²=filter rate, gpm sand area, ft²

Filter rate, gpm/ft² = $\frac{6284 \text{ gpm}}{308 \text{ ft}^2}$

Filter rate, $gpm/ft^2 = 20.4 gpm/ft^2$

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Backwash Gallons Used

Backwash Vol., = (Backwash Rate,)(Sand Area,)(time,) gal gpm/ft^2 ft^2 min

Backwash Vol., gal = $(20.4 \text{ gpm/ft}^2)(308 \text{ ft}^2)(12 \text{ min})$

Backwash Vol., gal = 75,398.4 gallons

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|-------------------------------|------------------|--|
| Backwash Flow Rate | Bed Expan., % | Action Needed |
| Low | <20% | ↑ backwash flow rate and repeat bed expan. analysis |
| Low | 20-30% | ↑ backwash flow rate and repeat bed expan. analysis |
| Low | >30% | Check water temp |
| Correct | <20% | "cementing" of filter? |
| Correct | 20-30% | None |
| Correct | >30% | Check effective size and uniformity coefficient |
| High | <20% | "cementing" of filter? |
| High | 20-30% | "cementing" of filter? |
| High | >30% | ↓ backwash flow rate and repeat bed expan. analysis |

Backwash Rate Analysis Worksheet

| | Filter Ba | y Dimensions | |
|----------------|------------------------------|----------------------------------|------------|
| Length | ft | Width | ft |
| | | | |
| | Filter Be | ed Dimensions | |
| Length | ft | Width | ft |
| | | | |
| | Time to | Drop 6 inches | |
| | Time₁ | Se | 9C |
| | Time ₂ | Se | 9C |
| | Time ₃ | Se | ec ec |
| | | | |
| | Backw | vash Volume | |
| vol, gal = (b | ed length, ft)(bed widti | h, ft)(0.5 ft rise)(7.48 g | al/ ft³) |
| | average time, min = Tin | $ne_1 + Time_2 + Time_3$ | |
| | | | |
| filter | bed area, $ft^2 = (bed let)$ | ength, ft)(bed width, ft) | |
| | backwash rate, gpm = | vol , gal | |
| | | | |
| bac | ckwash rate, gpm/ ft² = | backwash rate, gpm | |
| 200 | minden rate, gp ft | filter bed area, ft ² | |
| backwash water | r vol., gal = (backwash | rate, gpm)(time backwa | shed, min) |
| | | | |
| Is this suffic | ient backwash rate for | your media to achieve | at least |
| | 20% expai | nsion? | |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |

Backwash Math

1. A filter measures 28 feet by 20 feet. The backwash cycle is started and the water rises 6" in 12, 13, and 13 seconds. What is the backwash rate in gallons per minute per square foot (gpm/ft²)?

2. The Randyville Water Plant treats an average of 5.18 MGD. The water is split equally to each of the 8 filters. Each filter basin measures 12 feet wide by 16 feet long and by 24 feet deep. Each filter bed measures 12 feet by 14 feet by 11 feet deep. Filter 6 is taken offline to backwash. Using a hook gauge and a stopwatch, it is noted that the water level in the filter rises 6 inches in 14, 16, and 15 seconds. What is the backwash rate in gallons per minute per square foot (gpm/ft²) and how many gallons were used if the filter was backwashed for 9 minutes?

3. The Chrisburg Water Plant treats an average of 7.2 MGD. The water is split equally to each of 8 filters. Each filter basin measures 12.5 feet wide by 16.5 feet long by 24 feet deep. Each filter bed measures 12.5 feet by 14 feet by 10 feet deep. Filter 6 is taken offline to backwash. Using a hook gauge and a stopwatch, it is noted that the water level in the filter rises 6 inches in 12 seconds on test 1, 6 inches in 11 seconds on test 2 and 6 inches in 14 seconds on test 3. What is the backwash rate in gallons per minute per square foot (gpm/ft²)?

| 4. | Determine the backwash rate in gpm/ft² for a filter with a surface of 28 feet by 20 feet. The backwash cycle started and the water rose 6 inches in 15, 16, and 16 seconds. |
|----|--|
| 5. | Determine the backwash rate in gpm/ft² for a filter bay that is 10 by 14 feet and the filter bed is 10 by 12 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 17, 16, and 16 seconds. |
| 6. | Determine the backwash rate in gpm/ft² for a filter bay that is 15 by 22 feet and the filter bed is 15 by 20 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 18, 17, and 20 seconds |
| 7. | Determine the backwash rate in gpm/ft² for a filter bay that is 16 by 18 feet and the filter bed is 16 by 16 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 11, 10, and 9 seconds |

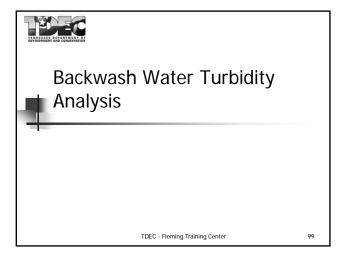
8. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 12 minutes for a filter bay that is 14 by 18 feet and the filter bed is 14 by 16 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 18, 17, and 20 seconds

9. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 14 minutes for a filter bay that is 20 by 32 feet and the filter bed is 20 by 30 feet. The test was run three times. The times required for the water to rose 6 inches were 13, 12 and 15 seconds.

10. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 9 minutes for a filter bay that is 24 by 36 feet and the filter bed is 24 by 34 feet. The test was run three times. The times required for the water to rose 6 inches were 14, 15 and 16 seconds.

Answers:

- 1. 17.72 gpm/ft²
- 2. 14.96 gpm/ft², 22,619.5 gal
- 3. 18.19 gpm/ft²
- 4. 14.32 gpm/ft²
- 5. 13.74 gpm/ft²
- 6. 12.24 gpm/ft²
- 7. 22.44 gpm/ft²
- 8. 12.24 gpm/ft², 32,901 gal
- 9. 16.83 gpm/ft², 141,372 gal
- 10. 14.96 gpm/ft², 109,866 gal





Backwash Water Turbidity

- Used to determine adequate backwashing duration
- Desired backwash time is determined by the amount of time to drop the backwash water turbidity in the range of 10-15 NTU
 - AWWA recommends 10 NTU as the cutoff for backwashing
- Target time is 6-8 minutes

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Backwash Water Turbidity cont.

- The Interim Enhanced Surface Water Treatment Rule (IESWTR) requires filters to produce water with <0.3 NTU within 30 minutes of the start of the filter run
- Extending backwash until water runs clear may be causing some spikes after backwash
 - The filter may become too clean and needs longer time to "ripen"

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Backwash Water Turbidity cont.

- Equipment needed:
 - Stop watch
 - Sampler for grabbing samples of backwash water
 - Turbidimeter
 - 30 100-mL sample bottles marked in oneminute intervals

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Backwash Water Turbidity cont.

- Procedure:
 - Place all bottles in order
 - One person needed to keep time with stopwatch and another person needed to collect samples
 - Start normal backwash cycle and stopwatch
 - Collect samples of backwash water in trough near discharge end (so it is well mixed) at one-minute intervals with sampler

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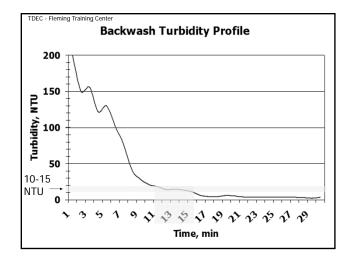
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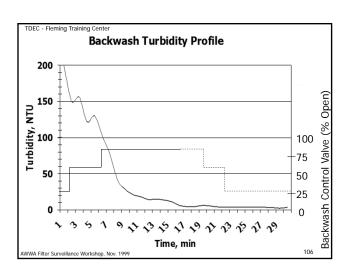


Backwash Water Turbidity cont.

- Procedure:
 - Fill 100-mL sample bottles to the line and dump remainder back into filter
 - Repeat this procedure every minute until backwash is complete, extend normal backwash time about 3-5 minutes
 - Take each sample to turbidimeter
 - Mix samples thoroughly and read on turbidimeter
 - Plot readings on graph paper

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Backwash Water Turbidity cont.

- Troubleshooting:
 - Water clears up after about 2-3 minutes of backwashing?
 - You may be only cleaning the top layer of anthracite
 - To fix this problem, raise backwash flow rate
 - Takes a long time to drop to 10-15 NTU range?
 - Filter may have been dirty for a long time and you are finally cleaning the filter

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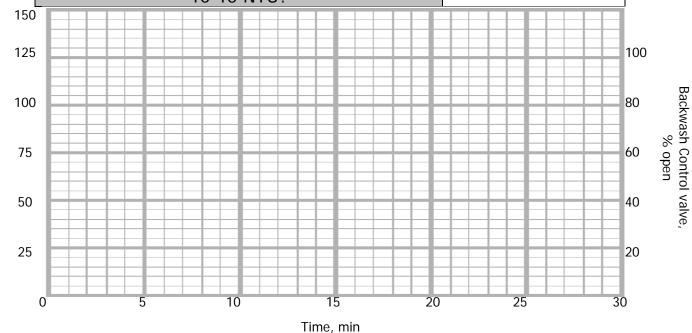
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Backwash Water Turbidity Analysis

| Time, min | Backwash Water | Time, min | Backwash Water |
|-----------|----------------------------|-------------|----------------|
| | Turbidity | | Turbidity |
| 1 | | 16 | |
| 2 | | 17 | |
| 3 | | 18 | |
| 4 | | 19 | |
| 5 | | 20 | |
| 6 | | 21 | |
| 7 | | 22 | |
| 8 | | 23 | |
| 9 | | 24 | |
| 10 | | 25 | |
| 11 | | 26 | |
| 12 | | 27 | |
| 13 | | 28 | |
| 14 | | 29 | |
| 15 | | 30 | |
| What time | did the backwash water for | all hatwaan | |

What time did the backwash water fall between 10-15 NTU?

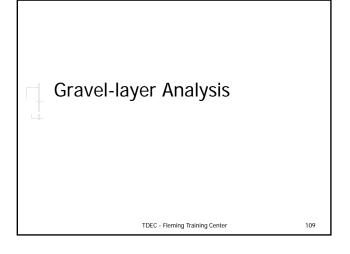
Turbidity, NTU

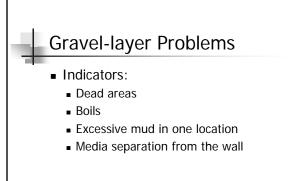


 Filter Number:

 Date:

Time:





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- Equipment needed:
 - 5-ft ruler or steel rod
- This can be done at the same time you are getting media depths

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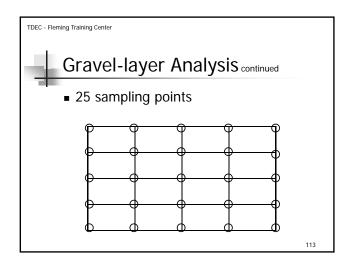
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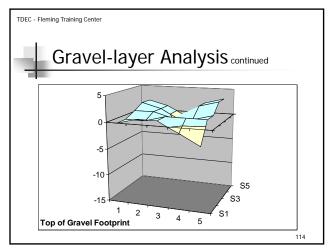


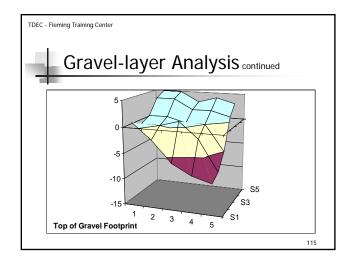
- Procedure:
 - Filter bed dimensions need to be determined, draw a layout of filter bed
 - Divide filter in half length-wise
 - Divide those halves in half
 - Divide filter in half width-wise
 - Divide those halves in half also
 - Where the lines cross are your sampling areas, along with where the lines touch the sides and the corners

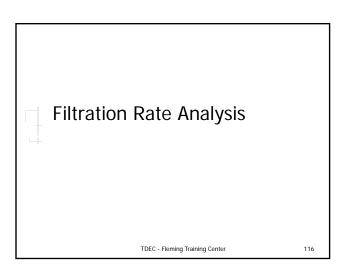
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Filtration Rates Allowed in TN

- Rapid Sand Filters
 - 2.0 gpm/ft² for turbidity removal
 - 3.0 gpm/ft² for iron removal
- High Rate Filters
 - 4.0 gpm/ft² for turbidity and iron removal

State Design Criteria 4.2.1 a. 1 & 2

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Filtration Rate Analysis

- Also known as Hook Gauge
- Determines actual filtration rate in gpm/ft²
- Determines the accuracy of the filtration rate flow meter
- Equipment needed:
 - Hook gauge two hooks 6 inches apart
 - Stop watch
 - Tape measure
 - Calculator

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Filtration Rate Analysis continued

- Steps
 - Measure the length and width of the filter bed and basin
 - Place hook gauge in filter with the top hook well below the surface of the water
 - Make sure the hook gauge is level front to back and side to side
 - Close the influent valve, leaving the effluent valve open
 - Record meter's flow

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Filtration Rate Analysis continued

- Steps
 - Start the timer when the water breaks the surface of the first hook
 - Stop timer when the water breaks the surface of the second hook
 - Record time
 - Refill basin and repeat two more times

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Filtration Rate Analysis continued

- Number Crunch
 - Calculate the volume of the water that passed through the filter

volume, gal = (filter bay length, ft)(filter bay width, ft)(0.5 ft depth)(7.48 gal/ ft³)

Calculate the average time in minutes

avg. time, min = $\frac{(Time_1 + Time_2 + Time_3)}{(3)(60 \text{ sec/ min})}$

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Filtration Rate Analysis continued

- Number Crunch
 - Calculate the filter bed area

filter bed area, ft² = (bed length, ft)(bed width, ft)

Calculate filtration rate in gpm

 $filtration rate, gal/min = \frac{volume, gal}{avg. time, min}$

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Filtration Rate Analysis continued

- Number Crunch
 - Calculate filtration rate in gpm/ft²

filtration rate, gpm/ $ft^2 = \frac{\text{filtration rate, gal/min}}{\text{filter bed area, } ft^2}$

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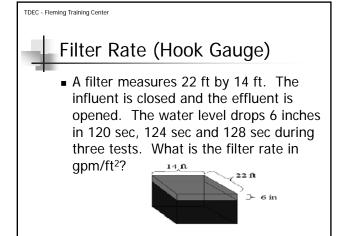
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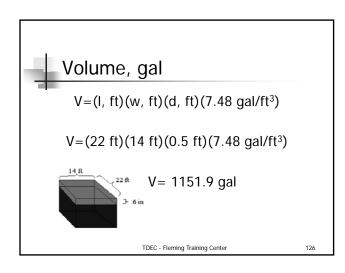


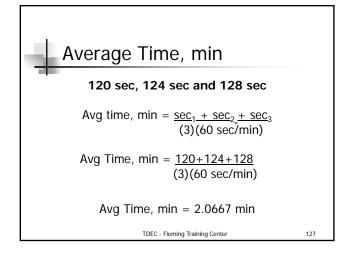
Filtration Rate Analysis continued

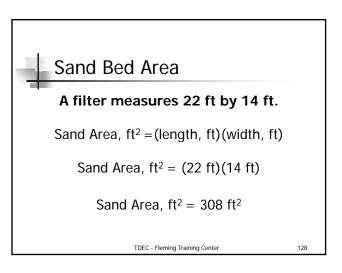
- Is the calculated flow rate greater than the State's allowable rate?
 - Slow down the filtration rate
- Is the calculated flow rate equal to the flow meter?
 - If not, re-do hook gauge
 - If it is still off, the flow meter needs to be calibrated

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Volume, gal = 1151.9 gal Time, min = 2.0667 min Area, ft² = 308 ft²

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Filter Rate, gpm/ft²

Filter rate, gpm= volume, gal (Hook Gauge) average time, min

Filter rate, gpm = $\frac{1151.9 \text{ gal}}{2.0667 \text{ min}}$

Filter rate, gpm = 557.4 gpm

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Filtration Rate, gpm = 557.4 gpm Volume, gal = 1151.9 gal Time, min = 2.0667 min Area, ft 2 = 308 ft 2

Filter rate gpm/ft²=<u>filter rate, gpm</u> sand area, ft²

Filter rate, gpm/ft² = $\frac{557.4 \text{ gpm}}{308 \text{ ft}^2}$

Filter rate, $gpm/ft^2 = 1.8 gpm/ft^2$

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Filtration Rate Analysis Worksheet

| Filter Bay Dimensions | | | | |
|-----------------------|---------------------------------------|--|----------|--|
| Length | ft | Width | ft | |
| | | | | |
| | Filter Be | ed Dimensions | | |
| Length | ft | Width | ft | |
| | | | | |
| | Time to | Drop 6 inches | | |
| | Time ₁ | Se | ec | |
| | Time ₂ | Se | ec | |
| | Time ₃ | Se | ec | |
| | | | | |
| | Filter | red Volume | | |
| vol, gal = (b | ay length, ft)(bay width | n, ft)(0.5 ft drop)(7.48 g | al/ ft³) | |
| | average time, min = ^{Tin} | $ne_1 + Time_2 + Time_3$ | | |
| • | average time, min = | (3)(60 <i>sec/min)</i> | | |
| filter | r bed area, ft² = (bed le | ength, ft)(bed width, ft) | | |
| filtration r | rate anm/ H^2 – | <i>vol</i> , <i>gal</i> <i>me</i> , min)(<i>filter bed area,</i> | | |
| muanom | $aic, gpiii, ii = \frac{1}{(avg.tii}$ | <i>me</i> , min)(<i>filter bed area,</i> | ft^2) | |
| Is this the allo | owable filtration rate | for the State of TN? | | |

| Rapid Sand Filters | | | | |
|--|--|--|--|--|
| 2.0 gpm/ft ² for turbidity removal 3.0 gpm/ft ² for iron removal | | | | |
| High Rate Filters | | | | |
| 4.0 gpm/ft ² for iron and turbidity removal | | | | |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |

Filtration Math

1. A filter measures 28 feet by 20 feet. The influent is closed and the effluent is opened and the water drains down 6" in 120, 125, and 113 seconds. What is the filter-loading rate in gallons per minute per square foot (gpm/ft²)?

2. The Randyville Water Plant treats an average of 5.18 MGD. The water is split equally to each of the 8 filters. Each filter basin measures 12 feet wide by 16 feet long and by 24 feet deep. Each filter bed measures 12 feet by 14 feet by 11 feet deep. The influent line to Filter 6 is closed while the effluent remains open. Using a hook gauge and a stopwatch, it is noted that the water level in the filter drops 6 inches in 80, 86, and 89 seconds. What is the filtration rate in gallons per minute per square foot (gpm/ft²)?

3. The Chrisburg Water Plant treats an average of 7.2 MGD. The water is split equally to each of 8 filters. Each filter basin measures 12.5 feet wide by 16.5 feet long by 24 feet deep. Each filter bed measures 12.5 feet by 14 feet by 10 feet deep. The influent line to Filter 6 is closed while the effluent remains open. Using a hook gauge and a stopwatch, it is noted that the water level in the filter drops 6 inches in 69 seconds on test 1, 6 inches in 67 seconds on test 2 and 6 inches in 70 seconds on test 3. What is the filtration rate in gallons per minute per square foot (gpm/ft²)?

| 4. | Determine the filtration rate in gpm/ft ² for a filter with a surface of 28 feet by 20 |
|----|---|
| | feet. With the influent valve closed, the water above the filter dropped 6 inches in |
| | 57, 56, and 60 seconds. |

5. Determine the filtration rate in gpm/ft² for a filter bay that is 10 by 14 feet and the filter bed is 10 by 12 feet. The test was run three times. The times required for the water to drop 6 inches were 135, 132 and 129 seconds.

6. Determine the filtration rate in gpm/ft² for a filter bay that is 15 by 22 feet and the filter bed is 15 by 20 feet. The test was run three times. The times required for the water to drop 6 inches were 79, 85 and 80 seconds.

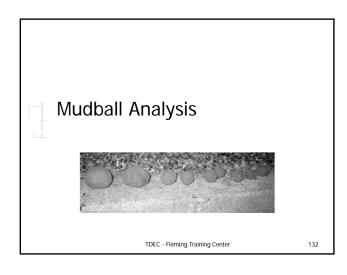
7. Determine the filtration rate in gpm/ft² for a filter bay that is 16 by 18 feet and the filter bed is 16 by 16 feet. The test was run three times. The times required for the water to drop 6 inches were 65, 62 and 64 seconds.

| 8. | Determine the filtration rate in gpm/ft ² for a filter bay that is 14 by 18 feet and the filter bed is 14 by 16 feet. The test was run three times. The times required for the water to drop 6 inches were 72, 75 and 76 seconds. |
|-----|--|
| | |
| 9. | Determine the filtration rate in gpm/ft ² for a filter bay that is 20 by 32 feet and the filter bed is 20 by 30 feet. The test was run three times. The times required for the water to drop 6 inches were 61, 59 and 58 seconds. |
| | the water to drop 6 inches were 61, 59 and 58 seconds. |
| | |
| 10. | Determine the filtration rate in gpm/ft ² for a filter bay that is 24 by 36 feet and the filter bed is 24 by 34 feet. The test was run three times. The times required for |

the water to drop 6 inches were 62, 60 and 59 seconds.

Answers:

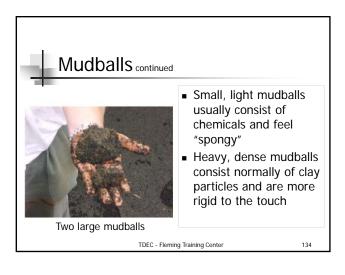
 1.98 gpm/ft²
 3.03 gpm/ft²
 3.97 gpm/ft²
 3.40 gpm/ft² 9. 4.03 gpm/ft² 10. 3.94 gpm/ft² 1. 1.88 gpm/ft² 2. 3.02 gpm/ft² 3. 3.85 gpm/ft² 4. 3.89 gpm/ft²

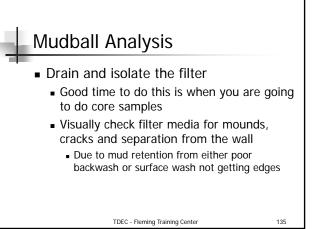


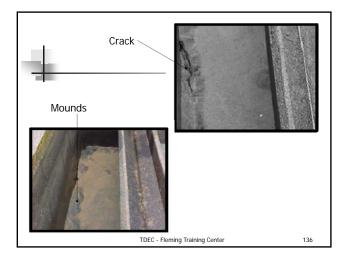


- Caused by grains of filter media covered with sticky floc material
 - If not effectively removed by backwashing, the grains clump together to form mudballs
- As they become larger, they sink into the filter bed and clog areas where they settle
- These areas become inactive, causing higherthan-optimal filtration rates in the remaining active areas and unequal distribution of backwash water

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Mudball Analysis By Hand

- Lay plywood boards down on top of filter media
 - To avoid stepping onto media
- Pick a location and start digging with your hands
 - This creates a smaller hole as opposed to digging with a shovel
- Gently sift through media with your hands searching for mudballs

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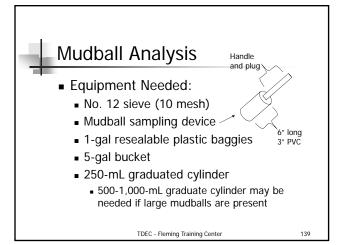


Mudball Analysis By Hand cont.

- As you are digging, look for separation of sand and anthracite
 - Measure depth of each separate media and make note of these depths
- Removal:
 - Manually
 - Soak the media in acidic water
- Backwash procedures will have to be modified to prevent accumulation of mudballs in the future

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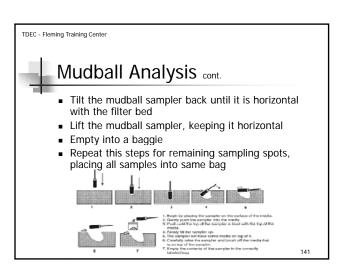


Mudball Analysis cont.

- Backwash filter
- Drain the water from the filter to a point below the media surface
- Select five sampling points at random
- Beginning with the first sampling point, push the mudball sampler 6 inches into the media

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Mudball Analysis cont.

- Put water in 5-gal bucket until about half-full
- Lower the No. 12 sieve into the water until nearly submerged
- Put sampled media into sieve, handful at a time
- Carefully raise and lower the sieve into the water to wash media through the mesh

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Mudball Analysis cont.

- Continue placing handfuls of media, lowering and raising sieve until all media has been sieved
- Gently wash any mudballs collected to one side of the sieve

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Mudball Analysis cont.

- Fill 250-mL graduated cylinder to the 200-mL mark
 - May need 500 to 1000-mL graduated cylinder if you have large mudballs
- Gently transfer the mudballs from the sieve to the graduated cylinder
- Read and record new volume

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Mudball Analysis cont.

■ Number crunch:

Media Sample Vol, mL = $\frac{(0.785)(D^2)(H)(N)(3,785mL / gal)}{231 \text{ in}^3 / gal}$

Where: D = diameter, in

H = height of sampler, inN = number of samples taken

Media Sample Vol, mL = $\frac{(0.785)(3^2)(6)(5)(3,785mL / gal)}{231 \ln^3 / gal} = 3472.6mL$

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Mudball Analysis cont.

■ Number crunch:

Mudball Volume, mL = Final Cylinder Vol, mL - Initial Cylinder Vol, mL

% Mudballs = $\frac{\text{(Mudball Vol, mL)}(100)}{\text{Media Sample Vol, mL}}$

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Mudball Analysis cont.

| % Mudballs | Filter Bed Condition | |
|------------------|----------------------|--|
| 0.0 - 0.1 | Excellent | |
| 0.1 – 0.2 | Very good | |
| 0.2 - 0.5 | Good | |
| 0.5 – 1.0 | Fair | |
| 1.0 – 2.5 | Fairly bad | |
| 2.5 – 5.0 | Bad | |
| Greater than 5.0 | Very bad | |

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Mudball Analysis cont.

- Easy mudball removal
 - Use of strainer basket during a low-rate backwash
 - Break up of mudballs by using a rake
 - Passing media through large sieves that will let media less than 1 inch pass through

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Mudball Analysis cont.

- More difficult mudball removal
 - Injection of high-pressure air or water into media to bring mudballs to the surface
 - Chemical addition to break up mudballs
 - Removal of media and cleaning or replacing it
 - Replacing does not fix the problem, backwash procedures need to be re-evaluated

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Mudball Analysis Worksheet

| Coring Do | | | | g Device | | |
|---|-------------------|-----------|-------------|---------------------|-----------|---------------------|
| Diamet | ter | <u>i</u> | n D | epth | | in |
| | | N.O | -U U M - I- | | | |
| | | IVIU | dball Volu | ime | | |
| Initial Cyli | nder Readi | ng (V1) | | | | mL |
| Final Cylin | der Readir | ng (V2) | | | | mL |
| | olume (V1 | | | | | mL |
| Media Sample Vol, $mL = \frac{(0.785)(D^2)(H)(N)(3.785mL / gal)}{231 in^3 / gal}$ | | | | | | |
| Where: D = diameter, in | | | | | | |
| H = height of sampler, in | | | | | ml | |
| N = number of samples taken (Mudball Vol. ml.)(100) | | | | | mL | |
| % Mudballs = \frac{(Mudball Vol., mL)(100)}{Media Sample Vol., mL} | | | | % | | |
| | | | | | | |
| Circle the range that corresponds to the value you got | | | | | | |
| 0.0- 0.1 | 0.1 – 0.2 Very | 0.2 – 0.5 | 0.5 – 1.0 | 1.0 – 2.5 Fairly | 2.5 – 5.0 | Greater than 5.0 |
| Excellent | Good | Good | Fair | Bad | Bad | Very Bad |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |

Mudball Math

1. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 250-mL graduated cylinder was filled up to the 200-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 235 mL mark. What is the percent of mudballs if 5 samples were taken?

2. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 500-mL graduated cylinder was filled up to the 300-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 425 mL mark. What is the percent of mudballs if 5 samples were taken?

3. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 250-mL graduated cylinder was filled up to the 200-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 247 mL mark. What is the percent of mudballs if 5 samples were taken?

Answers:

1. 1.0%

2. 3.6%

3. 1.4%





Acid-Soluble Mineral Analysis

Also known as Carbonate Precipitation Analysis

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Presence of Acid-Soluble Minerals

- Calcium carbonate or manganese dioxide may "cement" the filter particles together
 - Increases media weight
 - Decreases bed expansion
 - Reduces filter effectiveness
- Can use muriatic acid to dissolve calcium carbonate, but it may also damage concrete filter bay
 - Have example from a water plant on procedure

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Presence of Acid-Soluble Minerals continued

- Equipment needed
 - Balance
 - Drying oven
 - Dessicator
- Sample can be what is left in 5 gallon bucket from mudball analysis

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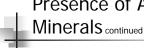
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Presence of Acid-Soluble Minerals continued

- AWWA B100-01 outlines analysis
 - Performed by immersing a known weight of filter media in 1:1 hydrochloric acid until the acid-soluble materials are dissolved, then determining the weight loss

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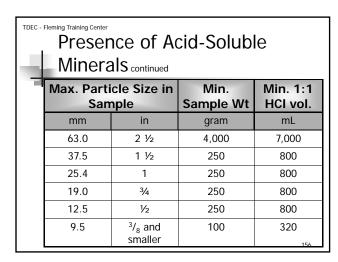


Presence of Acid-Soluble

- 5.3.1 Acid solubility test
 - \blacksquare Wash sample with distilled water and dry at 110 \pm 5°C to a constant weight
 - Cool in dessicator no more than 30 minutes
 - Weigh 200 grams dried sample to nearest 0.1 % of weight of sample
 - Place sample in beaker and add enough 1:1 HCl to immerse sample, but not less than volume indicated on next slide

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Presence of Acid-Soluble Minerals continued

- 5.3.1 Acid solubility test
 - Allow to stand in 1:1 HCl at room temperature for at least 30 minutes after fizzing stops
 - Wash sample with distilled water several times and dry at 110 ± 5°C to a constant weight
 - Cool in dessicator no more than 30 minutes
 - Weigh dried sample to nearest 0.1 % of weight of sample
 - Report loss in weight as acid-soluble material

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Acid-Soluble Mineral Analysis Worksheet

| Weigh Measurements | | | | | | |
|---|---------------------------|------------|-------|--|--|--|
| Initial Sample | | | | | | |
| Weight | grams | Weight | grams | | | |
| | Calcul | ations | | | | |
| | | | | | | |
| | Initial Weight, grams - F | | grams | | | |
| Percent Carbonate - | (Carbonate Weight, gr | rams)(100) | | | | |
| Percent Carbonate = $\frac{\text{(Carbonate Weight, grams)(100)}}{\text{Initial Weight, grams}}$ gram | | | | | | |
| | | | | | | |
| Additional Comments | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |





Sieve Testing Procedure

Effective Size & Uniformity Coefficient

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Uniformity Coefficient and Effective Size

- From the design specifications, find out what the uniformity coefficient and effective size was supposed to be for each type of media
 - Gravel
 - Sand
 - Coal

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Uniformity Coefficient

- The lower the uniformity coefficient, the more uniform the size of the media
- The more uniform the media size, the slower the head loss buildup of a filter
- Sand
 - Not greater than 1.7
- Anthracite
 - Not greater than 1.85

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Uniformity Coefficient continued

- Time consuming test
 - Takes 2-3 days
- The ratio of particle diameters as determined by sieve analysis
- It is a measure of how well or poorly sorted the sediment is

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Effective Size

- The smaller the media, the lower the effluent turbidity
- But less run time as well
- Sand
 - 0.35 mm to 0.55 mm
- Anthracite
 - 0.8 mm to 1.2 mm

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Determination of Uniformity Coefficient & Effective Size



- No. 200 sieve
- Set of sieves
 - Numbers 3½, 10, 20, 30, 40, 60, lid and receiver
- Drying oven
 - Set at a controlled temperature of 105-110°C
- Set of metal pans for drying and weighing samples
- A balance of 250 gram capacity and accurate to 0.01 gram

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Determination of Uniformity Coefficient & Effective Size cont.

- Drain and isolate filter
- Determine sampling sites
 - 3-4 sites for a representative sample
- Enter filter and stand on plywood
- Place coring device (metal pipe ~1.5 inches in diameter) into media and push down until you come to resistance or hear the crunch of gravel
- Place hand on top of coring device to provide suction

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Determination of Uniformity Coefficient & Effective Size cont.

- Slowly raise coring device out of media, still with hand on top to provide suction
- Lay aluminum foil sheet down on plywood
- Gently tip the end of the coring device so the contents are slowly emptied across the length of the aluminum foil
- Separate the sand and anthracite at the interface

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Determination of Uniformity Coefficient & Effective Size cont.

- Repeat these steps for the next samples
- Label two bags, one for sand and one for anthracite

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Determination of Uniformity Coefficient & Effective Size cont.

- Begin with about a 100-gram sample of sand
 - Repeat for anthracite as well
- Dry in 105-110°C oven for two hours
- Weigh dry sand sample (WD)
- Label and weigh metal sample pans, and set aside

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Determination of Uniformity Coefficient & Effective Size cont.

- Fill sand sample container with tap water, shake and decant wash water through No. 200 sieve
- Wash material retained on sieve back into sample container
- Repeat several times until wash water is clear

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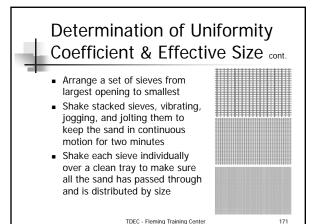


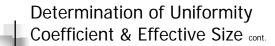
Determination of Uniformity Coefficient & Effective Size cont.

- Dry sand again in 105-110oC oven for two hours
- Weigh dry washed sand (WDS) and subtract from dry weight to determine weight of fines
- Wt. of fines = WD WDS

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- Pour the sand off each sieve into labeled, weighed pans
- Weigh and determine the sample weight (WS) by subtracting the weight of the pan
- Determine the percent passing for each sieve by:
 - % of material retained on the sieve = WS x 100% WDS

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Determination of Uniformity Coefficient & Effective Size cont.

- % passing = % passing the % retained next largest on sieve sieve
- An example calculation of percent passing each sieve for a 120 gram sample is summarized on the next slide

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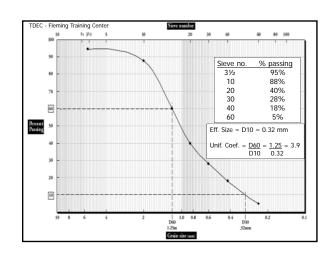
173

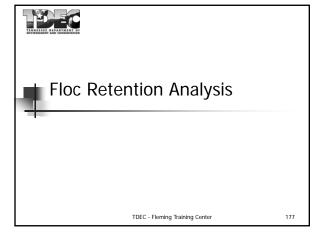
| TDEC - Fleming | TDEC - Fleming Training Center | | | | | | |
|-----------------|---|------------------|---------------|--------------|-----------------------------------|--|--|
| | Sand Particle Size Analysis: | | | | | | |
| Calcu | Calculating Percent Passing Selected Sieves | | | | | | |
| Sieve number | Sieve size | Sample weight | % retained | % passing | % passing next larger sieve | | |
| 3.5 | 5.6 | 6.0 | 5 | 95 | 100 | | |
| 10 | 2.0 | 8.4 | 7 | 88 | 95 | | |
| 20 | 0.85 | 57.6 | 48 | 40 | 88 | | |
| 30 | 0.425 | 14.4 | 12 | 28 | 40 | | |
| 40 | 0.425 | 12.0 | 10 | 18 | 28 | | |
| 60 | 0.25 | 15.6 | 13 | 5 | 18 | | |
| Pan | | 6.0 | 5 | | 5 | | |
| Total Weight | | 120.0 | | | 1/4 | | |

Determination of Uniformity Coefficient & Effective Size cont.

- Graph the percent passing results on semi-log paper
- From the graph, find the Effective Size as D10, where only 10% of the sample is a smaller size
- Also from the graph, find D60, where 60% of the sample is a smaller size
- The Uniformity Coefficient is D60/D10

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Retained Floc

- Some retained floc should remain
 - Too clean turbidity spikes
 - Too dirty mudball formation will occur
 - Just enough very few turbidity spikes will
- All depths of the media should retain a turbidity value of 30-60 NTU

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Floc Retention Analysis

- Some "dirt" should remain in filter
 - This floc retention profile is a way to determine how much "dirt" stays in the filter and at what depths
- AWWA video says to do this annually, but you should do this quarterly to see if seasonal changes affect your filters

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Floc Retention Analysis cont.

- Equipment Needed:
 - 24-36 1-gallon resealable plastic bags
 - Coring device
 - 100-mL graduated cylinder
 - Pint jar "mason" or "jelly" jar
 - 50-mL beaker
 - Turbidimeter
 - 1-liter Erlenmeyer flask



Floc Retention Analysis cont.

- Performed twice on a filter
 - Once before backwashing and
 - Once after backwashing

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Floc Retention Analysis cont.

- Procedure
 - Prepare 2 sets of plastic bags
 - 7 with "Before Backwash"
 - 7 with "After Backwash"
 - Each set needs media depths written on them as well:
 - 0-2 inches
 - ■18-24 inches
 - 2-6 inches
 - •24-30 inches •30-36 inches, just in case 6-12 inches
 - 12-18 inches

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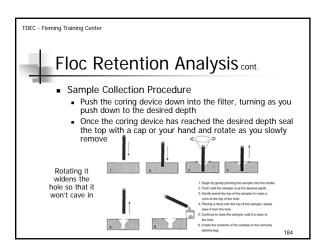


Floc Retention Analysis cont.

- Sample Collection Procedure
 - Select at least three sampling sites
 - Not in the same area
 - Try to get a good composite
 - Completely drain the filter
 - Lay down plywood and enter the filter

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Floc Retention Analysis cont.

- Sample Collection Procedure
 - Break the seal and deposit the media into the appropriate bag for that depth
 - Repeat this process in the same hole for each sample depths
 - Then repeat this whole process in at least two other areas
 - You should have 3 areas sampled at depth of 0-2 inches in one bag, 2-6 inches, etc.

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Floc Retention Analysis cont.

- Sample Collection Procedure
 - Backwash the filter
 - Repeat again, except this time place core samples in bags labeled "After Backwash"

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Floc Retention Analysis cont.

- Sample Analysis Procedure
 - Mix each bag thoroughly and then arrange in order of depth with before and after backwash separated
 - Weigh out approximately 50 grams of media
 - Approximately 50-mL
 - Place into "jelly" jar

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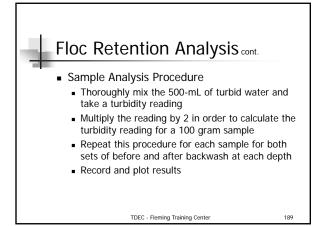




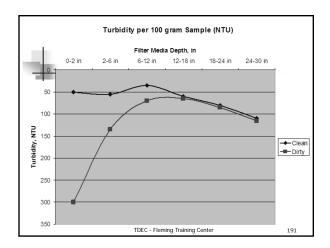
Floc Retention Analysis cont.

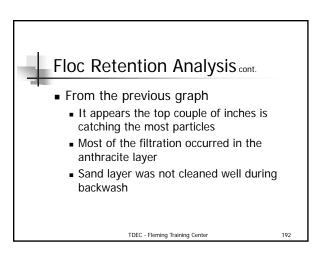
- Sample Analysis Procedure
 - Add 100-mL of tap water
 - Use same 50-mL beaker, filled twice to get 2:1
 - Cap and shake vigorously for 1 minute
 - Decant the turbid water into a 1000-mL flask
 - Repeat the steps of adding 100-mL tap water, shaking and decanting until you have a total of 500-mL

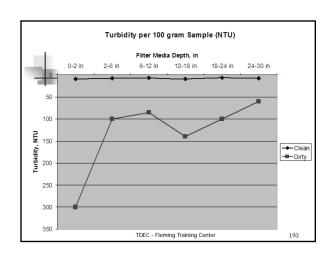
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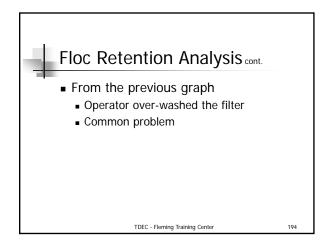


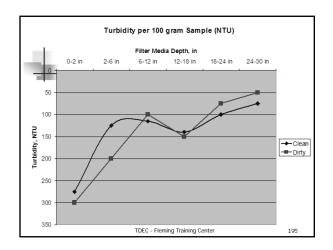
| Floc Retention Analysis cont. | | |
|-------------------------------|--|---|
| Turbidity | Filter Bed Condition | |
| 0-30 NTU | Media too clean, not well ripened | |
| 30-60 NTU | Media clean, slightly ripened; optimal filter performance | е |
| 60-120 NTU | Slightly dirty media, well ripened, should perform well | |
| 120-300 NTU | Dirty media, well ripened; re-evaluate backwash procedure | |
| 300-600 NTU | Dirty media, possible mudballs | |
| 600-1200 NTU | Very dirty media, many mudballs | |
| > 1200 NTU | Extremely dirty; chemical cleaning of media or replacement | |
| | TDEC - Fleming Training Center 190 | |

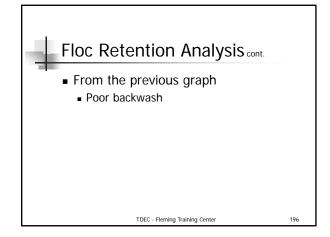










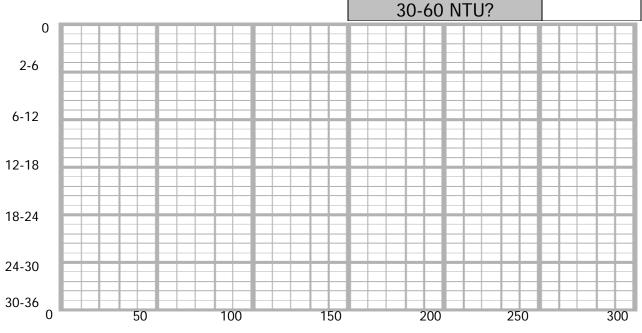




Floc Retention Analysis cont.

- You want most of your particles removed during backwash
 - Filter should be cleaned and ripened
 - Filter can be too clean or too dirty with improper backwash

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 Filter Number:
 Tester:

 Date:

Time, min

Media Depth, in



- Once filter surface is broken, filter bed must be disinfected
- If filter is dosed at 50 mg/L and let sit for 12-24 hours, it will remove mudballs, mud deposits, bacterial growth, iron and manganese deposits on filter walls and within media itself



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Disinfection cont.

AWWA Standard C653-03

- This applies to disinfection of filter basins and gravel, silica sand, anthracite and other mixed media materials except granular activated carbon (GAC)
- If GAC is part of the filter media, special care should be taken to protect the GAC from contamination

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Disinfection cont.

AWWA Standard C653-03

- The entire filter basin should be filled up to the maximum water level and disinfected by one of two methods:
 - Chlorine injected into backwash water
 - Chlorine injected into filter influent while filtering to waste

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Disinfection cont.

■ AWWA Standard C653-03

- Chlorine injected into backwash water
 - Enough chlorine injected to produce at least 25 mg/L free chlorine residual throughout entire filter
 - Chlorinated water shall be allowed to stand in the filter for at least 12 hours
 - Collect samples at the end of 12 hours, free residual chlorine shall not fall below 15 mg/L or else disinfection needs to be repeated

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Disinfection cont.

- AWWA Standard C653-03
 - Chlorine injected into filter influent while filtering to waste
 - Enough chlorine injected to produce at least 25 mg/L free chlorine residual throughout entire filter
 - Turn on filter to waste to get through filter
 - When water with at least 25 mg/L free chlorine residual chlorine reaches the filter-to-waste, the flow of water shall be stopped
 - Filter shall be held for at least 12 hours

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Disinfection cont.

- AWWA Standard C653-03
 - After 12 hour contact time
 - Samples should be collected from the top and bottom of the unit to ensure the free chlorine residual readings measure the lowest chlorine level existing in the unit at the end of the 12-hour period
 - May have to dose at 50-100 mg/L to get residual of 15 mg/L after 12 hours
 - If satisfactory levels of chlorine residuals are obtained, the filter shall be run to waste or backwashed thoroughly to remove highly chlorinated water

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Disinfection cont.

- AWWA Standard C653-03
 - Bacteriological sampling
 - After chlorination and before filter placed back into service, two or more samples shall be taken from the unit not less than 30 minutes apart and shall be tested for the presence of coliform
 - 50% have to be negative, therefore take at least 3 samples, if one is positive, then more than 50% were negative

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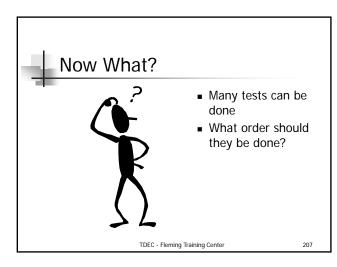


Disinfection cont.

- AWWA Standard C653-03
 - Bacteriological sampling
 - If none of the samples show the presence of coliform, the unit may be placed back into service
 - If positive, take repeat at least 24 hours apart until consecutive samples are negative
 - Or disinfect again and resample

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Order of Tests

- Set up hook gauge
- Establish a fixed point for bed expansion measurements
- Take the initial bed measurement
- Wash plywood sheets with strong hypochlorite solution

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Order of Tests cont.

- Drain filter
 - Run hook gauge (drop test)
 - Look for uneven drainage, cracks, mounding
 - Do not let filter dry out before next steps
- Set up ladders for safely entering and exiting the filter bay
- Lay down plywood to avoid standing on media

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Order of Tests cont.

- Measure levelness of troughs
- Take media depth measurements randomly throughout filter bed
- Take "Before Backwash" core samples for floc retention analysis
- Remove all people and equipment
- Lower hook gauge below troughs

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Order of Tests cont.

- Slowly start backwash to refill filter
 - Observe distribution of backwash water
 - Look for boils, mudballs

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Order of Tests cont.

- While the filter is being backwash:
 - Take samples for backwash water turbidity analysis
 - Take second measurement for bed expansion
 - Perform rise test for backwash water flow rate
 - Afterward raise again to repeat drop test later

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Order of Tests cont.

- After backwash, drain filter again
 - Run hook gauge (drop test)
 - Look for uneven drainage, cracks, mounding
 - Do not let filter dry out before next steps
- Set up ladders for safely entering and exiting the filter bay
- Lay down plywood to avoid standing on media

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Order of Tests cont.

- Take "After Backwash" core samples for floc retention analysis
- Take samples for mudball analysis
- Remove all people and equipment
- Backwash again
- Disinfect
- Run samples in lab

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References

- Filter Evaluation Procedures for Granular Media, 1st Edition. 2003. AWWA
- AWWA Standard B100-01
- Filter Evaluation and Optimization, TAUD – John Shadwick

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Acid Washing and Disinfecting Dual Media Filters

Each filter shall be acid washed and disinfected annually for proper maintenance of filter media. Proper PPE should be worn while handling Hydrochloric acid, Hydrogen Peroxide, Calcium Hypochlorite and Sodium Hypochlorite (respirators, chemical resistant gloves and apron).

Acid Washing:

Note: Before any work on a filter begins, be sure to check that the effluent valve is in the closed position and is placed in the off position.

- 1. Follow the backwashing procedures for a Manual backwash, except when you ramp the wash water back down to zero open the rewash valve and let the filter level go back down to about 0.7 0.9 feet on top of the filter. **Collect media sample after initial backwash. Record time.**
- 2. While running the air sour to mix the acid with filter media add 15 to 20 gallons of 31% Hydrochloric acid or until the water on top of the filter reaches a pH of 1.8 to 1.9, document the results. Let the air scour mix the acid for 1 hour.
- 3. Record beginning and end times.
- 4. Wash the filter again so that the pH is elevated back up to normal (6.5 7.0) and document the results (pH prior to disinfection) and time spent in air scour acid wash.
- 5. Once pH is adjusted back around 7.00, drop the water level on top of the filter to 1.00 foot.
- 6. Add 12 pounds of 65% HTH (Calcium Hypochlorite) (this number is not exact and should be adjusted accordingly with varying water levels on top of the filters) or 10 gallons of 12.5% Sodium Hypochlorite to the filter to achieve 200ppm total chlorine residual.
- 7. Turn air scour back on.
- 8. Check the total chlorine residual in the filter then let the filter air scour for 30 minutes to disinfect. Record total chlorine residual and start and end times for the disinfection.
- 9. After 30-minute disinfection, wash the filter again until the chlorine residual is back down to normal and collect the bacteriological sample. **Record the chlorine residual before collecting the bacteriological sample.**
- 10. Put the filter into rewash until it seasons and turbidity reaches 0.20NTU. Record the total backwash water used for the entire process. Make note of the filter media depth in comparison to the red indicating tile on the filter bed wall. **Make sure all information is clearly stated on filter disinfection form.**

Acid Washing and Disinfecting Record

| Acid Wash | | | | |
|----------------------|------------|--------------------------|----------|--|
| | 31% Hydrod | hloric Acid | | |
| pH dropped to | | pH prior to disinfection | | |
| Air Scour for 1 hour | | | | |
| Begin Time | AM PM | End Time | AM PM | |

| Disinfection | | | | | |
|---|--|----------|-------------|--|--|
| Slug Chlorination | | | | | |
| Required Chlorin | e Dose | | ppm or mg/L | | |
| Contact Time | | | hours | | |
| Begin Time | AM PM | End Time | AM PM | | |
| | Calculations | | | | |
| Volume = $\frac{(\text{Filter Area, ft}^2)(3.5 \text{ ft})(7.48 \text{gal/ft}^3)}{1,000,000}$ | | | | | |
| 3.5 = Water + Filter Media Depth | | | MG | | |
| HTH, lbs = (mg/L)(MG)(8.34 lbs/gal) | | | /gal) | | |
| ()%Chemical Purity, as decimal | | | | | |
| Bleach gal - | | | | | |
| bleach, gai = | Bleach, gal = (mg/L)(MG) ()%Chemical Purity, as decimal | | | | |

| Lab Results | | | | |
|--|-----------------------------------|-------------------|-----|--|
| Actual chlorine content initial (after chlorine was added) m/l | | | | |
| Chlorine residual | ual prior to pulling Bac'T sample | | m/L | |
| Bac'T sample | | Bac'T Sample | AM | |
| Results | | Date & Time | PM | |
| Total Backwash | | Date & Time put | AM | |
| Water Used | | back into service | PM | |

| Filter Number: | Tester: |
|----------------|---------|
| Date: | Time: |

Bed Expansion Math

1. While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 4 ¼ inches. The average media depth was 30 inches. Calculate the bed expansion in percent.

$$\frac{(4.25)(100)}{30} = 14\%$$

2. While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 6 ½ inches. The average media depth was 31 inches. Calculate the bed expansion in percent.

$$(6.5)(00) = 21\%$$

3. While evaluating a filter, a bed expansion test was performed. During the backwash the filter bed rose 8 inches. The average media depth was 36 inches. Calculate the bed expansion in percent.

$$\frac{(8)(100)}{310} = 22\%$$

4. Filter 5 at a water plant has an average media depth of 29 inches. The bed expanded by 8 inches during backwash. What is the bed expansion in percent?

$$\frac{(8)(100)}{29} = 28\%$$

5. Filter 2 at a water plant has an average media depth of 28 inches. The bed expanded by 4 inches during backwash. What is the bed expansion in percent?

$$\frac{(4)(100)}{28} = 14\%$$

6. Filter 16 at a water plant has an average media depth of 32 inches. The bed expanded by 10 inches during backwash. What is the bed expansion in percent?

$$\frac{(10)(100)}{32} = 31\%$$

7. Calculate the filter bed expansion if the average media depth is 33 inches and the bed expansion is 5.5 inches.

8. Calculate the filter bed expansion if the average media depth is 34 $\frac{1}{2}$ inches and the bed expansion is 7 inches.

$$(7)(00) = 20\%$$

9. Calculate the filter bed expansion if the average media depth is 28 inches and the bed expansion is 9 inches.

10. Calculate the filter bed expansion if the average media depth is 31 inches and the bed expansion is 5 inches.

Backwash Math

1. A filter measures 28 feet by 20 feet. The backwash cycle is started and the water rises 6" in 12, 13, and 13 seconds. What is the backwash rate in gallons per minute per square foot (gpm/ft²)?

2. The Randyville Water Plant treats an average of 5.18 MGD. The water is split equally to each of the 8 filters. Each filter basin measures 12 feet wide by 16 feet long and by 24 feet deep. Each filter bed measures 12 feet by 14 feet by 11 feet deep. Filter 6 is taken offline to backwash. Using a hook gauge and a stopwatch, it is noted that the water level in the filter rises 6 inches in 14, 16, and 15 seconds. What is the backwash rate in gallons per minute per square foot (gpm/ft²) and how many gallons were used if the filter was backwashed for 9 minutes?

vol.= (12 ft)(14 ft)(0,5ft)(7,48) = 628,32gel

unea= $(12ft)(14ft) = 168ft^2$ $gpm/ft^2 = \frac{608.30cal}{(0.25min)(168ft^2)} = \frac{14.96gpm/ft^2}{(0.25min)(168ft^2)} = \frac{14.96gpm/ft^2}{(2.25min)(168ft^2)}$ The Chrisburg Water Plant treats an average to each of 8 filters. Each fill 14 feet do-24 feet deep. Each filter bed measures 12.5 feet by 14 feet by 10 feet deep. Filter 6 is taken offline to backwash. Using a hook gauge and a stopwatch, it is noted that the water level in the filter rises 6 inches in 12 seconds on test 1, 6 inches in 11 seconds on test 2 and 6 inches in 14 seconds on test 3. What is the backwash rate in gallons per minute per square foot (gpm/ft²)?

vol.= (12.5 fr)(14 fr)(0.5 fr)(7.48) = 654.5 gal

$$time = 12s + 11s + 14s = 0.2056 min$$
(3)(60)

4. Determine the backwash rate in gpm/ft² for a filter with a surface of 28 feet by 20 feet. The backwash cycle started and the water rose 6 inches in 15, 16, and 16 seconds.

time =
$$\frac{15s + 16s + 16s}{(3)(60)} = 0.2611 \text{ min}$$

5. Determine the backwash rate in gpm/ft² for a filter bay that is 10 by 14 feet and the filter bed is 10 by 12 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 17, 16, and 16 seconds.

started and the water rose 6 inches in 17, 16, and 16 seconds.
$$vol. = (10 ft)(12 ft)(0.5 ft)(7.48) = 448.8 gal$$

time =
$$\frac{17s + 16s + 16s}{(3\times60)} = 0.2722 \text{ min}$$

6. Determine the backwash rate in gpm/ft² for a filter bay that is 15 by 22 feet and the filter bed is 15 by 20 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 18, 17, and 20 seconds vol = (15 fi)(20 fi)(0.5 fi)(7.48) = 1122

time=
$$\frac{18s+17s+20s}{(3)(6)} = 0.3050$$
 min

7. Determine the backwash rate in gpm/ft² for a filter bay that is 16 by 18 feet and the filter bed is 16 by 16 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 11, 10, and 9 seconds

started and the water rose 6 inches in 11, 10, and 9 seconds
$$vol.=(16f)(10f+)(0.5f+)(7.48)=957.44$$
 gal

time =
$$\frac{11s + 10s + 9s}{(3)(60)} = 0.1667 \text{ min}$$

8. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 12 minutes for a filter bay that is 14 by 18 feet and the filter bed is 14 by 16 feet. The test was run three times. The backwash cycle started and the water rose 6 inches in 18, 17, and 20 seconds

water rose 6 inches in 18, 17, and 20 seconds

$$Vol. = (14 ft \times 106 ft \times 0.5 ft)(7.48) = 837.7 logal$$

$$time = 18s + 17s + 20s = 0.305 lo min$$

$$(3 \times 100)$$

$$gpm | ft^2 ft^2 min$$

area= (14ft X16ft)= 204 ft2

9. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 14 minutes for a filter bay that is 20 by 32 feet and the filter bed is 20 by 30 feet. The test was run three times. The times required for the water to rose 6 inches were 13, 12 and 15 seconds.

$$vol. = (20 \text{ ft})(30 \text{ ft})(0.5 \text{ ft})(7.48 \text{ gal}) = 2244 \text{ gal}$$

 $time = \frac{13s + 12s + 15s}{(3)(60)} = 0.2222 \text{ min}$
 $area = (20 \text{ ft})(30 \text{ ft}) = 1000 \text{ ft}^2$

)
$$gpm|A^{2} A^{2} min$$

) = [141,372 gal]

10. Determine the backwash rate in gpm/ft² and the amount of water used if they backwashed for 9 minutes for a filter bay that is 24 by 36 feet and the filter bed is 24 by 34 feet. The test was run three times. The times required for the water to rose 6 inches were 14, 15 and 16 seconds.

$$Vol. = (24f)(34f)(34f)(7.48) = 3051.84 gal)$$

 $time = \frac{14s + 15s + 16s}{(3)(60)} = 0.25 min$
 $area = (24f)(34f) = 816ft^2$
 $apm | ft^2 = 3051.84 gal = 14.96 gpm | ft^2|$

Filtration Math

 A filter measures 28 feet by 20 feet. The influent is closed and the effluent is opened and the water drains down 6" in 120, 125, and 113 seconds. What is the filter-loading rate in gallons per minute per square foot (gpm/ft²)?

vol.=
$$(284)(204)(0.54)(7.48) = 2094.4 gol$$

time= $120s+125s+113s = 1.9889 min$
 $(3)(60)$
area= $(284)(204) = 5604^2$

2. The Randyville Water Plant treats an average of 5.18 MGD. The water is split equally to each of the 8 filters. Each filter basin measures 12 feet wide by 16 feet long and by 24 feet deep. Each filter bed measures 12 feet by 14 feet by 11 feet deep. The influent line to Filter 6 is closed while the effluent remains open. Using a hook gauge and a stopwatch, it is noted that the water level in the filter drops 6 inches in 80, 86, and 89 seconds. What is the filtration rate in gallons per minute per square foot (qpm/ft²)?

the filtration rate in gallons per minute per square foot
$$(gpm/ft^2)$$
?
 $vol. = (12ft)(16ft)(0.5ft)(7.48) = 718.08 gol$
 $time = (80s+86s+89s) = 1.4167 min$

3. The Chrisburg Water Plant treats an average of 7.2 MGD. The water is split equally to each of 8 filters. Each filter basin measures 12.5 feet wide by 16.5 feet long by 24 feet deep. Each filter bed measures 12.5 feet by 14 feet by 10 feet deep. The influent line to Filter 6 is closed while the effluent remains open. Using a hook gauge and a stopwatch, it is noted that the water level in the filter drops 6 inches in 69 seconds on test 1, 6 inches in 67 seconds on test 2 and 6 inches in 70 seconds on test 3. What is the filtration rate in gallons per minute per square foot (gpm/ft²)?

time =
$$\frac{695 + 1675 + 705}{(3)(60)}$$
 area = $\frac{(12.54)(144)}{(12.54)(144)} = \frac{175}{4^2}$ gpm/ftz = $\frac{771.315gel}{(1444min)(175ft^2)} = \frac{3.85}{3.85}$ gpm/ftz

4. Determine the filtration rate in gpm/ft² for a filter with a surface of 28 feet by 20 feet. With the influent valve closed, the water above the filter dropped 6 inches in 57, 56, and 60 seconds.

$$Vol = (20f4)(28f4)(0.5f4)(7.48) = 2094.4 gal$$

 $time = \frac{57s + 56s + 60s}{(3)(60)} = 0.9611 min$
 $area = (20f4)(28f4) = 560 ft^2$

5. Determine the filtration rate in gpm/ft² for a filter bay that is 10 by 14 feet and the filter bed is 10 by 12 feet. The test was run three times. The times required for the water to drop 6 inches were 135, 132 and 129 seconds.

$$vol = (10A)(14f+)(0.5f+)(7.48) = 523.10 gal$$

time = $135s+139s+199s = 0.2 min$
 $(3)(60)$
area = $(10f+)(12f+) = 120f+2$

6. Determine the filtration rate in gpm/ft² for a filter bay that is 15 by 22 feet and the filter bed is 15 by 20 feet. The test was run three times. The times required for the water to drop 6 inches were 79, 85 and 80 seconds.

$$vol. = (15ft)(22ft)(0.5ft)(7.48) = 1234.2 gal$$

 $time = \frac{79s + 85s + 80s}{(3)(60)} = 1.3556 min$
 $area = (15ft)(20ft) = 300ft^2$

7. Determine the filtration rate in gpm/ft² for a filter bay that is 16 by 18 feet and the filter bed is 16 by 16 feet. The test was run three times. The times required for the water to drop 6 inches were 65, 62 and 64 seconds.

Vol. = (10 ft)(18 ft)(0.5 ft)(7.48) = 1077.19 gal

8. Determine the filtration rate in gpm/ft² for a filter bay that is 14 by 18 feet and the filter bed is 14 by 16 feet. The test was run three times. The times

required for the water to drop 6 inches were 72, 75 and 76 seconds. gal=
$$(14 ft)(18 ft)(0.5 ft)(7.48) = 940.48 gal$$

9. Determine the filtration rate in gpm/ft² for a filter bay that is 20 by 32 feet and the filter bed is 20 by 30 feet. The test was run three times. The times required for the water to drop 6 inches were 61, 59 and 58 seconds.

gal =
$$(30 \text{ ft})(324)(0.5 \text{ ft})(7.48) = 2393.6 \text{ gal}$$

time = $(15+59s+58s) = 0.9889 \text{ min}$

10. Determine the filtration rate in gpm/ft² for a filter bay that is 24 by 36 feet and the filter bed is 24 by 34 feet. The test was run three times. The times required for the water to drop 6 inches were 62, 60 and 59 seconds.

Mudball Math

1. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 250-mL graduated cylinder was filled up to the 200-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 235 mL mark. What is the percent of mudballs?

 $\frac{\text{Sampler}}{\text{Vol}} = \frac{(0.785)(3 \text{ in})^2(\text{lo in})(5)(3785)}{231} = 3472.86 \text{ mL}$

235 (35mL)(100) 1.0% fairly bad
3472.8lmL [1.0%]

2. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 500-mL graduated cylinder was filled up to the 300-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 425 mL mark. What is the percent of mudballs?

425 -300 125ml (125ml)(100) = [3.6%) bad

3. Mudball samples were taken with a sampler that has a 3 in diameter and is 6 inches deep. The 250-mL graduated cylinder was filled up to the 200-mL mark with water. The mudballs were placed in the graduated cylinder and the water rose to the 247 mL mark. What is the percent of mudballs?

-247 -206 47ml) (100) = [1.47] fairly bad 3472.86ml

Answers:

1. 1.0%

2. 3.6%

3. 1.4%

Filter Math

Filter Dimensions:

Bay Length = 30 ft

Bed Length = 28 ft.

Bay Width = 24 ft

Bed Width = 24 ft

Media Depth Measurements:

| | 28" | 29" | 28" | |
|--|-----|-----|-----|--------------------|
| | 28" | 30" | 29" | } avq. media depth |
| | 31" | 29" | 29" | (- 28.83 in |
| | 30" | 28" | 27" | |
| The state of the s | * | | | |

Bed Expansion: 4 inches

Drop Test Times = 72 sec, 70 sec, 73 sec avg.time = 1.1944 min

Rise Test Times = 18 sec, 20 sec, 21 sec avg.time = 0.3278 min

What is the percent bed expansion; filtration rate in gpm and gpm/ft²; the backwash rate in gpm and gpm/ft² and the amount of water if backwashed for 12 minutes?

% bed expansion =
$$\frac{(4)(100)}{28.83} = 13.87\%$$

Section 3

Membrane Filtration
Science and Theory
Operations
Pilot Studies Regulations

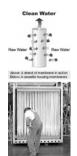
Membrane Technology CROSS SECTION CONTAMINANT PUMINID MATER MEMBRANE

History

- Mid-late 1980's- membrane filtration used primarily for industrial applications such as the wine and juice industries.
- Companies such as Aquasource and Memcor began to market membrane technology for treatment of drinking water in the early 1990's.
- Small scale pilot studies at drinking water facilities showed membranes improved filtrate quality and reduced DBP's.
- First full scale microfiltration membrane facility, the Saratoga WTP in California, went online in 1993.
- In 1994 a Rice University study showed that low pressure membrane filtration would be cost-effective at capacities of 5 MGD

2

History



- In 1997 a study showed that if membranes were installed downstream of conventional coagulation, flocculation and sedimentation that the membrane could be operated at a higher rate, making it cost effective for even 50 MGD capacity.
- The potential for large scale membrane facilities resulted in the formation of additional membrane manufacturers and improvements in membrane technology.
- Companies such as Pall, Zenon, and Koch began to develop new membrane technology
- The largest low pressure membrane filtration plant to date is in Singapore. It utilizes membrane technology developed by Zenon and treats 72 MGD.

Why Membrane Technology?

- Regulatory- the SWTR requires a higher level of turbidity and particulate removal. Membranes can consistently obtain that level of turbidity removal.
- Cost- since the early 1990's the capital cost of membrane treatment has decreased. In addition, the implementation of innovative backwash and cleaning strategies had reduced the operational costs.
- Operational flexibility- low pressure membrane filtration processes are highly flexible and can be used in conjunction with other processes to achieve specific treatment objectives. In addition, membrane facilities can be easy to operate because the process is not dependent on water chemistry or flow.

Pressure forces the water through the pores in the membrane.

Raw water is passed through a membrane poremeate pores in the membrane.

The particles that are too large to pass through are collected, and wasted.

The pure water, or permeate, is collected on the other side of the membrane.

Membranes: Science and Theory

- Pure water transport across a clean porous membrane is affected most by the trans-membrane pressure and the viscosity of the water
- Trans-membrane pressure: The force which drives liquid flow through a cross flow membrane. During filtration, the feed side of the membrane is under higher pressure than the permeate side. The pressure difference forces liquid through the membrane.

Flux

- The word flux comes from Latin: fluxus which means "flow".
- Volumetric flux describes the volume of flow across a unit of area.
- Typical units for membrane volumetric flux are gallons per square foot of membrane per day or liters per square meter of membrane per hour.

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Temperature Effects



- Think about maple syrup, when maple syrup is cold it is very thick and viscous.
- If you put it in the microwave and warm it up it pours much more easily.



Temperature Effects

- Water behaves much like maple syrup.
- The viscosity or resistance to flow of water is dependent of temperature.
- The colder the water, the higher the viscosity.
- Viscosity will affect membrane performance by either reducing the flux or by requiring an increase in trans-membrane pressure to keep the flux constant.

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Seasonal Effects



- Higher trans-membrane pressures may be required in the winter to offset the effect of temperature on the viscosity of the water.
- Membrane fouling may also change with season and temperature.
- Source water is variable, there is seasonal variation in the amounts of organics, metals, nitrates, etc.

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Reductions in Membrane Productivity

Reductions in membrane productivity can result for a number of reasons including:

- Membrane Compaction
- Membrane Fouling
 - ➤ Inorganic fouling
 - ➤ Organic fouling
 - ➤ Biofouling

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Membrane Compaction

- Membrane compaction is a physical compression of the membrane. This compression results in a decrease in flux. The rate of compaction is directly proportional to an increase in temperature and pressure.
- Compaction occurs naturally over time requiring a greater feed pressure.
- Compaction is permanent and can occur quickly in membranes if operated at higher pressures for any extended period of time.
- Usually membrane compaction results in a few percent flux decline, and has strongest effect during the initial operating period.

Fouling

 Fouling is defined as the reduction in flux at constant pressure resulting from the adsorption or deposition of suspended matter in the membrane pores or on the membrane surface.

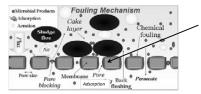
The three fouling mechanisms are:

- · Pore adsorption
- · Pore blocking
- Cake formation

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Fouling

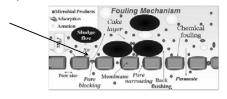
• **Pore adsorption:** occurs when particles smaller than the pore deposit themselves on the pore walls which reduces the effective size of the pores.



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Fouling

 Pore blocking: occurs when particles as large as the pore become lodged in the pore and block the passage. The effective number of pores is reduced.



Fouling

• Cake formation: this occurs when particles to large to enter the pores become deposited on the surface of the membrane. Cake formation results in a reduced flux across the membrane.



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Inorganic Fouling

 Inorganic fouling can occur when inorganic particles such as silt, clay, iron, manganese, nitrates, etc are deposited on the surface of the membrane.



Organic Fouling

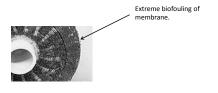
 Organic fouling occurs when natural organic matter (NOM) in source water prevent flux across the membrane by plugging pores in the membrane.



A membrane severely fouled by organics

Biofouling

 Biofouling occurs when microorganisms adhere to the membrane surface and begin to grow colonies on or in the membrane. The microbes will eventually obstruct the flow through the membrane



Membrane Materials

- The most common membrane materials are either organic polymers or ceramic materials.
- The polymer membrane materials vary with resistance to fouling, operating temperature and pH ranges and resistance to oxidants.



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Polymer Materials

| Membrane material | Туре | Oxidant tolerance | pH range | Resistance to fouling |
|------------------------|-------|----------------------|----------|-----------------------|
| PVDF | MF/UF | Very high | 2-11 | Excellent |
| Polypropylene(PP) | MF | Low | 2-13 | Acceptable |
| Polyethersulfone (PES) | UF | High | 2-13 | Very Good |
| Polysulfone (PS) | UF | Moderate | 2-13 | Good |
| Cellulose Acetate (CA) | UF | Moderate | 5-8 | Good |

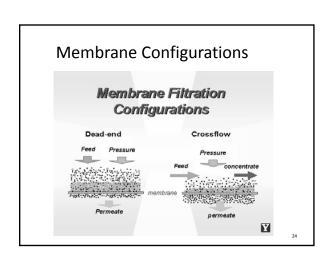
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Ceramic Membranes

- Ceramic membranes are made by heating materials like aluminum oxide, titanium dioxide or carbon composites into a brittle clay like ceramic form.
- The ceramic membranes are thicker and have a greater resistance to water transport, so the trans-membrane pressures may need to be increased.
- The benefits of ceramic membranes include: that they are easier to clean and maintain than polymer membranes, and that they are able to with stand higher temperatures and pressures and can operate at a pH of 0-14.

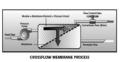
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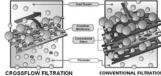
Ceramic Membranes **Ceramic Membrane Elements and Housings**



Crossflow Filtration

- In some cases crossflow filtration is used.
- The direction of the flow can help to prevent the deposition of materials on the membrane surface thereby reducing fouling.





Membrane Module Types

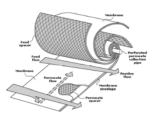
There are several commercially available membrane technologies including:

- · Spiral wound
- Tubular
- Hollow fiber
- Plate and Frame
- Cassette

6

Spiral Wound Membrane

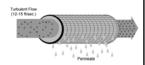
- Not commonly used for microfiltration or ultrafiltration.
- The flat sheet nature makes it difficult to keep clean.



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Tubular Membrane Module

- Rather than a sheet of microfiltration membrane, the membrane is made in a tube fit into a module.
- The membrane is on the inside of the tube with a HDPE support tube.
- This arrangement allows the membrane to be backwashed which controls fouling.





Tubular Membrane Module

- The membranes which are composed of polymer or ceramic are placed inside plastic or stainless steel modules and sealed by a gasket or ring clamp.
- The tubular membranes have relatively large inner diameters (1-2.5 cm).
- The feed water which is under pressure flows through the inner lumen of the tube. The permeate is collected in the outer shell of the module

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Tubular Membrane Module

Advantages

- Large diameter of channels allows for treatment of water with large particles or high solids.
- High cross flow velocities (up to 5 m per second) can be used to control fouling
- Easy to clean because of large diameter channels

Disadvantages

 Low surface area to volume ratio or "packing density" of membrane

Hollow Capillary Fiber Membrane

- Can be arranged in a tubular housing or as a cassette type module.
- Can be backwashed to prevent fouling.









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Hollow Fiber Membrane

- Consists of several hundred to several thousand fibers encased in a module.
- The fibers are bonded at each end with an epoxy or urethane resin.
- The inner lumens or internal fiber diameters are very small (0.4 to 1.5 mm).
- There are two different regimes in hollow fiber filtration: inside out, and outside in.

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Inside- Out Filtration



- A high cross-flow velocity over the membrane surface prevents membrane fouling.
- Easier to backwash
- This makes inside-out filtration suitable for concentration and purification of highly concentrated solutions.

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Outside -In Filtration



- Utilizing the lager area of the outer surface of the membrane fiber, the filtration load per unit area may be reduced.
- Lower head loss through the module.
- These features make this mode of operation well suited for high volume water clarification.
- It is more difficult to backwash and control flow to the membrane.
- Cleaning technique such as 'airscrubbing' may be utilized.

2

Hollow Fiber Membrane

Advantages

- Low pressure drop across the module
- High surface to volume ratio or "packing density".
- Low trans -membrane pressures 3-15 psi.
- Fibers can be backwashed.

Disadvantages

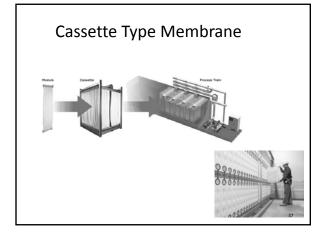
- Small tube diameter are susceptible to plugging
- The large number of fibers may cause difficulty in detecting the loss of membrane integrity.

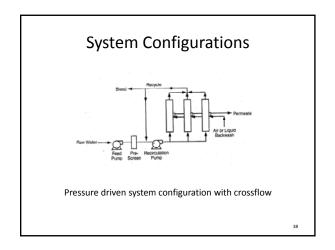
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Plate and Frame Type

- Membrane filter plates: a flexible membrane is fixed to the support body.
- Materials for the membranes include Polypropylene, synthetic rubber (for example NBR, EPDM) or thermoplastic elastomer (TPE).
- The membrane is impermeable and serves to compress the cake within the chamber after the filtration process is complete.
- Most often used in industrial applications, or wastewater, not used in water treatment.



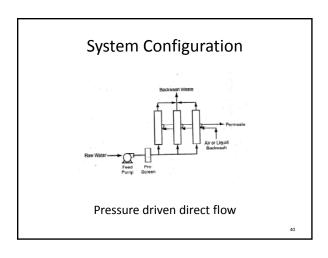




Crossflow

- Feed water is pumped with a crossflow tangential to the membrane.
- The water that does not pass through the membrane is recirculated as concentrate and blended with the feed water.
- Pressure on the concentrate side is conserved and deducted from the total head requirement.
- A bleed stream can be used to control the concentration of solids in the recirculation loop.
- Concentrate can be wasted at any time from the recirculation loop.

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Direct Flow

- Also called dead-end or deposition mode.
- Water is applied directly to the membrane.
- All feed water passes through the membrane between backwashings.
- There is 100% recovery of this water, however, some must be used for backwashing.
- Considerable energy savings because recirculation is not required.

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System Configuration Food Water Performance Based Direct flow submersible

Submersible

- Fibers are submerged in the feed water.
- A vacuum is applied to the inner lumen of the fibers to create a pressure differential necessary for filtration to occur.
- The outside of the fibers are scoured by air periodically or continuously.
- Backwashing with the permeate is conducted at regular intervals.

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System Operations

The two primary operational concepts are:

- To operate at a constant pressure
 - To operate at a constant flux

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Constant Pressure

Advantages:

- Feed pumps can be sized to maintain the constant pressure with simple on/off controls.
- Energy requirements are constant.

Disadvantages:

- Permeate flow will decrease over time due to membrane plugging prior to backwash.
- Output of plant is reduced.

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Constant Flux

Advantages:

- No over-sizing of the system is needed.
- Out-put remains the same
- Most often used by full scale membrane plants Disadvantages:
- Feed pressure must increase to maintain constant flux between backwashes
- Energy efficiency decreases with increased transmembrane pressure.

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Pump Requirements

- Variable speed centrifugal: used to deliver raw water to membranes at the required flow and pressure. (usually 20 -30 psi)
- Permeate vacuum pump: used for systems that operate under a vacuum, one dedicated to each membrane bank, sized to produce the permeate flow of each membrane bank.
- Recirculation pump: used for inside-out crossflow configurations, one dedicated for each membrane
- Backwash pump: used for backwashing, may use liquid or gas medium.

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Membrane Backwashing

- For most systems it is performed automatically.
- Can be set for a run time, usually every 30-120 minutes.
- Can also be set to backwash when a certain transmembrane pressure is reached or when a certain amount of permeate has been produced.
- The duration of backwash lasts from 1 -5 minutes.

Backwashing

- The permeate collected in a reservoir is employed to backwash the membrane.
- A liquid stream under pressure from a backwash pump dislodges solids from the surface of the membrane
- For submerged systems, backwashing occurs for 30 seconds every 15 minutes to several hours.
- The backpulsing dislodges any deposition that has accumulated.

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Pretreatment

- Prefiltration: may be required to remove large particles that could plug the inlet to the fibers.
- **pH adjustment:** may be required to keep feed water in the optimum range for the membrane polymer type.
- Adsorption and Coagulation: coagulants and PAC can be used to prevent fouling of the membrane.
- Pre-oxidation: used to oxidize metals such as iron and manganese so that they do not form in the membrane or the permeate.

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Post Treatment

• Disinfection: required by State and Federal Regulations.

Optional:

- Fluoridation
- Corrosion Control

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Cleaning

- When fouling materials can no longer be removed by backwashing, chemical cleaning is required.
- Considerations include the cleaning and rinse volumes, temperature of cleaning water, reuse and disposal of chemicals.
- Many different chemicals can be used including detergents, acids, bases, oxidizing agents and enzymes.
- Chlorine is often used on PVDF membranes in concentrations from 2- 2000 mg/L.
- Heating the cleaning solution to 35-40 C can enhance cleaning effectiveness.

Membrane Integrity Testing

- One of the most critical aspects of employing membrane technology is integrity testing.
- Integrity testing ensures that the membranes are an effective barrier between the feed water and the permeate being produced.

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Integrity Testing

There are several methods that can be used to monitor membrane integrity including:

- · Turbidity monitoring
- Particle counting
- · Particle monitoring
- Biological monitoring
- Air pressure decay testing
- Diffusive air flow testing
 Water displacement testing
 - Bubble testing
 - Sonic wave sensing
 - · Visual inspection

Turbidity Monitoring



- Most commonly used method of measuring the performance of filtration systems.
- Most membrane systems can provide permeate with turbidities less than 0.1 NTII
- Use of turbidity as the sole method for determining membrane integrity does not provide adequate sensitivity to detection of small pinholes in membrane fibers

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Particle Counting and Monitoring

- Multichannel particle counting is a standard particle counting method used in many water treatment plants.
- The advantage is that it is a continuous online measurement, however, several sensors are required to establish the sensitivity needed to detect loss of membrane integrity.
- Another method of measuring particles is particle monitoring which is based on dynamic light obscuration.
- Particle monitors are usually cheaper and easier to operate than particle counters, however, they also require multiple sensors for the sensitivity level of membranes.

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Biological Monitoring



- One of the most sensitive methods for evaluating membrane integrity is viral seeding.
- Viruses at densities in the range of 106-107 PFU/mL are introduced into the effluent.
 - Plaque: an area of cells in a layer which display a cytonathic effect
 - Plaque-forming unit (PFU): a virus or group of viruses which cause a plaque.
 - At various times, samples are collected from the permeate to determine if those viruses have passed through the membrane.
 - Often used for pilot- or bench scale studies, because you don't want to introduce viruses into water that is being consumed.

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Air Pressure Decay Testing

- The membrane module is pressurized to approximately 15 psi from the feed side.
- Minimal loss of held pressure (usually less than 1 psi every 5 minutes) at the filtrate side indicates a passed test.
- A significant decrease of the held pressure indicates a failed test.

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Diffusive Air Flow Testing

- The diffusive air flow test uses the same concept as the air pressure decay test but it is performed by monitoring the displaced liquid volume caused by leaking air from the compressed membrane fibers.
- This test is more sensitive than air pressure decay because it is easier to measure small changes in liquid volume than small changes in air pressure.

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Bubble Testing



- Bubble testing can identify a fiber or seal location that is leaking in a membrane module.
- This test is usually run after the compromised module is identified by another monitoring method such as air pressure decay or a sonic sensor.
- Basically the module is submerged while air is passed through it, bubbles formed by escaping air identify the location of the leaking fiber.
- The leaking fiber is either sealed using epoxy glue or by inserting a pin of the same diameter into the inlet.

Sonic Wave Sensing

- Sonic sensor equipment consists of a sound wave sensor attached to a headphone.
- The headphones are manually placed at the top, middle, and bottom of the membrane module during the air pressure decay test.
- The headphones can detect sound waves produced by air escaping from a compromised membrane.
- This test has to be followed by the bubble test and visual inspection.

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Visual Inspection

- If a pressure based integrity test is used, visual inspection can be conducted simultaneously by watching the fibers for bubbles escaping.
- Often the module may have to be removed from the housing so that visual inspection can be performed.

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Membrane Manufacturers: Pall Coagulant Addition Static or Inline Mising Clarifier Clarifier Distribution Distribution Distribution Addition

Pall

- Pall membrane systems may be stand alone or in combination with pretreatment processes.
- The Microza PVDF membranes work well with the addition of coagulant or PAC.
- Large MF or UF systems consist of module racks supporting up to 100 Microza modules.
- The Microza systems operate in an outside-in mode.
- Feed water flows under pressure through the large openings at the bottom of the module to the outside of the fibers
- Water permeates through the pores in the membrane and flows along the lumen to the discharge side of the module.

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Pall

- Once every 15 to 30 min the MF systems are air scrubbed and backwashed to remove particles from the surface of the membrane.
- Clean in place (CIP) required when transmembrane pressure(TMP) reaches 30-35 psi or every 3 to 6 weeks.
- The system is designed to recover CIP solution to minimize chemical use.
- System integrity is monitored by a pressure decay test, if failed a visual inspection, bubble test is used to isolate the affected fiber.

Pall

| Characteristic | |
|----------------------------|--------------------|
| Operating TMP | 4-35 psi |
| Pore size | 0.1 um |
| Ph tolerance | 1-10 |
| Coagulant tolerance | 60 mg/L |
| Typical flux rate | 55 gallons/ft2/day |
| Bacterial removal | 7 log |
| Giardia and crypto removal | 6 log |

US Filter-Memcor

US Filter-Memcor

- The simple modular membrane system is available in two product lines;
- Continuous Microfiltration(CMF)
- Continuous Microfiltration Submerged (CFMS)
- CMF systems has modules housed in pressure vessels connected to manifold assemblies that fit together in a grid.
- CFMS eliminates the module housing, the filters are submerged directly in the feed tank.

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US Filter-Memcor

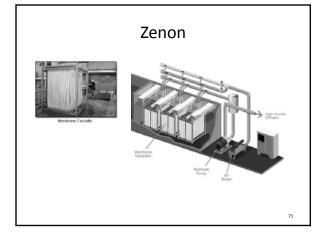
- Can be either polypropylene or PVDF
- Direct feed systems, crossflow is used only during back wash.
- 100% recovery of filtrate during the filtration cycle.
- Backwash and filtration cycle is automatically controlled.
- Integrity testing is in place pressure decay test and correlates with microbial removal.

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US Filter-Memcor

| Characteristic | |
|----------------|---------------|
| Operating TMP | 3-29 psi |
| Pore size | 0.1 to 0.2 um |
| Ph tolerance | 1.5 to 9.5 |

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Zenon

- Zenon's immersed membrane called ZeeWeed is a hollow fiber with filtration from the outside –in.
- The module is shell-less and is immersed directly in the feed water.
- The fibers are made of chlorine tolerant PVDF.
- UF membranes reject all suspended and colloidal solids including viruses.

Zenon

- Backwashing is by back pulsing with permeate.
- Air scour also aids in the prevention of membrane fouling.
- Integrity testing includes turbidity measurement, and air pressure decay testing.

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Zenon

| Characteristic | | |
|--------------------|---------------------|--|
| Operating TMP | Vacuum -3 to -7 psi | |
| Pore size | 0.1 um | |
| Ph tolerance | 5-9.5 | |
| Coagulant tolerant | yes | |
| permeability | 15 gfd/psi | |

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Plant Comparisons

| Category | Pall | USF Memcor | Zenon |
|------------------|--------------------------------------|---------------------------------|------------------------------------|
| Plant name | Abilene, TX | Bendigo, Australia | Collingwood, ONTARIO |
| Year operational | 2003 | 2002 | 2001 |
| Capacity MGD | 3 | 10.5 | 1.2 |
| Туре | MF | MF | UF |
| Filtration area | 538 ft2 | 6 cells | 400 ft2 |
| Feed water | High TOC level | Less than 10 NTU | NTU from 2 to 50 |
| Pre-treatment | Coagulation and flocculation | Coagulation and screen | Prechlorination |
| Backwash | Every 15 to 30 min for 1-5 min | Every 30 -60 min for 1-5 min | Every 30 -60 minutes for 60 sec |
| CIP | Every 30 days | Clean with citric acid. | 1-2/year |

Pilot Testing of Membrane Systems



- Pilot testing is a valuable tool in determining the appropriate design criteria of membrane systems prior to large scale installation.
- Pilot testing establishes the basis for evaluating operational parameters such as pathogen removal, efficiency, maintenance, and cost of operation.

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Pilot Testing

Prior to the start of pilot testing, specific goals should be established including the following;

- To verify or establish the design criteria so that plant capacity requirements are met.
- To demonstrate critical system procedures, backwashing and integrity testing
- To verify that the finished water meets expected standards
- To produce a feed water profile with special attention to parameters that affect membrane performance (TOC, algae, ph, temperature)
- To provide hand on training for the plant operators on membrane processes

Pilot Testing

- Funds for conducting pilot investigations are often limited so it is important to research the different types of products available prior to pilot testing.
- Membrane system suppliers should have satisfactory experience and a good history of providing customer service for there products.

Pilot Testing



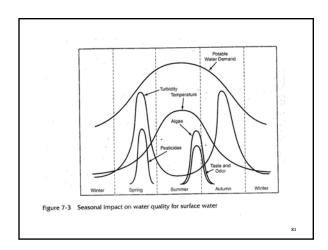
- Process integration
- Depending on the membrane selected, a high level of pretreatment may be required to reduce membrane fouling.
- It is critical that pilot tests take into account any pretreatment that may have to be used in large scale production.

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Pilot Testing

- Seasonal impact on water quality
- The initial pilot test period should take into account anticipated seasonal fluctuations in temperature, turbidity, total organic carbon, pesticides and taste and odors.
- Some state agencies require at least 12 months of membrane pilot testing.

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Pilot Testing

• Typical infrastucture requirements:

| Category | |
|-------------------|--|
| Feed water | 25 gpm |
| Footprint | 40-300 ft2 |
| Power | 480 volt, 20 to 60 amp |
| Residual disposal | For backwash and CIP waste, access to sanitary sewer or other means of treatment |

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Pilot Testing

- Water quality of the feed water and permeate should be monitored regularly.
- Ph, temperature, TOC, DOC, alkalinity, algae, turbidity, odor, TDS, hardness, and microbial counts should be monitored.
- Parameters such as the ph, TOC, DOC, and turbidity of the waste or (concentrate) should be monitored on a monthly basis.

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Results of Pilot Studies

 The results should include a summary of hydraulic and water quality data collected through out the pilot study.

Results of Pilot Testing

| Basis for design | Membrane A | Membrane B |
|--------------------------------|------------------|------------------|
| Flux at 20 °C (gal/ft2/day) | 3.58 gal/ft2/day | 3.29 gal/ft2/day |
| Module surface area | 15 ft2 | 55 ft2 |
| Production per module | 6.9 gpm | 21.5 gpm |
| Downtime for backwash | 2.5 min | 1.5 min |
| Backwash frequency | 30 min | 20 min |
| CIP frequency | 23 days | 7 days |
| Total downtime percent | 8.4 % | 8.1 % |

System Design

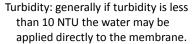
Considerations:

- <u>Site specific issues:</u> capacity and demand of the facility, raw water quality, finished water quality goals, space available for equipment (footprint).
- Membrane specific issues: factors unique to the membrane supplier including flux, backwash approach, cleaning and residual disposal.

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System Design

Raw Water quality parameters that may affect membrane system design.



If turbidity is greater than 10 NTU it may be more economical to install pretreatment processes





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System Design

- Membrane flux: should be measured from the feed side of the membrane.
- Varies with membrane material, pore size, the direction of flow (whether inside out or outside in) and the percentage of active membrane that is porous.
- The useful life of a UF or MF membrane is a function of the membrane material as well as the backwash and cleaning techniques employed.
- It may last from 5 to 20 years.

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System Design

The major reason hollow fibers are used for most UF and MF processes is because:

- Hollow fibers have bi-directional strength and can be backwashed.
- Hollow fibers have higher membrane area per volume.

System Design

- Backwashing occurs more frequently in membranes than in conventional filters.
- Backwashing usually lasts for 1-3 minutes.
- Total water lost from backwashing is usually low from 5 to 10%.
- Ideally the backwash will restore TMP pressure to the same value after each backwash, if not, cleaning may be required.

System Design

- The use of softened or de-mineralized water is highly desirable in some locations to get effective cleaning.
- Cleaning solution should be heated to 40 C or 105 F to enhance cleaning and reduce cleaning time.





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Cleaning Chemicals

- Acids-citric acid is most commonly used, it works well on inorganic contaminants such as iron.
 Other acids such as hydrochloric or sulfuric may be used
- Bases- caustic soda is the most commonly used, also good on inorganics
- Oxidants- free chlorine is very effective at removing organic contaminants.
- Surfactants- release contaminants instead of dissolving them. Works well on PAC or if the membrane has a limited ph range.

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Process Residuals

- Waste characteristics depend on the source water being treated.
- Waste usually contains inorganic and organic colloids, pathogens, and turbidity.
- If coagulants, PAC or other pretreatment chemicals are used the residual is similar to that produced by conventional treatment plants.
- Chemical cleaning waste has a different composition and usually a small volume compared with the concentrate and backwash residuals.

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Process Residuals

Methods of disposal include:

- Surface Water Discharge
- Sewer Discharge
- Land Application
- Recycling

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Process Residuals

Surface Water Discharge-

- Surface water discharge must meet the requirements of a site specific NPDES permit.
- May require treatment prior to surface water discharge.
- For most installations, a settling basin or lagoon will suffice.



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Process Residuals

Sewer discharge-

- Most commonly used method of backwash waste disposal.
- Sewer disposal of backwash wastes is controlled by the receiving wastewater treatment plant's NPDES permit and available sewer capacity.
- May not be feasible at all locations.





Process Residuals

Land application-

- Includes percolation ponds or lagoons, spray irrigation and leach fields.
- May require chemical neutralization.
- Periodic removal of accumulated solids from lagoons may be required.





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Process Residuals

Recycling-

 At large installations recycling is accompanied by some type of settling process to concentrate solids.



- Backwash water and cleaning water are sent to a clarifier or settling hasin.
- The supernatant is collected off the surface of the settling basin and mixed with feed water.

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Operations

Membrane Filtration

- Treatment is independent of pre-treatment conditions and raw water turbidity.
- Pore size in membranes forms an effective barrier to cyst sized particles.
- No need for a filter to waste step at the beginning of a filtration run.

Conventional Filtration

- Requires optimized chemical pretreatment (coagulation, flocculation, sedimentation).
- Operators must adjust treatment for changing water conditions.
- Giardia and Cryptosporidium may pass through filter.
- Must filter to waste prior to returning to the filtration cycle after backwashing.

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Operations

Membrane Filtration

- Increased turbidity may have no effect on performance or it may cause a decline in flux or a decrease in time interval between backwashing and cleaning.
- Goal is to maintain finished water productivity, quality of the filtrate remains the same.

Conventional Filtration

- Increased turbidity will require additional coagulant to be added, or increased flocculation/settling, shorter filter runs, increased backwashing or may result in reduced finished water quality.
- Goal is to maintain finished water quality.

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Operations

Modes of Operation

- Filtration
- Backwash
- Air scrub
- · Chemically enhanced backwash (some systems)
- · Chemical clean in place (CIP)
- · Membrane Integrity Testing

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Operations

Generally filtration, backwash and air scrubbing are automatically controlled by the system based on operator selected points such as:

- Trans-membrane pressure (TMP)
- Flux rate or volume filtered
- Filter run time

Clean in place is usually selected manually.

Integrity testing is conducted automatically or at operator selected intervals.

Operations

Data Collection- careful data collection and good recordkeeping are important to the successful long-term performance of membrane systems.

Data should be collected as soon as the unit begins service and should include:

- Flow of reed water, filtrate, and retentate
- Temperature
- Turbidity of feed and filtrate
- Results of integrity testing
- TMF

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Operations



- Most data is collected automatically using a SCADA system
- It is important to collect both pre and post cleaning data.

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Troubleshooting

| Condition | Ideas to consider |
|-----------------------|---|
| Failed Integrity Test | Verify readings |
| | Determine if membranes are fully wetted or have become hydroscopic |
| | Locate and isolate modules with flaws or leaking seals or O rings |
| | Conduct new integrity test with problem modules removed to make sure all the problems have been found |
| | Determine the nature of the failure |
| | Repair flawed module and return to service |
| | Conduct new integrity test to make sure the problem is resolved |

Troubleshooting

| Condition | Ideas to Consider |
|----------------------------|---|
| High turbidity in filtrate | Conduct integrity test |
| | If integrity test indicates no broken fibers or leaks, verify turbidity reading |
| | Measure turbidity in a grab sample |
| | Clean and calibrate turbidimeter, look from problems (air bubbles) |

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Troubleshooting

| Condition | Ideas to consider |
|--------------------------------|---|
| High rate of fiber breakage | Check pressures and water hammer potential being applied during operating cycles. Inaccurate pressure can result in damage during a backwash or integrity test. |
| | Check for exposure to highly concentrated chemicals, evaluate quality of CIP and CEB chemicals |
| | Check for exposure to extreme temperatures |
| | Consider the age of the membranes |
| | Have the integrity and strength of membranes evaluated by the manufacturer (membrane autopsy) |
| | If fibers are not old, consider a warranty claim |
| | Old or improperly operated membranes may become brittle, they need to be operated wet. |

Troubleshooting

| Condition | Ideas to Consider |
|---|---|
| Interval between cleanings is too short | Verify that the data are normalized for temperature, flux may be too high for the application |
| | Raw water quality may have changed |
| | Evaluate pretreatment processes, mishandled polymer can result in significant irreversible flux loss. |
| | Evaluate backwash and chemically enhanced backwash (CEB) procedures, and the chemicals used. |
| | Consider the effects of pH, may cause aluminum scale on membrane if alum is used in pretreatment |
| | Evaluate CIP procedures with manufacturer and engineers, compare with other utilities |
| | Chemically enhanced backwash if not already in use may increase the interval between CIPs. |

| Troubleshooting | | |
|--------------------------------------|---|--|
| Condition | Ideas to consider | |
| CIP does not return unit to baseline | Check normalized clean water resistance and permeability values | |
| | Evaluate CIP procedure, more aggressive cleaning may be needed (higher temp, stronger chemical concentration if compatible with membrane) | |
| | Consider changing the order of chemicals 9acid before caustic, etc) | |
| | Consider the effects of pH, may cause aluminum scale on membrane if alum is used in pretreatment | |
| | Evaluate CIP procedures with manufacturer and engineers, compare with other utilities | |
| | Consider using soft water for CIP solutions | |

Regulations

- Currently state primacy agencies award different log removal credits for MF/UF membrane systems.
- In 2003 USEPA proposed specific language relative to the use and application of membranes to meet requirements of the Long-Term 2 Enhanced Surface Water Treatment Rule (LT2SWTR).
- A draft of a guidance manual (Membrane Filtration Guidance Manual) is available to assist the drinking water community and regulatory agencies in permitting membrane systems.

TN Rules for Membranes

Systems receive LT 2 Cryptosporidium treatment credit for membrane filtration that meets the following criteria:

- · The removal efficiency is demonstrated during challenge testing
- The maximum removal efficiency can be verified through direct integrity testing used with the membrane filtration process.
- The system must conduct continuous indirect integrity monitoring.

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TN Rules for Membranes

Challenge Testing

- Challenge testing must be conducted on either a full-scale membrane module or a smaller-scale membrane module, identical in material and similar in construction to the fullscale module.
- Challenge testing must be conducted using Cryptosporidium oocysts or a surrogate that is removed no more efficiently than Cryptosporidium oocysts.
- The organism or surrogate used during challenge testing is referred to as the challenge particulate.
- The concentration of the challenge particulate, in both the feed and filtrate water, must be determined using a method capable of discretely quantifying the specific challenge particulate used in the test; gross measurements such as turbidity may not be used.

TN Rules for Membranes

Challenge Testing-

- The maximum feed water concentration that can be used during a challenge test is based on the detection limit of the challenge particulate in the filtrate and must be determined according to the following equation: Maximum Feed Concentration = 3.16 × 106 × (Filtrate Detection Limit)
- Challenge testing must be conducted under representative hydraulic conditions at the maximum design flux and maximum design process recovery specified by the manufacturer for the membrane module.

TN Rules for Membranes

Challenge Testing-

- Removal efficiency of a membrane module must be calculated from the challenge test results and expressed as a log removal value (LRV) according to the following equation: LRV = LOG10(Cf) × LOG10(Cp)
- Cf = the feed concentration measured during the challenge test; and Cp = the filtrate concentration measured during the challenge test

TN Rules for Membranes

Challenge Testing-

- The removal efficiency of a membrane filtration process demonstrated during challenge testing must be expressed as a log removal value (LRVCTest).
- If fewer than 20 modules are tested, then LRVC-Test is equal to the lowest of the representative LRVs among the modules tested. If 20 or more modules are tested, then LRVC-Test is equal to the 10th percentile of the representative LRVs among the modules tested.
- The challenge test must establish a quality control release value (QCRV) for a non-destructive performance test that demonstrates the Cryptosporidium removal capability of the membrane filtration module

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TN Rules for Membranes

Direct Integrity Testing-

- Systems must conduct direct integrity testing in a manner that demonstrates a removal efficiency equal to or greater than the removal credit awarded to the membrane filtration process.
- A direct integrity test is defined as a physical test applied to a membrane unit in order to identify and isolate integrity breaches (i.e., one or more leaks that could result in contamination of the filtrate).

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TN Rules for Membranes

Direct Integrity Testing-

- The direct integrity method must have a resolution of 3 micrometers or less.
- The direct integrity test must have a sensitivity sufficient to verify the log treatment credit awarded to the membrane filtration process by the State.
- Systems must establish a control limit within the sensitivity limits of the direct integrity test that is indicative of an integral membrane unit capable of meeting the removal credit awarded by the State.
- If the result of a direct integrity test exceeds the control limit established, the system must remove the membrane unit from service.
- Systems must conduct a direct integrity test to verify any repairs, and may return the membrane unit to service only if the direct integrity test is within the established control limit.

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TN Rules for Membranes

Direct Integrity Testing-

• Systems must conduct direct integrity testing on each membrane unit at a frequency of not less than once each day that the membrane unit is in operation. The State may approve less frequent testing, based on demonstrated process reliability, the use of multiple barriers effective for *Cryptosporidium*, or reliable process safeguards.

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TN Rules for Membranes

Indirect Integrity Monitoring-

- Indirect integrity monitoring is defined as monitoring some aspect of filtrate water quality that is indicative of the removal of particulate matter.
- Unless the State approves an alternative parameter, continuous indirect integrity monitoring must include continuous filtrate turbidity monitoring.
- Continuous monitoring must be conducted at a frequency of no less than once every 15 minutes.
- Continuous monitoring must be separately conducted on each membrane unit.

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TN Rules for Membranes

Indirect Integrity Monitoring-

- If indirect integrity monitoring includes turbidity and if the filtrate turbidity readings are above 0.15 NTU for a period greater than 15 minutes (i.e., two consecutive 15-minute readings above 0.15 NTU), then direct integrity testing must immediately be performed on the associated membrane unit.
- If indirect integrity monitoring includes a State-approved alternative parameter and if the alternative parameter exceeds a State- approved control limit for a period greater than 15 minutes, direct integrity testing must immediately be performed on the associated membrane units.

Helpful information

EPA's Membrane Filtration Guidance Manual

 $\underline{http://epa.gov/OGWDW/disinfection/lt2/pdfs/guide_lt2_membranefiltration_final.pdf}$

AWWA Manual of Water Supply Practices

M53 Microfiltration and Ultrafiltration Membranes for Drinking Water

and Ultrathitration
Membranes
M53

Membrane Filtration Vocabulary

Asymmetric – Having a varying consistency throughout (e.g. a membrane that varies in density or porosity across its structure).

Backpulse – A very short-duration backwash.

Backwash – The intermittent waste stream from a microfiltration or ultrafiltration membrane system; also, a term for a cleaning operation that typically involves periodic reverse flow of clean water and/or air from the filtrate aide to the feed side to remove foulants accumulated at the membrane surface.

Bank – A group of pressure vessels that share common valving and that can be isolated as a group for testing, cleaning, or repair; synonymous with the terms train, skid, rack and membrane unit.

Biofouling – Membrane fouling that is attributed to the deposition and growth of microorganisms on the membrane surface and/or the adsorptive fouling of secretions of microorganisms.

Bleed – The continuous waste stream from a microfiltration or ultrafiltration system operated in a crossflow mode (synonymous with the terms reject and concentrate).

Cartridge – A type of module consisting of a disposable backwashable or nonbackwashable filter element contained in an external casing.

Chemical Cleaning (also, Clean-In-Place or CIP) – The periodic application of a chemical solution (or series of solutions) to a membrane unit for the intended purpose of removing accumulated foulants and thus restoring permeability and resistance to baseline levels; a commonly used term for in situ chemical cleaning.

Crossflow – The application of water at high velocity tangential to the surface of a membrane to maintain contaminants in suspension.

Differential Pressure – A pressure drop across a membrane module or unit form the feed inlet to concentrate outlet.

Fiber – A single hollow fiber or hollow fine fiber.

Filtrate – The water produced from a filtration process.

Flux – The throughput of a pressure-driven membrane filtration system, expressed as flow per unit of membrane area.

Foulant – Any substance that causes fouling.

Fouling – The gradual accumulation of contaminants on a membrane surface or within a porous membrane structure that inhibits the passage of water, therefore decreasing productivity.

Hydrophilic – The water-attracting property of membrane material.

Hydrophobic – The water-repelling property of membrane material.

Inside-out – A flow pattern associated with hollow fiber membranes in which the feedwater enters the inside of the fiber and is filtered as it passes through the lumen wall to the outside of the fiber.

Log Removal – The filtration removal efficiency for a target organisms, particulate, or surrogate expresses as log_{10} .

Lumen – The center or bore of a hollow fiber membrane.

Microfiltration (MF) – A pressure-driven membrane filtration process that typically employs hollow fiber membranes with a pore size range of approximately $0.10 - 0.5 \mu m$.

Nanofiltration (NF) – A pressure-driven membrane separation process that employs the principles of reverse osmosis to remove dissolved contaminants from water; typically applied for membrane softening or the removal of dissolved organic contaminants.

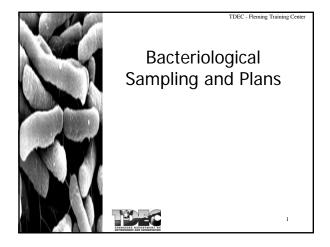
Outside-In – A flow pattern associated with hollow fiber membranes in which the feedwater is filtered through the lumen wall as it passes from the outside of the fiber to the inside where the filtrate is collected.

Reverse Osmosis (RO) – The reverse of the natural osmosis process, i.e. the passage of a solvent (e.g. water) through a semipermeable membrane from a solution of higher concentration to a solution of lower concentration against the concentration gradient, achieved by applying pressure greater than the osmotic pressure to the more concentrated solution; also, the pressure-driven membrane separation process that employs the principles of RO to remove dissolved contaminants from water.

Scaling – The precipitation or crystallization of salts on a surface (e.g. on the feed side of a membrane).

Ultrafiltration (UF) – A pressure-driven membrane filtration process that typically employs hollow fiber membranes with a pore size range of approximately 0.01- $0.05 \mu m$.

Section 4 Bacteriological Sampling & Plans



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Bacteriological Sampling Plan

- Developed to insure the water quality within the distribution system
- Major steps are:
 - Sample sites
 - Maps
 - Number of samples
 - Sampling procedures

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Sampling Sites

- Sampling sites will include:
 - Residential areas
 - Dead end lines
 - Low use areas
 - Commercial areas
 - Areas near storage tanks

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Sampling Sites cont.

 Samples will be distributed to ensure that no area served by the system is neglected during the year

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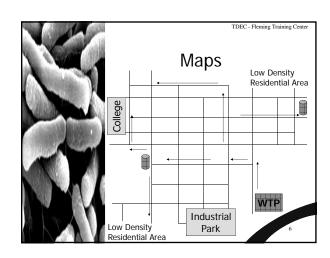


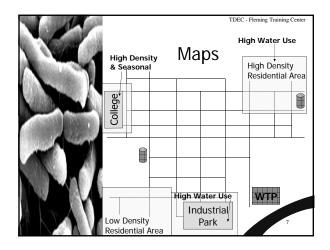
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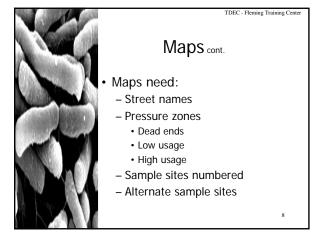
Sampling Sites cont.

- The reason for selecting sampling zones and specific sites is to aid the operators in:
 - Understanding the bacteriological quality of the water throughout the system
 - Zones should have the same water quality
 - Describing the quality of the water consumed by all the customers in the system

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Number of Samples

 Number of samples to be taken monthly is determined by TN Department of Environment and Conservation, Division of Water Supply

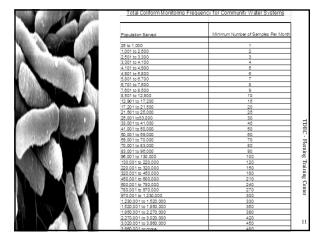
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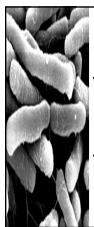
Number of Samples cont.

1200-5-1-.07(1)(c)

Coliform samples shall be taken at regular time intervals and in number proportional to the population served by the system during the reporting period as set forth

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Coliform MCL

1200-5-1-.06(4)(a)(1)

- For a system that collects at least 40 samples per month, if no more than 5.0 % of samples collected during a month are total-coliform positive, the system is in compliance with the MCL
- For a system that collects fewer than 40 samples per month, if no more than one sample collected during a month are total-coliform positive, the system is in compliance with the MCL



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Repeat Samples

1200-5-1-.07(2)(a)

- For systems that take only one routine sample per month, a set of no fewer than 4 repeat samples must be taken
- For systems that take more than one routine sample per month, a set of no fewer than 3 repeat samples must be taken

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Repeat Samples cont.

- Routine samples should be taken on Mondays and Tuesdays to avoid problems with repeats
 - If repeats are needed, this should give time to resample, take to the lab and start test before weekend

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Selecting Sampling Sites

- The system should take at least 30% of the required samples from residential areas
 - Residential areas are defined as locations in the distribution system which are served by the smallest distribution lines

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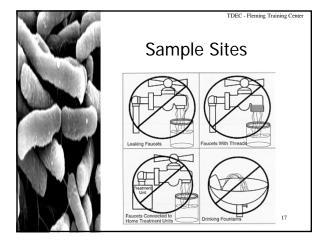


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Selecting Sampling Sites cont.

 The plan must include maps of the distribution system that would allow the sanitary surveyor to determine if samples were collected at dead ends, low use areas, near storage tanks or other high probability areas for coliform

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Sample Sites cont.

- Avoid sampling from hydrants, taps from water softeners and leaking faucets
 - Very good chance for contamination
- Collect sample from a non-swivel faucet



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Sample Sites cont.

- Mixing faucets should not be used because water passing through the "hot" waterside may not be representative of the water in the distribution system
 - Water in the hot water tank is more likely to grow bacteria because the warm water may promote growth

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Sample Sites cont.

- Threaded taps should be avoided
 - Bacteria can grow in the grooves of the threads
 - Never take samples from taps that are clearly contaminated with scum or build up around faucet

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Sample Sites cont.

- Avoid faucets close to the ground or sink bottom
 - Close to the ground can be contaminated with dirt
 - Close to the sink bottom may not allow room for bottle to be put under flow without touching the inside of the bottle

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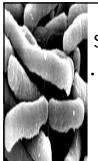
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Sample Sites cont.

- Good sample sites:
 - Water tank
 - Dead end with sampling tap
 - Fire halls
 - Public buildings



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Sampling Procedure cont.

 If a faucet has a strainer, aerator or any other attachment, remove before sampling



 Let the water run for several minutes (3-5 min) to insure fresh water from the main

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Sampling Procedure cont.

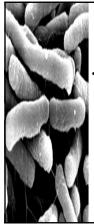
Take Free Chlorine Residual using DPD method and record



Disinfect faucet with either a difute bleach spray (~200 mg/L), rubbing alcohol (~25%) or flame it with a propane or butane torch

- 200 mg/L equals 4 mL of 5% bleach into 1 L

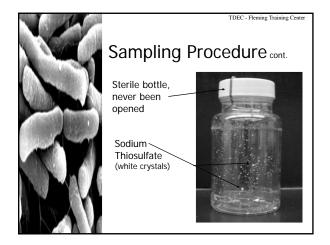
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Sampling Procedure cont.

- Reopen the faucet and let the water run in a stream about the size of a pencil to prevent splashing during sampling
 - Remember the bottles are sterile
 - DO NOT rinse the bottle
 - If you feel you have contaminated the bottle, dispose & start with a new one
 - Use fresh bottles, old bottles left out in the sun may not eliminate chlorine as well



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Sampling Procedure cont.

- Hold the bottle in one hand near the bottom and with the other hand remove the top
 - Care should be taken in removing the lid so as not to touch the inside of the bottle or

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Sampling Procedure cont.

- Hold the bottle under the faucet, allowing only a small, steady stream to flow from the faucet
 - When filling the bottle, hold the bottle so as to avoid water contacting the hand and running into the bottle
 - Collect 100 mL ± 2%
 - Meniscus needs to touch the 100 mL mark
 - Immediately remove bottle from underneath the faucet and replace

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Sampling Procedure cont.

- Document the required information from the sample site
 - Time and date collected
 - Location or address
 - Free chlorine residual
 - Collector's name
 - Sample type
 - Routine DS sample
 - Check sample
 - Raw or finished water sample
 - · Repeat or confirmation sample
 - Other special purpose sample

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Sample Label

Site 196 E. Main Street Billieville, TN

Date / Time August 15, 2005 8:15 AM

Sampled by Billy Joe Smith

Commentsgrab sample, monthly Bac't
Residual chlorine = 2.1 mg/L

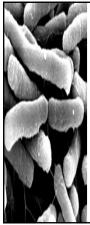


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Sampling Procedure cont.

- Replace all attachments after sampling is completed
- All samples must be tested within 30 hours of collection

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Positive Samples

- Repeat samples shall be collected within 24 hours of positive results
 - One repeat sample at original site of total coliform-positive sample
 - At least one at a tap within 5 service connections upstream
 - At least one at a tap within 5 service connections downstream

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|--------------------------------|--|
| EPA Lab # | |
| TN Lab # | |

Bacteriological Sample Analysis Report

Membrane Filter and/or Presence/Absence

| Sample | | Colle | ected | Collected Free Cl Time | | Free CI Time Residual Received | | Time in Incubator Analyst | | Results Read | | Results | | Read |
|----------|-------|-------|-------|------------------------|--------|-----------------------------------|------|---------------------------|----------|--------------|------|---------|---------|------|
| Location | Type* | Date | Time | Ву | (mg/L) | in Lab | Date | Time | AllalySt | Date | Time | Total | E. coli | Ву |
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*Sample Type: D = Distribution System

R = Repeat Sample

N = New Line

S = Special Sample

Section 5

Fluoride

Health Benefits
Regulations
Additives
Lab Analysis
Equipment



Water Fluoridation **Principles and Practices** For Water Facility **Operators**



Water Fluoridation

Health Benefits Regulatory Perspective Fluoride Additives Equipment/Facilities Laboratory Analysis Personnel Safety Operations



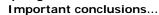
Who, What, Where, Why, How

- Fluoridation is adjustment of water fluoride
- Used for optimum oral health benefits
- One of ten great public health achievements of the twentieth century (CDC)
- Water fluoridation has a 60-year history of success





 Dr. Frederick S. McKay initiated a study in 1908 of "Colorado Brown Stain" in Colorado **Springs**

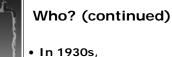


- Affected teeth more resistant to dental decay
- Life-long residents had stained teeth, more recent residents did not
- High fluoride content of water identified in 1931







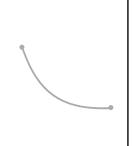


- Dr. H. Trendley Dean conducted the "21 Cities Study"
- Important conclusions:
 - Optimum levels of fluoride for enhancing oral health (natural breakpoint at 1 mg/L)
 - 1.0 mg/L provided best combination of reduction in tooth decay (caries) and low risk of fluorosis
 - Established community fluorosis index (increased incidence at 2 mg/L)



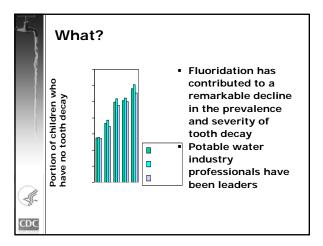
What?

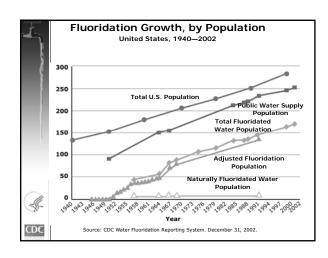
- Adjustment of fluoride in water to an optimum range of 0.7-1.2 mg/L
- Recommended CDC control range is 0.1 below to 0.5 mg/L above optimum
- **Decreased benefits** below optimum
- No additional benefit and more severe fluorosis above 2 mg/L

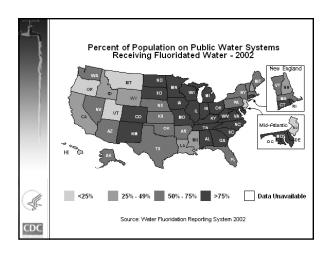


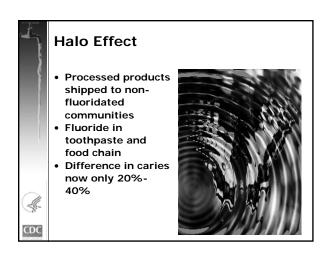
Water fluoride content mg/L

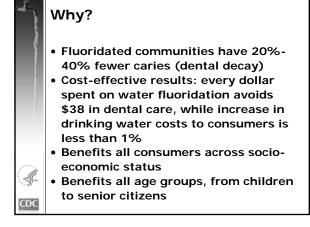
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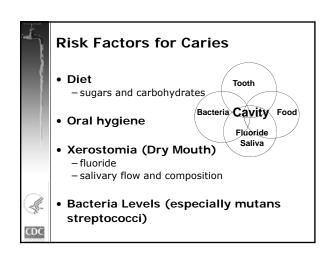


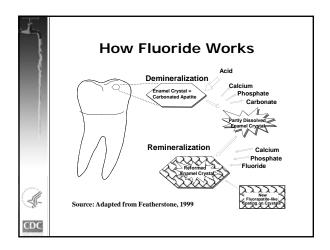


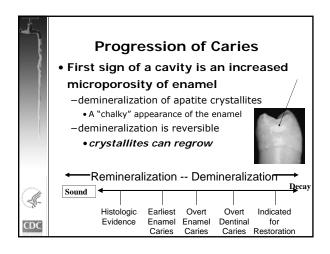


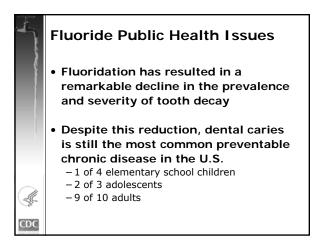


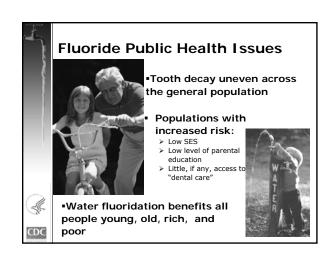


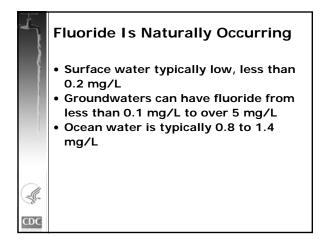


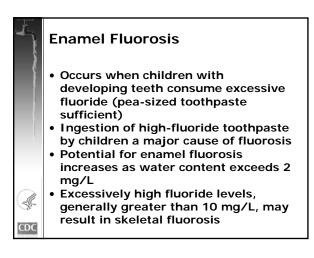


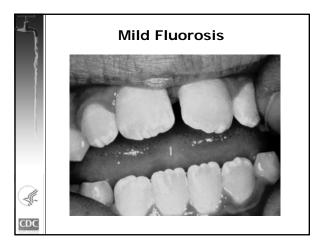


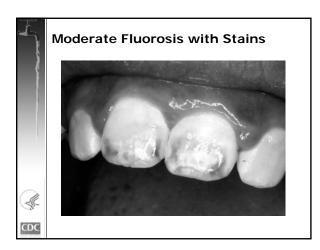


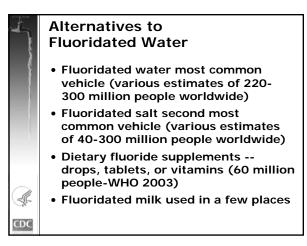


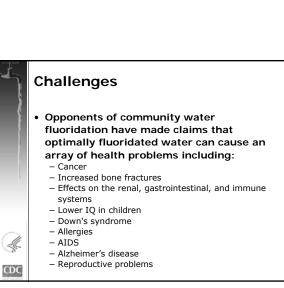




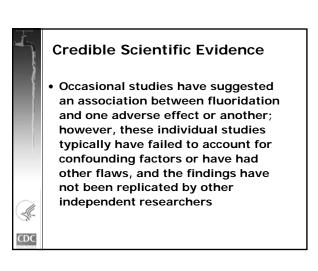




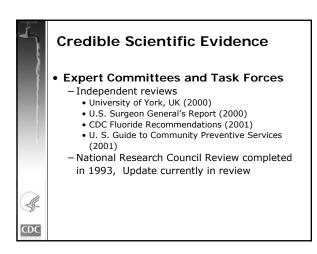


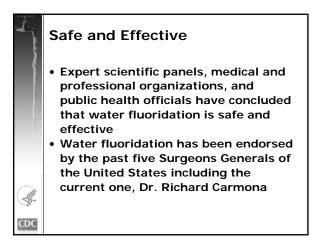




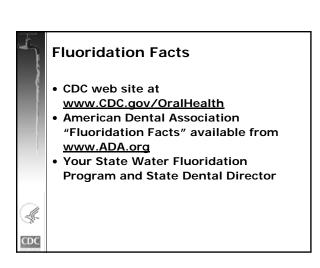


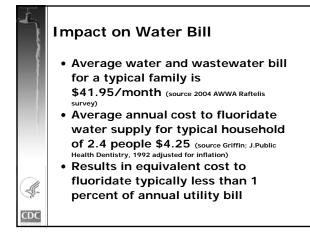
CDC





Public Policy on Fluoridation Recognized by the American Dental Association, U.S. Public Health Service, American Medical Association, World Health Organization, American Water Works Association, and virtually every scientific and professional organization in the health field



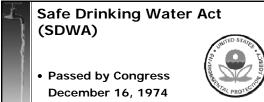






Water Fluoridation

Health Benefits Regulatory Perspective Fluoride Additives Equipment/Facilities Laboratory Analysis Personnel Safety Operations



- · Reauthorized in 1986 and 1996
- · Assures that drinking water supplied to the public is safe
- · Administered and enforced by individual states when they adopt criteria equal or exceeding the federal standards





- Contaminant
 - Any physical, chemical, biological, or radiological substance or matter in water
 - Some contaminants are nutrients that promote good health at low concentrations including fluoride, copper, iron, and others



CDC



EPA and Water Fluoridation

- . EPA and the PHS were early partners in promoting water fluoridation
 - 1962 and 1972 Engineering Manual was predecessor to AWWA MOP #4
 - Regional Fluoridation **Engineers**
- 1974 SDWA defined water fluoridation as a state program, not an EPA program







K.

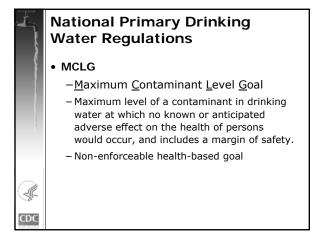
Water Additives Not Regulated by EPA

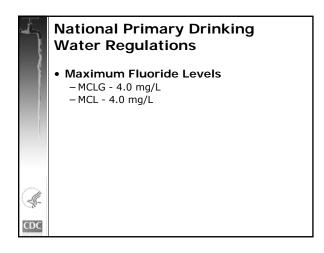
- EPA focuses on safe water and contaminant levels that result in unfavorable health outcomes
- Other entities provide standards covering water additives (AWWA, **NSF International)**
- · Water fluoridation is a state program, not a federal program

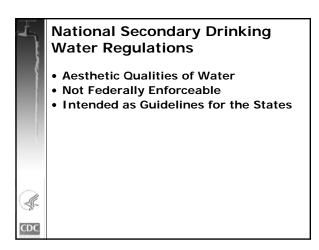


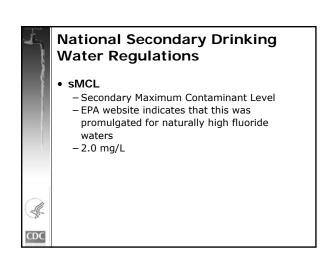


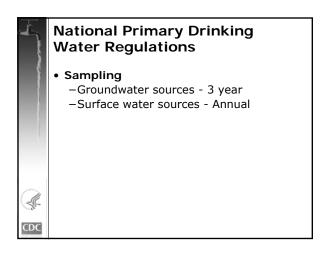
- MCL
 - -Maximum Contaminant Level
 - The maximum permissible level of a contaminant in water which is delivered to any user of a public water system.
 - Assure no short-term or long-term health
 - Economically and technologically feasible
 - States can set stricter standards

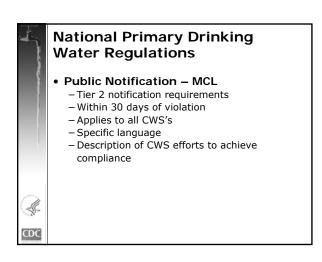


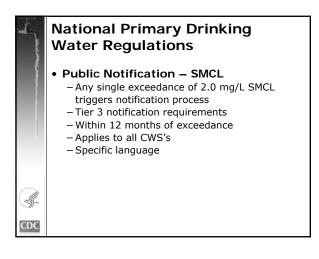


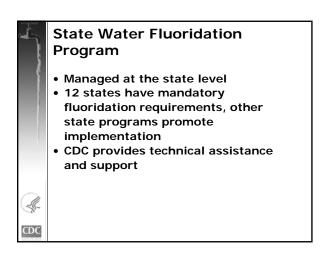


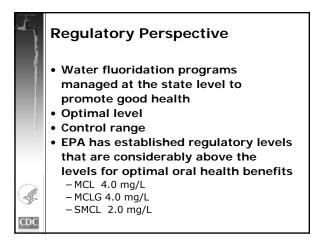










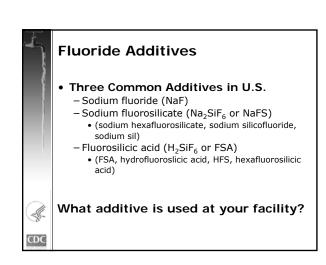


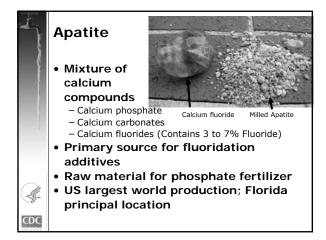


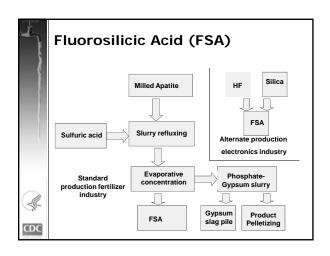


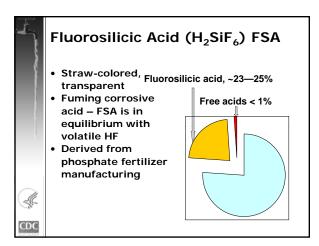
Water Fluoridation

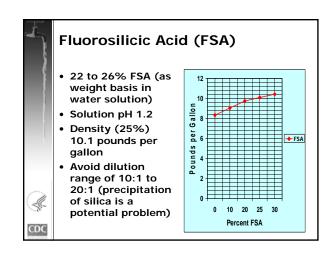
Health Benefits
Regulatory Perspective
Fluoride Additives
Equipment/Facilities
Laboratory Analysis
Personnel Safety
Operations





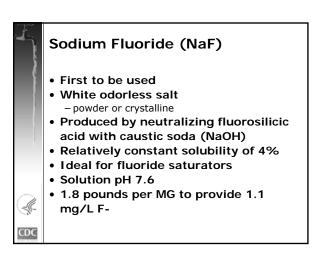




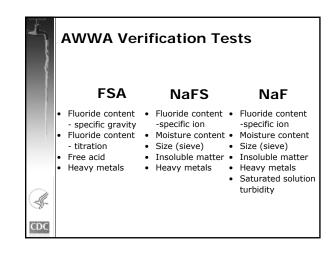


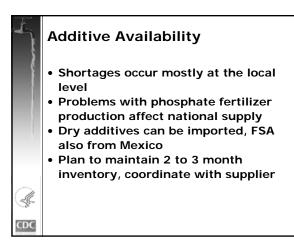
Sodium Fluorosilicate (NaFS)

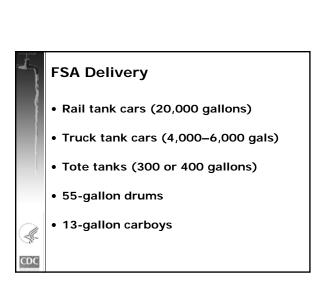
• Old name: "Sodium Silicofluoride"
• White odorless crystalline powder
• Produced by neutralizing fluorosilicic acid with sodium carbonate or sodium chloride
• Solubility varies with temperature
• Solution pH 3.0 to 4.0
• 14.0 pounds per million gallons to provide 1.1 mg/L F-

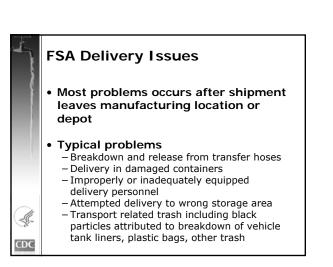


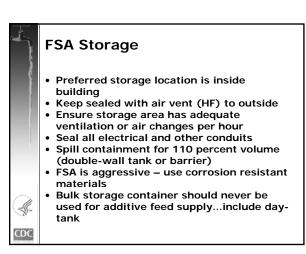












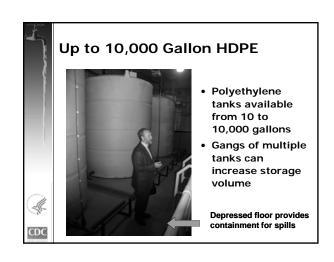


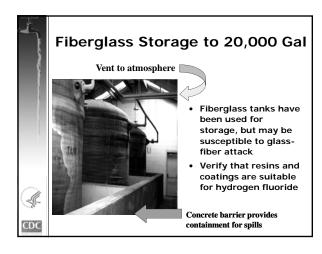
Fluoridation Unrelated to Pipe Corrosion or Lead Levels

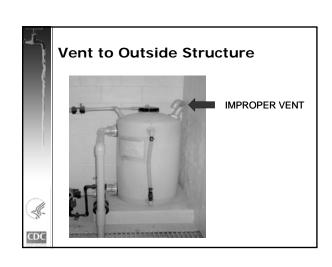
- Some operators may think that since HF gas released from concentrated H₂SiF₆ storage results in corrosion, water fluoridation will corrode pipes
- EPA and University of Michigan (Ann Arbor) researchers have proven that at temperatures and concentrations for water fluoridation, FSA achieves complete dissociation to fluoride, hydrogen, and silica and cannot produce HF
- Silicates are actually used as a stabilizer for water corrosion













- FSA will damage concrete surfaces
- A dual application of epoxy undercoat with urethane topcoat provides corrosion resistance
- Consult with coating manufacturer for acceptable products

Dry Additive Containers

- Sizes
 - 50-pound bags
 - 100-pound bags
 - 125 to 400-pound fiber drums
 - -2,500-pound supersacks
- Handling
 - Use knife to slit bag
 - Secured disposal to avoid personnel exposure





Dry Additive Delivery Issues

- Most problems occurred after shipment leaves manufacturing location or depot
- Typical problems
 - Delivery in damaged packaging
 - Improperly or inadequately equipped delivery personnel
 - Attempted delivery to wrong storage area
 - Mixing with other chemicals
 - Degradation of product during transport



Dry Additive Storage

- Separate room
 - do not mix additives secured access
- · Convenient to feed location
- **Good ventilation**
- Elevated platform
 - keep dry additives on pallets
- · Limit stacks to 6 bags
- Protected from elements











2,500 lbs Supersack Delivery





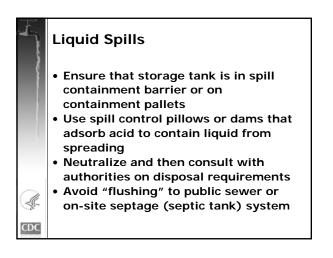
CDC

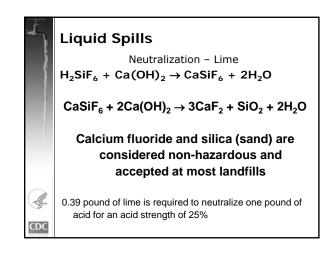
Dry Spills

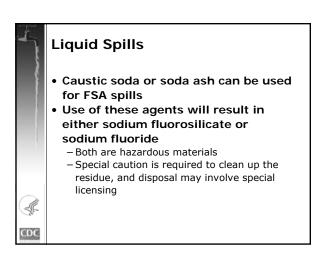
- · Sweep and place in secure container
- Typically, supplier will agree to pick up for disposal
- Check Codes and Regulations
 - State hazardous waste agency
 - Local Fire Marshall

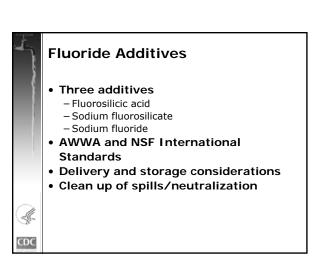


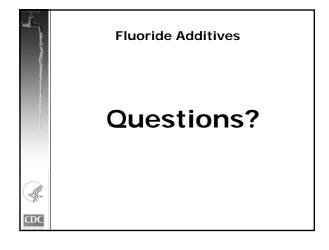
CDC

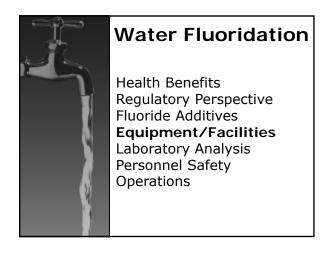


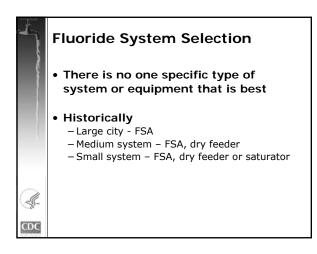


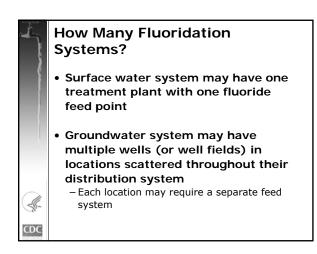


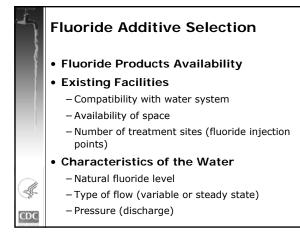


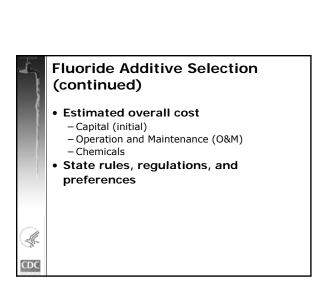


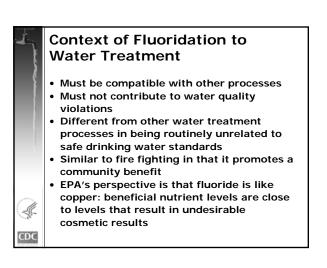


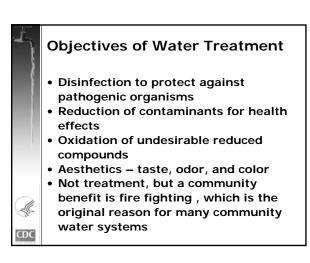


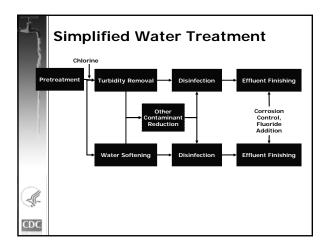


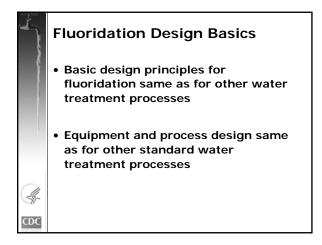


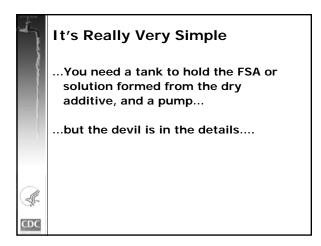


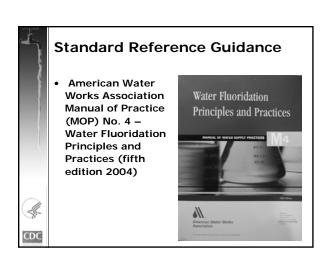


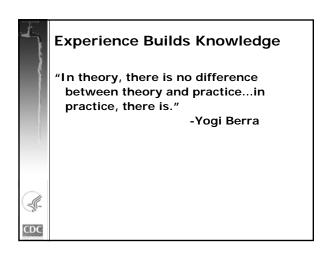




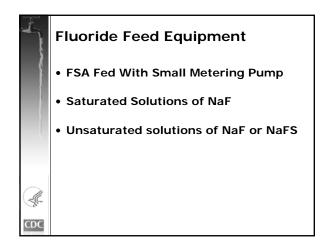


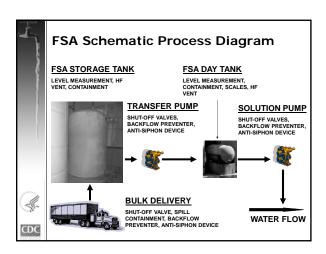


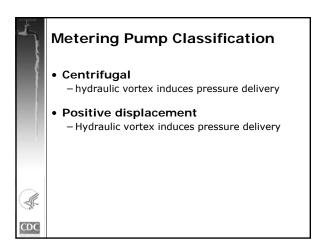


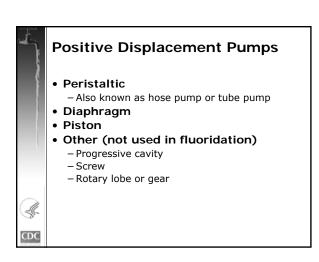


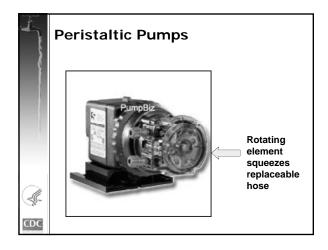


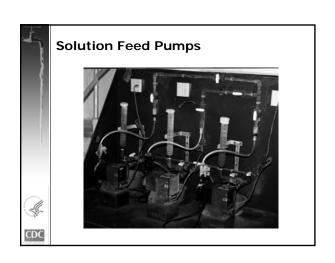


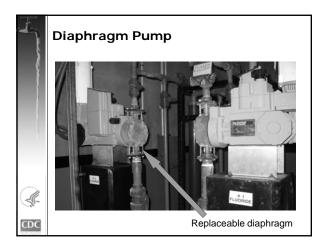


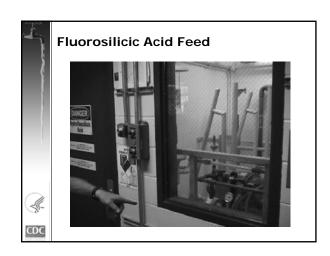


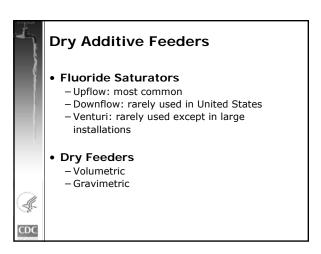


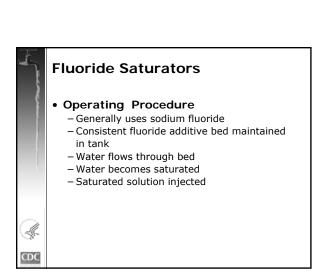


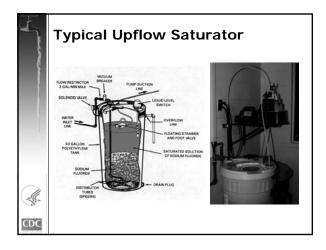


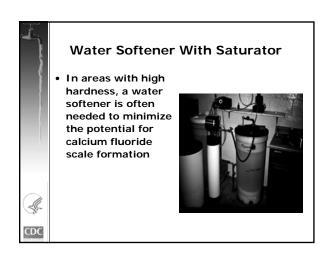


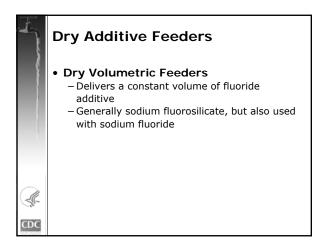


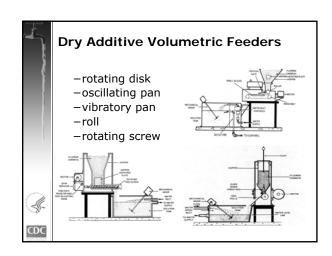


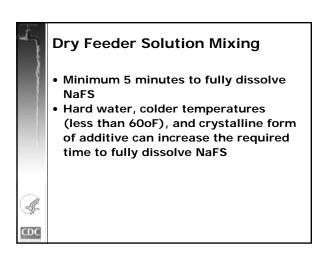




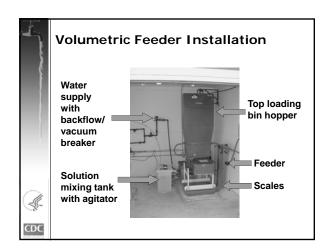


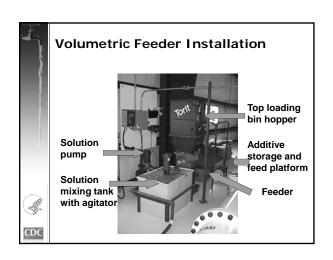


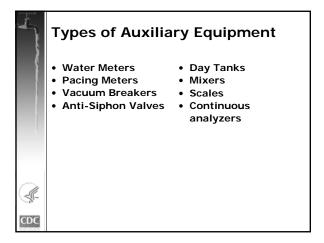


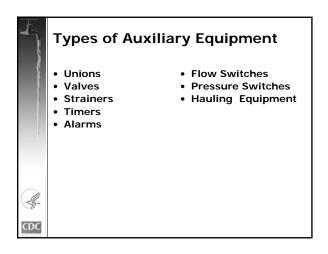


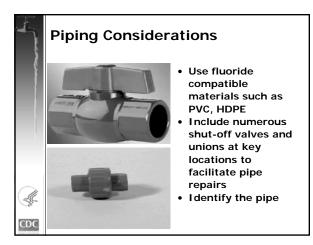


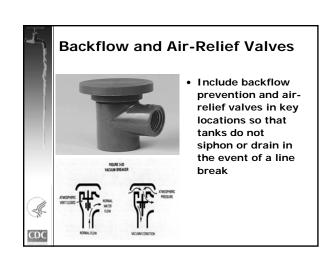


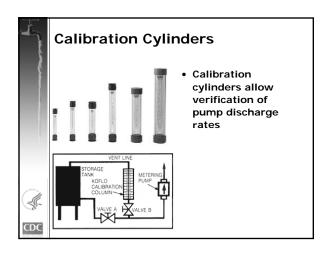


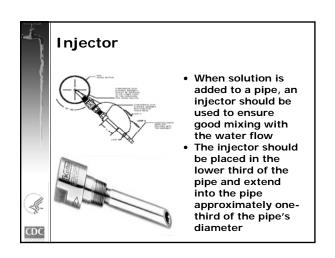


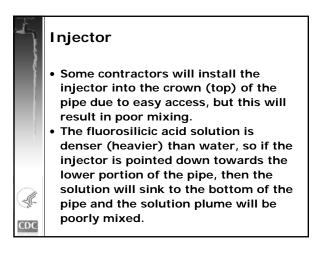


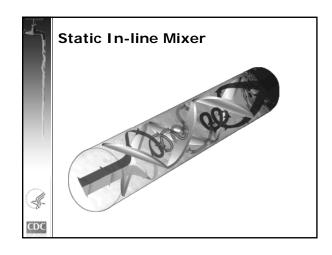


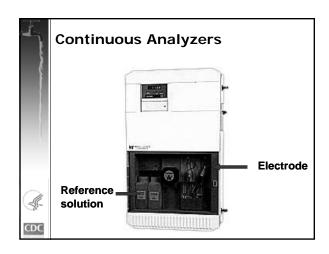


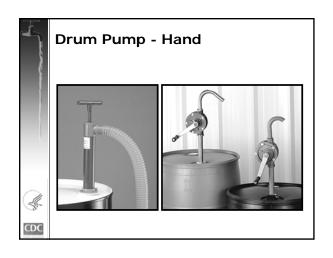


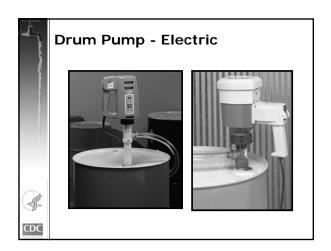


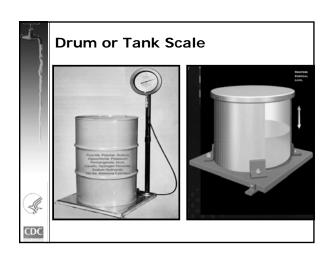


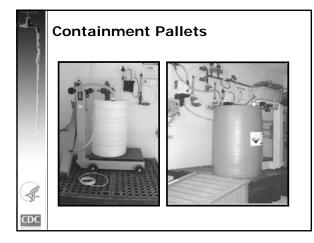


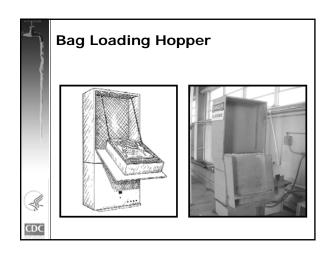


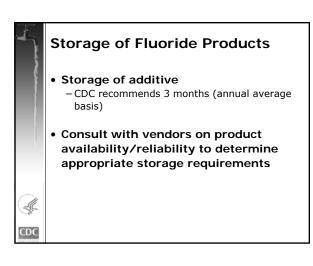


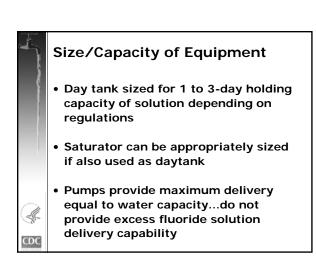


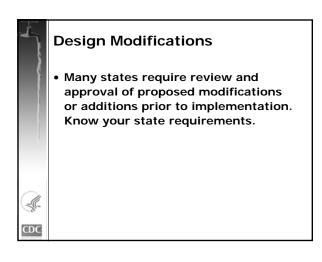


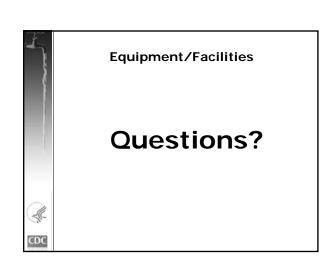


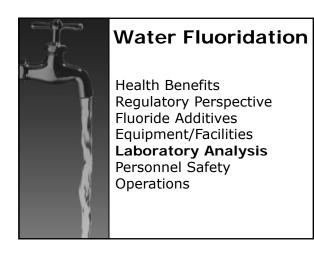


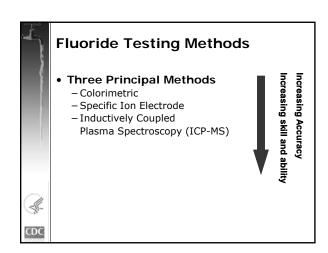


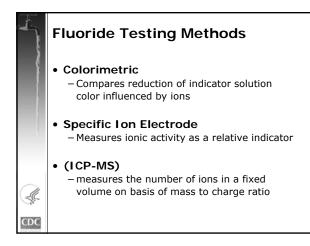


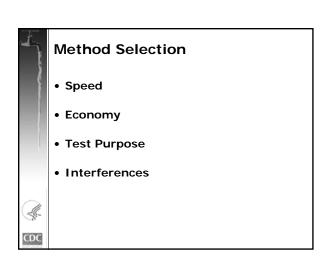


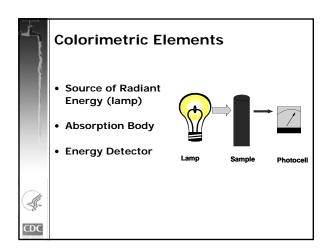


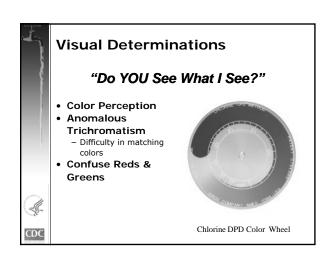


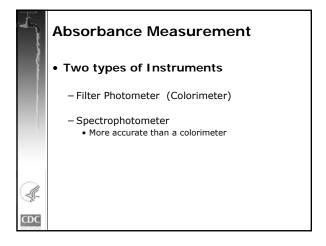


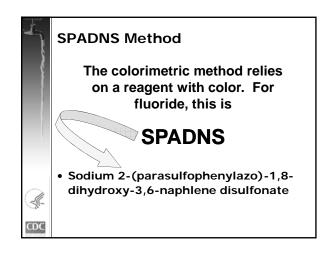


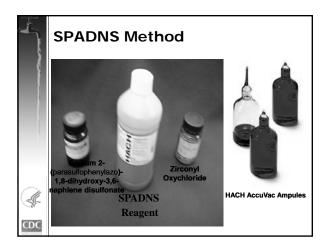


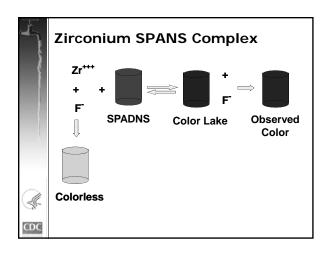


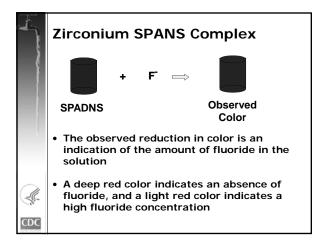


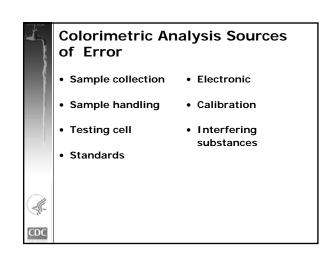


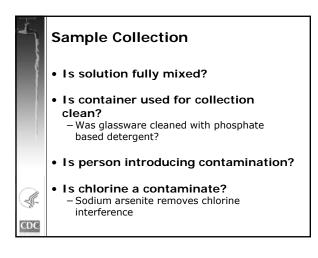


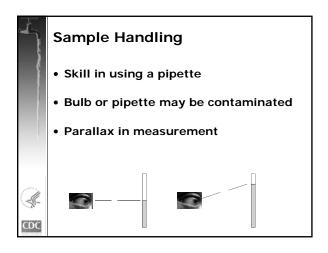


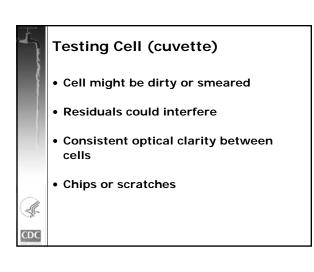


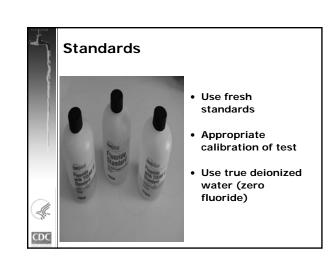


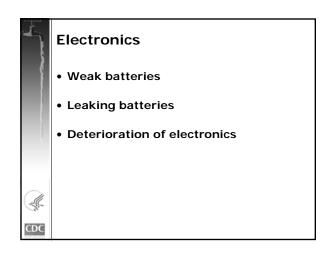


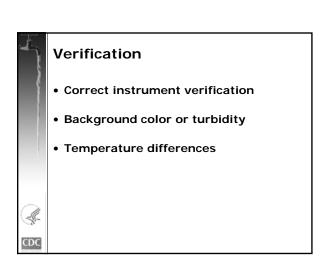






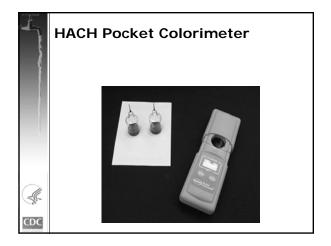


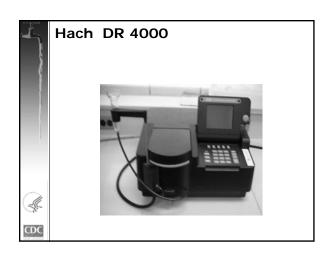


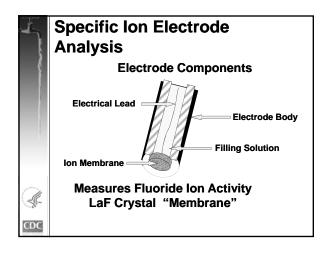


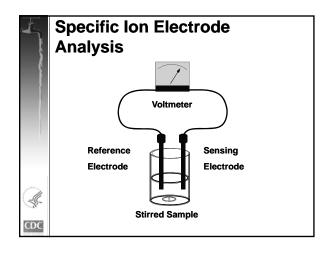
| F | SPADNS Interferences | | | | | | | | |
|-----|--|-----------|------------|--|--|--|--|--|--|
| | Concentration of substance (mg/L) req. to cause error of plu or minus 0.1 mg at 1.0 mg/L fluoride | | | | | | | | |
| | Interfering Substance | SPADNS | Electrode | | | | | | |
| | Alkalinity | 5,000 (-) | 7,000 (+) | | | | | | |
| | Aluminum | 0.1 (-) | 3.0 (-) | | | | | | |
| | Chloride | 7,000 (+) | 20,000 (-) | | | | | | |
| | Iron | 10 (-) | 200 (-) | | | | | | |
| | Hexametaphosph ate | 1.0 (+) | 50,000 | | | | | | |
| Sir | Phosphate | 16 (+) | 50,000 | | | | | | |
| CDC | Sulfate | 200 (+) | 50,000 (-) | | | | | | |

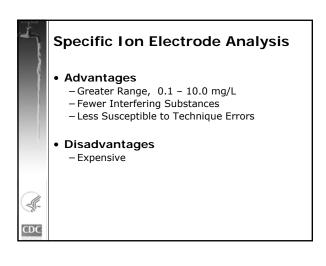
| SPADNS In | terferences | 3 | | | | | |
|--|--|-----------|--|--|--|--|--|
| Concentration of substance (mg/L) req. to cause error of plu or minus 0.1 mg at 1.0 mg/L fluoride | | | | | | | |
| Interfering Substance | SPADNS | Electrode | | | | | |
| Chlorine | Must be completely removed with arsenite* | 5,000 | | | | | |
| Color & Turbidity | Must be removed or compensated for | | | | | | |
| 11 \ | *Most suppliers (Hach is one of them) have ars their SPADNS to remove up to 5.0mg/L free ch | | | | | | |

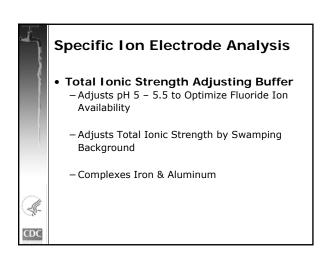


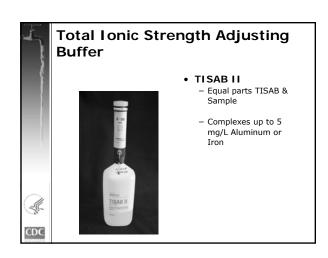


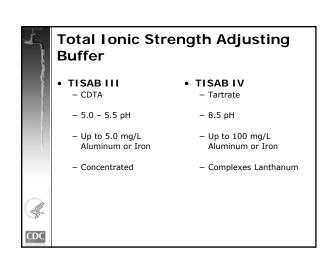


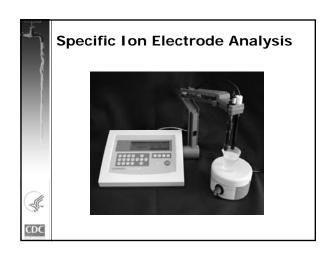


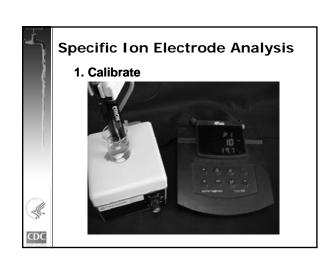


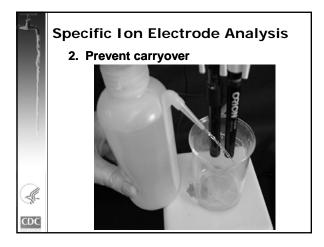


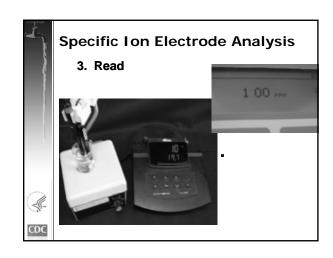


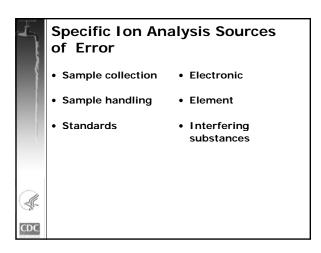




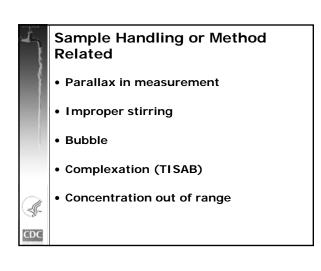


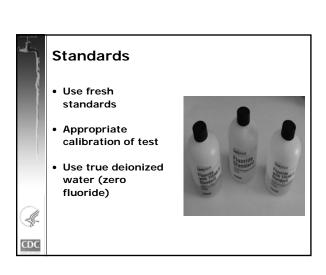


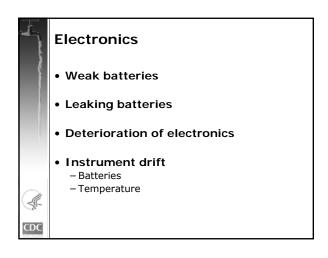


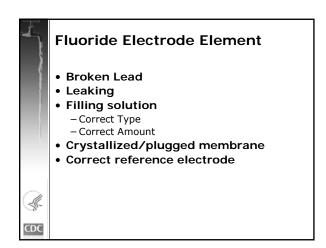


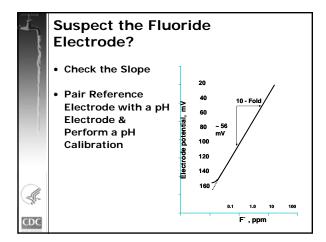


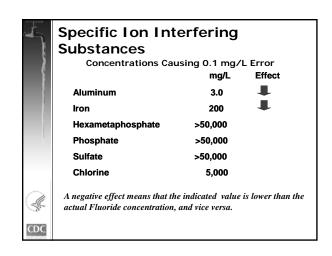


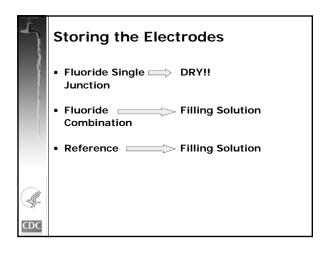


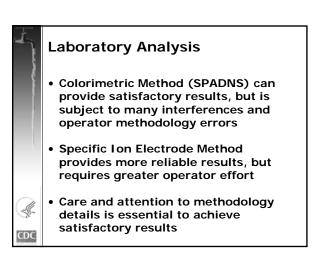


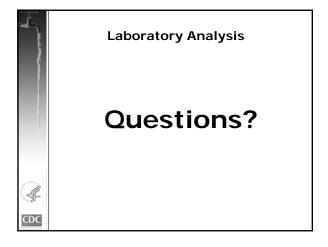


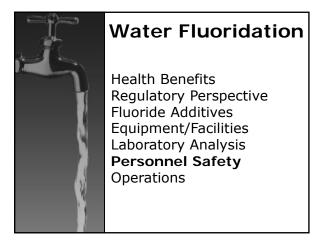


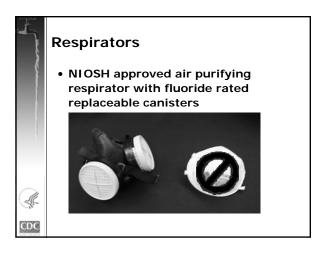


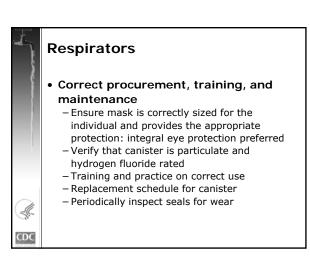










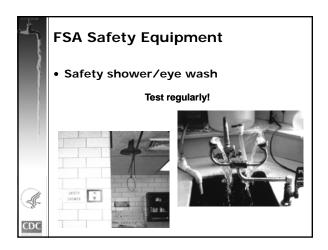


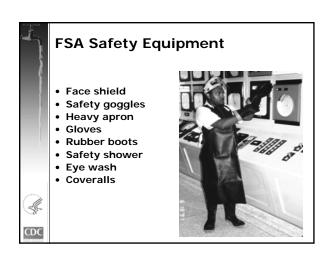




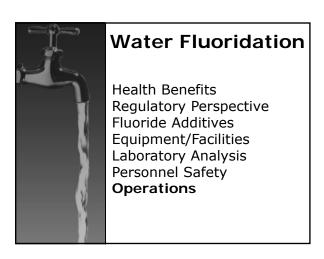


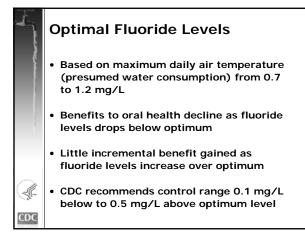


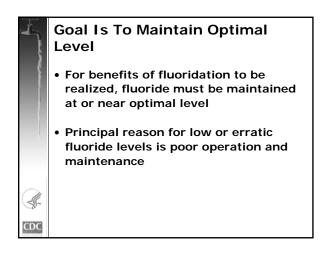


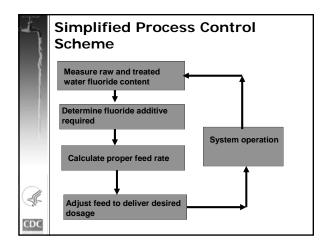


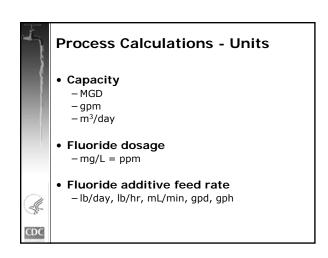


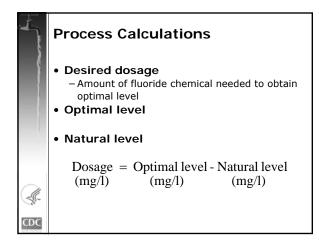


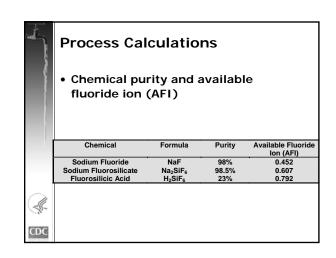


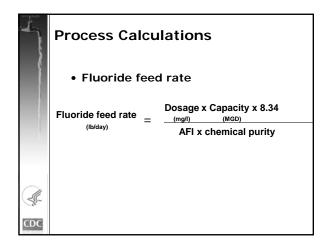


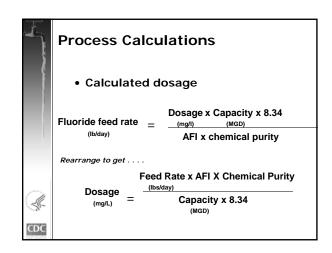


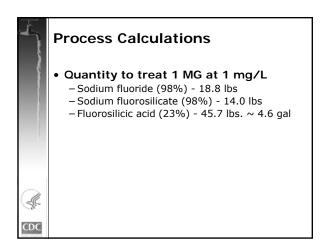


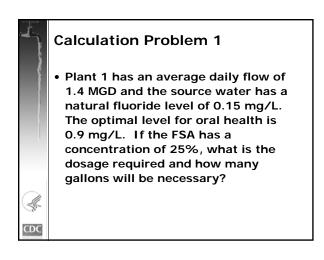


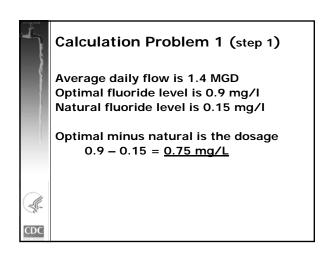


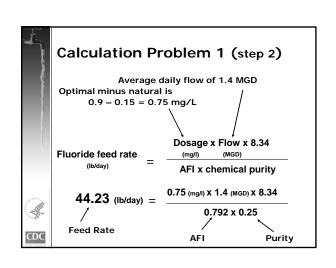


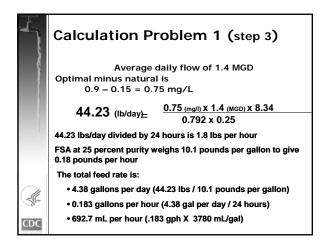


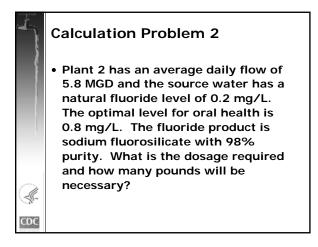


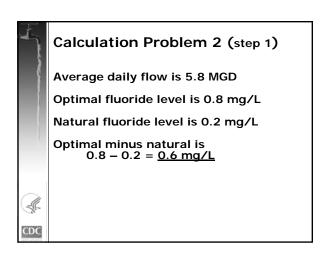


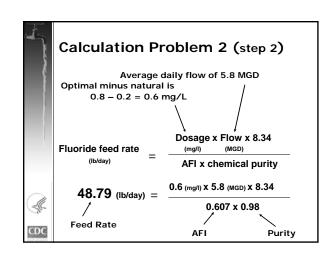


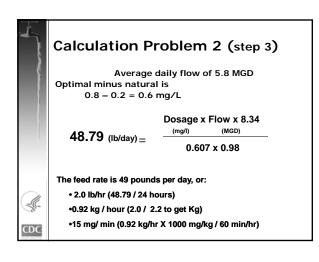


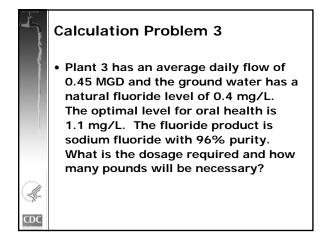


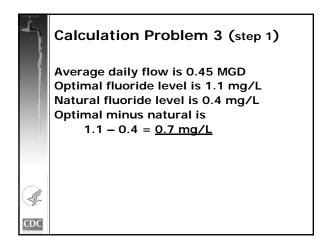


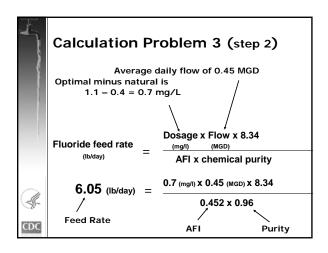


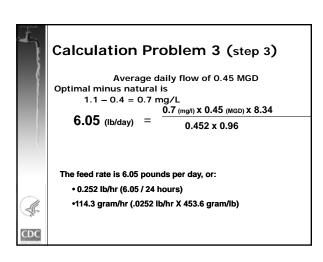


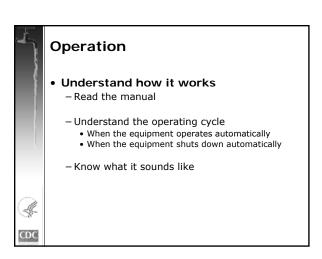


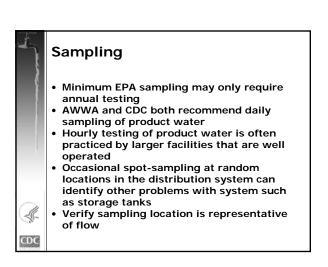


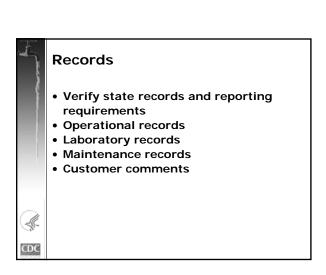














Operational Records

- Source/product water fluoride level (daily)
- · When and where sampling occurred
- · Amount of fluoride additive used (daily)
- Pump or feeder calibration curves and pump or feeder operational settings (quarterly)
- Make-up water for saturators and feeders
- Assay on chemical purity (with each delivery)
- Check with state on other record or documentation requirements



Operational Records

- Reporting of operating results important for public health
- Results are compiled and help public health officials, medical doctors, dentists, and other health care providers make good decisions for communities and patients



. Submit results monthly





- Dates, times, technician, location, methodology, etc. for sampling events
- Results of split-sampling with state proficiency laboratory
- Verification of analytical procedure against standards
- Maintenance of laboratory equipment



Maintenance Records

- · Dates of maintenance activities
- Documentation when pump hoses or heads are replaced
- Electrical records related to possible fluoride system operation
- Vendor for parts, supplies, and equipment manuals



Preventative maintenance not repairs: – continuous, dependable operation



CDC



Suggested Maintenance

- Daily
 - Watch for trouble
 - Inspect system, listen to sounds
 - Look for leaks or differences
 - Liquid systems
 - Check solution levels, check level switch
 - Check hoses for air locks
 - Check pump for prime
 - Refill day tank



- Dry feeders
 - Check for compaction
 - Refill additive hopper



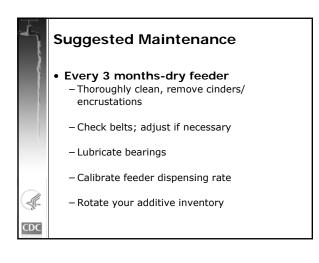
Suggested Maintenance

- Every 3 months-FSA feed system
 - Check all piping for leaks, and gas venting for integrity
 - Check pipes/hoses for encrustations
 - Inspect tank level measurement (floats, gauges, etc)

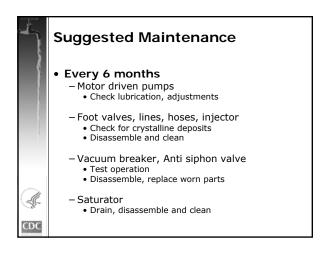


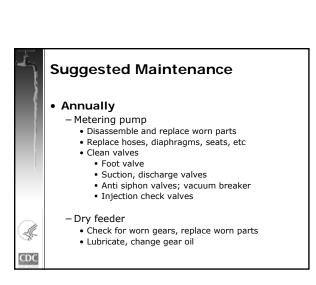
- Calibrate pump delivery rate

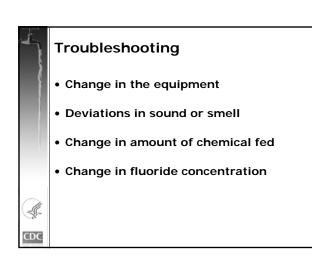
CDC

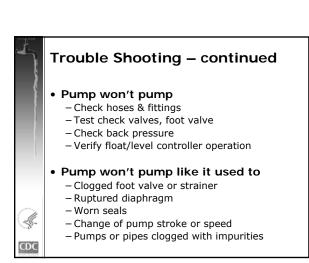


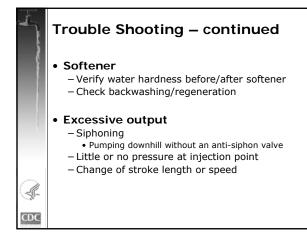


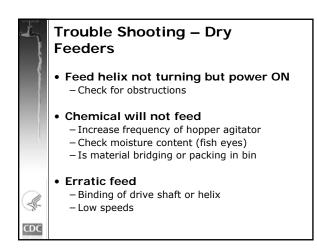


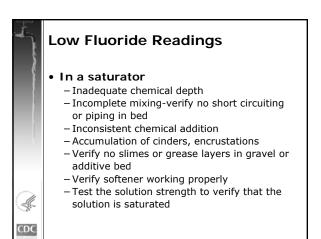


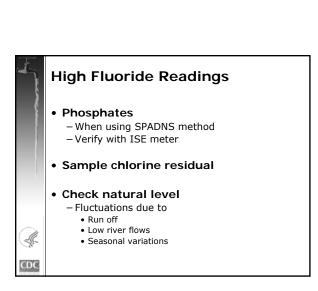


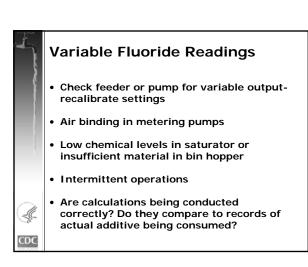


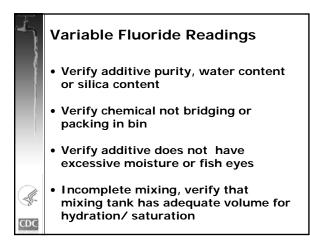


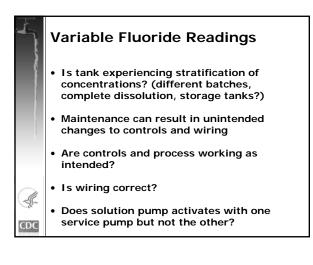


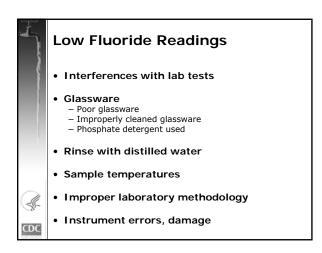


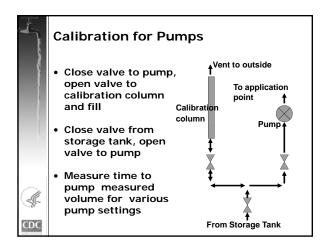


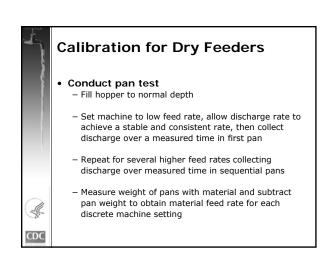


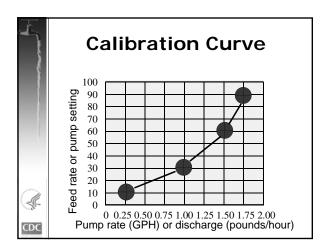


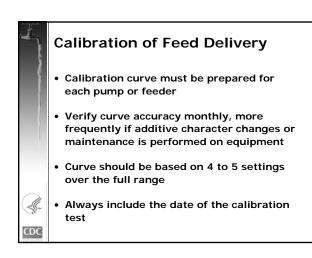


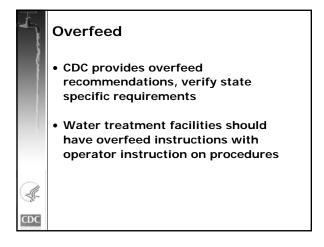


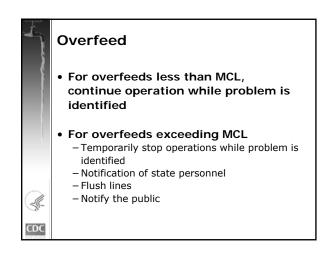


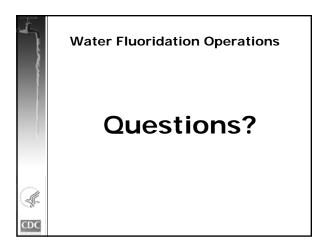




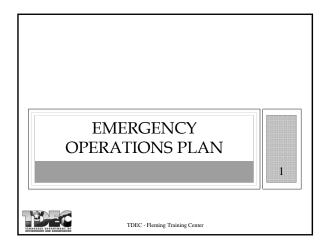








Section 6 Emergency Operation Plans



PROTECTING THE PUBLIC HEALTH

- Safe and reliable drinking water should be delivered to the public
- Should meet federal and state requirements
- Should be delivered in adequate quantities and at adequate pressures

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EMERGENCY OPERATIONS PLAN

- Also called EOP
- Identifies natural disasters and other emergencies that may strike a water system
- Assists water system in responding to emergencies quickly and effectively

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EMERGENCY OPERATIONS PLAN

- A carefully planned EOP will:
 - Reduce property damage
 - Minimize downtime
- Prevent illness
- Save lives
- Reduce system liability
- Emergency response planning is essential

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EMERGENCY OPERATIONS PLAN

- EOP's include specific responses to:
- Routine emergencies
- Natural disasters
- Accidents
- Intentional man-made acts
- Or any other incident that causes casualties, damage or disruption to the water system

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ROUTINE EMERGENCIES

- Line breaks
- Power outage
- Mechanical failure
- Water contamination





- Tornado
- Flood
- Earthquake
- Ice storm
- Drought





ACCIDENTS



- Chemical spill
- Explosion



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INTENTIONAL MAN-MADE ACTS

- Vandalism
- Terrorism
- Threats





VULNERABILITY ASSESSMENT

• For those systems who have done the Vulnerability Assessment (VA), the EOP should include response actions to potential threats and malicious acts identified in your VA

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EMERGENCY OPERATIONS PLAN

- The Tennessee Division of Water Supply defines a document that prepares for an emergency response as an "Emergency Operations Plan".
- The US EPA refers to this document as an "Emergency Response Plan (ERP)"

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EOP

- State Rules require all community water systems to have an EOP
 - 1200-5-1-.17(7)
 - "... all community water systems shall prepare an emergency operations plan in order to safeguard the water supply and to alert the public of unsafe drinking water in the event of natural or man-made disasters."

HISTORY

 After September 11, 2001 the federal government amended the Safe Drinking Water Act (SDWA) to add regulations on emergency preparedness for utilities, including community water systems

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HISTORY CONTINUED

 The BioTerrorism Act of 2002 added amendments to the SDWA that required the revision of water system emergency response plans to incorporate the results of the water system's vulnerability assessment

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HISTORY CONTINUED

 The Terrorism Act required that emergency response plans include plans, procedures and the identification of equipment that can be used in the event of a terrorist or other intentional attack on the water system

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EOP

- The EOP is a living document and should be reviewed and updated every two years
 - \bullet When there is a change to the water system configuration
 - Or when required by state or federal regulations

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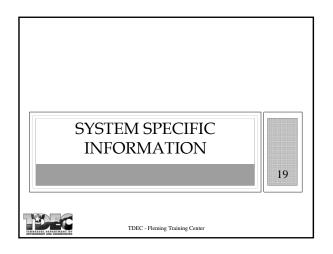
EOP ELEMENTS 17 TDEC - Fleming Training Center

EIGHT ELEMENTS OF EOP

- System Specific Information
- Roles and Responsibilities
- Communication Procedures
- Personnel Safety
- Alternate Water Source
- Equipment and Spare Parts
- Property Protection
- Water Sampling & Monitoring

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SYSTEM SPECIFIC INFORMATION

- Water system info
- Maps & critical info
- Water source
- Water treatment process
- Distribution system
- Pumping facilities
- Storage facilities
- SCADA system
- Chemical inventoryMaterials/parts
- Materials/parts inventory
- Critical customers
- Largest customers
- Security features
- Communication equipment
- Office computer equipment

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WATER SYSTEM INFORMATION

- Lists general information about the water system
 - System name & PWSID#
 - Address and directions to plant, office and emergency operations center (EOC)
 - Number of employees and certified distribution operators
 - Utilities used by water plant: electric, phone, gas and cell phone companies
 - Number of connections and population served

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MAPS AND CRITICAL INFO

- EOP should reference
- · Location of distribution maps
- Detailed plan drawings
- Site plans
- Valve and hydrant maps/books
- Process flow diagrams
- Operations reports
- Operating manuals
- Permits
- Etc.

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MAPS AND CRITICAL INFO CONTINUED

- Maps and other critical plans may be kept at a secure location and given out only on a "need-toknow" basis at the discretion of the water system manager
- Maps need to be kept-up to date
- Keep duplicate copies secured off-site

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WATER SOURCE

- There are different templates for
 - Surface water
 - Well water
 - Purchased water
 - Spring water

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WATER SOURCE CONTINUED

- Give location for intake or master meter
- Intake pipe size
- Raw water pump info
- Manufacturer, HP, capacity, year installed
- Well depth, diameter, static water levels
- Chemicals added at intake and quantity stored at intake building

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WATER TREATMENT PROCESS

- Dimensions and detention times for
 - Flash mix
 - Flocculation basins
- Sedimentation basins
- Filters
- Chemicals added and point of application, especially chlorine and fluoride

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DISTRIBUTION SYSTEM

- Population served
- Number of residential and commercial meters
- Miles of pipe
- Number of booster pumps and backflow preventers
- Peak, average and minimum daily demands

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PUMPING FACILITIES

- Name/location
- Whether it is a building or underground vault
- Elevation
- Capacity
- Suction and discharge pressure

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STORAGE FACILITIES

- Total number of elevated and ground level tanks
- Storage facility name/location
- Description
 - Welded steel, concrete, elevated, etc.
- Overflow or ground level elevation
- Capacity
- Level control
- Access and security

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SCADA SYSTEM

- Manufacturer of SCADA, Computer hardware running SCADA, Network software, Firewall/Security software, Antivirus software
- Outside access to SCADA
 - Phone line, DSL, cable, other, none
- Is system password protected?

CHEMICAL INVENTORY

- Chemical brand and common name
- What process is it used for?
- Point of use
- · Solid, liquid, gas?
- Strength
- Daily consumption
- Suppliers and their contact info

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MATERIALS & PARTS INVENTORY

- Description
- Serial # or VIN #
- Quantity
- Location

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CRITICAL CUSTOMERS

- Critical customers should be listed and prioritized based on community health issues
 - Hospitals, nursing homes, schools, daycares, etc.
- Name
- Description
- Address
- Phone #
- gal/day needed

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LARGEST CUSTOMERS

- List in prioritized order based on critical products or services to the community
- Name
- Description
- Address
- Phone #
- gal/day needed

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SECURITY FEATURES

- Location of buildings
- · Gates, fences
- Doors/windows
- Locks/card key
- Alarm systems
- Security lighting
- Cameras/monitors

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COMMUNICATION EQUIPMENT

- Cell phones
- Pagers
- 2-way radios
- Satellite phones
- Laptops with phone service
- Need description, serial #, quantity and location for all these

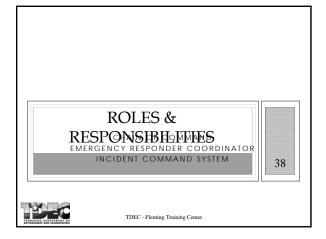
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OFFICE COMPUTERS & EQUIPMENT

- Name and contact info for internal and outsource IT person
- Office computer hardware
- Manufacturer
- Serial #
- Description/Processor
- Location

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CHAIN OF COMMAND

- In an emergency, system personnel should know
 - Where to report
 - Whom to report to
 - What their responsibilities are during the emergency response

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CHAIN OF COMMAND CONTINUED

- Chain of command establishes lines of authority that preserve order and prevent confusion
- Check this document quarterly to confirm accuracy of personnel and phone numbers

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EMERGENCY RESPONSE COORDINATOR

- The first response in any emergency is to notify the lead person
 - This is the person at the top of the chain of command
 - Referred to as the Emergency Response Coordinator (ERC)
- An alternate ERC should be designated in case primary ERC is unavailable

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EMERGENCY RESPONSE COORDINATOR

CONTINUED

- The ERC will asses the emergency and initiate the appropriate response actions
- The ERC will manage the entire emergency response unless an Incident Command Structure (ICS) facilitates a transfer of command

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EMERGENCY RESPONSE COORDINATOR

CONTINUED

- Other names given for lead person are
- Emergency operations coordinator (EOC)
- Emergency operations leader (EOL)
- Incident commander (IC)
- Water utility emergency response manager (WUERM)

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INCIDENT COMMAND SYSTEM

- In a major disaster, emergency or terrorist act, the ERC may need to initiate and/or defer to an Incident Command System (ICS)
- ICS is the model tool for coordinating the response efforts of several agencies as they work an emergency response

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INCIDENT COMMAND SYSTEM CONT

 If another agency takes over command in an ICS situation, the ERC and water system personnel remain in charge of all water system repairs and operations

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COMMUNICATION PROCEDURES 46

COMMUNICATION PROCEDURES

- Internal contact list and responsibilities
- External contact list
- Emergency communications plan
- Effective communications
- Personnel safety
- Alternate water source
- Equipment and spare parts
- Property protection
- Water sampling and monitoring

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INTERNAL CONTACTS

- Contact information should be maintained for all people that may need to respond in an emergency
- List should be reviewed quarterly to keep up-todate
- List should have home and cell number to contact people day or night
- Store back-up file/list at secure off-site location

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EXTERNAL CONTACTS

- Obtain cell phone or 24-hour emergency numbers for all external contacts
- · List should be reviewed quarterly to keep up-to-

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EXTERNAL CONTACTS CONTINUED

- · Local police
- Fire and first responders
- Local Government
 - Mayor, Chamber of commerce
- · Local media
- TV, radio, newspaper
- Utilities
- Electric, natural gas, phone
- Cell phone companies
- Diesel fuel suppliers
- Outside vendors
- Water plant pipes/parts, chemicals, SCADA
- Contractors
- Pump specialist
- Electricians & Plumbers
- Regulatory agencies
- Critical customers Water testing labs

Can you think of other external contacts?

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EXTERNAL CONTACTS CONTINUED

- The TN Department of Homeland Security should be notified of any acts against the water system that may be caused by terrorist
- FBI becomes the lead agency in this case

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EMERGENCY COMMUNICATIONS PLAN

- Communication procedures should be documented
- Alternate communications plans should be included in your EOP in the even that land lines, cell phones or walkie-talkies don't work
- Communicate with cellular companies on the availability of priority channels during an emergency
- Satellite phones should be considered an alternative

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EMERGENCY COMMUNICATIONS

PLAN CONTINUED

Emergency Communications Plan

Template A-25 Example

- Walkie-talkie phones will the be first line of communication in an emergency. If walkie-talkie phones are inoperable, land phones, personal cell phones, and/or 2-way radios should be used to communicate with water system staff and external responders. Office managers will attempt to call phone company/cell phone company to request priority in restoring cell phone signals. (Two trucks and the office currently have three pair of 2-way radios. Two additional pair of 2-way radios are located in the manager's office at the Water System office.) Do not use 2-way radios are located in the manager's diffice at the Water System office.) radio for communications that should not be released to the public.
- If phone and radio communication are inoperable, water system personnel should drive to the Emergency Operations Center (EOC) for emergency communication /assignments. Responders should communicate in person by walking or driving until phone service is restored.
- Contact TEMA immediately for communication /emergency management assistance

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EFFECTIVE COMMUNICATIONS

- · Plan how you will communicate with customers and media before emergencies happen
- Designate a media spokesperson
- If 10% of the population speaks Spanish or another language, additional translated versions of public notifications should be made available

PERSONNEL SAFETY

- The water system should have procedures for securing the safety of utility personnel and the immediate community
- Schedule training sessions on
 - Basic safety procedures
 - Alarm response
 - First aid
 - Personal protection equipment (PPE) usage
 - Evacuation procedures

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ALTERNATE WATER SOURCE

 Identify the sources and procedures for obtaining a short-term and a long-term alternate water supply in the event of an emergency

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PUBLIC NOTICES

- Boil Water Notice
 - No alternate source is required
- Do Not Drink Notice
 - Alternate water source must be provided for drinking and food preparation
- Do Not Use Notice
 - Alternate water source must be provided for drinking, cooking, bathing and even fire fighting (in certain contamination scenarios)

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TANKER TRUCKS

- If tanker trucks are used to transport or store water as an alternate water source, make sure you allow time to disinfect the trucks properly
- See Appendix F for tanker truck disinfection procedures



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EQUIPMENT AND SPARE PARTS

- Identify these that can reduce the impact of an emergency
 - Vehicles
 - Chemicals
 - Tools
 - Spare parts
- Special equipment
- All heavy equipment, portable generators, spare pumps, etc should be listed here

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EMERGENCY EQUIPMENT

- SCBA
- Toxic gas meters
 - · Check and calibrate chlorine alarms and test
- \bullet Chlorine repair kits: A, B and/or C kits
- Plan for chlorine repair parts and supplies
- All PPE for emergency

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PROPERTY PROTECTION

- Establish a procedure for locking down the facility and establishing a secure perimeter to the plant grounds and buildings
- Enter a potential crime scene with caution, if you believe suspects are still present, call 911

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PROPERTY PROTECTION CONTINUED

- The ERC will communicate with local police and emergency response teams to determine if the building should be locked down and site perimeter secured
- Look over the grounds and note any persons or vehicles in the vicinity
- · Look, listen and smell for dangerous signs

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Total Control

PROPERTY PROTECTION CONTINUED

- If you find victims, check out their physical condition, provide comfort and medical attention (if trained)
- Do not clean up, remove items or otherwise disturb the crime scene
- Document any statements/comments made by victims, suspects or witnesses on the scene

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PROPERTY PROTECTION CONTINUED

- After the site is secured and victims are stabilized, begin assessing potential contamination and/or damage to the water system
- Follow the water system's EOP

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WATER SAMPLING & MONITORING

- DWS and approved water lab should be consulted to determine appropriate testing and sampling
- Identify the certified operator or team (and alternates) who is/are responsible for taking samples

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WATER SAMPLING & MONITORING

- Sampling procedures should be outlined for:
- Decision-making process to determine the tests to run
- Location and/or source of test kits and/or sample containers
- When to use preservatives or dechlorinating agents
- Sample quantity to collect
- Proper collection procedures

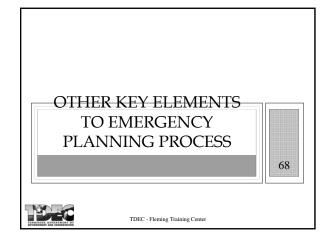
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WATER SAMPLING & MONITORING

- Provide a water sampling plan of your water distribution system
 - Sampling plan is to provide sample protocol and chain of custody
- Laboratory agreements are needed and contacts of outside labs are needed to secure monitoring requirements

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WATER CONSERVATION & DROUGHT MANAGEMENT 69 TDEC - Fleming Training Center

DROUGHT MANAGEMENT

- Public water systems and local communities should plan for conditions of low water supply by having an approved drought management plan in place
- · Local Drought Management Planning Guide for Public Water Suppliers

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DROUGHT MANAGEMENT CONTINUED

- Plan may include, but not limited to the following restrictions
 - Use of water to wash any motor vehicle, motorbike, boat, trailer, or airplane or other
 - Use of water to wash sidewalks, driveways, decks, home siding, gutters, parking lots or other hard-
 - Use of water to irrigate lawns, trees, shrubs, plants and flowers

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DROUGHT MANAGEMENT CONTINUED

- Plan may include, but not limited to the following restrictions (cont.)
- Use of water to fill indoor or outdoor swimming pools or hot-
- Use of water in fountain or pond except where necessary to support aquatic life
- Use of water from a fire hydrant for other than fire fighting purposes

WATER CONSERVATION

- Voluntary water conservation measures should be emphasized
 - Take short showers
 - Fix leaky faucets and running toilets
 - Don't allow water to run while brushing teeth or shaving
 - Collect rainwater for watering plants, gardens and flowers



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THREAT EVALUATION

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THREAT EVALUATION

- All threats should be taken seriously
- Threats may be reported or delivered in many different forms
 - Consumer complaint of water taste or odor
 - Witness account of tampering with water tank
 - Phone call from alleged perpetrator
 - Emergency room reporting patients with symptoms after drinking water

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THREAT IDENTIFICATION CHECKLIST

- Should be kept next to every phone at the office and water treatment plant
- If a threat is received, the checklist should be completed
 - See A-32 Threat Identification Checklist

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THREAT IDENTIFICATION CHECKLIST

- If you receive a suspicious letter or package, set it aside and do not open it
- Calmly instruct everyone to leave the room immediately
- Close the door
- Wash your hands with soap and water
- Notify your supervisor and/or call 911 if a suspicious substance is visible

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FOLLOW-UP EOP ACTIVITIES

- EOP approval and review date
 - Keep log on approvals
- Update every two years
- EOP distribution
- Keep copies numbered for control purposes
- Keep log on who has what copy and where
- Training
 - Minimum training once a year

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TRAINING

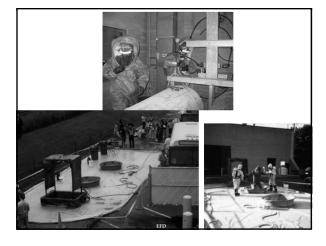
- Orientation or classroom sessions
- Basic instruction on EOP procedures
- Tabletop workshop
 - Fabricated event with actions/verbal responses and close with evaluation
- Functional exercise
 - Team of simulators develops a realistic major event and staff responds to the event
- Full-scale drills
 - More costly

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TRAINING CONTINUED

- Successful implementation of the EOP plan is going to depend on:
 - Training of employees and contacts
 - · Yearly mock trial
 - Rotate personnel on the response teams
 - Annual revisions and updates

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CHLORINE LEAK AT PLANT

- Water plant should have a current evacuation plan for chlorine gas evacuation
- Current plan should evacuate the plant grounds and a minimum ½ mile radius of affected area

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CHLORINE LEAK AT PLANT CONTINUED

- 1. Chlorine alarms go off and start a response
- Phone call made of chlorine gas leak in plant
- Operator makes investigation on site to chlorine room and alarms
- 4. Leak found and starts response

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CHLORINE LEAK AT PLANT CONTINUED

- Incident commander notified and incident command started
- Chlorine alarms acknowledged and evacuation
- Chlorine response and repair team activates to contain the leak; locate and isolate chlorine gas leak if possible

CHLORINE LEAK AT PLANT CONTINUED

- 8. Water Plant evacuated and secured
- Staging Area for incident command and safe zone established
- 10. Notify: 911, Hazmat, Police and Fire Department
- 11. Coordinate neighborhood evacuated with Police and Fire Department

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CHLORINE LEAK AT PLANT CONTINUED

- Response Teams are working to isolate the chlorine leak
- Chlorine repair team finds the leak and repairs the chlorine pressure diaphragm to the chlorine manifold
- 14. Area is checked for air monitor by gas detector for chlorine gas levels

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CHLORINE LEAK AT PLANT CONTINUED

- 15. Two hours into the event, the area is secure
 - Incident commander determines that the water plant is safe to return to normal water plant operations
- 16. Incident command is shut down
- 17. Normal plant operations and chlorine process are monitored for further compliance
- 18. Evacuation is canceled

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REFERENCES

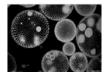
 Emergency Operations Planning Guide, TN DWS along with templates can be found at: http://www.state.tn.us/environment/dws/security/svadocuments.shtml

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Section 7

Algae Identification/ Microscopic Examination
Types of Algae
Significance to Water Supplies
Control Measures Identification with Microscopes

Algae Identification



Algae

 Algae is a diverse group of organisms that range from single celled forms to giant marine kelps.

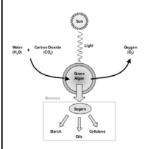


- Algae occupy a wide variety of habitats including fresh and salt waters, moist soils, hot springs, snowfields and even deserts.
- Algae use light energy to convert carbon dioxide and water into simple sugars, which they use to grow new cells. This process is called photosynthesis.



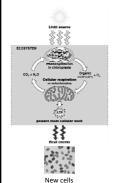
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Photosynthesis



- Plants and algae use light energy from the sun, carbon dioxide and water to produce simple sugars.
- Oxygen is released as a byproduct.

Cellular Respiration



- Algae use the sugars they produce as a food source to grow new cells.
- This process is called cellular respiration. It usually occurs at night when solar energy is not available.
- Oxygen is taken in by the algae and sugars are converted into carbon dioxide water and energy.

Algae's significance to water supplies

- Tastes and odors are caused by the release of certain compounds by both living algae and decomposing algae.
- A massive bloom of algae can cause rapid and severe oxygen depletion, which can lead to fish kills.
- Some algal species produce toxins, which have caused deaths in cattle, horses, and wildlife. There is some evidence that humans can be affected by the toxins as well.

Algae's significance to water supplies



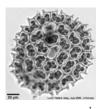
- A variety of algae when abundant in water can rapidly cover the surface of a sand filter. Filter runs are reduced, backwashing must be increased.
- Algae can be an obstruction to water conveyance by plugging screens, and weirs
- Algae can also lead to the formation of disinfection by-products when water containing algae or their metabolites is chlorinated.
- Algae can affect the pH of water in reservoirs. A pH as high as 9.5 during an algal bloom has been observed. The pH can interfere with treatment processes such as coagulation and disinfection.

Algae morphology

• Algae can be single- celled



• Algae can be colonial



Algae morphology

• Algae can be filamentous



• Algae can be membranous



Algae can be tubular



Algae morphology

• Algae can be complex and multi-cellular





Algal Divisions

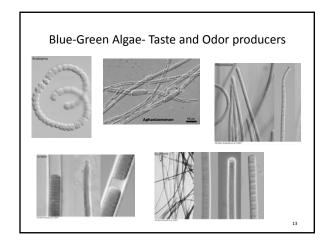
- Chlorophyta- (Green Algae)
- The largest and most diverse group of freshwater algae.
- They can be single celled, filamentous, colonial, membranous or tubular.
- They are common in lakes, ponds, an even in treated water reservoirs.
- They are generally harmless in water supplies.
- Some species can cause taste and odor problems when abundant.
- Filamentous species can form wiry growths and tangled mats.

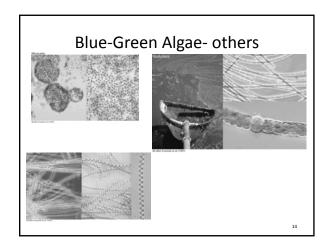
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Green Algae Pandarina Two Views of the Same Colony Wolvex Rhizoclonium Cladophora glomerata

Algal Divisions

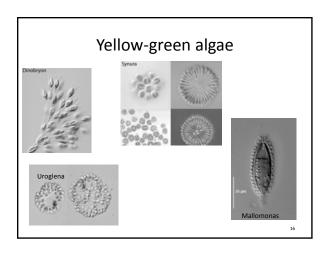
- Cyanophyta- (blue-green algae)
- Bacteria-like organisms
- Can be single celled, filamentous, or colonial.
- Common is all aquatic environments, soils, and extreme environments.
- Many problems in water supplies are attributed to this group including taste and odors, oxygen depletion, toxins, filter clogging and disinfection byproduct formation.

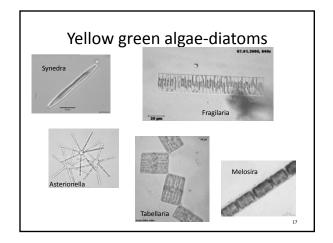


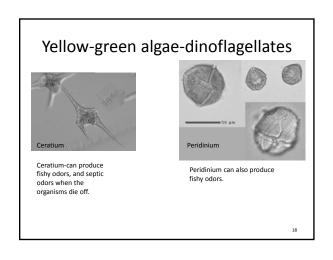


Algal divisions

- Chrysophyta-(yellow-green algae)
- Abundant in lakes and reservoirs.
- Includes the diatoms, and dinoflagellates.
- Significant because they are known to cause tastes and odors.
- Fishy and cucumber odors typically
- Some are known filter cloggers.



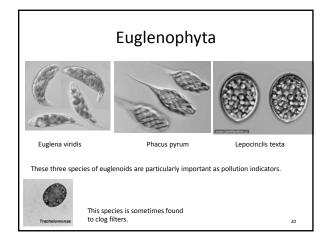




Algal Divisions

- Euglenophyta- euglenoids
- More animal like type of algae.
- Swim by means of flagella.
- Widely distributed in freshwater.
- Especially in bodies of water high in organic matter, such as ponds accessed by livestock.
- Indicators of water pollution due to sewage effluent.
- · One species is known to clog filters

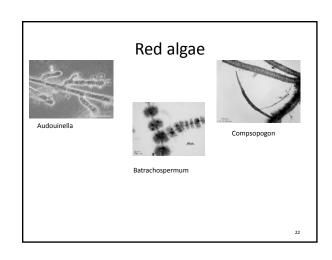
19



Algal Divisions

- Rhodophyta-red algae
- Usually found in cold waters, and rapidly flowing streams.
- Minor constituents of drinking water supplies.
- Three species can grow on reservoir walls.
- May lead to disinfection by-products if contacting chlorine compounds

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Control Strategies

- Copper sulfate has been used for algae control in reservoirs for many years.
- Copper sulfate is usually only applied in shallow areas of reservoirs because it becomes to dilute and less effective in deeper waters.
- When copper sulfate is used it should be accompanied by a monitoring program to determine effectiveness and to minimize chemical usage.
- Excessive amounts of copper can build up in sediments and become toxic to wildlife, beneficial plants and organisms.

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Control strategies

- Another new way to treat algae growth is by restricting light.
- Basins and clarifiers can be enclosed or covered to prevent growth of algae.
- Shade balls are being used in some reservoirs to prevent light penetration, thereby preventing the growth of algae.

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Shade balls- California Ivanhoe Reservoir





A total of 3 million plastic balls were poured into Ivanhoe Reservoir in Silver Lake, California in 2008.

Each ball cost approximately 34 cents and are expected to last for 5 years.

The reservoir needed to be covered to prevent the formation of disinfection byproducts resulting from algae compounds contacting chlorine.

2

Control strategies

- Other compounds can be fed to kill algae.
- Chlorine- used to be the oxidant of choice, but prechlorination had led to more disinfection byproduct formation.
- Permanganate- both sodium and potassium permanganate are useful in treating algae.
- Hydrogen peroxide- is sometimes used to treat algae in reservoirs

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Microscopic Examination

- Parts of a microscope
- Eyepiece Lens: the lens at the top that you look through. They are usually 10X or 15X power.
- Arm: Supports the tube and connects it to the base
- Base: The bottom of the microscope, used for support.
- Always carry the microscope with two hands supporting the arm and the base.
- Never hold it by the eyepiece!



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Microscopic Examination

- Light source: A steady light source (110 volts) .
- Stage: The flat platform where you place your slides. Stage clips hold the slides in place. If your microscope has a mechanical stage, you will be able to move the slide around by turning two knobs.
- Coaxial stage controls one moves it left and right, the other moves it up and down.
- Revolving Nosepiece: This is the part that holds two or more objective lenses and can be rotated to easily change power.



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Microscopic Examination

- Objective Lenses: Usually you will find 3 or 4 objective lenses on a microscope. They almost always consist of 4X, 10X, 40X and 100X
- Diaphragm or Iris lever: This diaphragm has different sized holes and is used to vary the intensity and size of the cone of light that is projected upward into the slide.
- Coarse focus knobs: The larger of two sets of knobs located on either side of the arm. This adjustment is used to make large adjustments in focusing by moving the lenses up and down. Never use this adjustment when using the 40X objective.
- opjective.

 Fine focus knobs: The smaller of two sets of knobs located on either side of the arm. This adjustment is used to make small adjustments in focusing. It has a limited amount of movement and is most efficiently used after focusing with the 4X objective and coarse focus.



Care and Handling of Microscopes

- A microscope is a **delicate** piece of equipment and should be treated with
- Use ${\bf two\ hands}$ when carrying the microscope. Place one hand around the arm of the microscope and the other under the base for support.
- Carry the microscope upright and close to the body.
- Place the microscope **flat on the table**, but not too near the edge where it might be knocked off.
- DO NOT slide the microscope back and forth on the lab table.
- If it becomes necessary to clean the lenses on the microscope, ask your instructor for a piece of **lens paper**. Other materials, such as paper towel, can scratch the surface of the lens.

Care and Handling of Microscopes

- Throw used slides in the glass disposal container

When storing the microscopes:

- Always rotate the nosepiece so that the LOW POWER objective lens is in line with the eyepiece.
- Wrap the power cord around the base.
- Place the dust cover on top of the microscope.
- Return the microscope to storage.

Viewing Specimens



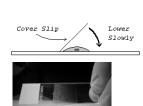
- · Collect a sample (10-50 ml) of raw water or water from areas where you suspect algae might be a problem.
- Prepare a wet mount slide and attempt to identify organisms.
- **Standard Methods for the Examination of Water and** Wastewater contains color plates illustrating several species of problem algae.

Making a wet-mount slide

- Place a clean slide on the lab table. **Handle slides at the ends**, not the center, to avoid getting fingerprints in the viewing area of the slide.
- Add specimen to the slide.
 - For liquid samples, place one small drop in the center of the slide.
 - For solid samples, place the sample in the center of the slide and add one drop of water or stain.
- Hold the coverslip by the edges to avoid fingerprints. Set one edge against the slide and lower it until it contacts the liquid. The liquid should spread across the whole area of the coverslip.
- **Never view a slide without a coverslip.** The coverslip protects the objective lens from the liquid on the slide.

Making a Wet-Mount Slide





Viewing Specimens

- Because the microscope uses lenses and mirrors, the image you see through most light microscopes will be upside down and backward.
- In most instances, light must pass through any object to be viewed with a light microscope. For this reason, the object must be **fairly thin**. Thick objects must be sliced into thin sections for viewing.



On the stage

Through the lens

Viewing Specimens

- Plug in the microscope and turn the power on.
- Place the slide on the stage so that the area of the slide containing the specimen is over the opening.
- Always start with the low power lens (4X).
- Look through the eyepiece, use the course adjustment knob to focus on the object.
- Use coaxial stage controls to view all areas of the slide for organisms.
- Next change the objective to medium power (10X). The object will almost be in focus.
- Use the coarse adjustment knob slowly to focus.

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Viewing specimens

- To see more details of the organisms on the slide you can change to objective to high power (40X).
- You should only have to use the fine focus in this objective.
- Do not use the coarse adjustment or you could crack the lens.

Worksheet for Microscopic Examination Algae Identification

| Date: | - | |
|------------------|---|-------------|
| Sample Location: | | |
| Temperature: | | |

| Algae Group | Slide 1 | Slide 2 | Total |
|---------------------------------|---------|---------|-------|
| Chlorophyta-green algae | | | |
| Cyanobacteria- blue-green algae | | | |
| Chrysophyta | | | |
| Chrysophyta-diatoms | | | |
| Chrysophyta-dinoflagellates | | | |
| Rhodophyta | | | |
| Euglena | | | |
| | | | |

| Species Identified | Significance to drinking water |
|--------------------|--------------------------------|
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Section 8

Safety
General Safety
Personal Protective Equipment
Chlorine Safety





General Duty Clause

- FEDERAL 29 CFR 1903.1
- EMPLOYERS MUST: Furnish a place of employment free of recognized hazards that are causing or are likely to cause death or serious physical harm to employees. Employers must comply with occupational safety and health standards promulgated under the Williams-Steiger Occupational Safety and Health Act of 1970.

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USHA ■Occur

- Occupational
- Safety
- ■Health
- Administration



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General Safety Procedures

- Preliminary checks
 - Unsafe circumstances or unusual conditions
 - Equipment check
 - ✓ Unusual noise in machinery
 - √ Fumes or odd odors



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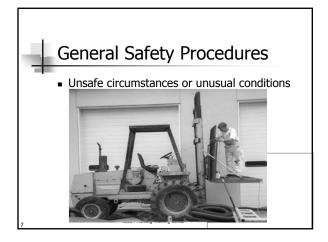


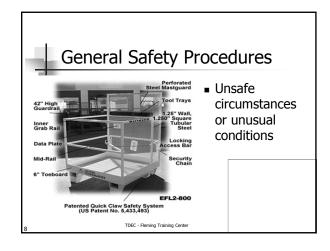
General Safety Procedures

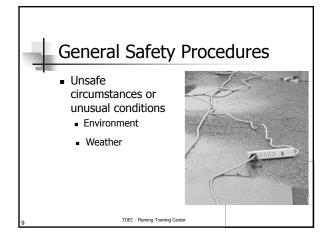
- Unsafe circumstances or unusual conditions
- ■29 CFR 1910.23(c)(1)

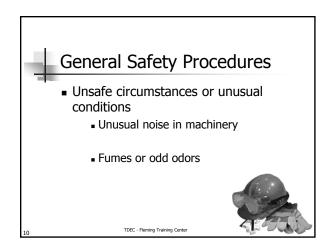
Every open-sided floor or platform 4 feet or more above adjacent floor or ground level shall be quarded by standard railing on all sides except where there is entrance to a ramp, stairway, or fixed ladder.

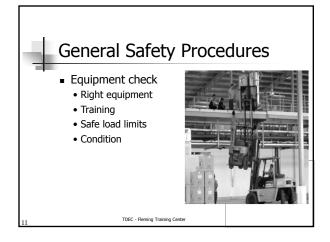
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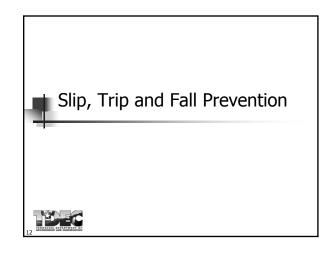










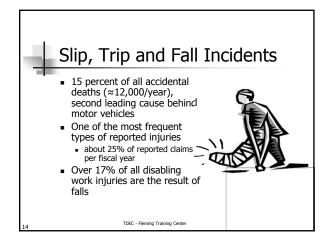


Leading Cause of Industry Accidents

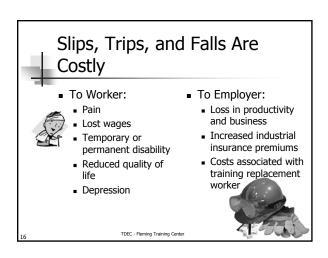
- For the past three years, slips, trips, and falls have been responsible for the majority of reportable accidents in the workplace.
- Approximately three workers are fatally injured every work day in the U.S.
- Over 300,000 fall injuries reported annually

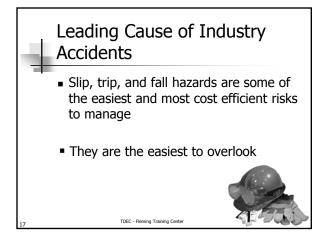


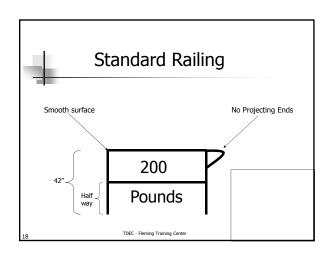
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Causes of Slips, Trips, and Falls

- Poor housekeeping (water, oil, trash)
- Openings in travel ways
- Improper guardrails and handrails
- Failure to use or improper use of PPE
- Wet and slippery surfaces
- Failure to use fall protection



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Causes of Slips, Trips, and Falls

Bucket man & Idiot boy



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Slips

- Occur when there is little or not enough friction or traction between footwear and walking/working surfaces
- According to OSHA, coefficient of friction shall be more than 0.5
 - Coefficient of friction is a measure of slip resistance

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Causes of Slips

- Some common causes of slips include the following:
 - "wet" contamination/spills on smooth floors or surfaces: water, fluids, mud, grease, oil, food, etc.
 - "dry" contamination making surfaces slippery: dusts, powders, granules, wood, lint, plastic wrapping, etc.

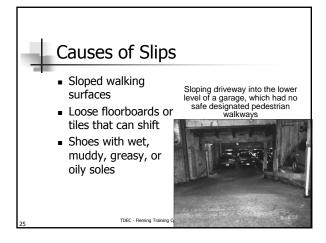
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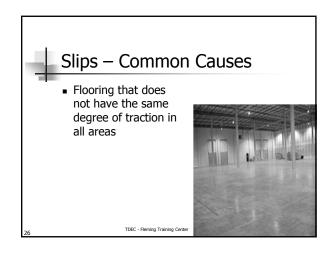


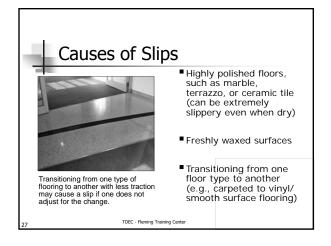
Water on floor of PVC pipe manufacturing plant

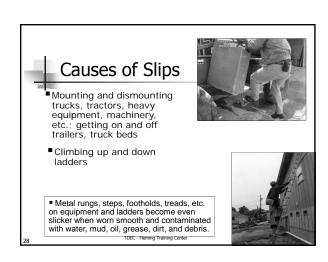


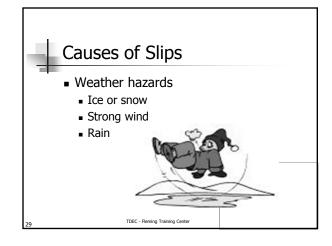


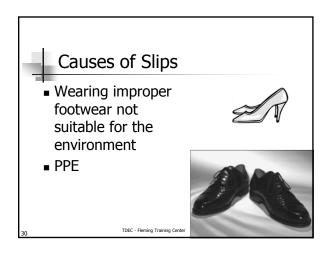


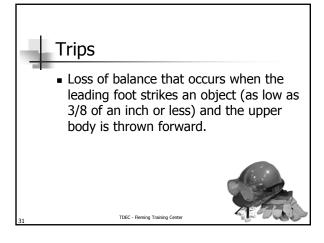




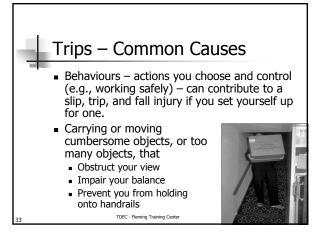


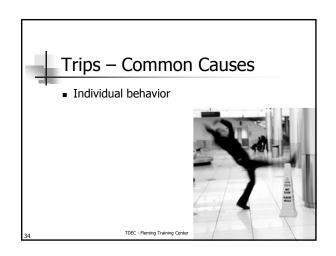


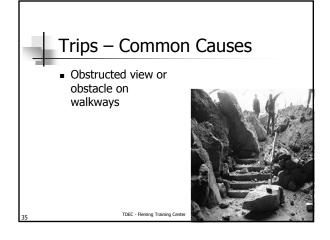


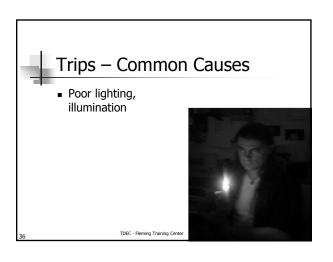








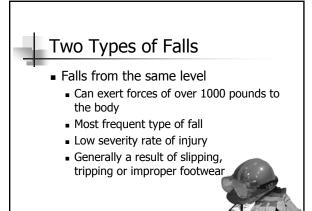


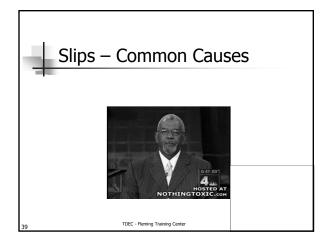




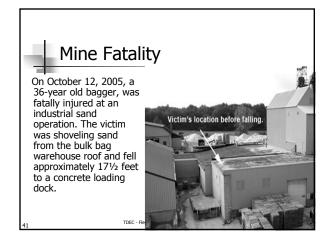
- Falls are usually in conjunction with a slip or trip
- One quarter of all disabling injuries are a result of falling
 - Eight percent are falls from the same level
 - Seventeen percent are falls from the next level

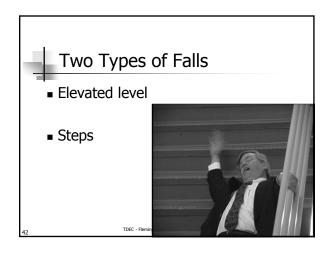
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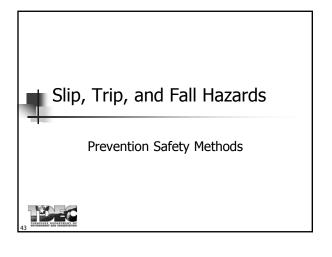


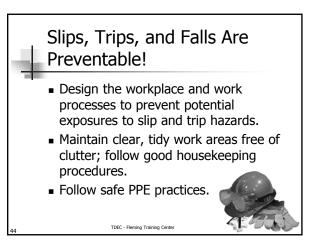






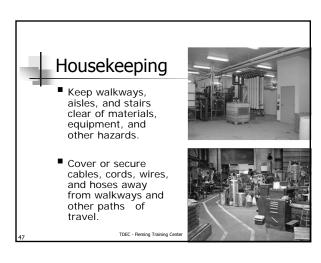


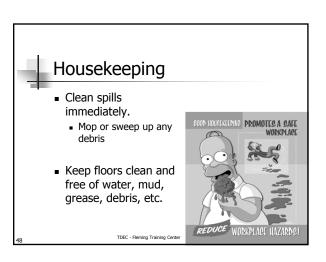














Proper PPE

- Proper PPE can help prevent or reduce the risk of a slip, trip, and fall incident.
- Right PPE for the right job
- Wear slip-resistant shoes/boots with good tread.
- Inspect regularly for any damage



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Safe Walking Practices

- Pay attention to your surroundings.
- Walk, don't run or rush.
- Give yourself enough time.
- Do not engage in activities that distract your attention. Do not read, write, or work while you are walking.
- Use the handrails when climbing or descending the stairs. Do not rush and skip steps.





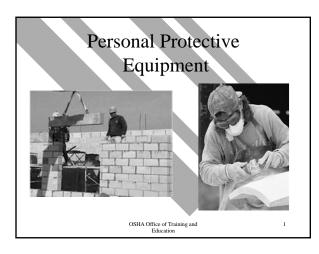


Safe Walking Practices

- Walk carefully and slowly when you transition from one type of walking surface to another.
 - Adjust your walking (pace, stride).
- Take extra care when you come indoors with wet shoes or boots.
- Slow down and take small careful steps if the surface is uneven, cluttered, slippery or at an angle.
- Wear stable shoes with non-slip soles.



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Protecting Employees from Workplace Hazards

- Employers must protect employees from hazards such as falling objects, harmful substances, and noise exposures that can cause injury
- Employers must:
 - Use all feasible engineering and work practice controls to eliminate and reduce hazards
 - Use personal protective equipment (PPE) if the controls don't eliminate the hazards.
- PPE is the <u>last</u> level of control!

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Engineering Controls

If 🔻

The work environment can be physically changed to prevent employee exposure to the potential hazard,

Then . . .

The hazard can be eliminated with an engineering control

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Engineering Controls

Examples . . .

- Initial design specifications
- Substitute less harmful material
- Change process
- Enclose process
- Isolate process

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Work Practice Controls

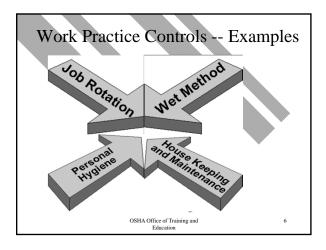
If . .

Employees can change the way they do their jobs and the exposure to the potential hazard is removed,

Then . . .

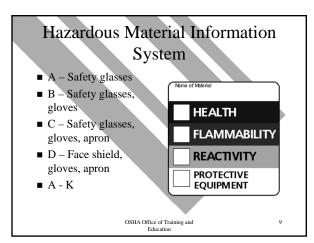
The hazard can be eliminated with a work practice control

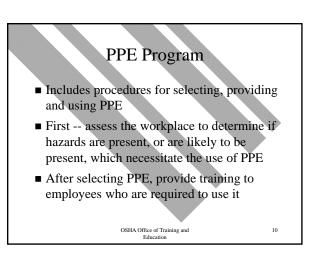
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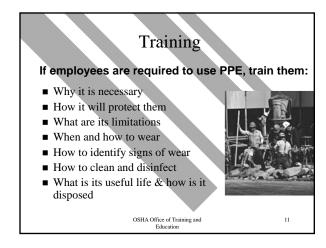


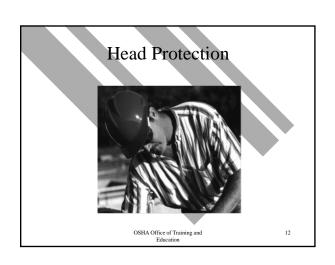
Responsibilities - Employer - Assess workplace for hazards - Provide PPE - Determine when to use - Provide PPE training for employees and instruction in proper use - Employee - Use PPE in accordance with training received and other instructions - Inspect daily and maintain in a clean and reliable condition

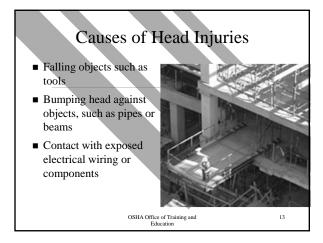
Examples of PPE Body Part Protection Eye safety glasses, goggles Face face shields Head hard hats Feet safety shoes Hands and arms gloves Bodies vests Hearing earplugs, earmuffs











Selecting the Right Hard Hat

Class A

- General service (building construction, shipbuilding, lumbering)
- Good impact protection but limited voltage protection

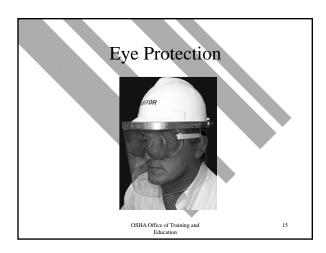
Class B

- Electrical / Utility work
- Protects against falling objects and high-voltage shock and burns

Class C

- Designed for comfort, offers limited protection
- Protects against bumps from fixed objects, but does not protect against falling objects or electrical shock

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When must Eye Protection be Provided?

When any of these hazards are present:

- Dust and other flying particles, such as metal shavings or sawdust
- Corrosive gases, vapors, and liquids
- Molten metal that may splash
- Potentially infectious materials such as blood or hazardous liquid chemicals that may splash
- Intense light from welding and lasers

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Eye Protection

Criteria for Selection

- Protects against specific hazard(s)
- Comfortable to wear
- Does not restrict vision or movement
- Durable and easy to clean and disinfect
- Does not interfere with the function of other required PPE

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Eye Protection for Employees Who Wear Eyeglasses

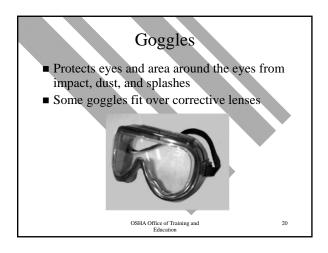
Ordinary glasses do not provide the required protection

Proper choices include:

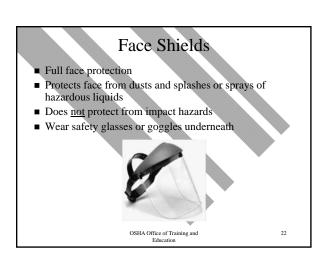
- Prescription glasses with side shields and protective longer
- Goggles that fit comfortably over corrective glasses without disturbing the glasses
- Goggles that incorporate corrective lenses mounted behind protective lenses

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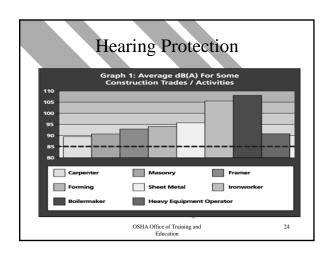




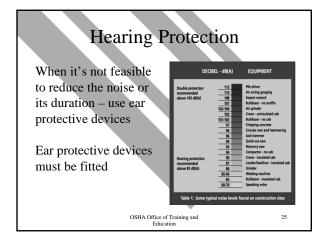








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When Must Hearing Protection be Provided?

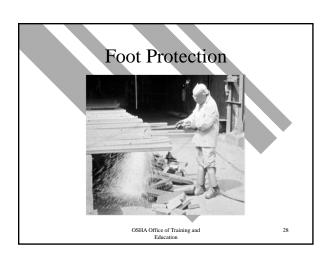
After implementing engineering and work practice controls

When an employee's noise exposure exceeds an 8-hour time-weighted average (TWA) sound level of 90 dBA

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When Must Foot Protection be Provided?

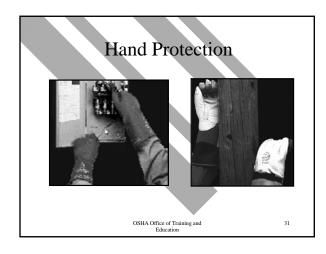
When any of these are present:

- Heavy objects such as barrels or tools that might roll onto or fall on employees' feet
- Sharp objects such as nails or spikes that might pierce ordinary shoes
- Molten metal that might splash on feet
- Hot or wet surfaces
- Slippery surfaces

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Safety Shoes

- Impact-resistant toes and heatresistant soles protect against hot surfaces common in roofing and paving
- Some have metal insoles to protect against puncture wounds
- May be electrically conductive for use in explosive atmospheres, or nonconductive to protect from workplace electrical hazards
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When Must Hand Protection be Provided?

When any of these are present:

- Bruises
- Abrasions
- Cuts
- Punctures
- Fractures
- Amputations
- Chemical Exposures

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What Kinds of Protective Gloves are Available?

- Durable gloves made of metal mesh, leather, or canvas
 - Protects from cuts, burns, heat
- Fabric and coated fabric gloves
 - Protects from dirt and abrasion
- Chemical and liquid resistant gloves
 - Protects from burns, irritation, and dermatitis
- Rubber gloves
 - Protects from cuts, lacerations, and abrasions

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Types of Rubber Gloves

Nitrile protects against solvents, harsh chemicals, fats and petroleum products and also provides excellent resistance to cuts and abrasions.



Butyl provides the highest permeation resistance to gas or water vapors

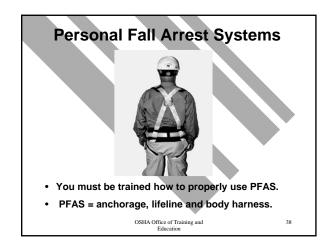


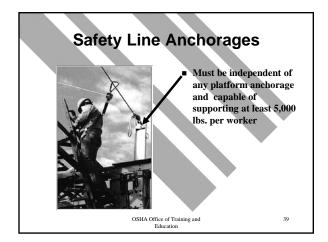
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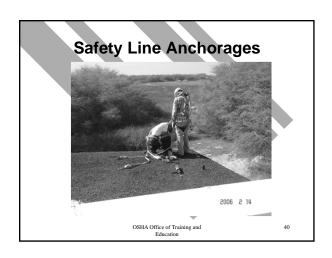
Other Types of Gloves Kevlar protects against cuts, slashes, and abrasion Stainless steel mesh protects against cuts and lacerations OSHA Office of Training and Education

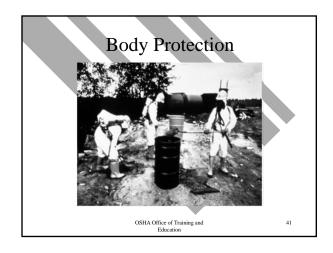


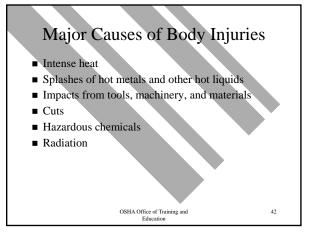


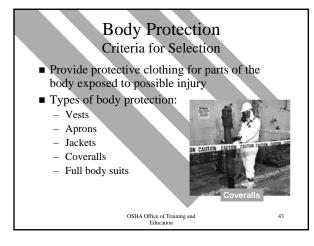


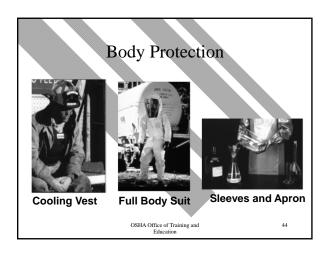












Summary

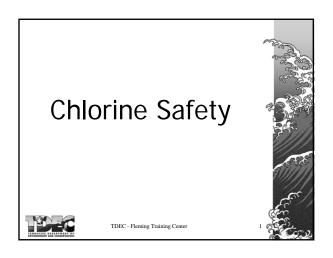
Employers must implement a PPE program where they:

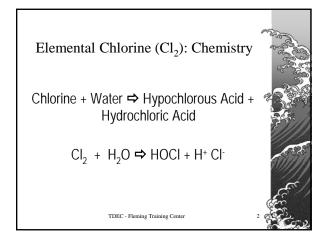
- Assess the workplace for hazards
- Use engineering and work practice controls to eliminate or reduce hazards before using PPE
- Select appropriate PPE to protect employees from hazards that cannot be eliminated
- Inform employees why the PPE is necessary, how and when it must be worn
- Train employees how to use and care for their PPE, including how to recognize deterioration and failure
- Require employees to wear selected PPE

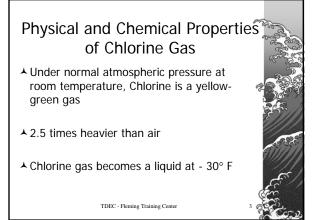
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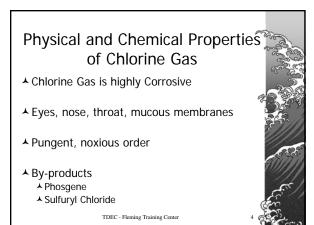
Safety

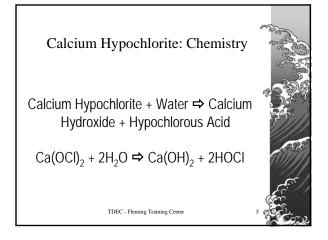
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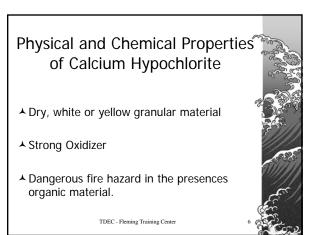


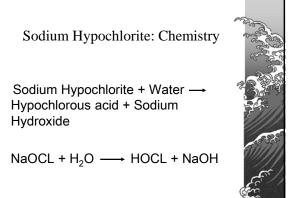




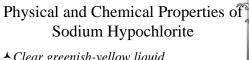






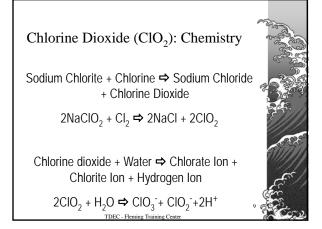


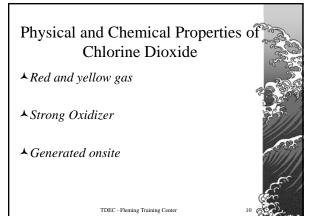
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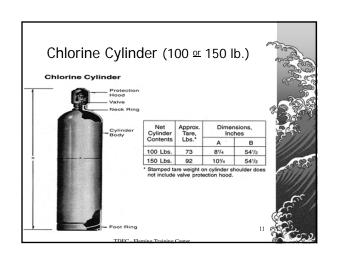


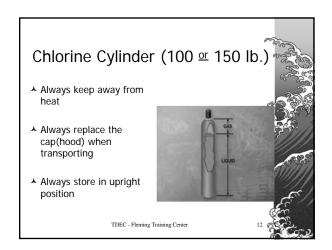
- ▲ Clear greenish-yellow liquid
- ▲ Strong Oxidizer
- **▲** Corrosive
- **▲** 15-5% chlorine

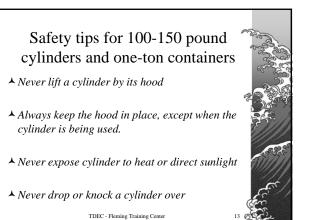
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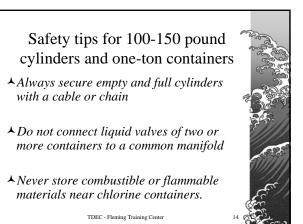


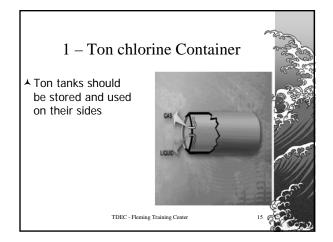


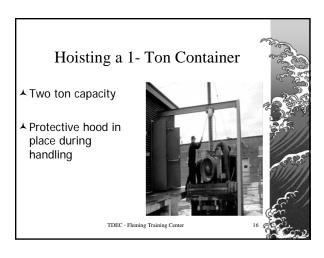


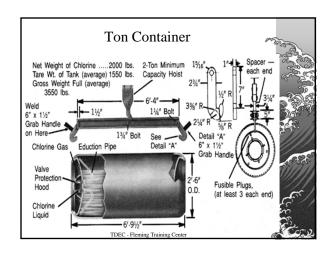


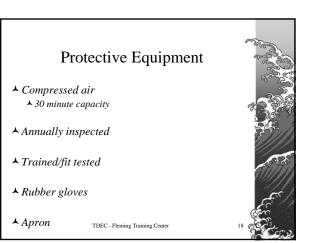












Protective Equipment

- **▲** Goggles
- ▲ Eye-wash station
- **▲** Deluge shower
- **▲** Water-holding tank

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Rules and Regulations

▲ From Community Public Water Systems Design Criteria Division of Water Supply Tennessee Department of Environment and Conservation, 2008



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Separate Chlorine Room

- 5.3.4 Chlorine gas feed and storage shall be:
 - a. enclosed and separated from other operating areas in order to prevent injury to personnel and damage to equipment.
 - b. provided with an inspection window to permit viewing of the interior of the room and the equipment.
 - c. Provided with doors opening outward with a crash bar, assuring ready means of exit.

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Separate Chlorine Room

- 5.3.5 Where Chlorine gas is used, ventilation for each room shall be provided for one complete air change per minute; and
 - a. The air outlet from the room shall be near the floor and the point of discharge shall be so located as not to contaminate air inlets to any rooms or structures, or adversely affect the surrounding environment.
 - b. Air inlets shall be through louvers near the ceiling, and temperature controlled to prevent adverse affect on chlorinator.

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Separate Chlorine Room

- 5.3.5 (cont.)
 - c. Switches for fans and lights shall be outside of the room, at the entrance.
 - d. Vents from feeders and storage shall discharge t the outside atmosphere, above grade.
- 5.3.6 Chlorinator rooms should be heated to 60° F, but should be protected from excess heat; cylinders and gas lines should be protected from temperatures above that of the feed equipment.

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Separate Chlorine Room

5.3.7 gaseous feed chlorine installations shall be equipped with a gas detection device connected to an audible alarm to prevent undetected, potentially dangerous leakage of chlorine gas.



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Operator Safety

5.4 Operator Safety

e. All gaseous feed chlorine installations shall be equipped with appropriate leak repair kits.





Chlorine First Aid

▲ Inhalation

- ▲ Remove victim from contaminated area
- ▲ Keep victim in a reclining position with head and shoulders elevated
- ▲ Administer oxygen as soon as possible

▲ Skin Contact

- ▲ Shower victim, removing all contaminated clothing.
- ▲ Wash affected area with soap and water

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Chlorine First Aid

▲Eye Contact

- ▲ *Irrigate eyes with water for 15 minutes*
- ▲ Irrigate a second 15- minute period if a physician is not immediately available

▲ Health Effects

- Low concentrations: Burning eyes, nose, and throat; coughing, redness in the face
- ► High concentrations: Tightness in the throat and difficulty breathing

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Chlorine First Aid

- ▲ Health Effects
 - ▲1,000 parts per million (ppm) is fatal after a few breaths.
 - ▲Even an hour later, 35-51 ppm can be fatal.

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Emergency Numbers

- *▲ Make a list of relevant contact numbers:*
 - ▲Fire Department
 - ▲ Police Department
 - ▲ County Emergency Management Office
 - $begin{array}{l} begin{array}{l} beg$

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A look at Chlorine Equipment TDEC - Fleming Training Center 30

