# Performance Evaluation of the Hydrotech Belt Filter in Intensive Recirculating Aquaculture Systems

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#### Introduction

### Problem: TSS in Aquaculture Discharged Effluent

- EPA: Best Management Practices (BMP)
- NPDES permits: state or regional NPDES permits
- Concentration of suspended solids
- Reduce quantity of discharge water
- Minimize storage volume

# Hydrotech Belt Filter (Water Management Technologies)

Belt Filter System, Hydrotech Model HBF537-1H



Influent: 600 - 1400 mg/L

Effluent: 15% Solids





# Objectives

- Summary of the current waste treatment systems
- Coagulation/Flocculation
- Performance evaluation of Hydrotech Belt filter

# Freshwater Institute Intensive Recirculating Aquaculture Production Systems

- Partial-Reuse Fingerling System
- Recirculating Growout System





# Partial-Reuse Fingerling System

#### Partial-reuse system:

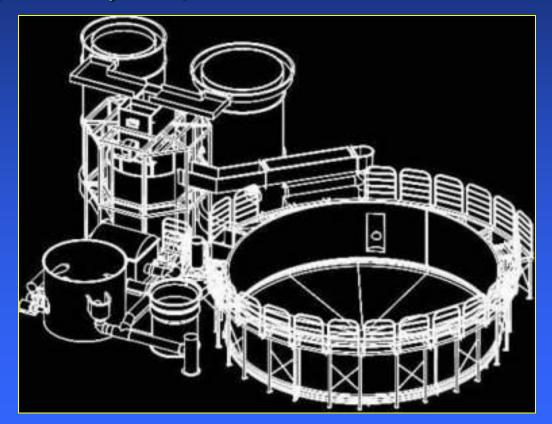
- NH<sub>3</sub>-N controlled by pH
- pH controlled by CO<sub>2</sub>
- 1500 lpm recirc
- bottom drain flow is discharged from system
- 12-15% of water flow
- sidewall flow is reused after microscreen filtration
- 45-50 kg feed/day



# Recirculating Growout System

#### Fully-recirculating system

- 4 8% make-up rate on a flow basis (0.5-1.0 day HRT)
- 4,800 lpm recir. water flow
- 150 m<sup>3</sup> culture volume
- 7% through bottom drain
- 93% through side drain
- 200 kg/day feed



# Current Aquaculture Waste Management





Polishing Microscreen Filter Model RFM 4848, Manufacturing, Ltd.

Backwash Water Sump

# Current Aquaculture Waste Management



# Current Aquaculture Waste Management

#### **Pumping Settling Cones**





**Land Application / Composting** 



Aerobic Lagoon

BOD In: 6 mg/L BOD out 2 mg/L

# Waste Management – Discharge Parameters

Parameter	Mean		
pH Temp Alkalinity Turbidity		7.43 19.4 292 Over range	
TP RP	(mg/L - P) (mg/L - P)	77.8 12.3	
	(mg/L) (mg/L)	1015 753	
TN TAN NO <sub>2</sub> NO <sub>3</sub>	(mg/L - N) (mg/L - N)	77.8 14.8 0.43 38.8	
cBOD <sub>5</sub>	(mg/L)	548	





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### Coagulation/Flocculation

#### Coagulation

Process of decreasing or neutralizing the electric charge on suspended particles

#### **Flocculation**

Process of bringing together the microfloc particles to form large agglomerations by the binding action of flocculants

### Suspended Solids Removal

Alum in wastewater yields the following reaction:

$$Al_2(SO_4)_3 - 14 H_2O + 3Ca(HCO_3)_2 \Leftrightarrow 3Ca SO_4 + 2Al(OH)_3 + 6CO_2 + 14H_2O$$

Insoluble aluminum hydroxide is a gelatinous floc

Ferric Chloride in wastewater yield the following reaction:

$$2\text{FeCl}_3 \bullet 6\text{H}_2\text{O} + 3\text{Ca}(\text{HCO}_3)_2 \Leftrightarrow 3\text{CaCl}_2 + 2\text{Fe}(\text{OH})_3 + 6\text{CO}_2 + 12\text{H}_2\text{O}$$

Insoluble ferric hydroxide is a gelatinous floc

# Phosphorus Removal

#### Basic reaction:

$$Al^{+3} + H_nPO_4^{3-n} \Leftrightarrow AlPO_4 + nH^+$$

$$Fe^{+3} + H_nPO_4^{3-n} \Leftrightarrow FePO_4 + nH^+$$

Simplest form of reaction, bench-scale test required to establish actual removal rate

# Coagulation/Flocculation Aids

#### Advantages:

#### High Molecular Weight Long-chain Polymers

- lower dosages requirements
- reduced sludge production
- easier storage and mixing
- MW and charge densities optimized "designer" aids
- no pH adjustment required
- polymers bridge many smaller particles
- improved floc resistance to shear forces

# Polymers

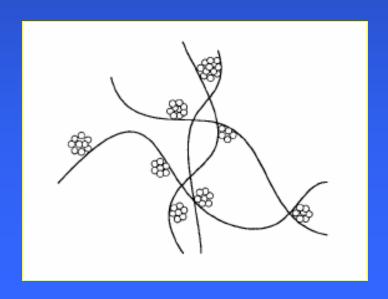
#### Process Efficiency depends on:

- polymer concentration
- polymer charge (anionic, cationic, and nonionic)
- polymer molecular weight and charge density
- raw wastewater characteristics (particle size, concentration, temperature, hardness, pH)
- physical parameters of the process (dosage, mixing energy, flocculation energy, duration)
- discharge water treatment levels required

# How Polymers Work

• charge neutralization (low molecular weight polymers) neutralize negative charge on particle

bridging between particles (high molecular weight polymers)
 long loops and tail connect particles



# Polymer Evaluation

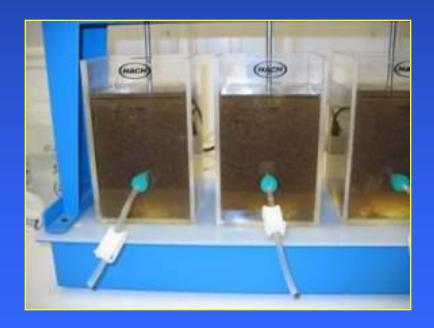
#### Similitude Studies with Jar Tests

- Jar Tests of coagulant and flocculant aids
  - Effect of mixing speed, (velocity gradient)
  - Effect of flocculation speed
  - Effect of coagulant type and dosage
  - Effect of flocculant (polymer) type and dosage

### Jar Tests

#### Water Quality

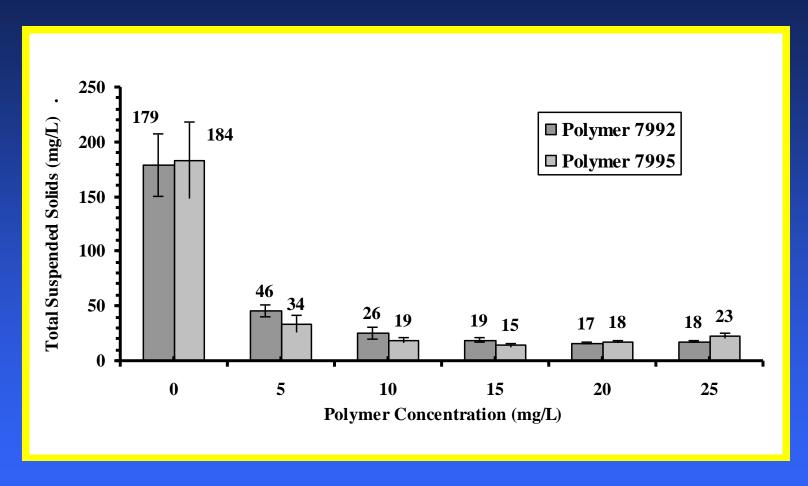
- □ pH
- Turbidity
- RP (orthophosphate)
- Alkalinity
- TSS





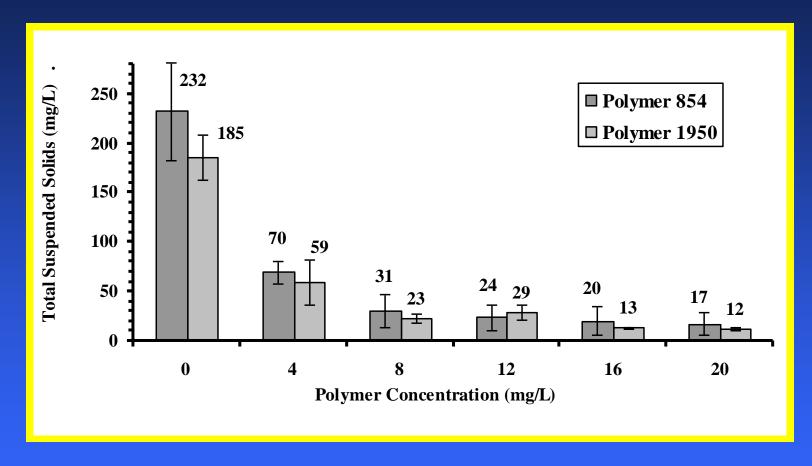
Phipps and Bird Six-Paddle Stirrer with Illuminated Base

#### Similitude Results



Total Suspended Solids removed using very high degree of cationic charge, very low Molecular Weight Polymers

#### Similitude Results



Total Suspended Solids removed using high degree of cationic charge, very high molecular weight Polymers

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- Performance evaluation of Hydrotech Belt filter

# Hydrotech Belt Filter System







Coagulation/Flocculation Tank





Belt Filter

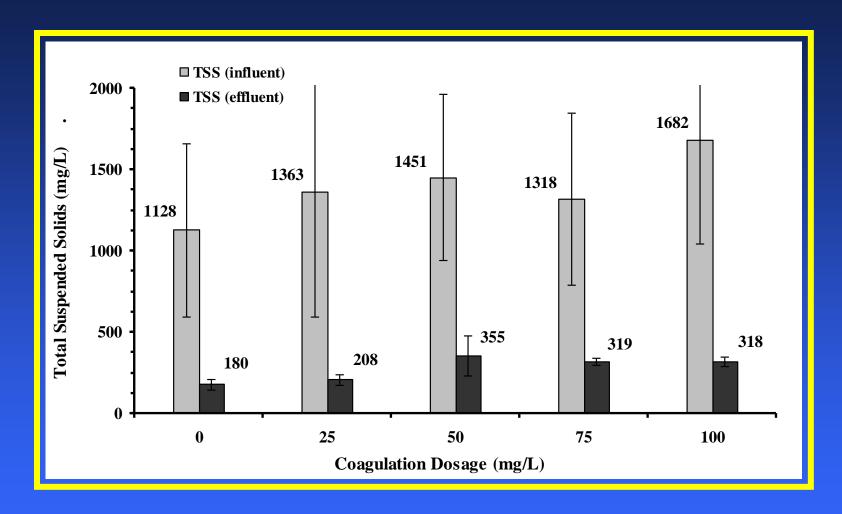


# Objectives

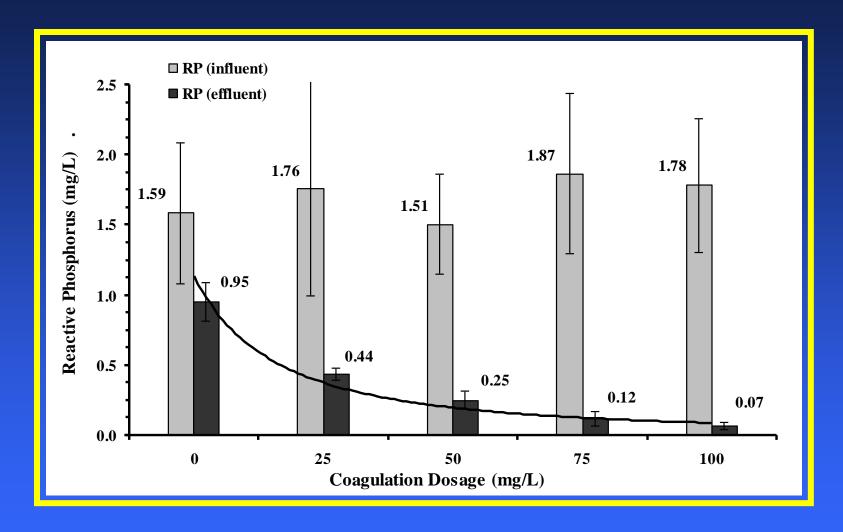
- Summary of the current waste treatment systems
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  - Alum as Coagulation Aid
  - Polymer as Coagulation Aid
  - Alum and Polymer as Coagulation/Flocculation Aids

### Alum

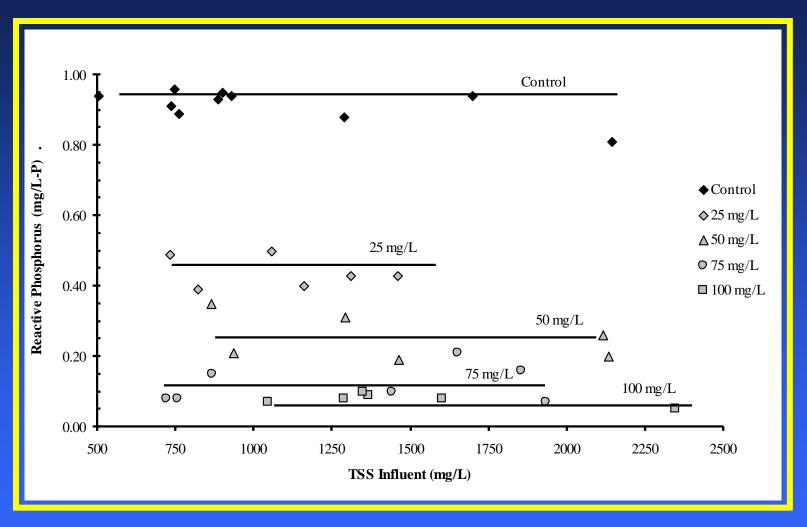
Alum		рН	Alkalinity	TSS (mg/L) RP (mg/L-P)	
Dosage			(mg/L)	Mean: StDev:	Mean StDev:
0 mg/L	Influent	7.37	286	1128 534	1.59 0.50
(11)	Effluent	7.39	287	180 33	0.95 0.14
	% Removal			82%	38%
25 mg/L	Influent	7.32	303	1363 768	1.76 0.77
(7)	Effluent	7.33	302	208 34	0.44 0.04
	% Removal		1%	83%	71%
50 mg/L	Influent	7.29	283	1451 509	1.51 0.36
(7)	Effluent	7.24	270	355 122	0.25 0.07
	% Removal		4%	75%	82%
75 mg/L	Influent	7.29	292	1318 527	1.87 0.57
(7)	Effluent	7.19	274	319 21	0.12 0.05
	% Removal		6%	72%	93%
100 mg/L	Influent	7.30	288	1682 635	1.78 0.48
(7)	Effluent	7.06	242	318 31	0.07 0.03
	% Removal		16%	79%	96%



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of alum dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of alum dosage (mg/L).



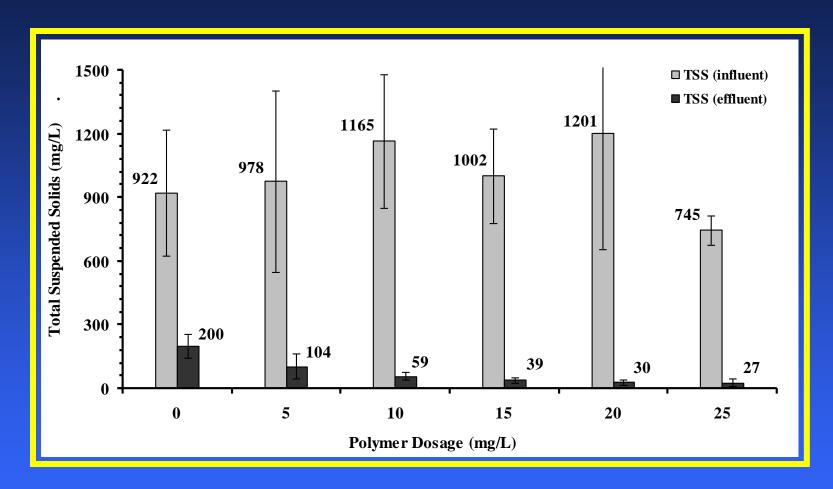
Reactive phosphorus for the effluent from the belt filter as a function of total suspended solids of the influent (mg/L).

# Objectives

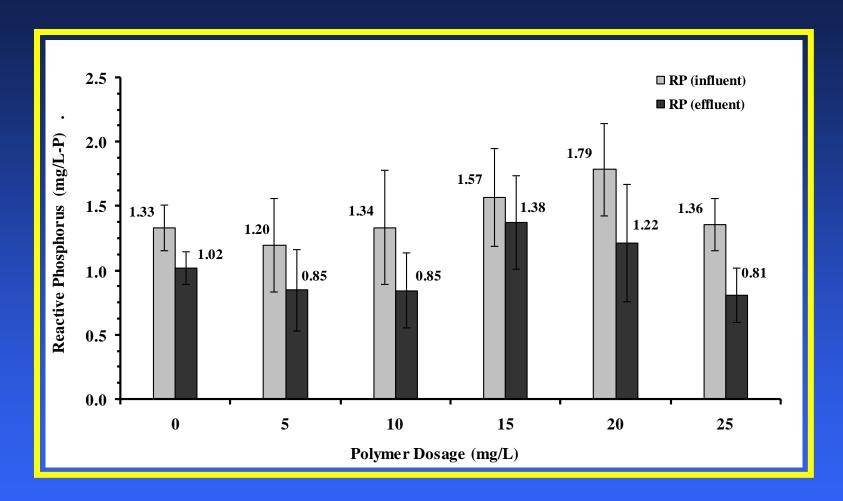
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# Polymer

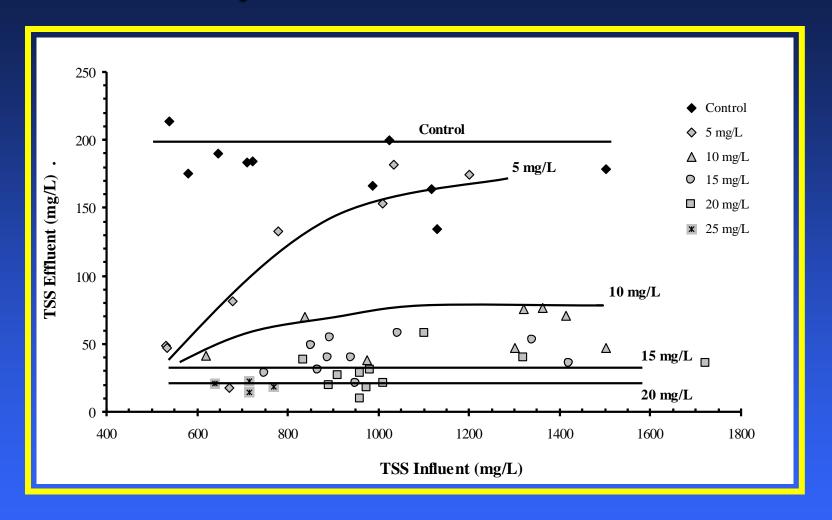
		рН	TSS (mg/L)		RP (mg/L-P)	
Polymer Dosage			Mean:	StDev:	Mean:	StDev:
0 mg/L	Influent	7.55	922	297	1.33	0.18
(12)	Effluent	7.62	200	55	1.02	0.13
	% Removal		76.1%		23%	
5 mg/L	Influent	7.52	978	428	1.20	0.36
(8)	Effluent	7.55	104	60	0.85	0.31
	% Removal		88.6%		26%	
10 mg/L	Influent	7.44	1165	316	1.34	0.44
(8)	Effluent	7.41	59	16	0.85	0.29
	% Removal		94.7%		41%	
15 mg/L	Influent	7.45	1002	223	1.57	0.38
(14)	Effluent	7.31	39	12	1.38	0.36
	% Removal		96.0%		14%	
20 mg/L	Influent	7.47	1201	548	1.79	0.36
(12)	Effluent	7.39	30	13	1.22	0.46
	% Removal		97.3%		32%	
25 mg/L	Influent	7.42	745	69	1.36	0.20
(8)	Effluent	7.31	27	17	0.81	0.21
	% Removal		96.3%		39%	



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of polymer dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of polymer dosage (mg/L).



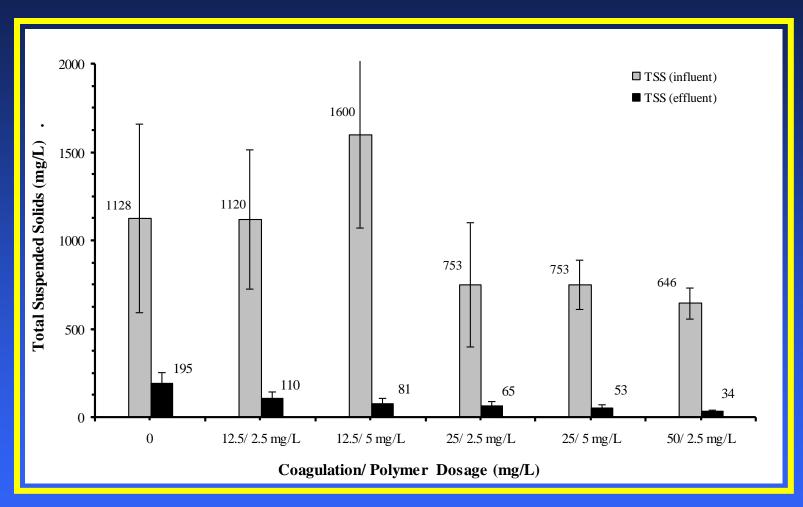
Impact of the influent TSS concentration on the effluent TSS from the belt filter as a function of polymer dosage (mg/L).

### Objectives

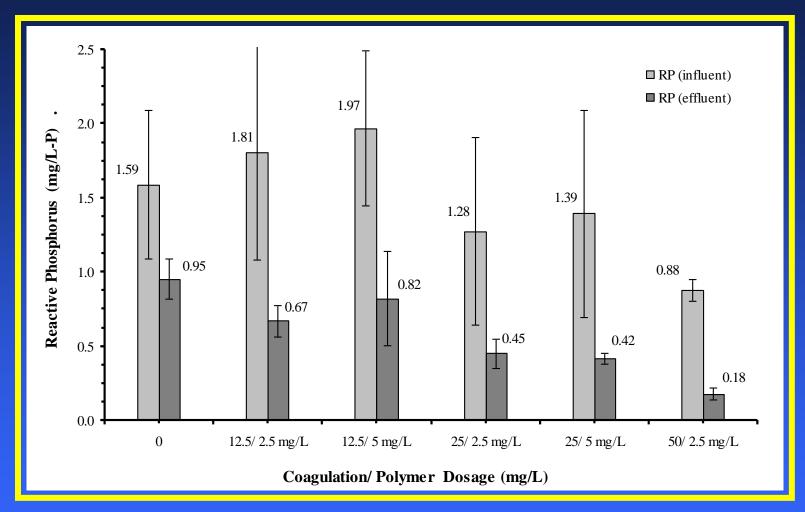
- Summary of the current waste treatment systems
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## Alum/ Polymer

Alum/Polymer		рН	TSS (mg/L)		RP (mg/L-P)	
Dosage			Mean:	StDev:	Mean:	StDev:
0 mg/L /	Influent	7.37	1128	534	1.59	0.50
0 mg/L	Effluent	7.39	195	58	0.95	0.14
	% Removal		81%		38%	
12.5 mg/L /	Influent	7.23	1120	396	1.81	0.73
2.5 mg/L	Effluent	7.26	110	36	0.67	0.11
	% Removal		90%		59%	
12.5 mg/L /	Influent	7.26	1600	526	1.97	0.52
5 mg/L	Effluent	7.22	81	29	0.82	0.32
	% Removal		94%		55%	
25 mg/L/	Influent	7.34	753	352	1.28	0.63
2.5 mg/L	Effluent	7.27	65	28	0.45	0.10
	% Removal		91%		57%	
25 mg/L /	Influent	7.30	753	140	1.39	0.70
5 mg/L	Effluent	7.13	53	20	0.42	0.04
	% Removal		93%		65%	
50 mg/L /	Influent	7.38	646	87	0.88	0.07
2.5 mg/L	Effluent	7.14	34	11	0.18	0.04
	% Removal		95%		80%	



Total suspended solids for the influent from the microscreen backwash sump and effluent from the belt filter as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).



Reactive phosphorus for the influent from the microscreen backwash sump and effluent from the belt filter as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).

Sludge

- Alum
  - $13.2\% \pm 1.1$
- Polymer
  - $11.6\% \pm 2.2$
- Alum/Polymer
  - $12.6\% \pm 1.4$



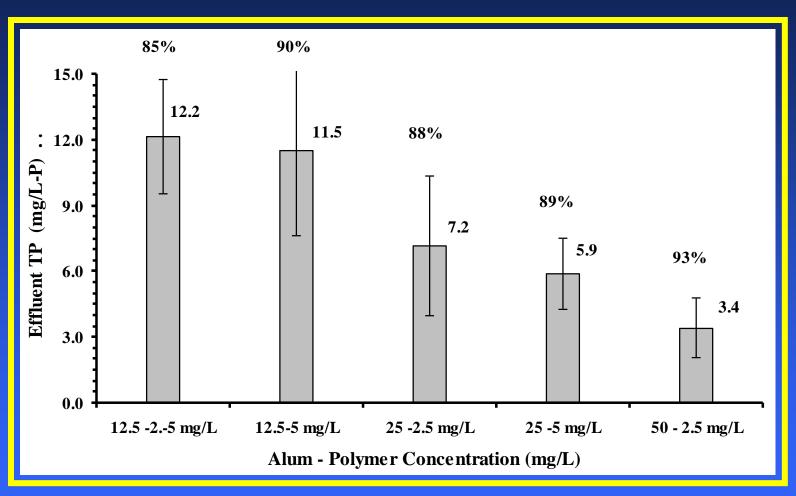


## Secondary Objectives

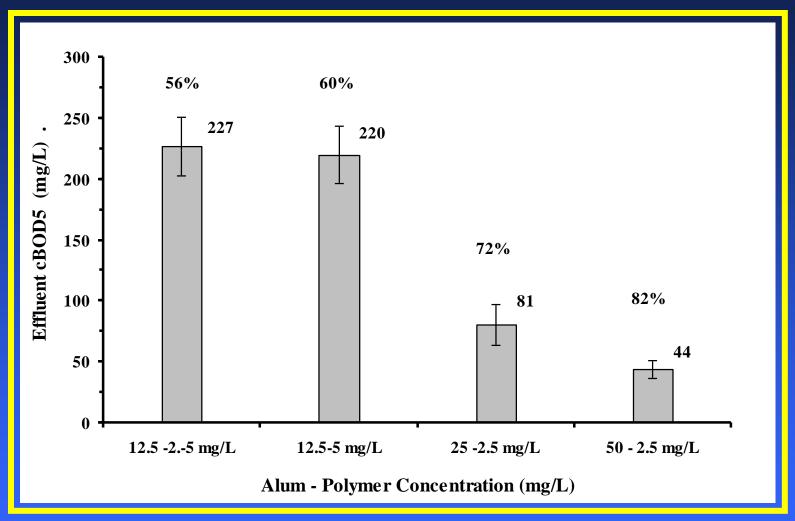
- Other Water Quality Parameters
  - Total Phosphorus
  - Total Nitrogen
  - cBOD<sub>5</sub>
  - COD

# Other Water Quality Parameter

Alum/Polymer		TP (mg	g/L-P)	P) TN (mg/L-N)		cBOD <sub>5</sub> (mg/L)		COD	
Dosage		Mean:	StDev:	Mean:	StDev:	Mean:	StDev:	Mean:	StDev:
12.5 mg/L /	Influent	95.1	39.9	49.1	20.6	498	89		
2.5 mg/L	Effluent	12.2	2.6	8.5	3.8	227	24		
	% Removal	85%		81%		56%			
12.5 mg/L /	Influent	124	54	95	9.3	549	42		
5 mg/L	Effluent	11.5	3.9	16.4	1.7	220	23		
	% Removal	90%		83%		60%			
25 mg/L/	Influent	705	46.4	36.2	19.8	359	214	758	162
2.5 mg/L	Effluent	4.7	1.1	4.7	1.1	81	17	112	14
	% Removal	83%		83%		72%		85%	
25 mg/L /	Influent	37	19.8	37	19.8			880	140
5 mg/L	Effluent	7.0	3.0	6.3	2.3			87	22
	% Removal	88%		83%				90%	
50 mg/L/	Influent	50.3	12.4	31.1	6.8	251	50	808	170
2.5 mg/L	Effluent	3.4	1.4	4.0	1.8	44	8	62	15
	% Removal	93%		87%		82%		92%	



Effluent Total Phosphorus from the belt filter and percent removal for the microscreen backwash wastewater as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage.



Effluent cBOD<sub>5</sub> from the belt filter and percent removal for the microscreen backwash sump wastewater as a function of coagulant (alum) and polymer (Hychem CE 1950) dosage (mg/L).

## **Economics**

Polymer	Cost of Polymers	Cost per kg	Cost per metric tonne of feed
LT 7991	\$247.50 / 450lb drum	\$1.21	\$7.26
LT 7992	\$148.50 / 450 lb drum	\$0.73	\$4.38
LT 7995	\$252.00/ 450 lb drum	\$1.23	\$7.38
CE 854	\$418.50/ 450 lb drum	\$2.05	\$13.08
CE 1950	\$418.50/ 450 lb drum	\$2.05	\$13.08





### Unexpected Difficulties

Polymer induced foam at high dosage



#### Conclusions

- Alum:

96% of RP, 0.07 mg/L-P

Polymer:

96% of TSS, 30 mg/L

Alum/Polymers:

95% of TSS and 80% of RP

Sludge:

13% solids

- □ TP 93%,
- □ TN 87%,
- BOD<sub>5</sub> 82%,
- COD 92%

#### Future Research

- Continued evaluation of other potential coagulant aids, such as Acid Mine Drainage Sludge
- Evaluation of other polymer
- Increase belt porosity to improve Hydraulic Loading Rate
- Additional performance evaluation of belt filter systems in terms of several operating parameters, including flow rates and belt speed.

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# Questions?









