

# Introduction to Environmental Engineering

Water Treatment

# **Unit Processes in Water Treatment**

- **Surface Water Treatment**
  - 1. Chemical Mixing (Rapid Mixing)**
  - 2. Flocculation**
  - 3. Sedimentation**
  - 4. Rapid Sand Filter**
  - 5. Disinfection**
  - 6. Flouridation**
  - 7. Pumped to community**

# Unit Processes

- Groundwater Treatment
  1. Aeration (if necessary to release any gases)
  2. Disinfection
  3. Fluoridation
  4. Pumped to community

# Coagulation & Flocculation

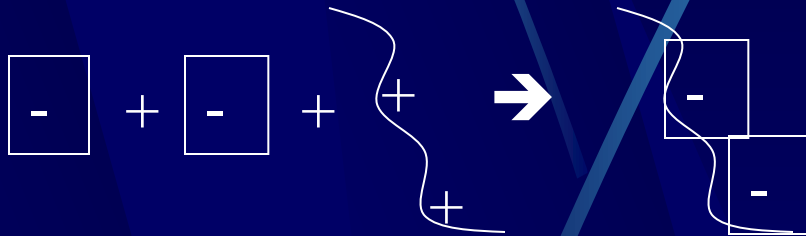
# Coagulation & Flocculation

- Coagulation

- the chemical alteration of the colloidal particles to make them stick together
- Hydrophilic particles – water loving – absorbs to water
- Hydrophobic particles – water hating – does not absorb to water
  - Hydrophobic particles are negatively charged and don't like to aggregate and are hydrophobic
  - A positively charge coagulant destabilizes the negatively charged particles and brings them together.
- Coagulants lower the negative repulsion force of colloids

# Coagulation & Flocculation

- Effect of coagulants
  - Bridging



# Coagulation & Flocculation

- **Rapid Mixing - 20 to 60 seconds**
- **Flocculation Gentle mixing 20-60 minutes to aggregate the particles**
- **Coagulants**
  - Aluminum sulfate (alum) – corrosive alone, packaged in water
  - Ferrous sulfate (ferric)
  - Ferric chloride

# Coagulation & Flocculation

- **Coagulant aids**
  - **Polyelectrolytes – long chain SOC to assist floc formation**
  - **Lime alkalinity addition – for  $\text{Al}(\text{OH})_3$  formation**
  - **pH correction: lime, sulfuric acid – for optimum floc formation**



# Coagulation & Flocculation

## ● Example

- Traditional Surface water treatment plant
  - Suspended solids = 500 mg/L
  - $Q = 36,400 \text{ m}^3/\text{day}$
  - Alum dose = 50 mg/L
  - 98% of Total Solids are removed by the plant.
  - Compute solids produced from plant daily.

# Coagulation & Flocculation

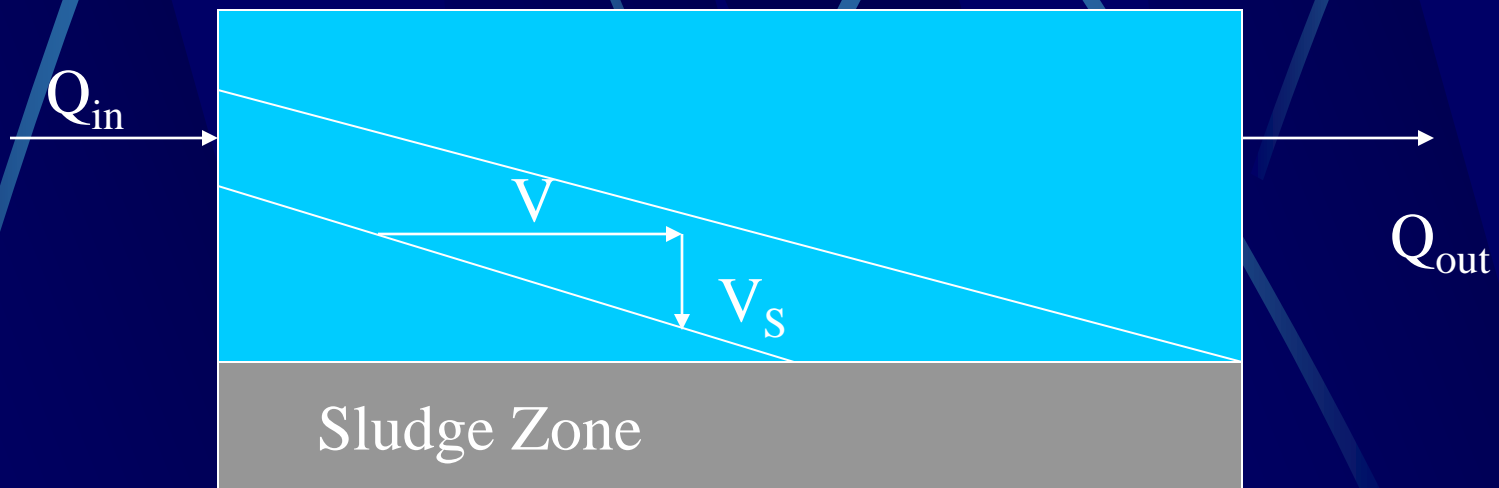
- $0.98 \times 500 \text{ mg/L} \times 36,400 \text{ m}^3/\text{day} \times 1000 \text{ L/m}^3 \times 1\text{g}/1000\text{mg} \times 1\text{day}/86,400\text{s} =$ 
  - 206 g/s suspended solids
- Aluminum Hydroxide produced
- $\text{Al}_2(\text{SO}_4)_3 \cdot 14\text{H}_2\text{O} + ? \rightarrow 2\text{Al}(\text{OH})_3 + ? + ?$ 
  - MW = 594 g/mol                      MW = 156 g/mol
- Ratio of  $2\text{Al}(\text{OH})_3 : \text{Al}_2(\text{SO}_4)_3 \cdot 14\text{H}_2\text{O} = 0.26$ 
  - $50 \text{ mg/L} \times 36,400 \text{ m}^3/\text{day} \times 1000 \text{ L/m}^3 \times 1\text{g}/1000\text{mg} \times 1\text{day}/86,400\text{s} = 21 \text{ g/s}$
  - $21 \text{ g/s} \times 0.26 = 5.5 \text{ g/s}$
  - Total Sludge =  $206 \text{ g/s} + 5.5 \text{ g/s} = 211.5 \text{ g/s}$

Note: Design of rapid mixers and flocculation basins are dependent on detention time.

# Settling

- When flocs have been formed they have to be separated from the water.
- Gravity Settling Tanks
  - All sedimentation tanks are modeled as plug flow reactors.
  - Rectangular or Circular design.
  - Their design is determined by the  $V_s$  of the particle size to be removed.
  - $\theta = H/V_s = L/V$
  - $V_s$  = Stokes velocity
  - $H$  = tank height – sludge depth
  - $L$  = tank length
  - $V$  = horizontal velocity

# Settling



# Settling

- PFR,  $L \geq 2W$ ,  $L \gg H$
- Surface Overflow Rate =  $V_s = Q/A_p = Q/LW$
- Weir overflow rate =  $Q/WH$ 
  - Therefore, the settling velocity is the major design parameter
- Surface Overflow rates  $\approx 20\text{-}35 \text{ m}^3/\text{day}/\text{m}^2$
- Detention times  $\approx 2\text{-}8 \text{ hr}$
- Weir overflow rate  $\approx 150\text{-}300 \text{ m}^3/\text{day}/\text{m}^2$

# Settling

- Example

- **Small Water treatment plant with:**
  - $Q = 0.6 \text{ m}^3/\text{s}$  inflow of the plant
  - $V_s = 0.004 \text{ m/s}$  (not a good assumption)
  - Effective settling zone,  $L = 20\text{m}$ ,  $H = 3\text{m}$ ,  $W = 6\text{m}$
  - Can 100% removal be expected?
- **Surface Overflow rate, is the critical settling velocity**
  - $V_s = Q/A_p = Q/LW = 0.6 \text{ m}^3/\text{s} / (20\text{m})(6\text{m}) = 0.005 \text{ m/s}$
- **$0.005 > 0.004 \text{ m/s}$ , removal not expected**

# Settling

- Can also be solved realizing settling is a problem of triangles:
- $V = \text{horizontal velocity} = \text{Weir Overflow rate} = Q/WH = 0.6\text{m}^3/\text{s} / (6\text{m})(3\text{m})$
- $= 0.033 \text{ m/s}$
- $V_s/V = H/L'$
- $0.004\text{m/s}/0.033\text{m/s} = 3\text{m}/L' \quad L' = 25 \text{ m},$   
thus particles would need 25 m to be totally removed.

# Filtration

- **Two types of Filtration**
  - **Slow Sand Filtration = 0.1 to 0.2 m/h**
  - **Rapid Sand Filtration (Rapid Gravity Filtration) = 5-20 m/h**
- **In the 1930's switch to RSF from SSF, (higher loading, less space, lower construction costs)**
- **However, SSF resurgence due to its removal of smaller particles.**



# Filtration

- Slow Sand Filter
  - Schmutzdecke – scrape off, bio growth
  - Filter runs last 3 – 6 months
  - Top of filter doing most of the work
- Rapid Sand Filter
  - Backwashing – filter runs, hours to 2 days
  - The entire filter is removing
  - Multi-media – activated carbon, garnet, sand

# Disinfection

- All of the previous treatment processes remove > 90% of bacteria and viruses
- A disinfectant is used to:
  - Kill microbes fast and efficiently
  - Not kill humans or other animals
  - Last long enough to prevent regrowth in distributions systems
- Factors that inhibit disinfection:
  - Turbidity: particles shelter bacteria
  - Resistant organisms
  - NOM: form THM wit chlorine
  - $\text{Fe}^{+2}$  and  $\text{Mn}^{+2}$ : form particles that shield bacteria

# Disinfection

- **Oxidizable compounds: become food for microbes in distribution system**
- **Commonly used disinfectants:**
  - Chlorine
  - Chlorine Dioxide
  - Chloramines
  - Ozone
  - UV light