Egyptian Environmental Affairs Agency (EEAA)

Egyptian Pollution Abatement Project (EPAP)

Industrial Wastewater Treatment Plants Inspection Procedures Manual

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TABLE OF CONTENTS

List	t of Fig t of Ta t of Ac		S	iii Iv V
I			INTRODUCTION TO INSPECTION OF INDUSTRIAL WWTP	
	1.1		Preface	1
	1.2		Design of Inspection Manual	1
II	PI	INT LANTS	RODUCTION TO INDUSTRIAL WASTEWATER TREATMENT	
	2.1		re & Characteristics of Industrial Wastewater	4
			Physical Characteristics	5
			Chemical Characteristics	7
			Biological Characteristics	11
	2.2		For Industrial Wastewater Treatment Plants	11
	2.3		non Types of Wastewater Treatment Methods	13
			Physical Unit Operations	13
			Chemical Unit Processes	13
		2.3.3	Biological Unit Processes	13
III	DES EGY		FION OF MAIN TREATMENT TECHNOLOGIES APPLIED IN	
	-		nanical Processes	
			Screening	14
			Oil Separation	14
			Flow Equalization	15
	3.2		cal Treatment	19
		3.2.1	Sedimentation	19
		3.2.2	Flotation	22
		3.2.3	Coalescence	23
	3.3	CHE	MICAL TREATMENT	25
		3.3.1	Chemical Pre-treatment	25
			L	26
			Physico Chemical Treatment	27
	3.4.		gical Treatment	30
		3.4.1		30
			Anaerobic Biological Treatment	36
	~ -		Pond Treatment Processes	37
	3.5		Dinations of Technologies Commonly Applied in Egypt	41
		3.5.1	Physical / Chemical Treatment	41
		3.5.2	e	42
		3.5.3	Anaerobic/aerobic Treatment	42

	3.6	Sludg	ge Treatment And Disposal	44
		3.6.1	Preliminary Operations	44
			Sludge Thickening	45
		3.6.3	Sludge Stabilization	45
		3.6.4	Sludge Dewatering	46
		3.6.5	Sludge Disposal and Utilization	51
	3.7	Auxil	liary Operations	52
		3.7.1	Disinfection	52
		3.7.2	Reuse of Treated Effluent	53
	3.8	Integ	rated Model For Industrial Wastewater Treatment	55
		3.8.1	Primary Treatment	55
			Secondary Treatment	56
		3.8.3	Tertiary Treatment	56
		3.8.4	Sludge Treatment	57
3.9		Emiss	sions,Effluents and Solid Wastes Generated from IWWTP	59
3.10			nary of Industrial Waste: Character and Treatment Methods	60
IV	EG	YPTI/	AN LEGISLATION ON INDUSTRIAL WASTEWATER	
			ONS AND SLUDGE TREATMENT	
	4.1	Backs	ground	63
	4.2		erning Wastewater Effluents To Different Receiving Bodies	65
			erning Solid Waste And Sludge	65
			erning Work Environment	68
			erning Hazardous Material And Waste	68
			erning Environmental Register	69
V	INS	SPECT	TION PRINCIPLES AND EXAMPLES	
			ets Of Inspection	70
			ection Visit	70
			Gathering Information and Auditing	70
			Collection of Samples for Analysis	73
			Typical Cases of Malfunctioning & Process Failure	75
			Examples Cases of Process Failure	77
	5.3		ection Results	78
			Observations on operation of IWWTP Performance	78
			Preparation of Final Inspection Report	79
			Guidance to the inspectors	79
			L	

REFERENCES

ANNEX

List of Figures

		page
2-1	Classification of Total Solids	6
2-2	De-oxygenation rates of sewage, a certain industrial waste and a combination of the two.	9
3-1	Typical mechanically cleaned bar rack	17
3-2	Typical screening devices for wastewater treatment	17
3-3	Corrugated plate for CPI, Cross section of CPI units	18
3-4	Schematic diagram of a rectangular horizontal flow settling basin	20
3-5	Schematic diagram of gravity thickener	21
3-6	Schematic diagram for Induced Air Flotation for Oily Wastes & Suspended	22
	Solids.	
3-7	Schematic diagram for The Slant Rib Coalescing Separator.	24
3-8	Schematic diagram for DAF system	29
3-9	Schematic diagram for DAF system with Lamella separator & type flocculator	29
3-10	Activated sludge Processes	31
3-11	Typical operation sequence for SBR system.	33
3-12	Schematic diagram for Typical Trickling Filters	35
3-13	Two Stage Anaerobic – aerobic system	43
3-14	Schematic diagram for Horizontal belt filter press unit	49
3-15	Schematic diagram for Filter press unit	49
3-16	Possible choice for wastewater treatment and their sequence.	58

List of Tables

		Page
2-1	Typical range of BOD & S.S load for industrial and municipal wastewater	4
2-2	Typical range of concentration values for industrial and municipal wastewater	4
2-3	Important contaminants of concern in industrial wastewater treatment	5
2-4	Parameters setting the standards for the discharge of industrial wastewater	12
3-1	Types of Mechanical Screens	16
3-2	Chemicals used in industrial wastewater treatment	27
3-3	Description of the operation steps for the sequencing batch reactor	33
3-4	Main Treatment Technology, advantage & disadvantage	38
3-5	Main Treatment Technology and applicability in Egypt	41
4-1	Comparison of Egyptian Laws Related to Wastewater	64
4-2	Egyptian environmental requirements	66
5-1	Specific Inspection Issues for Main Treatment Methods	77

1. INTRODUCTION TO INSPECTION OF INDUSTRIAL WASTEWATER TREATMENT PLANTS:-

1.1 **PREFACE**

The Egyptian Environmental Affairs Agency (EEAA) has developed a General Inspection Manual (GIM) and several industrial specific manuals for inspection and self-monitoring.

Meanwhile, other manuals are being designed and produced for inspection and monitoring of industrial, wastewater treatment plants, hazardous waste management, and industrial energy production.

This manual concerns with inspection guideline for the industrial wastewater treatment facilities, which may be present or will be installed in various industrial sectors and sub-sectors.

The manual is designed to be used by RBO & EMU inspectors together with the sector specific manual to check the performance and efficiency of the industrial wastewater treatment plants.

In order to do that the inspector should be familiar with the different types of the wastewater treatment operations and processes commonly applied in Egypt.

Based on above, this manual has been developed for the industrial wastewater treatment plants the main objective of this manual are:-

- To familiarize the inspectors with the Nature and Characteristics of the industrial wastewaters discharged from the different Egyptian industries as well as corresponding parameters used for measuring pollution levels.
 - To recognize the main wastewater treatment technologies applied in the Egyptian Industries.
 - To be familiar with different treatment packages and their suitability for use in different applications.
 - To know the part of the Egyptian legislation relevant to wastewater emissions and sludge treatment and disposal.
 - To apply the inspection principles outlined in the General Inspection Manual "GIM" for inspection of the wastewater treatment plants using a cheek list specially developed for this purpose and included with this manual.

Using this manual side by side with the specific sector manual in any inspection mission to any industry will help in evaluating the performance of the treatment facilities that may be used by the industry to treat the waste effluent to comply with environmental laws.

The General Inspection Manual GIM is used as a reference to provide the general guidelines required to prepare a specific chapter on Inspection principles and procedures for wastewater treatment plants. This way redundant repetition can be avoided.

1.2 DESIGN OF THE INSPECTION MANUAL

The Inspection Manual for the wastewater treatment plants contains five main chapters. The manual started by table of contents, list of figures and list of tables included in the manual.

1

The first chapter gives an introduction to the whole project then focuses on demonstrating the main idea describing the main objectives and ways of use the manual in parallel with GIM and sector specific manual.

The second chapter of the manual provides a comprehensive introduction to industrial wastewater treatment plants, which includes nature & characteristics of wastewater with a description in simple terms the meaning of BOD₅, COD, TDS.... etc and the environmental impacts related to these parameters.

In this chapter the need for industrial wastewater treatment plants is explained related the compliance with regulatory limits for discharging effluent to Nile, Sea, Canals, municipal sewer and reuse of effluent...etc. Also in this chapter, the common types of wastewater treatment plants are briefly described.

Chapter 3 describes thoroughly the main treatment technologies commonly applied in Egypt including mechanical, physical, chemical and biological processes.

Combinations of these technologies are also provided mainly: physiochemical, chemical biological and anaerobic aerobic treatment systems. Both schematics and flow diagrams are used for demonstration.

The advantage and disadvantage of each process are explained. Key operation parameters and parameters for measuring performance are also compared.

Sludge treatment and disposal techniques are also covered in chapter 3 including preliminary operation, sludge thickening, stabilization, dewatering, drying beds, sludge disposal and utilization. Auxiliary operation mainly disinfection and reuse of treated effluent are also described in chapter 3 as related to real applications in the Egyptian Industries.

Chapter 4 Provides the Egyptian legislation related to industrial wastewater Discharge to different receiving bodies, treatment and disposal of solid waste and sludge.

Environmental Impacts in work environment (e.g. Noise and odor), Regulations dealing with hazardous materials and hazardous waste are also covered in this chapter.

Preparing environmental register for wastewater treatment plant as per Egyptian law requirement is also demonstrated.

Chapter 5 has designed to provide the inspection principles with reference to General Inspection Manual (GIM). Also this chapter indicates:-

- The inspection targets are mainly include inspection of emissions, operation control and self monitoring systems.... etc.
- The main activities to be conducted during the inspection visit is also outlined in Chapter 5 starting by gathering information, auditing and samples collection for analysis.
- Typical cases of violations and troubleshooting are presented in Chapter 5 as examples. (Check by- passing, normalities or abnormalities in industrial process during inspection,

detection of malfunctioning in the treatment process, detection of dubious analysis results provided by the industry).

Comparing operation values with design values, and inspection of self-monitoring system are also included. In addition, chapter 5 provides the inspectors with simple techniques for evaluation of IWWTP performance and for preparation of final inspection report.

Some guidance are also included in chapter 5 about the role of inspectors in giving advice on issues related to best management practice to companies which are not directly related to compliance management.

At the end of the manual two annexes are attached, Annex 1 provides a set of definitions and terminology related to industrial wastewater treatment while, Annex 2 is an inspection checklist designed especially for IWWTP.

A list of references used in preparing the manual is also included.

2. INTRODUCTION TO INDUSTRIAL WASTEWATER TREATMENT PLANTS

2.1 NATURE & CHARACTERISTICS OF INDUSTRIAL WASTEWATER

It is only natural for industry to presume that its wastewater can best be disposed of in the domestic sewer system. However, city authorities should not accept any wastewater discharges into the domestic sewer system without first learning the facts about the characteristics of the wastewater, the sewage system's ability to handle them, and the effects of the wastewater upon all components of the city disposal system. Institution of a sewer ordinance, restricting the types or concentrations of wastewater admitted in the sewer leading to a treatment plant, is one means of protecting the system. The following table gives a comparison between the typical range of BOD and S.S. load for industrial and municipal domestic wastewater. While table (2-2) gives a comparison in concentration values.

Origin of waste	Biochemical oxygen demand "BOD" (kg/ton product)	Total Suspended solids "TSS" (kg/ton product)
Domestic sewage	0.025 (kg/day/person)	0.022 (kg/day/person)
Dairy industry	5.3	2.2
Yeast industry	125	18.7
Starch & glucose industry	13.4	9.7
Fruits & vegetable canning industry	12.5	4.3
Textile industry	30 - 314	55 - 196
Pulp & paper industry	4 - 130	11.5 - 26
Beverage industry	2.5 - 220	1.3 - 257
Tannery industry	48 - 86	85 - 155

Table (2-1): Typical range of BOD and S.S. load for industrial and municipal wastewater *

* Rapid assessment for industrial pollution

for industrial and municipal wastewater **							
Origin of waste	рН	T.S.S, mg/l	BOD, mg/l	COD, mg/l	TDS, mg/l	O&G, mg/l	
 Domestic Sewage 	7	220	250	500	500	-	
 Dairy Industry 	4	12150	14000	21100	19000	320	
 Yeast Industry 	5.3	540	2100	3400	3500	9	
 Fruits & Vegetable Canning 	5.5	2200	800	1400	1270	94	
 Textile Industry 	6.5	1800	840	1500	17000	155	
Pulp & Paper Industry	8	1640	360	2300	1980	-	
– Beverage Industry	9	760	620	1150	1290	-	
– Tannery Industry	10	2600	2370	4950	8500	115	
– Fish Canning	11	565	890	2350	8218	290	

Table (2-2): Typical range of concentration values for industrial and municipal wastewater **

** Previous analysis conducting in several companies.

The important contaminants of concern in wastewater treatment are listed in the table 2-3. Secondary treatment standards for wastewater are concerned with the removal of biodegradable organics, suspended solids, and pathogens. Many of the more stringent standards that have been developed recently deal with the removal of nutrients and priority pollutants. When wastewater is to be reused, standards normally include requirements for the removal of refractory organics, heavy metals, and in some cases dissolved inorganic salts.

Contaminants	Reason for importance			
Suspended solids	Suspended solids can lead to the development of sludge			
	deposits and anaerobic conditions when untreated wastewater			
	is discharged in the aquatic environment.			
Nutrients	Both nitrogen and phosphate, along with carbon, are essential nutrients for growth. When discharged to the aquatic			
	environment, these nutrients can lead to the growth of			
	undesirable aquatic life. When discharged in excessive			
	amounts on land, they can also lead to the pollution of			
	groundwater.			
Priority pollutants	Organic and inorganic compounds selected on the basis of			
Thomy ponduants	their known or suspected carcinogenicity, mutagenicity,			
	teratogenicity, or high acute toxicity. Many of these			
	compounds are found in wastewater.			
Refractory organics	These organics tend to resist conventional methods of			
	wastewater treatment. Typical examples include surfactants,			
	phenols, and agricultural pesticides.			
Heavy metals	Heavy metals are usually discharged to wastewater from			
·	commercial and industrial activities and have to be removed if			
	the wastewater is to be reused.			
Dissolved inorganics	Inorganic constituents such as calcium, sodium, and sulfate			
	are added to the original domestic water supply as a result of			
	water use and may have to be removed if the wastewater is to			
	be reused.			

2.1.1 Physical Characteristics

The most important physical characteristic of wastewater is its total solids content, which is composed of floating matter, settleable matter, colloidal matter, and matter in solution. Other important physical characteristics include odor, temperature, color, and turbidity.

a) Total Solids

Analytically the total solids content of a wastewater is defined as all the matter that remains as residue upon evaporation at 103 to 105 °C. Matter that has a significant vapor pressure at this temperature is lost during evaporation & is not defined as a solid. Settable solids are those solids that will settle to the bottom of a cone-shaped container (called an Imhoff cone) in a 60-minute period.

Settable solids, expressed as mL/L, are an approximate measure of the quantity of sludge that will be removed by primary sedimentation. Total solids, or residue upon evaporation, can be further classified as non-filterable (suspended) or filterable by passing a known volume of liquid through a filter.

The filterable-solids fraction consists of colloidal and dissolved solids. The colloidal fraction consists of the particulate matter with an approximate size range of from 0.001 to 1 μ m. The dissolved solids consist of both organic & inorganic molecules and ions that are present in true solution in water. The colloidal fraction cannot be removed by settling. Generally, biological oxidation or coagulation, followed by sedimentation, is required to remove these particles from suspension.

The suspended solids are found in considerable quantity in many industrial wastewater, such as cannery and paper-mill effluents. They are screened and/or settled out at the treatment plant. Solids removed by settling and separated from wash water are called *sludge*, which may then be pumped to drying beds or filtered for extraction of additional water (dewatering).

Each of the categories of solids may be further classified on the basis of their volatility at 550 ± 50 °C. The organic fraction will oxidize and will be driven off as gas at this temperature, and the inorganic fraction remains behind as ash. Thus the terms "Volatile suspended solids" and "Fixed suspended solids" refer, respectively, to the organic and inorganic (or mineral) content of the suspended solids. The volatile-solids analysis is applied most commonly to wastewater sludge to measure their biological stability.

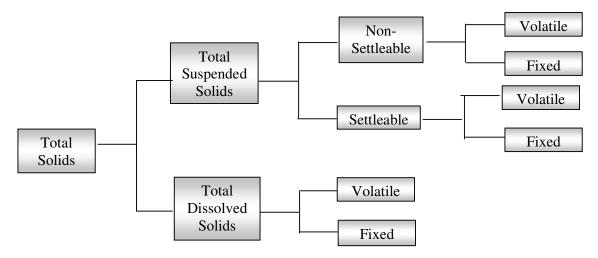


Fig. (2-1) Classification of Total Solids

b) Odors

Odors are usually caused by gases produced by the decomposition of organic matter or by substances added to the wastewater. Industrial wastewater may contain either odorous compounds or compounds that produce odor during the process of wastewater treatment.

c) Temperature

The temperature of water is a very important parameter because of its effect on chemical reactions and reaction rates, aquatic life, and the suitability of the water for beneficial uses. Increased temperature, for example, can cause a change in the species of fish that can exist in the receiving water body. Industrial establishments that use surface water for cooling-water purposes are particularly concerned with the temperature of the intake water.

In addition, oxygen is less soluble in warm water than in cold water. The increase in the rate of biochemical reactions that accompanies an increase in temperature, combined with the decrease

in the quantity of oxygen present in surface waters, can often cause serious depletions in dissolved oxygen concentration in the summer months. When significantly large quantities of heated water are discharged to natural receiving water, these effects are magnified. It should also be realized that a sudden change in temperature can result in a high rate of mortality of aquatic life. Moreover, abnormally high temperatures can foster the growth of undesirable water plants and wastewater fungus.

d) Color

Color of industrial wastewater varies according to the type of industry. Knowledge of the character and measurement of color is essential. Since most colored matter is in a dissolved state, it is not altered by conventional primary devices, although secondary treatment units, such as activated sludge and trickling filters, remove a certain percentage of some types of colored matter. Sometimes color matters needs chemical oxidation procedures for removal.

e) Turbidity

Turbidity, a measure of the light-transmitting properties of water, is another test used to indicate the quality of wastewater discharges and natural waters with respect to colloidal and residual suspended matter. In general, there is no relationship between turbidity and the concentration of suspended solids in untreated wastewater. There is, however, a reasonable relationship between turbidity and suspended solids for the settled secondary effluent from the activated sludge process.

2.1.2 Chemical Characteristics

a) Organic Matter

Organic compounds are normally composed of a combination of carbon, hydrogen, and oxygen, together with nitrogen in some cases. Other important elements, such as sulfur, phosphorus, and iron, may also be present. Also, industrial wastewater may contain small quantities of a large number of different synthetic organic molecules ranging from simple to extremely complex in structure. Typical examples include surfactants, organic priority pollutants, volatile organic compounds and agricultural pesticides as shown in table (2-3). The presence of these substances has complicated industrial wastewater treatment because many of them either cannot be or are very slowly decomposed biologically.

Fats, Oils, and Grease. Fats are among the more stable of organic compounds and are not easily decomposed by bacteria. Kerosene, lubricating oils reach the sewer from workshops and garages, for the most part they float on the wastewater, although a portion is carried into the sludge on settling solids. To an even greater extent than fats, oils, and soaps, the mineral oils tend to coat surfaces causing maintenance problems. If grease is not removed before discharge of the wastewater, it can interfere with the biological life in the surface waters and create unsightly floating matter and films. The oil and grease (O & G) is a very important test used to determine the hydrocarbon content of industrial wastewaters. O&G tests include free O&G and emulsified O&G measures. These tests will determine the type of treatment required. Free O&G can be removed by flotation & skimming using gravity oil separator (GOS). However, emulsified oil is removed by Dissolved Air Flotation system after chemical de-emulsification of oil. In any case, O&G have to be removed prior biological treatment as they will clog the flow distributing devices and air nozzles.

Surfactants. Surfactants are large organic molecules that are slightly soluble in water and cause foaming in wastewater treatment plants and in surface waters into which the wastewater effluent is discharged. Surfactants tend to collect at the air-water interface. During 7

aeration of wastewater, these compounds collect on the surface of the air bubbles and thus create a very stable foam.

- **Phenols.** Phenols and other organic compounds are also important constituents of water. Phenols cause taste problems in drinking water, particularly when the water is chlorinated. They are produced primarily by industrial operations and find their way to surface waters via industrial wastewater discharges. Phenols can be biologically oxidized at concentrations up to 500 mg/liter.
- Volatile Organic Compounds (VOCs). Organic compounds that have a boiling point less than < 100 °C and/or a vapor pressure > 1 mm Hg at 25 °C are generally considered to be volatile organic compounds (VOCs). The release of these compounds in sewers and at treatment plants is of particular concern with respect to the health of collection system and treatment plant workers.
 - **Pesticides & Agricultural Chemicals.** Trace organic compounds, such as pesticides, herbicides, and other agricultural chemicals, are toxic to most life forms and therefore can be significant contaminants of surface waters.

Parameters of Organic Content

\blacktriangleright Biochemical Oxygen Demand (BOD₅)

The most widely used parameter of organic pollution applied to wastewater is the 5-day BOD (BOD_5) . The BOD₅ is usually exerted by dissolved and colloidal organic matter and imposes a load on the biological units of the treatment plant. Oxygen must be provided so that bacteria can grow and oxidize the organic matter. An added BOD₅ load, caused by an increase in organic waste, requires more bacterial activity, more oxygen, and greater biological-unit capacity for its treatment.

Figure (2-2) illustrates one possible effect of a given industrial wastewater on a sewage plant. In this instance the industrial wastewater, with its constant rate of degradation, tends to smooth out the rate of decomposition of the sewage so that the result shows less upsurge due to nitrogenation. Also, the rate of decomposition of the industrial wastewater tends to slow down the initial rapid rate of domestic sewage.

The determination of the BOD₅ involves the measurement of the dissolved oxygen used by microorganisms in the biochemical oxidation of organic matter. Several dilutions of the wastewater are put into standard BOD₅ bottles with water that has been saturated with oxygen, and contains bacteria. A control bottle is also prepared with only water and bacteria. The bottles are put into a standard incubator for five days, hence this is called the "Five-Day BOD Test (BOD₅)." The difference in oxygen levels between the control bottle and the bottles with oxygen remaining is used to calculate the BOD₅ in mg/L.

The BOD 5 test results are used to:

- * Determine the approximate quantity of oxygen that will be required to biologically stabilize the organic matter present.
- * Determine the size of wastewater treatment facilities.
- * Measure the efficiency of some treatment process.
- * Determine compliance with wastewater discharge permits.

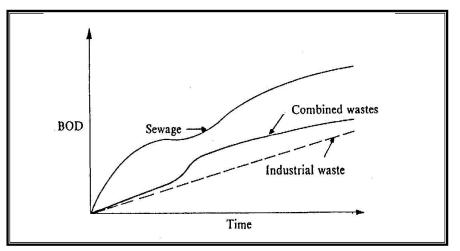


Fig. (2-2) Deoxygenation rates of sewage, a certain industrial wastewater and a combination of the two.

The limitations of the BOD₅ test are as follows:

- * A high concentration of active, acclimated seed bacteria is required.
- * Pretreatment is needed when dealing with toxic wastes, and the effects of nitrifying organisms must be reduced.
- * Only the biodegradable organics are measured.
- * The test does not have stoichiometric validity after the soluble organic matter present in solution has been used.
- * An arbitrary, long period of time is required to obtain results.

Chemical Oxygen Demand (COD)

The COD test is used to measure the organic matter in industrial wastewater that contains compounds that are toxic to biological life. It oxidizes the reduced compounds in wastewater through a reaction with a mixture of chromic and sulfuric acid at high temperatures. There is another COD test using permanganate as the oxidizing agent but this test will give lower values and is not directly relatable to the standard COD test.

The COD of wastewater is, in general, higher than that of the BOD₅ because more compounds can be chemically oxidized than can be biologically oxidized. For many types of wastewater, it is possible to correlate COD with BOD₅. This can be very useful because COD can be determined in 3 hours, compared with 5 days for the BOD₅. Once the correlation has been established, COD measurements can be used to good advantage for treatment-plant control and operation.

The ratio of COD to BOD_5 is usually 1.5: 2 for industrial wastewater containing biodegradable material (e.g. Food Industry). For wastewaters with ratios higher than 3, it is assumed that some oxidizable material in the sample is not biodegradable. Nonbiodegradable material sometimes is called refractory and found mainly in wastewater from chemical and pulp & paper industries.

b) Inorganic Matter

Several inorganic components of wastewater are important in establishing and controlling wastewater quality. Industrial wastewater has to be treated for removal of the inorganic constituents that are added in the use cycle. Concentrations of inorganic constituents also are

increased by the natural evaporation process, which removes some of surface water and leaves the inorganic substance in the wastewater.

- **pH**. The hydrogen-ion concentration is an important quality parameter of wastewater. The concentration range suitable for the existence of most biological life is quite narrow and critical. Wastewater with an adverse concentration of hydrogen ion is difficult to treat by biological means, and if the concentration is not altered before discharge, the wastewater effluent may alter the concentration in the natural waters.
- Alkalinity. Alkalinity in wastewater results from the presence of the hydroxides, carbonates, and bicarbonates of elements such as calcium, magnesium, sodium, potassium, or ammonia. Of these, calcium and magnesium bicarbonates are most common. Borates, silicates, phosphates, and similar compounds can also contribute to the alkalinity. The alkalinity in wastewater helps to resist changes in pH caused by the addition of acids. The concentration of alkalinity in wastewater is important where chemical treatment is to be used, in biological nutrient removal, and where ammonia is to be removed by air stripping.
- **Nitrogen**. Because nitrogen is an essential building block in the synthesis of protein, nitrogen data will be required to evaluate the treatability of wastewater by biological processes. Insufficient nitrogen can necessitate the addition of nitrogen to make the wastewater treatable. Where control of algal growth in the receiving water is necessary to protect beneficial uses, removal or reduction of nitrogen in wastewaters prior to discharge may be desirable. The total nitrogen, as a commonly used parameter, consists of many numerous compounds such as; NH₃, NH₄-N, NO₃-N, NO₂-N, urea, organic-N (amines, amino acids, ...etc).
- **Phosphorus.** Phosphorus is also essential to the growth of algae and other biological organisms. The organically bound phosphorus is an important constituent of industrial wastewater and sludge.
- **Sulfur.** Sulfate is reduced biologically under anaerobic conditions to sulfide, which in turn can combine with hydrogen to form hydrogen sulfide (H₂S). Hydrogen sulfide released to the atmosphere above the wastewater in sewers that are not flowing full tends to accumulate at the crown of the pipe. The accumulated H₂S can then be oxidized biologically to sulfuric acid, which is corrosive to steel pipes and equipment.
- **Toxic Inorganic Compounds.** Because of their toxicity, certain cations are of great importance in the treatment and disposal of wastewater. Many of these compounds are classified as priority pollutants. Copper, lead, silver, chromium, arsenic, and boron are toxic in varying degrees to microorganisms and therefore must be taken into consideration in the design of a biological treatment plant. Many plants have been upset by the introduction of these ions to the extent that the microorganisms were killed and treatment ceased. Other toxic cations include potassium and ammonium at 4000 mg/L. Some toxic anions, including cyanides and chromates, are also present in industrial wastewater. These are found particularly in metal-plating wastewater and should be removed by pretreatment at the site of the industry rather than be mixed with the municipal wastewater. Fluoride, another toxic anion, is found commonly in wastewater from electronics manufacturing facilities. Organic compounds present in some industrial wastewater are also toxic.
- **Heavy Metals.** Trace quantities of Many metals, such as nickel (Ni), manganese (Mn), lead (Pb), chromium (Cr), cadmium (Cd), zinc (Zn), copper (Cu), iron (Fe), and mercury (Hg)

are important constituents of some industrial wastewaters. The presence of any of these metals in excessive quantities will interfere with many beneficial uses of the water because of their toxicity; therefore, it is frequently desirable to measure and control the concentration of these substances.

2.1.3 Biological Characteristics

Some industries have certain pathogenic organisms like slaughter houses others have molds and fungi as starch and yeast factories. Biological tests on wastewater determine whether pathogenic organisms are present by testing for certain indicator organisms. Biological information is needed to assess the degree of treatment of the wastewater before its discharge to the environment. The parameters setting the standards for the discharge of different industrial wastewater effluents are outlined in table (2-4). Total nitrogen is a commonly used parameter that includes a number of parameters , NH3, NH4-N, NO3-N, NO2-N, urea, organic N such as amines, amino acids, proteins, etc.) and process chemicals. The presence of these compounds depends on the production.

2.2 NEED FOR INDUSTRIAL WASTEWATER TREATMENT PLANTS

Industry views wastewater treatment as an imposed necessity which it employs when it is compelled to, especially when wastewater's effect on the receiving watercourse is readily visible or when public approval and claim will be gained for the expenditure and effort.

Industry should attempt to treat its wastewater at the lowest cost that will yield a satisfactory effluent for the particular receiving stream, which may necessitate considerable study, research, and pilot investigations. Planning ahead will provide time to make appropriate decisions. Conversely, lack of planning on minimizing wastewater treatment costs may mean that a sudden demand for an immediate solution will cause industry to decide to cease production.

The public attitude toward pollution control, which bordered on apathy during the first half of the twentieth century, has undergone drastic change in the early 1970s as part of the surge in public concern for the quality of the environment. Sincere public concern will be required over a long period of time to make the necessary changes in society to bring about significant improvements in our environment. Major changes in our political, social, legal, and economic approaches to pollution control will be required and therefore much more than clever technological advances will be needed.

To prevent any health hazards caused by discharging wastewater to water streams, the wastewater must be treated before discharge. Such treatment should comply with the terms of the legislation defining the characteristics of the effluent discharging in water streams. The concept of planing and development should be based on the criteria to protect land, water resources, aquatic life in streams and rivers and marine life from pollution and to safeguard public health as a high priority. Egyptian standards for quality of wastewater to be discharged in water streams have been updated in 1994 by law 4 and by decree 44/ 2000 of law 93, 1962 for discharging effluent to public sewer and by Law 48, 1982 for discharging to fresh water bodies including River Nile.

The environmental inspection on wastewater treatment plants aims to support and strengthen the Protection of both the environment and the public health, since the pollution generated from the industrial establishments has a negative impact not only on the environment, but also on the health of the individuals. Therefore, it is noted that most of the procedures that could be implemented by industrial establishments to reduce the negative environmental impacts, will also lead to reducing the effects that present a threat to the health of workers within the plants and the public living in regions affected by the various emissions from the plants.

In this respect, the effectiveness of the inspection on industrial wastewater treatment plants will lead to the protection of the environment and the protection of workers and public health.

Table (2-4) Parameters setting the standards for the discharge of industrial wastewater

BOD2 x	Parameter							Indu	stry						
BOD, x									-			ຽມ			
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polynuclear aromatics	polynuclear aromatics					X				X					
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2.3 COMMON TYPES OF WASTEWATER TREATMENT METHODS

After treatment objectives have been established for a specific project and the applicable regulations have been reviewed, the degree of treatment can be determined by comparing the influent wastewater characteristics to the required effluent wastewater characteristics. A number of different treatment and disposal or reuse alternatives are then developed and evaluated, and the best alternative is selected.

The contaminants in wastewater are removed by physical, chemical, and biological means. The individual methods usually are classified as physical unit operations, chemical unit processes, and biological unit processes.

2.3.1 Physical Unit Operations

Treatment methods in which the application of physical forces predominates are known as physical unit operations. Because most of these methods evolved directly from man's first observations of nature, they were the first to be used for wastewater treatment. Screening, mixing, flocculation, sedimentation, flotation, filtration, and gas transfer are typical unit operations.

2.3.2 Chemical Unit Processes

Treatment methods in which the removal or conversion of contaminants is brought about by the addition of chemicals or by other chemical reactions are known as chemical unit processes. Precipitation, adsorption, and disinfection are the most common examples used in wastewater treatment. In chemical precipitation, treatment is accomplished by producing a chemical precipitate that will settle. In most cases, the settled precipitate will contain both the constituents that may have reacted with the added chemicals and the constituents that were swept out of the wastewater as the precipitate settled. Adsorption involves the removal of specific compounds from the wastewater on solid surfaces using the forces of attraction between bodies.

2.3.3 Biological Unit Processes

Treatment methods in which the removal of contaminants is brought about by biological activity are known as biological unit processes. Biological treatment is used primarily to remove the biodegradable organic substances (colloidal or dissolved) from wastewater. Basically, these substances are converted into gases that can escape to the atmosphere and into biological cell tissue that can be removed by settling. Biological treatment is also used to remove nutrients (nitrogen & phosphorus) from wastewater. With proper environmental control, wastewater can be treated biologically in most cases.

3. DESCRIPTION OF MAIN TREATMENT TECHNOLOGIES APPLIED IN EGYPTIAN INDUSTRIES

The treatment processes and technologies described in this text are those most commonly applied in Egypt for the industrial wastewater treatment. Primary, secondary and tertiary treatment schemes are applied for every specified case, see Table (3-16) showing a schematic diagram for various treatment schemes.

3.1 MECHANICAL PROCESSES

3.1.1 Screening

The first unit operation encountered in wastewater-treatment plants is screening. A screen is a device with openings, generally of uniform size that is used to retain the coarse solids found in wastewater.

The screening element may consist of parallel bars, rods or wires, grating, wire mesh, or perforated plate, and the openings may be of any shape but generally are circular or rectangular slots. A screen composed of parallel bars or rods is called a rack. Although a rack is a screening device, the term "screen" should be limited to the type with wire cloth or perforated plate. However, the function performed by a rack is called screening and the materials removed by it are known as screening or raking. Bar racks normally have clear openings between bars of 15mm.

According to the method of cleaning, racks and screens are designated as hand cleaned or mechanically cleaned. According to the size of openings, screens are designated as coarse or fine. Coarse screens have openings of ¹/₄ inch or more, and fine screens have openings of less than ¹/₄ inch. The principle types of screening devices in use are described in table (3-1) and illustrated in Figures (3-1 & 3-2).

The aquarake is a self cleaning filter system, which can be installed directly into an open channel. While, the vibrating curved screen uses a motor, which vibrates the screen. This vibrator ensures a clog free screen and quicker removal of solids from the screen. The vibrating curved screen can also be equipped with a spray-cleaning device.

In the rotary screen the water flows from the top through a rotating drum and leaves the drum from the inside to the outside at the bottom. The rotary screen can be equipped with a scraper blade, which intermittently cleans the drum and a spray-cleaning device if deemed necessary.

3.1.2 Oil Separation

Floatables, namely non-emulsified oil and organics, are usually the main consideration in designing industrial primary treatment devices, rather than settleables. For this reason, most refineries, many chemical plants, and other industrial facilities use oil-water separation devices instead of primary clarifiers.

> API separators

An API separator is an oil-water separator that is designed to American Petroleum Institute "API" standards, and is used extensively in refineries and many other industrial plants. There are standards for both rectangular and circular units, however, one rarely finds circular units in the field as the size of most units is more compatible with the rectangular configuration. These units frequently handle storm flows and storm flows can impose a very high flow rate, relative to process flows, on the unit, requiring a large unit. In general, this separator can handle very large flow. However, its disadvantage is the long retention time required for efficient oil separation.

CPI Units

Corrugated Plate Interceptors (CPI), sometimes called Tilted Plate Interceptors (TPI), are replacements for API separators and primary clarifiers. They consist of stacks of plates or bundles of tubes slanted, usually at 60 degrees, in a vessel or tank. It has been found that if the plates are titled at 60 degrees, the solids will slide down the plates and be collected at the bottom. A cross section in a typical down flow of CPI unit are shown in figure (3-3).

The projected horizontal area of the plates form the settling surface, thus a CPI surface area can be placed in a small space.

CPIs are widely used for oil-water separation in many industries, but have found only limited acceptance in refineries. The reason is the units cannot take shock loads and high flows as well as a conservatively designed API separator, and oil in refinery wastewater usually separates quite well not requiring the large surface or coalescing area. They have some advantages over API Separators. They are usually more efficient than API separators and primary clarifiers in removing oil and solids, as more surface area can be provided.

3.1.3 Flow Equalization

Flow equalization is used to overcome the operational problems caused by flow variations, to improve the performance of the downstream processes, and is also used as an emergency tank to equalize wastewater effluent in case of any process failure in the treatment process.

Flow equalization simply is the damping of flow rate variations so that a constant or nearly constant flow rate is achieved. This technique can be applied in a number of different situations, depending on the characteristics of the collection system.

The principal benefits that are cited as deriving from the application of flow equalization are as follows:

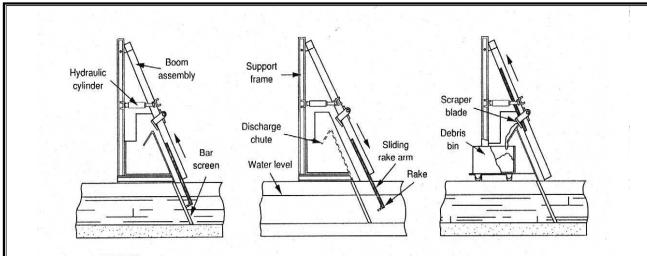
- Wastewater treatability is enhanced after equalization.
- Biological treatment is enhanced, because shock loading is eliminated or can be minimized, inhibiting substances can be diluted, and pH can be stabilized.
- The effluent quality and thickening performance of secondary sedimentation tanks following biological treatment is improved through constant solids loading.
- Filter performance is improved and more uniform filter backwash cycles are possible.
- In chemical treatment, damping of mass loading improves chemical feed control and process reliability.

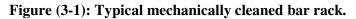
Flow equalization is an attractive option for upgrading the performance of overloaded treatment plants because of the relatively low costs involved.

The best location for equalization facilities to be at existing and proposed treatment – plant sites. In some cases, equalization after primary treatment and before biological treatment may be appropriate but the design must provide for sufficient mixing to prevent solids deposition and concentration variations and also to provide aeration to prevent odor problems.

Screening Surface								
Type of screen	Size classification	Size range in ^a	Screen material	Application				
Bar rack	Coarse	0.6 – 1.5	Steel, Stainless steel	Pretreatment				
Inclined:								
Fixed	Medium	0.01 - 0.1	Stainless-steel wedge-wire screen	Primary treatment				
Rotary	Coarse	0.03×0.09×2	Milled bronze or copper plates	Pretreatment				
	Coarse	0.1 - 0.2	Stainless-steel wedge wire cloth	Pretreatment				
Drum (rotary)	Medium	0.01 - 0.1	Stainless-steel wedge-wire screen	Primary treatment				
Drum (roury)	Fine	6-35 µm	Stainless-steel and polyester screen cloths	Removal of residual secondary suspended solids				
Potomy disk	Medium	0.01 - 0.4	Stainless-steel	Primary treatment				
Rotary disk	Fine	0.001 - 0.02	Stainless-steel	Primary treatment				
Centrifugal	Fine	0.002 - 0.02	Stainless-steel, polyester and various other fabric screen cloths.	Primary treatment, secondary treatment with settling tank and the removal of residual secondary suspended solids				

Table (3-1) Types of Mechanical Screens





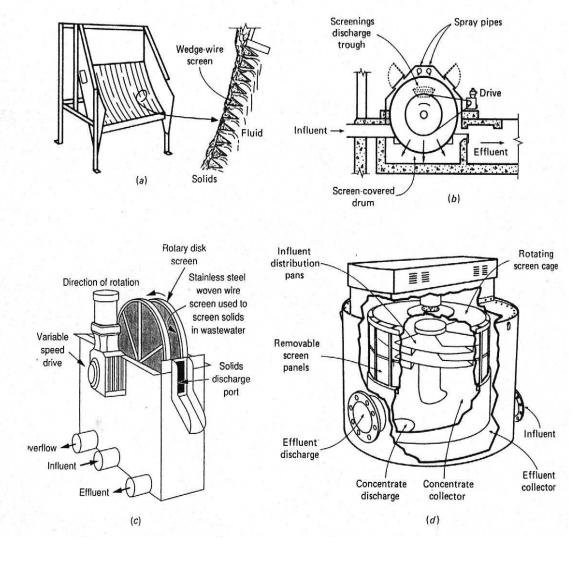
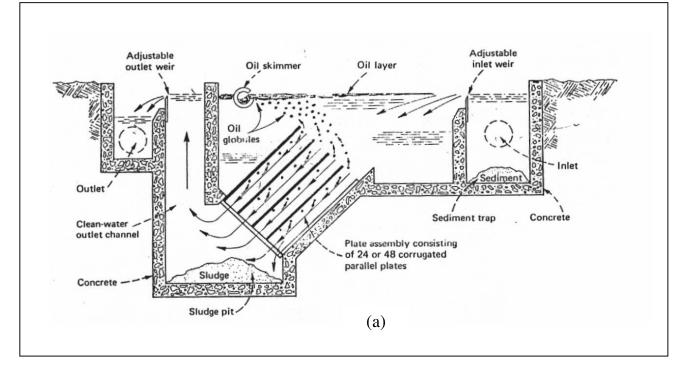


Figure 3-2: Typical screening devices used for wastewater treatment: (a) inclined fixed screen (shown with cover removed, and (b) rotary drum screen, (c) rotary disk screen, and (d) centrifugal screen 17



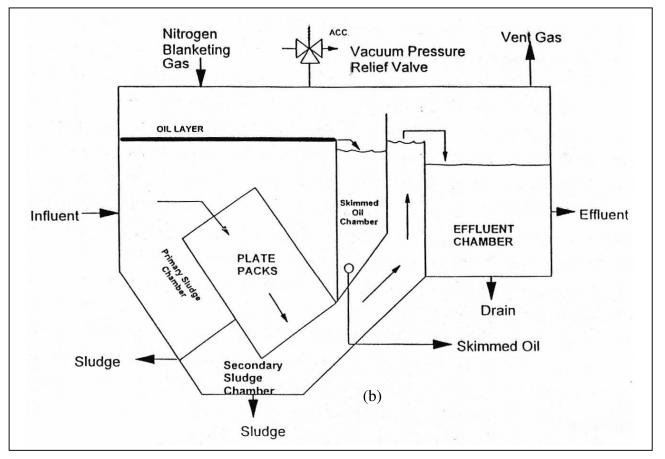


FIGURE (3-3)

- (a): Corrugated plate Interceptor (CPI) for refinery wastewater
- (b): Cross section of a typical down flow (CPI)

3.2 PHYSICAL TREATMENT

3.2.1 Sedimentation

Sedimentation is the separation from water, by gravitational settling, of suspended particles that are heavier than water. It is one of the most widely used unit operations in wastewater treatment. The terms sedimentation and settling are used interchangeably. A sedimentation basin may also be referred to as a sedimentation tank, settling basin, or settling tank.

Sedimentation is used for separation of grit & particulate-matter in the primary settling basin, separation of biological-floc in the activated-sludge settling basin, and separation of chemical-floc when the chemical coagulation process is used. It is also used for solids concentration in sludge thickeners.

Sedimentation basins are often referred to as either clarifiers or thickeners. If the main purpose of the operation is to produce an effluent stream with low suspended solids, the vessel is usually called a clarifier. If the major concern is the production of a concentrated suspension, the vessel is normally called a thickener. The terms clarifier and thickener are often used interchangeably in describing settling tanks for effluent streams from activated sludge reactors since both clarification and thickening occur in any sedimentation basin.

In wastewater treatment plants, sedimentation is applied to separate a variety of organic and inorganic solids from raw or treated wastewaters.

Primary settling tanks are used to remove solids from the waste stream entering the plant. Secondary settling tanks handle the solids in the effluent from a biological reactor.

The settling characteristics of suspended particles depend upon the nature of the particles, their concentration and the conditions in the settling device

Ideal settling basins

An ideal settling basin is defined as a tank in which settling occurs in the same manner as in a quiescent settling container of the same depth. A schematic diagram of a rectangular horizontal flow-settling basin is shown in Fig. (3-4).

This basin is comprised of four zones according to function. The inlet zone is a region where the incoming suspension is distributed uniformly over the cross-section of the tank. Thus, the concentration of suspended particles of each size is the same at all points in the vertical cross-section at the inlet end.

In the settling zone, the particles settle at the same rate as they would in a quiescent. At the outlet zone, the clarified liquid is collected uniformly over the cross-section of the basin. The solids collect in a sludge zone at the bottom of the tank. All particles reaching the sludge zone are permanently removed from suspension.

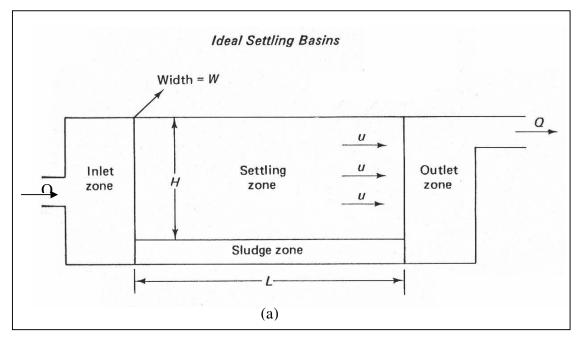


Figure (3-4) Schematic diagram of a rectangular horizontal flow-settling basin.

Tube settlers

If the tubes are horizontal or slightly inclined, the solids will accumulate on the bottom and must be removed by periodical draining. If the tubes are inclined at a steep angle, the solids will slide down the tubes countercurrent to the liquid flow and can be collected at the bottom.

Thickeners

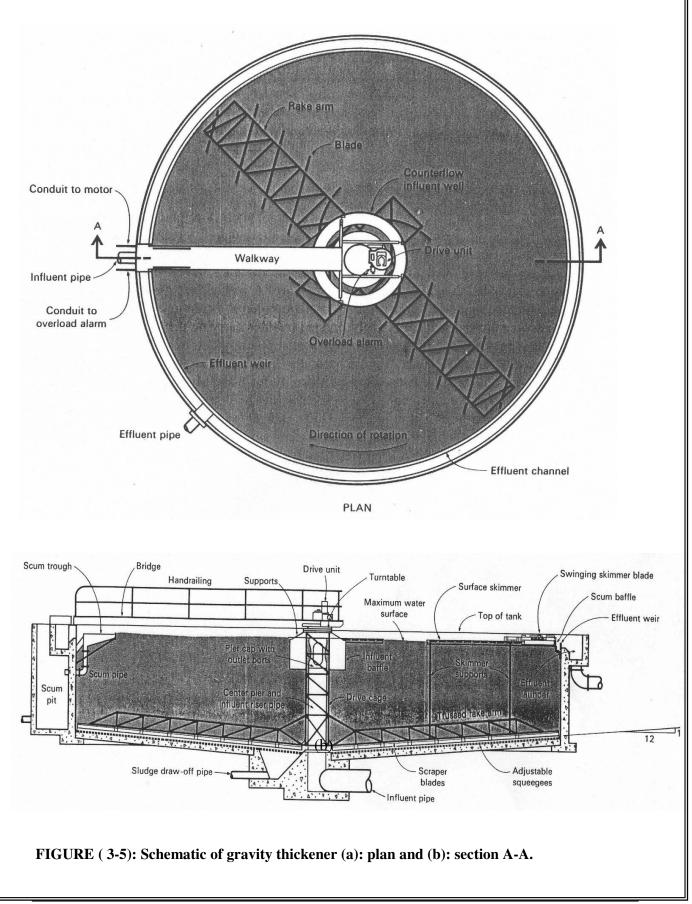
A thickener is a sedimentation basin that is used to concentrate a suspension. The particles in a thickener generally settle collectively in the zone-settling regime. As shown in Figure (3-5), the bottom part of a thickener is filled with a bed of suspended solids, which increases in concentration with greater depths. A clarified liquid separates from the suspended solids at the interface and the clear liquid is removed at the top. A thickener thus fulfills the dual function of providing a concentrated underflow and a clarified liquid overflow.

A thickener is often used to concentrate the solids in the effluent stream of an activated sludge reactor. Part of the concentrated underflow is generally recycled to the reactor to maintain a high concentration of biological solids in the reactor.

Sedimentation basins are constructed in a variety of shapes and sizes, circular tanks or rectangular tanks. Solids are removed either by mechanical devices, which move the solids to a central collection point, or by hydraulic collectors, which remove the solids near the point of deposit.

Primary sedimentation basins generally remove 40 to 65% of suspended solids along with 25 to 50% of BOD₅ Settled solids concentration usually range from 4 to 10% for primary sedimentation basins and from 0.5 to 2% for thickeners handling effluent from activated sludge reactors.





3.2.2 Flotation

Flotation is a unit operation used to separate solid or liquid particles from a liquid phase. Separation is brought by introducing fine gas (usually air bubbles) into the liquid phase. The bubbles attach to the particulate matter, and the buoyant force of the combined particle and gas bubble is great enough to cause the particle to rise to the surface. Particles that have a higher density than the liquid can thus be made to rise.

Flotation is used to remove suspended matter and to concentrate biological sludge. Principal advantage of flotation over sedimentation is that very small or light particles that settle slowly can be removed more completely and in a shorter time. Once the particles have been floated to the surface, they can be collected by a skimming operation.

Types of flotation systems

Air Flotation:- In this system, as shown in figure (3-6) air bubbles are formed by introducing the gas phase directly into the liquid phase through a revolving impeller through diffusers. Aeration alone for a short period is not particularly effective in bringing about the flotation of solids, although some success with these units has been experienced on certain scum-forming wastes.

Vacuum Flotation:- This process consists of saturating the wastewater with air either directly in an aeration tank or by permitting air to enter on the suction side of a sewage pump. The bubbles and the attached solid particles rise to the surface to form a scum blanket, which is removed by a skimming mechanism. Grit and other heavy solids that settle to the bottom are raked to a central sludge for removal.

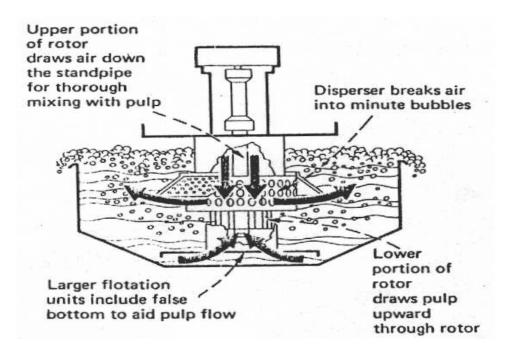


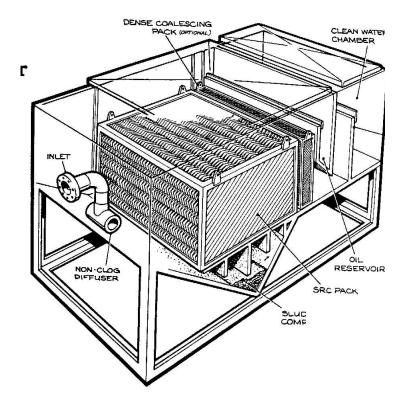
Figure (3-6) Induced Air Flotation for Oily Wastes & Suspended Solids.

3.2.3 Coalescence

Coalescence are also used for removal of low concentrations of free and emulsified oil, and are used as a single unit process or are used to polish effluents from other types of oil- water separators. Coalescence as shown in figure (3-7) is merely beds of oleophilic material such as shells, resins, straw, plastics in shredded form, ball, or packing ring form. The oleophilic material attracts small free oil droplets and can also attract some types of emulsified oils. The oil coalesces on the material into larger drops and rises to the surface.

Figure (3-7)

Figure (3-7) Slant Rib Coalescing Separator



3.3 CHEMICAL TREATMENT

3.3.1 Chemical Pre-treatment

Neutralization

Industrial wastewaters often contain acidic or alkaline components which require neutralization before discharge or treatment. For wastewater discharged to receiving waters, a pH between 6 and 9 is frequently specified by regulatory agencies. For wastewater entering biological treatment processes, the pH should be maintained between 6.5 and 8.0 for optimum growth of the microorganisms. Aerobic biological processes generate CO₂, which also affects the pH of the system. Spent acid, especially sulfuric acid, constitutes the majority of plant wastewater requiring neutralization. Lime is the most widely used alkaline material for neutralization acid wastes because of its low cost. The solid lime, however, maybe slow to react and may form insoluble precipitates such as CaSO₄.

Sodium carbonate (soda ash), sodium hydroxide, and ammonia react faster with acids than lime but they are more expensive. Alkaline wastewater are usually neutralized with sulfuric acid or with waste acids from other operations. A flue gas can also be used to neutralize alkaline wastes since the CO_2 in flue gas forms carbonic acid when contacted with water.

Neutralization is probably the oldest and most frequent of chemical methods of acidic and alkaline waste streams to keep the pH of the effluent in the range of 6 to 8 required by many regulatory agencies. Many chemical wastewater streams exceed these limits and fluctuate sharply with time.

Acidic wastewater is commonly neutralized with waste alkaline streams, lime, dolomite, ammonia, caustic soda, or soda ash. The choice of the alkaline regent used depends on the volume of the waste stream, the variability of pH, and the price of the neutralizing alkali. Lime is most often used, despite the frequent formation of precipitates or suspended solids, which must be separated by sedimentation or filtration before the wastewater is discharged to the receiving waters because of its low cost.

Highly alkaline wastes usually require treatment with a wastewater acidic stream, sulfuric acid, hydrochloric acid, or flue gas containing carbon dioxide.

Neutralization is usually accomplished in two steps since pH varies in concentration increments of 10: rough neutralization with wastewater streams or with cheap chemicals, followed by final polishing, often with instrumented controls, using caustic soda solutions or sulfuric acid.

> Oxidation/Reduction

Oxidants are used in wastewater treatment as a first step in the removal of heavy metals to oxidize organics or as a last step in a treatment process, to oxidize odoriferous compounds such as hydrogen sulphide or to oxidize inorganics such as cyanide and for disinfection.

Air is the least expensive and most common oxidant. Ferrous iron is readily oxidized to the ferric state by contact with air. This is usually accomplished with oxidation towers that are similar in construction to cooling towers. Other chemical oxidants are chlorine and its variant hypochlorite in both sodium and calcium versions. Another widely used oxidant is potassium permanganate, chlorine and its variants have been alleged to form carcinogenic compounds when used to oxidize organics. Before using chlorine in a process, even a non-wastewater process, it would be well to check to see if any carcinogens could be formed. Potassium permanganate is used to oxidize odoriferous compounds and for organics reduction. Hydrogen peroxide is effective in

reducing organics such as COD, and is worth considering when faced a COD, organic or odor reduction problem.

Coagulation

It takes place in rapid mix, or flash mix basins they are very rapid, the primary function of rapid mix basin is to disperse the coagulant so that it contacts all of the wastewater.

Two theories have been advanced to explain basic mechanisms involved in the stability and instability of colloid systems.

• Chemical theory assumes that colloids are aggregates of definite chemical structural units, it occurs because of specific chemical reactions between colloidal particles and the chemical coagulant added.

• Physical theory proposes that reduction of forces tending to keep colloids apart occurs through the reduction of electrostatic forces, such as the zeta potential good coagulation, flocculation and sedimentation is difficult to obtain in wastewater treatment.

Flocculation

The purpose of flocculation is to form aggregates or flocs from the finely divided matter. The flocculation of wastewater by mechanical or air agitation may be worthy of consideration when it is desired to: -

- Increase the removal of suspended solids and BOD₅ in primary settling facilities.
- Condition wastewater containing certain industrial wastes.

• Improve the performance of secondary settling tanks, especially the activated sludge process also to increase the collisions of coagulated solids, they agglomerate to form settleable or filterable solids. It is accomplished by prolonged agitation of coagulated particles in order to promote an increase in size and density.

It can be carried out in a separate basin of an integral part of the clarifier structure. Air flocculation is employed, the air supply system should be adjusted so that the flocculation energy level can be varied throughout the tank. In both mechanical and air agitation flocculation systems .It is common practice to taper the energy input so that the flocs initially formed will not be broken as they leave the flocculation facilities.

3.3.2 Chemical Precipitation

Chemical precipitation in wastewater treatment involves the addition of chemicals to alter the physical state of dissolved and suspended solids and facilities their removal by sedimentation. In some cases the alteration is slight, and removal is effected by entrapment within a voluminous precipitate consisting primarily of the coagulant itself. Another result of chemical addition is a net increase in the dissolved constituents in the wastewater.

In the past, chemical precipitation was used to enhance the degree of suspended solids and BOD_5 removal (1) where there were seasonal variations in the concentration of the wastewater (such as in cannery wastewater), (2) where an intermediate degree of treatment was required, and (3) as an aid to the sedimentation process. The need to provide more complete removal of the organic compounds and nutrients (nitrogen and phosphorus) contained in wastewater has brought about renewed interest in chemical precipitation. Chemical processes in conjunction with various chemical operations have been developed for the complete secondary treatment of under treatment wastewater, including the removal of either nitrogen or phosphorus or both. Other chemical processes have also been developed to remove phosphorus by chemical precipitation and are designed to be used in conjunction with biological treatment.

26

Chemical Precipitation for improving plant performance

Over the years a number of different substances have been used as precipitants.

The most common ones are listed in Table (3-2). The degree of clarification obtained depends on the quantity of chemicals used and the care with which the process is controlled. It is possible by chemical precipitation to obtain a clear effluent, substantially free from matter in suspension or in the colloidal state.

From 80 to 90 percent of the total suspended matter, 50 to 80 percent of the BOD_5 and 80 to 90 percent of the bacteria can be removed by chemical precipitation. In comparison, when plain sedimentation is used, only 50 to 70 percent of the total suspended matter, 25 to 40 percent of the BOD_5 and 25 to 75 percent of the bacteria can be removed.

The chemicals added to wastewater interact with substances that are either normally present in the wastewater or added for this purpose in order to maintain chemical precipitation.

Chemical	Formula	Molecular Weight
Alum	Al ₂ (SO ₄) ₃ .18H ₂ O	666.7
Ferrous Sulfate	FeSO ₄ .7H ₂ O	278.0
Lime	Ca(OH) ₂	56 as CaO
Ferric Chloride	FeCl ₃	162.1
Ferric Sulfate	$Fe_2(SO_4)_3$	400

Table (3-2): Chemicals used in industrial wastewater treatment

3.3.3 Physico Chemical Treatment

Dissolved Air Flotation (DAF) System

In dissolved air flotation (DAF), air is intimately contacted with an aqueous stream at high pressure, dissolving the air. The pressure on the liquid is reduced through a back pressure valve, thereby releasing micron-sized bubbles that sweep suspended solids and oil from the polluted stream to the surface of the air-flotation unit. The produced from is skimmed.

Applications include treating effluents from refinery API separators, metal finishing, pulp and paper industry, cold-rolling mill, poultry processing, grease recovery in meat-packing plants, cooking-oil separation from French-fry processing and some dairy industries. An increasingly important application is the thickening of sludge.

DAF units usually remove oil down to 5 ppm or less, and the released air may have to be treated in a control unit.

DAF units are generally sized with an overflow rate of 1500 to 3000 gal. /day/sq.ft. and a retention time of 30 to 40 minutes.

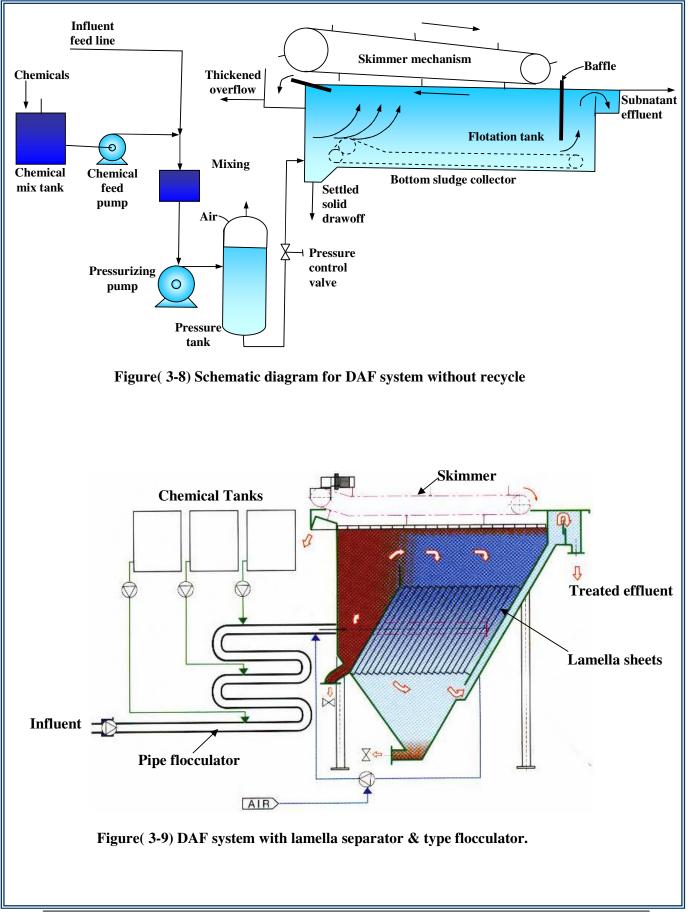
A variant of the DAF unit that is commonly used in oil fields and for ballast water treatment is the Induced Air Floatation (IAF) unit. In the past it was rarely used in chemical plants and refineries but interest in it is increasing because the unit is totally enclosed and can use recycled gases for floatation. The unit utilizes polymer feed and usually has four eggbeater type frothing units for floatation. The unit has a high power consumption, but uses much less space than a DAF Unit. It is as efficient or more efficient than a DAF unit depending on oil and emulsion characteristics. Attachment of gas bubbles to suspended-solids/gas mixture is carried to the vessel surface after accumulation of air on the particle; collision of a rising bubble with a suspended particle; trapping of gas bubbles, as they rise, under a floc particle; and adsorption of the gas by a floc formed or precipitated around the air bubble.

To dissolve air for flotation, three types of pressurized systems are used. Full-flow or total pressurization is used when the wastewater contains large amounts of oily material. The intense mixing occurring in the pressurization system does not affect the treatment results. Partial-flow pressurization is used where moderate to low concentrations of oily material is present. Again, intense mixing by passage through the pressurization systems does not affect treatment efficiency significantly. The recycle-flow pressurization system is for treatment of solids or oily materials that would degrade by the intense mixing in the other pressurization systems. This approach is used following chemical treatment of oil emulsions, or for clarification and thickening of flocculent suspensions.

A schematic drawing of dissolved-air flotation system is shown in Fig (3-8). The solids-laden or oily-water influent mixture enters the flotation vessel, and the air solids or oily-water mixture rises to the liquid surface. The air-solids or oily- water mixture has a specific gravity less than water. Solids having a specific gravity greater than water tend to settle to the bottom and are removed by a rotating scraper arm. Attached to the same shaft is a rotating skimmer blade that removes the flotating matter from the surface of the vessel into a skimming hopper. Clean water passes underneath a skirt and then must leave the vessel through a launder, which is located in the peripheral region.

A portion of the effluent water is recycled for pressurization. Compressed air is introduced into the discharge of the recycle pump, and intimate contact with the water is achieved in the aeration tank. Maximum solubilization efficiency is important at this point. The aerated recycle water is then returned through a back-pressure valve, where the pressurized air is released, and mixed with the influent for flotation.

Floccultants such as synthetic polymers may be used to improve the effectiveness of dissolved air flotation. Also coagulants such as filter alum may be used to break emulsified oils and to coagulate materials for improved flotation recovery. DAF unit is equipped sometimes with a Lamella plate as shown in figure (3-9) which increases the separation area, and to ensure that even the smallest flocs are removed from the wastewater.



3.4. BIOLOGICAL TREATMENT

The major biological processes used for wastewater treatment are five major groups: aerobic processes, anoxic process, anaerobic process, combined aerobic anoxic and anaerobic/aerobic processes.

3.4.1 Aerobic Biological Treatment

The aerobic biological processes are further subdivided depending on whether treatment is accomplished in suspended-growth systems, attached-growth systems, or combinations thereof. All the biological processes used for the treatment of wastewater are derived from processes occurring in nature.

A) Aerobic suspended growth:-

- Activated sludge Processes
- Plug flow with recycle
- Aerated lagoons.
- ► SBR

B) Aerobic attached growth:-

- Trickling filter
- Roughing filter
- Rotating biological contactor.
- Fixed film nitrification reactor.

A) Aerobic suspended growth

Activated-Sludge Process

Activated sludge is a secondary treatment process in which wastewater has normally received primary sedimentation is allowed to flow through the aeration tank or "reactor" where aerobic bacterial culture is maintained in suspension. The reactor contents are referred to as the "mixed liquor"

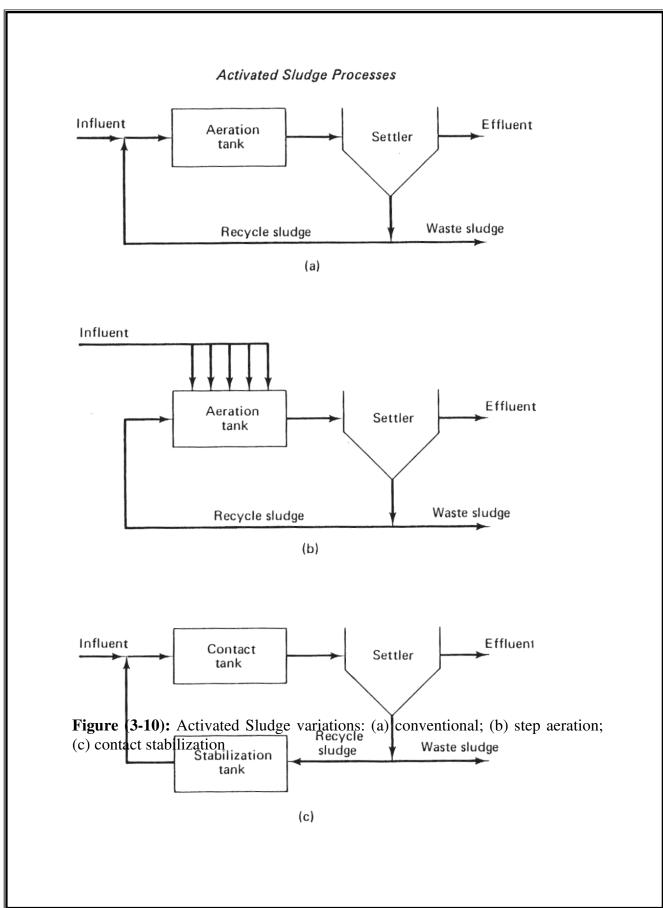
The aerobic environment in the reactor is achieved by the use of diffused or mechanical aeration, which also serves to maintain the mixed liquor in a completely mixed regime. After a specified period of time, the mixture of new cells and old cells is passed into a settling tank, where the cells are separated from the treated wastewater. A portion of the settled cells is recycled to maintain the desired concentration of organisms in the reactor, and a portion is wasted. The portion wasted corresponds to the new growth of cell tissue, associated with a particular wastewater.

The major types of activated sludge treatment processes used for secondary treatment are:-

- Conventional Activated Sludge and variation of the conventional systems.
- Extended Aeration.

Conventional Activated Sludge

The conventional activated sludge system contains a tank for wastewater aeration followed by a settler and a solids recycle line. The wastewater flows through under constant aeration in the presence of activated sludge and exits at the end of the tank after 4-8 hours of residence time. As the flow passes through the tank, the high oxygen demand gradually will decrease. The oxygen concentration in the reactor should be 0.5-2 mg/l throughout, where values over 2 mg/l are considered lost energy. Most conventional plants use tapered aeration to adjust the air rate along the reactor length to satisfy the local oxygen demand. A process flow diagram for different conventional treatment systems are shown in figure (3-10).



Extended Aeration

This is the modified form of a conventional activated sludge process in which the production of excess sludge is minimized by oxidation and an increase in residence time, i.e. through the larger size of the aeration tank. The retention time is extended to 1-2 days, which results in a very low net yield of sludge due to its consumption by endogenous respiration. The main advantage of the extended aeration system is in having the minimum of sludge handling facilities as compared with other conventional activated sludge processes.

The sludge in extended aeration effluents is very light, of non-degradable nature, and settles with difficulty. Therefore, settling tanks are provided with a longer retention time of approximately 4 hours versus 2 hours for the conventional treatment process.

Plug flow with recycle

The plug-flow system with cellular recycle can be used to model certain forms of the activatedsludge process. In a true plug-flow system, all the particles entering the reactor stay in the reactor an equal amount of time. Some particles may make more passes through the reactor because of recycle, but, while they are in the tank, they all pass through in the same amount of time. The true plug-flow-recycle system is theoretically more efficient in the stabilization of most soluble wastes than the complete-mix recycle system. However, the plug-flow system cannot handle shock loads as well as the complete-mix system.

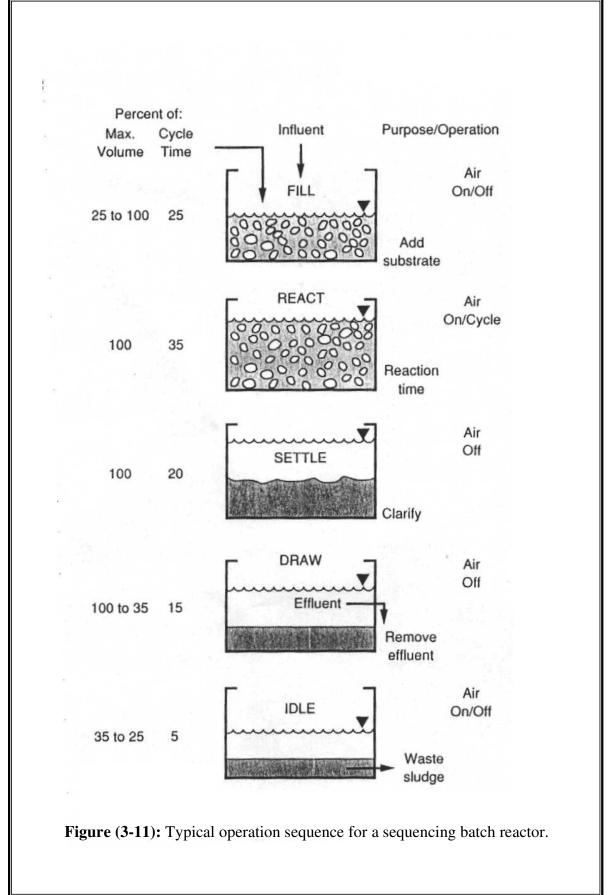
Aerated Lagoons

Aerated lagoons (sometimes called "aerated ponds") evolved from facultative stabilization ponds when surface aerators were installed to overcome the odors from organically overloaded ponds. The aerated-lagoon process is essentially the same as the conventional extended-aeration activated-sludge process, except that an earthen basin is used for the reactor, and the oxygen required by the process is supplied by surface or diffused aerator. In aerobic lagoon, all the solids are maintained in suspension. In the past, aerated lagoons were operated as flow-through activated-sludge systems without recycle, usually followed by large settling ponds, many aerated lagoons are now used in conjunction with settling facilities and incorporate the recycle of biological solids.

Sequential Batch Reactor "SBR"

Sequential Batch Reactor (SBR) is a fill-and-draw activated-sludge treatment system. The unit processes involved in the SBR and conventional activated-sludge systems are identical. Aeration and sedimentation/clarification are carried out in both systems. However, there is one important difference. In conventional plants, the processes are carried out simultaneously in separate tanks, whereas in SBR operation the processes are carried out sequentially in the same tank.

As currently used, all SBR systems have five steps as illustrated in figure (3-11) and shown in table (3-3) and in common that are carried out in sequence as follows: (1) fill, (2) react (aeration), (3) settle (sedimentation/clarification), (4) draw (decant), and (5) idle. Sludge wasting is another important step in the SBR operation that greatly affects performance. In an SBR operation, sludge wasting usually occurs during the settle or idle phases. A unique feature of the SBR system is that there is no need for a return activated-sludge (RAS) system. Because both aeration and settling occur in the same chamber, no sludge is lost in the react step, and none has to be returned from the clarifier to maintain the sludge content in the aeration chamber. All wastewaters commonly treated by conventional activated-sludge plants can be treated with SBRs.



Operational step	Description		
Fill	The purpose of the fill operation is to add substrate (raw wastewater or primary effluent) to the reactor. The fill process typically allows the liquid level in the reactor to rise from 25 percent of capacity (at the end of idle) to 100 percent. If controlled by time, the fill process normally lasts approximately 25 percent of the full cycle time.		
React	The Purpose of react is to complete the reactions that where initiated during fill. Typically, react takes up 35 percent of the total cycle time.		
Settle	The purpose of settle is to allow solids separation to occur. Providing a clarified supernatant to be discharged as effluent. In an SBR, this process is normally much more efficient than in a continuous flow system because in the settle mode the reactor contents are completely quiescent.		
Draw	The purpose of draw is to remove clarified treated water from the reactor. Many types of decant mechanisms are in current use, with the most popular being floating or adjustable weirs. The time dedicated to draw can range from 5 to 30 percent of the total cycle time (15 minutes to 2 hours), with 45 minutes being a typical draw period.		
Idle	The purpose of idle in a multi tank system is to provide time for one reactor to complete its fill cycle before switching to another unit. Because idle is not a necessary phase, it is sometimes omitted.		

Table (3-3) Description of the operation steps for the sequencing batch reactor

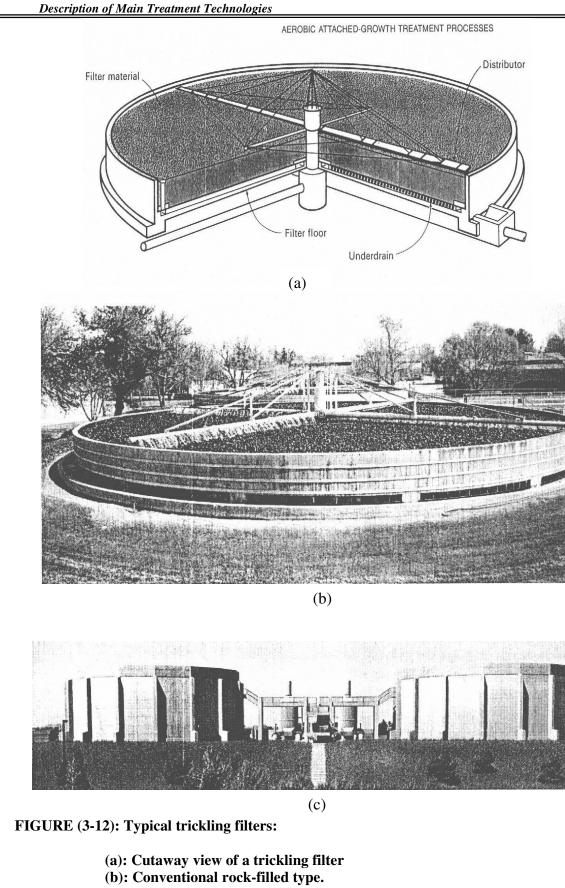
B- Aerobic Attached – Growth Treatment Processes

Aerobic attached-growth biological treatment processes are usually used to remove organic matter found in wastewater. They are also used to achieve nitrification. The attached – growth processes include the trickling filter, the roughing filter, rotating biological contactor, and fixed-film nitrification reactor.

Trickling Filter "Biological Air Filters"

The concept of a trickling filter grew from the use of contact filters, which were watertight basins filled with broken stones. In operation, the contact bed was filled with wastewater from the top, and the wastewater was allowed to contact the media for a short time. The bed was then drained and allowed to rest before the cycle was repeated, A typical cycle required 12 hours (6 hours for operation and 6 hours of resting). The limitations of the contact filter included a relatively high incidence of clogging, the long rest period required, and the relatively low loading that could be used.

The modern trickling filter figure (3-12) consists of a bed of a highly permeable medium to which microorganisms are attached and through which wastewater is percolated or trickled.. The filter media usually consist of either rock (slag is also used) or a variety of plastic packing materials. In rock-filled trickling filters, the size of the rock typically varies from 1 to 4 in (25 to 100mm) in diameter. The depth of the rock varies with each particular design but usually ranges from 3 to 8 ft (0.9 to 2.5m) and average 6-ft (1.8 m). Rock filter beds are usually circular, and the liquid wastewater is distributed over the top of the bed by a rotary distributor.



(c): Tower trickling filters.

35

Trickling filters that use plastic media have been built in round, square, and other shapes with depths varying from 14 to 40 ft (4 to 12m). Three types of plastic media are commonly used: (1) vertical-flow packing cross-flow packing a variety of random packing.

The collected liquid is passed to a settling tank where the solids are separated from the treated wastewater. In practice, portion of the liquid collected in the under drain system or the settled effluent is recycled, usually to dilute the strength of the incoming wastewater and to maintain the biological slime layer in a moist condition.

Roughing Filters

Roughing filters are specially designed trickling filters operated at high hydraulic loading rates. Roughing filters are used principally to reduce the organic loading on downstream processes and in seasonal nitrification applications where the purpose is to reduce the organic load so that a downstream biological process will dependably nitrify the wastewater during the summer months.

Although the earliest roughing filters were shallow, stone media systems, the present trend is toward use of synthetic media or redwood at depths of 12 to 40 ft.

Packed-Bed Reactors

Still another attached-growth process is the packed-bed reactor, used for both the removal of carbonaceous BOD_5 and nitrification. Typically, a packed-bed reactor consists of a container (reactor) that is packed with a medium to which the microorganisms can become attached. Wastewater is introduced from the bottom of the container through an appropriate under drain system or inlet chamber. Air or pure oxygen necessary for the process is also introduced with the wastewater.

In the past ten years a number of different anaerobic process have been developed for the treatment of sludge and high-strength organic wastes. The most common anaerobic suspended-growth process used for the treatment of wastewater is complete-mix anaerobic digestion process.

3.4.2 Anaerobic Biological Treatment

The anaerobic process has been developed for the treatment of sludge and high strength organic load.

The disadvantages and advantages of the anaerobic treatment as compared to aerobic treatment that the slow growth rates required a relatively long detention time in the digester for adequate waste stabilization to occur. Most of the organic waste is converted to methane gas, which is combustible and therefore a useful end product. The high temperature necessary to achieve adequate treatment are often listed as disadvantages of the anaerobic treatment process; however, high temperature are necessary only when sufficiently long mean cell-residence time cannot be obtained at nominal temperatures.

a) Anaerobic Contact Process

Some industrial wastes that are high in BOD_5 can be stabilized very efficiently by anaerobic treatment. In the anaerobic contact process, untreated wastes are mixed with recycled sludge and then digested in a reactor sealed off from the entry of air. After digestion, the mixture is separated in a clarifier or vacuum flotation unit, and the supernatant is discharged as effluent, usually for further treatment. Settled anaerobic sludge is then recycled to seed the incoming wastewater.

3.4.3 Pond Treatment Processes

Ponds systems can be classified as (1) aerobic, (2) maturation, (3), facultative, and (4) anaerobic with respect to the presence of oxygen. Among those, the most commonly process used in the Egyptian Industry is the aerobic stabilization pond.

a) Aerobic Stabilization Ponds

In their simplest form, aerobic stabilization ponds are large, shallow earthen basins that are used for the treatment of wastewater by natural processes involving the use of both algae and bacteria.

Tables (3-4 & 3-5) illustrate the main treatment technologies in Egypt, advantage, typical risks and problems for each type and applicability in different industries in Egypt.

Treatment	Advantage	Typical Risks & Problems	Key operation parameters	Monitoring parameter
Screening	Remove large suspended particles and consequently partially reduce pollution load. -Flow Homogenization	Blockage, overflows or odor problem could arise due to infrequent cleaning.	T.S.S	T.S.S
API & CPI separators	Simple design Handle larger capacity. Minimum mechanical & electrical equipment requirements. Low operation & maintenance cost.	Large area requirement Limited to removal of free O&G	Free O&G	Free O&G
Flow Equalization	Reduce size and cost of downstream treatment facilities.	It needs large area in case of high flow rate. Anaerobic condition if not aerated	Retention time	Turbidity
Settling Basins	Easy to operate. Steadiness of treatment operations (Reduce shock loads)	Improper control over sedimentation tanks may cause solids and BOD overloading problems. Fouling Large area requirement.	T.S.S COD	T.S.S

Table (3-4) Main Treatment Technology, Advantage & Disadvantage

Lamella separator	Higher separation efficiency. Easy discharge of settled sludge. Less area required	Cleaning problems	T.S.S, COD	T.S.S
Coalescence	Small & compact Easy operation & maintenance. Low cost.	Limited capacity. Partial removal of emulsified oil	Total O&G	Total O&G
DAF System	Remove both free and emulsified oil. Remove both floating and settable solids. Very small and light particles can be removed completely in short time.	High chemical consumption. Relatively high sludge formation	O&G T.S.S COD	T.S.S Total O & G
Conventional Activated Sludge	Low land required No problems of fly	High-energy consumption. Sludge bulking. Need very highly skilled professionals to operate.	MLSS, MLVSS, DO levels	BOD
Extended Aeration System	Sludge is partially digested within air tank. More resistance to incoming shock load.	Retention time in final clarifier twice that of conventional system.Higher consumption of oxygen.	MLSS, MLVSS, DO levels	BOD
Aerated Pounds	Good BOD removal.	Higher sludge production. High suspended solids in effluent	DO levels	BOD

SBR	Higher Efficiency Save on area as no separate clarifier. Less sludge formation	High power consumption. Failure if any problem occurs in the automatic control system.	S.S, COD	COD
Trickling Filter.	Low equipment and power cost. Shock loading can be absorbed. Minimum sludge produce.	Fly and odor nuisance. Limited capacity pounding and clogging of filters.	BOD COD	BOD COD
Bio tower	Minimum sludge formation. Vertical design, less area required	Fly and odor nuisance. Limited capacity pounding and clogging of filters. Limited capacity	R.O	COD
Anaerobic Treatment	High organic pollution load. Less sludge production.	Biogas production. Temperature required (30°C). Very sensitive to shock load	T.S.S, BOD, COD	BOD

Treatment	Applicability in Egypt	
Screening	Food Industries (Edfina for Preserved Food Company)	
	Textiles Industries (El Nasr Wool and Selected Textile Company – STIA)	
API & CPI separators	Amria Oil Refineries.	
	Suez Oil Refineries. Sumed.	
Flow Equalization	Dairy Industries (Siclam for Dairy Products)	
Settling Basins	Textile Industries (UNIRAB)	
Lamella separator	Pharmaceutical Industries (The Nil- Pharmaceutical Company)	
Coalescence	In several Gas Stations	
DAF System	Oil & Soap Industries (Tanta Oil & Soap Company). Food Industries (Edfina for Preserved Food Company)	
Conventional Activated Sludge	Pharmaceutical Industries (Amerya Pharmaceutical Company)	
Extended Aeration System	Pharmaceutical Industries (The Nile Pharmaceutical Company)	
Aerated Pounds	Centralized unit for Borg El Arab Industrial estate	
SBR	El Masryreen Dairy.	
Trickling Filter.	Misr Rayon, Kafr El Dawar El Nasr Spinning & Weaving, Mehalla.	
Bio tower	Carbon Black	
	Starch & Yeast Industries	

Table (3-5) Main Treatment Technology, Applicability in Egypt

3.5 COMBINATIONS OF TECHNOLOGIES COMMONLY APPLIED IN EGYPT

3.5.1 Physical / Chemical Treatment

Due to the presence of high levels of suspended particles and high levels of oil & grease, the preliminary physical treatment is carried out to reduce the pollution load prior the chemical treatment. The first treatment procedure is frequently a physical separation of insoluble or immiscible materials from the wastewater.

The industrial waste effluent is passed first through a suitable screen for debris removing then transfer to the oil trap unit to remove free oil. Clarification may be used for removing turbidity, sediment and floating material usually the first step in treatment since these impurities are

objectionable and interfere with any subsequent treatment. This step occurs before the balancing tank. The function of the balancing tank is to control fluctuation in wastewater characteristics.

In the chemical treatment, coagulant & flocculent chemicals are dosed and mechanically mixed to enhance solid coagulation flocks formation, which separated in the primary clarifier tank.

DAF unit can be used as a physical /chemical to remove suspended matter, grease and oils, organic pollution load can also substantially reduced.

3.5.2 Chemical / Biological

Due to the high level of TDS or T.S.S and to minimize the load on the biological treatment plant, chemical treatment will be carried out to reduce the pollution load.

Sand, oil and grease, other toxic materials are not allowed to enter the biological treatment plant. Otherwise they will poison and kill the useful microorganisms so, good pretreatment to the plant shall assist a good performance for long time.

From the point of view of industrial wastewater treatment, the preliminary & primary treatments are imported to allow the biological treatment under the steady conditions. The following measure are important prior the biological step:-

- * Prevention of the introduction of toxic or inhibiting substances.
- * Equalization of the wastewater inlet by buffering hydraulic or pollutant fluctuations possibly combined with aeration of the equalization basin.
- * Previous separation of inorganic and organic sediments.
- * Neutralization and buffering of pH fluctuations.

3.5.3 Anaerobic/aerobic Treatment

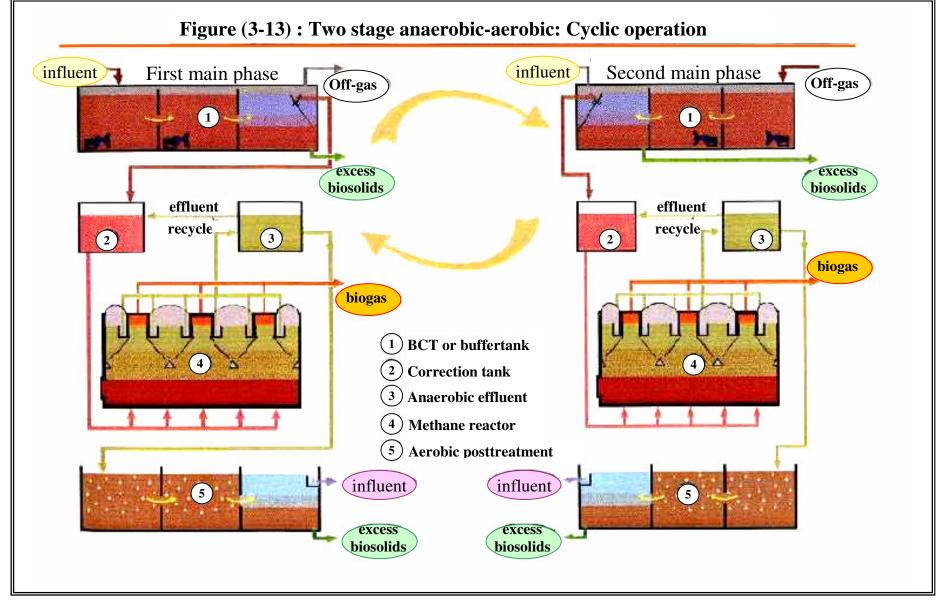
The anaerobic /aerobic treatment is used when:-

- The organic load reach a very high limited
- When the organic load contain a large fraction of complex organic matter

In the anaerobic stage the removal efficiency reaches 75-80% then the anaerobic effluent will flow to the aerobic treatment stage for consumption of the rest of organic matters.

The excess aerobic biosolids will be pumped to the aerobic sludge storage whereas the excess anaerobic biosolids will be pumped to the anaerobic sludge storage and then to the dewatering unit.

The anaerobic / aerobic treatment are very limited experience and know-how in Egypt but it is very often found in Europe or America to treat industrial wastewater with a very good performance and with the high process stability which only a two step process can guarantee. The cycle operation of the anaerobic/aerobic system is shown in figure (3-13).



3.6 SLUDGE TREATMENT AND DISPOSAL

The constituents removed in wastewater treatment plants include screenings, grit, scum, and sludge. The sludge resulting from wastewater treatment operations and processes is usually in the form of a liquid or semisolid liquid that typically contains from 0.25 to 12 percent solids by weight, depending on the operations and processes used. Sludge is by far the largest in volume, and its processing and disposal is perhaps the most complex problem facing the engineer in the field of wastewater treatment.

The problems of dealing with sludge are complex because it is composed largely of the substances responsible for the offensive character of untreated wastewater; the portion of sludge produced from biological treatment requiring disposal is composed of the organic matter contained in the wastewater but in another form which can also decompose and become offensive; and only a small part of the sludge is solid matter.

Thickening (concentration), conditioning, dewatering, and drying are used primarily to remove moisture from sludge; digestion, composting, incineration, wet-air oxidation, and vertical tube reactors are used primarily to treat or stabilize the organic material in the sludge.

3.6.1 Preliminary Operations

Sludge grinding, degritting, blending, and storage are necessary to provide a relatively constant, homogenous feed to sludge – processing facilities. Blending and storage can be accomplished either in a single unit designed to do both or separately in other plant components.

a) Sludge Grinding

Sludge grinding is a process in which large and string material contained in sludge is cut or sheared into small particles to prevent the clogging of or wrapping around rotating equipment.

b) Sludge Degritting

In some plants where separate grit removal facilities are not used ahead of the primary sedimentation tanks or where the grit removal facilities are not adequate to handle peak flows and peak grit loads, it may be necessary to remove the grit before further processing of the sludge. Where further thickening of the primary sludge is desired, a practical consideration is sludge degritting. The most effective method of degritting sludge is through the application of centrifugal forces in a flowing system to achieve separation of the grit particles from the organic sludge. Such separation is achieved through the use of cyclone degritters, which have no moving parts.

c) Sludge Blending

Sludge is blended to produce a uniform mixture to downstream operations and process. Uniform mixture is most important in short detention time systems, such as sludge dewatering, heat treatment, and incineration. Provision of a well – blended sludge with consistent characteristics to these treatment units will greatly enhance plant operability and performance.

Sludge from primary, secondary, and advanced processes can be blended in several ways:

- In Primary settling tanks
- In pipes
- In sludge processing facilities with long detention times.
- In a separate blending tank

Blending tanks are usually equipped with mechanical mixers and baffles to ensure good mixing.

d) Sludge storage

Sludge storage must be provided to smooth out fluctuations in the rate of sludge production and to allow sludge to accumulate during periods when subsequent sludge processing facilities are not operating. Sludge storage is particularly important in providing a uniform feed rate ahead of the following processes: lime stabilization heat treatment, mechanical dewatering, drying, and thermal reduction.

In small installations, sludge is usually stored in the settling tanks and digesters. In large installations that do not use aerobic and anaerobic digestion, sludge is often stored in separate blending and storage tanks. Such tanks may be sized to retain the sludge for a period of several hours to a few days. If sludge is stored longer than two or three days, it will deteriorate and will be more difficult to dewater.

3.6.2 Sludge Thickening

Thickening is a procedure used to increase the solids content of sludge by removing a portion of the liquid fraction. Thickening is generally accomplished by physical means, including gravity and flotation thickening. The gravity thickening is extensively used. While, the flotation method is not commonly used.

Gravity Thickening

Gravity thickening is accomplished in a tank similar in design to a conventional sedimentation tank. Normally, a circular tank is used.

The supernatant flow that results is returned to the primary settling tank or to the head works of the treatment plant. The thickened sludge that collects on the bottom of the tank is pumped to the digesters or dewatering equipment as required, gravity thickening is most effective on primary sludge.

3.6.3 Sludge Stabilization

Sludge is stabilized to (1) reduce pathogens, (2) eliminate offensive odors, and (3) inhibit, reduce, or eliminate the potential for putrefaction.

The technologies for sludge stabilization are (1) lime stabilization (2) heat treatment (3) anaerobic digestion, and (4) aerobic digestion. Lime stabilization is used in Egypt while the rest of methods are not commonly used.

Lime Stabilization

In the lime stabilization process, lime is added to untreated sludge in sufficient quantity to raise the pH to 12 or higher. Two methods for lime stabilization used are addition of lime to sludge prior to dewatering, termed "lime pre-treatment" and the addition of lime to sludge after dewatering, or "lime post-treatment" Either hydrated lime, Ca (OH)₂, or quicklime, CaO, may be used for lime stabilization. Fly ash, cement kiln dust, and carbide lime have also been used as a substitute for lime some cases.

Post-lime stabilization has several significant advantages when compared to pre-lime stabilization: (1) dry lime can be used: therefore, no additional water is added to the dewatered sludge; (2) there are no special requirements for dewatering; and (3) scaling problems and associated maintenance problems of lime sludge dewatering equipment are eliminated.

3.6.4 Sludge Dewatering

Dewatering is a physical (mechanical) unit operation used to reduce the moisture content of sludge. Sludge dewatering is commonly combined with chemical treatment step (sludge conditioning) to improve its characteristics.

Chemical Conditioning

The use of chemical to condition sludge for dewatering is economical because of the increased yields and greater flexibility obtained. Chemical conditioning can reduce the 90 to 99 percent incoming sludge moisture content to 65to85 percent, depending on the nature of the solids to be treated. Conditioning is used in advance of mechanical dewatering systems such as vacuum filtration, centrifugation, belt filter press, and pressure filter presses. Chemicals used include ferric chloride, lime, alum, and organic polymers.

Adding conditioning chemicals to sludge may increase the dry solids. Polymers do not increase the dry solids significantly, whereas iron salts and lime can increase the dry solids by 20 to 30 percent.

Chemical are most easily applied and metered in the liquid form. Dissolving tanks are needed if the chemicals are received as powder. In most plants, these tanks should be large enough for at least one day's supply of chemicals and should be furnished in duplicate. The tanks must be fabricated or lined with corrosion resistant material. Polyvinyl chloride, polyethlene, and rubber are suitable materials for tank and pipe lining for acid solutions. Metering pumps must be corrosion resistant. These pumps are generally of the positive displacement type with variablespeed or variable-stroke drives to control the flow rate.

Polymers are used commonly in centrifuge and belt press dewatering but are used less frequently for vacuum and pressure filtration.

Dosages of ferric chloride and lime, two of the chemicals used most commonly to condition sludge for vacuum filter dewatering.

Intimate admixing of sludge and coagulant is essential for proper conditioning. The mixing must not break the floc after it has formed, and the detention should be kept to a minimum so that sludge reaches the dewatering unit as soon after conditioning as possible.

Mechanical Dewatering

The available dewatering process include centrifuges, belt filter presses, recessed plate filter presses, drying beds, and lagoons.

– Centrifugation

For separating liquids of different density, thickening slurries, or removing solids, the centrifugation process is widely used in the industry. The centrifugal devices used for thickening sludge, solid bowl and imperforate basket centrifuges.

Solid Bowl Centrifuge

In the solid bowl machine, sludge is fed at a constant flow rate into the rotating bowl, where it separates into a dense cake containing the solids and a dilute stream called "centrate". The centrate contains fine, low-density solids and is returned to the wastewater treatment system. The sludge cake, which contains approximately 70 to 80 percent moisture, is discharged from the bowl by a screw feeder into a hopper or onto a conveyor belt.

Solid bowl centrifuges are suitable generally for a variety of sludge dewatering applications. The units can be used to dewater sludge with no prior chemical conditioning, but the solids capture and centrate quality are improved considerably when solids are conditioned with polymers.

Imperforate Basket Centrifuge

Imperforate basket centrifuges are particularly suitable for small plants. Basket centrifuges can be used to concentrate and dewater waste activated sludge, with no chemical conditioning at solids capture rates up to 90 percent.

After the centrifuge is filled with solids, the unit starts to decelerate. In the dewatering mode, a "skimming" step takes place before the initiation of plowing. Skimming is the removal of soft sludge from the inner wall of sludge in the basket. The Skimming volume is normally 5 to 15 percent of the bowl volume. The skimming stream is returned to the wastewater treatment system.

Belt Press

Belt filter presser are continuous-feed sludge-dewatering devices that involve the application of chemical conditioning, gravity drainage, and mechanically applied pressure to dewater sludge. In most of belt filter presses, conditioned sludge is first introduced on a gravity drainage section where it is allowed to thicken. In this section, a majority of the free water is removed from the sludge by gravity. On some units, this section is provided with a vacuum assist, which enhance drainage and may help to reduce odors. Following gravity drainage, pressure is applied in a low-pressure section is following by a high-pressure section, where the sludge is subjected to shearing force as the belts pass through a series of rollers. The squeezing and shearing forces thus induce the release of additional quantities of water from the sludge. The final dewatered sludge cake is removed from the belts by scraper blades as shown in figure (3-14).

A typical belt filter press system consists of sludge-feed pumps, polymer-feed equipment, a sludge- conditioning tank (flocculator), a belt filter press, a sludge cake conveyor, and support systems (sludge-feed pumps, wash water pumps, and compressed air).

Filter Press

In a filter press as shown in figure (3-15), dewatering is achieved by forcing the water from the sludge under high pressure. Advantages cited for the filter press include (1) high concentrations of cake solids, (2) filtrate clarity, and (3) high solids capture. Disadvantages include mechanical complexity, high chemical costs, high labor costs, and limitation on filter cloth life. Various types of filter presses have been used to dewater sludge. The two types used most commonly are the fixed-volume and variable-volume, recessed plate filter presses.

Fixed-Volume, Recessed Plate Filter Press

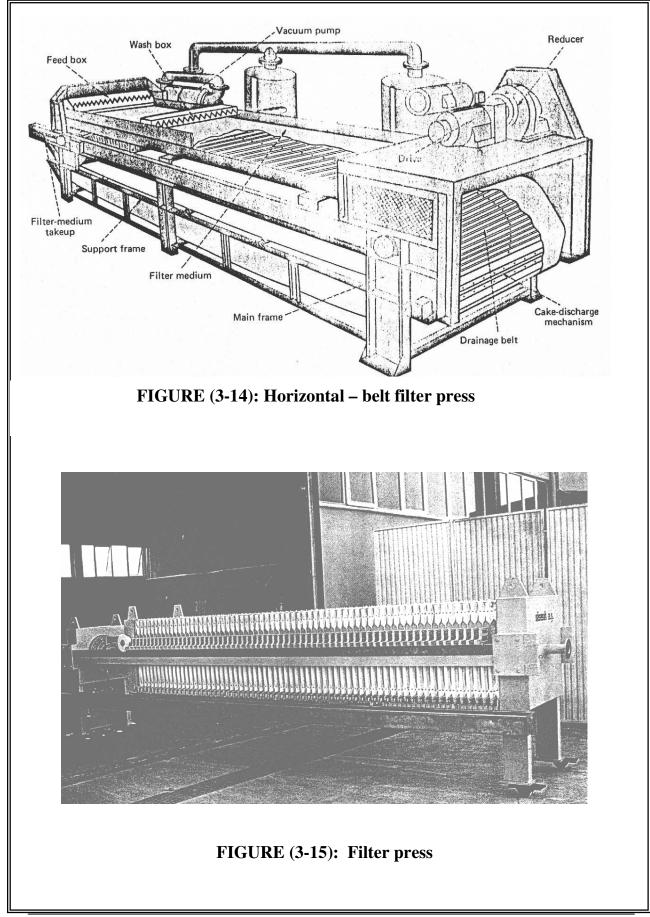
The fixed-volume, recessed plate filter press consists of a series of rectangular plates, recessed on both sides, that are supported face to face in a vertical position on a frame with a fixed and movable head. A filter cloth is hung or fitted over each plate. The plates are held together with sufficient force to seal them so as withstand be pressure applied during the filtration process.

In operation, chemically conditioned sludge is pumped into the space between the plates, and pressure of 100 to 225 1bf/in2 (690 to 150 kN/m2) is applied and maintained for 1 to 3 h, forcing the liquid through the filter cloth and plate outlet ports. The plates are then separated and the sludge is removed. The filtrate is normally returned to the head works of the treatment plant. The sludge cake thickness varies from about 1 to 1.5 in (25 to 38mm), and the moisture

content varies from 48 to 70 percent. The filtration cycle time varies from 2 to 5h and includes the time required to (1) fill the press, (2) maintain the press under pressure, (3) open the press, (4) wash and discharge the cake, and (5) close the press.

Variable-Volume, Recessed Plate Filter Press

Another type of filter press used for wastewater sludge dewatering is the variable-volume recessed plate filter press, commonly called the "diaphragm press" This type of filter press is similar to the fixed-volume press except that rubber diaphragm is placed behind the filter media, The rubber diaphragm expands to achieve the final squeeze pressure, thus reducing the cake volume during the compression step.



49

- Sludge Drying Beds

Sludge drying beds are typically used to dewater digested sludge. After drying, the sludge is removed and either disposed of in a landfill or used as a soil conditioner.

The principal advantages of drying beds are low cost, infrequent attention required, and high solids content in the dried product. Four types of drying beds are used: (1) conventional sand, (2) paved, (3) artificial media, and (4) vacuum-assisted. Conventional sand drying beds are most extensively used.

Conventional Sand Drying Beds.

Conventional sand drying beds are generally used for small medium-sized. In a typical sand drying bed, sludge is placed on the bed in a 8 to 12 in (200 to 300 mm) layer and allowed to dry. Sludge dewater by drainage through the sludge mass and supporting sand and by evaporation from the surface exposed to the air. Most of the water leaves the sludge by drainage, thus the provision of an adequate under drainage system is essential. Drying beds are equipped with lateral drainage lines.

The drainage lines should be adequately supported and covered with coarse gravel or crushed stone. The sand layer should be from 9 to 12 in (230 to 300 mm) deep with an allowance for some loss from cleaning operations.

The moisture content in approximately 60 percent after 10 to 15 d under favorable conditions. Sludge removal is accomplished by manual shoveling into wheelbarrows or trucks or by a scraper or front-end loader. Provisions should be made for driving a truck onto or alongside of the bed facilitate loading.

Open beds are used where adequate area is available and is sufficiently isolated to avoid complaints caused by occasional odors. Open sludge beds should be located at least 300 ft (about 100m) from dwellings to avoid odor nuisance. Covered beds with greenhouse types of enclosures are used where it is necessary to dewater sludge continuously throughout the year regardless of the weather and where sufficient isolation does not exist for the installation of open beds.

– Lagoons

Drying lagoons may be used as a substitute for drying beds for the dewatering of digested sludge. Lagoons are not suitable for dewatering untreated sludge, limed sludge, or sludge with a high-strength supernatant because of their odor and nuisance potential.

Dewatering by subsurface drainage and percolation is limited by increasingly stringent environmental and groundwater regulations. If a groundwater aquifer used for a potable water supply underlies the lagoon site, it may be necessary to line the lagoon or otherwise restrict significant percolation. Sludge depths usually range from 2.5 to 4 ft (0.75 to 1.25m). Evaporation is the prime mechanism for dewatering. Facilities for the decanting of supernatant are usually provided, and the liquid is recycled to the treatment facility. Sludge is removed mechanically, usually at a solids content of 25 to 30 percent. The cycle time for lagoons varies from several months to several years. A minimum of two cells is essential, even in very small plants, to ensure availability of storage space during cleaning, maintenance or emergency conditions.

3.6.5 Sludge Disposal and Uitilization

A) Beneficial Uses of Sludge

The fertilizer value of biological sludge, which should be evaluated where the sludge is to be used as a soil conditioner, is based primary on the content of nitrogen, phosphorus, and potassium.

Trace elements in sludge are those inorganic chemical elements that, in very small quantities, can be essential or detrimental to plants and animals. The term "heavy metals" is used to denote several of the trace elements present in sludge. For land application of sludge, concentrations of heavy metals may limit the sludge application rate and the useful life of the application site.

Sludge may also be treated chemically to stabilizer the sludge for use as landfill cover or for landscaping or land reclamation projects.

The chemical fixation/solidification process has been applied to the treatment of industrial sludge and hazardous wastes to immobilize the undesirable constituents for use as landfill cover and for land reclamation projects. Stabilized sludge may also be disposed of in landfills. The chemical fixation process consists of mixing untreated or treated liquid or dewatered sludge with stabilizing agents such as cement, sodium silicate, pozzolan and lime so as to chemically react with or encapsulate the sludge. For many chemical treatment processes, the product is similar in consistency to natural clay.

B) Sludge Disposal

Final disposal for the sludge and solids that are not beneficially used usually involves some form of land disposal. In addition to spreading sludge on land, other methods of final disposal include landfilling and lagooning.

Landfilling

There are two types of landfills for industrial sludge: those which accept non-hazardous wastes and those that accept hazardous wastes.

Landfills are designed to prevent the contamination of ground water and to prevent the migration of the wastes from the landfill. For this reason, landfills usually have thick, 3 to 10 feet, covers of clean impermeable clay or dirt on top. The cover designed to shed water from the landfill and to prevent penetration of the landfill contents by rainwater. In some cases, plastic barriers are embedded in the cover for this purpose also.

Landfill bottom and sides are also made of impermeable clays or dirt. The sump collects leachate from the landfill and is pumped to a wastewater treatment plant.

Hazardous landfills must meet very stringent requirements. The bottoms and sides must be double contained, which is usually accomplished by installing two liquid barriers, usually plastic. Liquid is collected from the space between the barriers in a leachate collection system and is properly disposed of. The top of a hazardous waste landfill must be impermeable, which is usually accomplished by installing a plastic water barrier in the dirt cover.

Landfills have been known to catch fire and fires in landfills can be very difficult to control and contain. Landfills are filled in sections (cells) isolated by dirt barriers to prevent fire.

Landfill operations must control blowing materials, and this is usually done with fences. Proper records must be kept to ensure no hazardous material are put into non -hazardous landfills, and there are numerous legal requirements for record keeping for hazardous landfills. Landfills

should be surrounded by a strong industrial type fence to keep people and animal out. Landfills can be dangerous places for those not aware of the dangers. Storm water runoff from landfill requires control measures.

Lagooning

A lagoon is an earth basin into which untreated or disgested sludge is deposited. In untreated sludge lagoons, the organic solids are stabilized by anaerobic and aerobic decomposition, which may give rise to objectionable odors. The stabilized solids settle to the bottom of the lagoon and accumulate. Excess liquid from the lagoon, if there is any is returned to the plant for treatment. Lagoons should be located away from highways and dwellings to minimize possible nuisance conditions and should be fenced to keep out unauthorized persons.

3.7 AUXILIARY OPERATIONS

3.7.1 Disinfection

Disinfection refers to the selective destruction of disease-causing organisms. All the organisms are not destroyed during the process. This differentiates disinfection from sterilization, which is the destruction of all organisms.

Description of Disinfection Methods and Means

Disinfection is most commonly accomplished by the use of the following agents:

- 1. Chemical Agents
- 2. Physical Agents
- 3. Radiation

a) Chemical Agents

Chemical agents that have been used as disinfectants include chlorine and its compounds, bromine, iodine, ozone, phenol and phenolic compounds, alcohols, heavy metals and related compounds, dyes, soaps and synthetic detergents, quaternary ammonium compounds, hydrogen peroxide and various alkalies and acids. Of these, the most common disinfectants are the oxidizing chemicals where chlorine is the one most universally used. Bromine and iodine occasionally are used for swimming pool water but have not been used for treated wastewater. Ozone is a highly effective disinfectant, and its use is increasing even though it leaves no residual. Highly acid or alkaline water can also be used to destroy pathogenic bacteria, because water with a pH greater than 11 or less than 3 is relatively toxic to most bacteria.

b) Physical Agents

Physical disinfectants that can be used are heat and light. Heating water to the boiling point, for example, will destroy the major disease-producing non-spore forming bacteria. Heat is commonly used in the beverage and dairy industry, but it is not a feasible means of disinfecting large quantities of wastewater because of the high cost.

Sunlight is also a good disinfectant. In particular, ultraviolet radiation can be used. Special lamps that emit ultraviolet rays have been used successfully to sterilize small quantities of water. The efficiency of the process depends on the penetration of the rays into water. The contact geometry the ultraviolet-light source and the water is extremely important, because suspended matter, dissolved organic molecules, and water itself will absorb the radiation, in addition to the microorganisms. It is therefore difficult to use ultraviolet radiation in aqueous systems, especially when particulate matter is present.

c) Radiation

The major types of radiation are electromagnetic, acoustic, and particle. Gamma rays are emitted from radioisotopes, such as cobalt 60. Because of their penetration power, gamma rays have been used to disinfect (sterilize) both water and wastewater.

Mechanisms of Disinfectants

These are four mechanisms that have been proposed to explain the action of disinfectants are (1) damage to the cell wall, (2) alteration of cell permeability, (3) alteration after colloidal nature of the protoplasm, and (4) inhibition of enzyme activity. Damage or destruction of the cell wall will result in cell lysis or death. Same agents, such as penicillin, inhibit the synthesis of the bacterial cell wall. Agents such as phenolic compounds and detergents alter the permeability of the cytoplasmic membrane. These substances destroy the selective permeability of the membrane and allow vital nutrients, such as nitrogen and phosphorus.

Heat radiation, and highly acid or alkaline agents alter the colloidal nature of the protoplasm. Heat will coagulate the cell protein and acids or bases will produce a lethal effect.

3.7.2 Reuse of Treated Effluent

Reuse of treated wastewater in various industries is becoming very popular being a cheaper source of water supply where the industrial plant can reuse its own wastewater through recycling or after treatment or it can be used for irrigation. There are many possibilities that some of hazardous and toxic chemicals may pass to the treated effluents. In order to eliminate health hazards several advanced methods of tertiary treatment for the industrial effluents with disinfection are available world wide to meet the standards for effluent reuse for several purposes. However, the following describing techniques are the commonly applied for water reuse in Egypt.

Advanced Treatment Techniques "tertiary treatment" a) Filtration

Filtration devices include cartridge filters, diatomaceous earth filters, and granular-media filters. Cartridge filters are rarely used in wastewater treatment for economic reasons.

Granular Media Filters

Granular media filters are widely used in wastewater treatment for the removal of both organic and inorganic suspended solids. Granular media filters can operate either by gravity flow (gravity filters) or by pressure (pressure filters). Both down flow and up flow filters are used by industry.

The most common types of filters are two and three media filters. A common design for a two media filter would have a bed of 0.5mm sand layer below a 0.9mm anthracite layer. A common design for a three-media filter would have a 30 to 40 mesh garnet layer below the sand layer. Specialty filters could use different media with different effective sizes.

Solids are captured by the bed and eventually have to be removed by scouring and backwashing.

Carbon Adsorption

Carbon adsorption is used to remove certain types of organic contaminants that are resistant to primary and secondary treatment when such removal is required. These include contaminants that are toxic, and contaminants that are resistant to biological treatment, but require a higher degree of removal. There are some cases where an organic stream contains contaminants that are valuable enough to recover with carbon adsorption.

Another use of carbon columns is to remove Volatile Organic Compounds (VOCs) from wastewater. All VOCs can be adsorbed onto activated carbon to a greater or lesser extent. Some companies provide carbon columns and remove then when spent and recharge them in their own facility. This is cost effective for small streams, but not for large streams. Spent carbon from the columns may be disposed of however it is usually classified as a hazardous waste that makes disposal expensive. Carbon can be regenerated by passing a stream of steam through it or by removing it and heating in a furnace. In both a stream of VOC containing steam or off-gas is produced which must be properly disposed of. Condensing the steam and either burning the condensate in a furnace or sending it to a hazardous waste disposal company (if hazardous) would be the usual methods of disposal.

Activated carbon can be regenerated with steam, heat, solvent wash, acid or caustic wash, or using a wet oxidation regenerator.

Adsorbability can be described by the following general list, which shows the most absorbable type of compound on top and least absorbable:

* Organic Acids
* Aldehydes
* Esters
* Ketones
* Alcohols
* Glycols

Filtration system "granular media and carbon adsorption" followed by desinfection are in use in some industries in Egypt for water reuse in irrigartion.

b) Membrane Separation

Membrane separation techniques are used to remove very fine particles from water, to desalinate water, and recently, membranes have been developed to remove organics from water, such as oil and other organics that have clogged and degraded membranes in the past. Membranes are made of various materials but all have a consistent pore size that will permit particles or molecules of a given size to pass through the membrane and will prevent molecules or particles of a size larger then the pore size from passing through. Basically, membranes are filters, that present a physical barrier of a definite and specific pore size.

Ultrafiltration

Ultrafiltration utilizes membranes that are sized to remove a given particle size and larger, as required. The particles removed usually have a molecular weight in the ranger of 500 to 1000. The feed is the wastewater stream, the permeate the filtered wastewater, and the bleed would contain the concentrated solids. Ultrafiltration is generally preceded by conventional filters or cartridge filters to prevent blinding of the membranes. The membranes must be cleaned and back flushed periodically. A gel layer can form on the membrane that further increases resistance to flow.

There are three manufacturing processes for membranes, namely the phase inversion process, the track-etched membrane, and the anopore inorganic (anodized aluminum) membrane.

An interesting variant of ultrafiltration is a system that uses a backwash preceded by an air wash. This system is less likely to clog and is used as tertiary treatment for wastewater and to replace clarifiers in water treatment where clarifiers cannot remove sufficient turbidity.

Microfilters normally have a reject rate of 10%, but the 10% can be further filtered so that only 1% of the water is lost as reject.

• Reverse Osmosis (R.O system)

A great of technology has been developed to minimize the flow resistance of the membrane by making it as thin as possible.

Industrially, valuable products can be recovered from a wastewater stream by using membranes of different pore sizes. For example, in cheese production the liquid whey fraction, which is left when the milk is coagulated to produce the cheese, is 93% water. Since the whey has a BOD₅ of > 30,000 mg/l, municipal sewage treatment systems have difficulty handling this waste. However, if the whey is passed over a RO unit, the proteins are concentrated while the lactose and other components and most of water pass through the membrane. The permeate is passes to a second membrane where the water is removed as permeate with BOD₅ below 1000 mg/l and the concentrate is an enriched lactose solution.

There are three types of membrane systems on the market today.

- * Tubular Membrane System
- * Spiral Wound Membrane Systems
- * Hollow Fine Fiber Membrane System

Reverse Osmosis systems can be used to concentrate heavy metals or other salts, and to recover diluted solutions of chemicals. It is also used as a pretreatment step prior to ion exchange to improve the efficiency of the ion exchange process by concentrating the wastewater stream.

3.8 INTEGRATED MODEL FOR INDUSTRIAL WASTEWATER TREATMENT

All treatment technologies described earlier under section 3.1 - 3.7 can be used to develop a model for sequential treatment of industrial wastewater which can be described as follows and shown in Figure (3-16).

3.8.1 Primary Treatment

As industrial wastewater enters a plant for treatment, it flows through a screen, which removes large objects such as rags and sticks that might clog pipes or damage equipment. After sewage has been screened, it passes into a grit chamber, where cinders, sand and small stones settle to the bottom.

Sedimentation is currently the most widely used primary treatment operation. In a sedimentation unit, solid particles are allowed to settle to the bottom of a tank under quiescent conditions. Chemicals may be added in primary treatment to neutralize the stream or to improve the removal of small-suspended solid particles. Primary reduction of solids reduces oxygen requirements in a subsequent biological step and also reduces the solids loading to the secondary sedimentation tank. After screening is completed and grit has been removed, sewage still contains organic and inorganic matter along with other suspended solids. These solids are minute particles that can be removed from sewage in a sedimentation tank.

Primary treatment alone has proved to meet some industries demands for higher water quality in order to comply with environmental regulations for effluent discharge to various water bodies.

3.8.2 Secondary Treatment

Secondary treatment generally involves a biological process to remove organic matter through biochemical oxidation. The particular biological process selected depends upon such factors as quantity of wastewater, biodegradability of waste and availability of land. The principal secondary treatment techniques used are the activated sludge process and the trickling filter.

In the activated sludge process, wastewater is fed to an aerated tank where microorganisms consume organic wastes for maintenance and for generation of new cells. The resulting microbial floc (activated sludge) is settled in a sedimentation vessel called a clarifier or thickener. A portion of the thickened biomass is usually recycled to the reactor to improve performance through higher cell concentrations.

Trickling filters (bio-filters) are beds packed with rocks, plastic structures, or other media. Microbial films grow on the surface of the packing and remove soluble organics from the wastewater flowing over the packing. Excess biological growth washes off the packing and is removed in a clarifier.

The trend today is towards the use of the activated sludge process instead of trickling filters. The activated sludge process speeds up the work of the bacteria by bringing air and sludge heavily laden with bacteria into close contact with sewage. After the sewage leaves the settling tank in the primary stage, it is pumped into an aeration tank, where it is mixed with air and sludge loaded with bacteria and allowed to remain for several hours. During this time, the bacteria break down the organic matter into harmless by-products. The sludge, now activated with additional billions of bacteria and other tiny organisms, can be used again by returning it to the aeration tank for mixing with air and new sewage. From the aeration tank, the partially treated sewage flows to another sedimentation tank for removal of excess bacteria.

3.8.3 Tertiary Treatment

Many industrial effluent standards require tertiary or advanced wastewater treatment to remove particular contaminants or to prepare the water for reuse. Some common tertiary operations are removal of phosphorus compounds by coagulation with chemicals, removal of nitrogen compounds by ammonia stripping with air or by nitrification - denitrification in biological reactors, removal of residual organic and color compounds by adsorption on activated carbon and removal of dissolved solids by membrane processes (reverse osmosis and electrodialysis). The effluent water is often treated with chlorine or ozone to destroy pathogenic organisms before discharge into the receiving waters.

Tertiary treatment is intended primarily for upgrading the quality or polishing of effluent and to remove further the suspended solids, BOD_5 and excess nutrients. The various processes of tertiary treatment applied to industrial effluents are as follows:

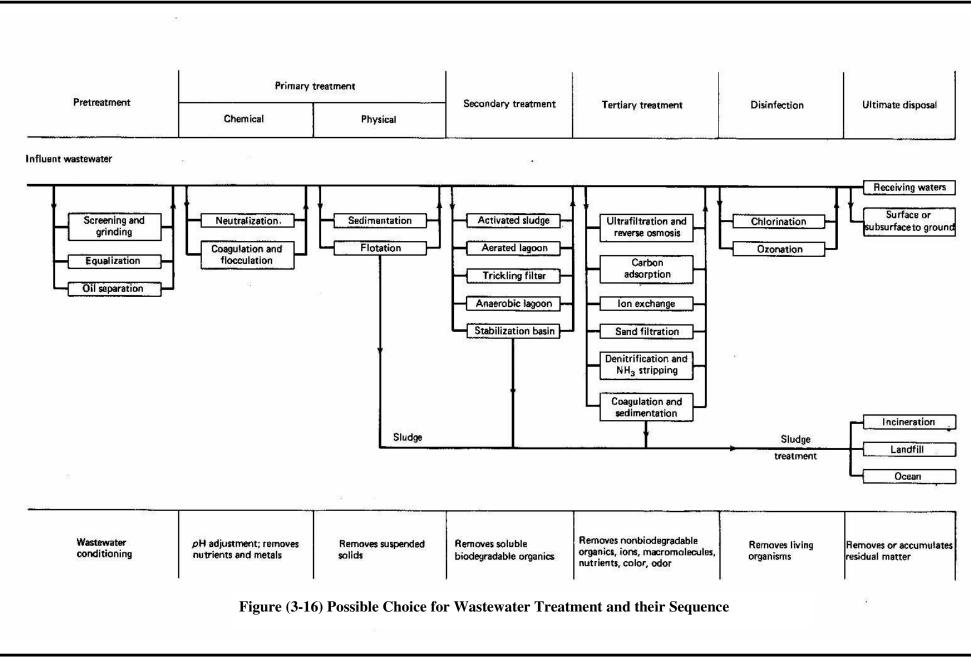
- * Coagulation and sedimentation
- * Activated carbon adsorption
- * Electrodialysis
- * Biological Nitrification
- Ion Exchange
- * Ultrafiltration.

In general, tertiary treatment requires considerable sophistication in design, construction and operation.

3.8.4 Sludge Treatment

Selection of a treatment sequence for sludge depends upon the nature of the sludge, environmental factors and ultimate disposal options. Wastewater treatment processes generate significant quantities of sludge from suspended solids in the feed, biomass generated by biological operations and precipitates from added chemicals.

Sludge conditioning by chemicals or heat improves rates of dewatering. In dewatering operations, the water content of sludge is reduced to a level where they can be handled as damp solids. Vacuum filtration, centrifugation and sand beds are the most common dewatering methods. Thermal processes, such as heat drying and incineration are used to either dry the sludge or to oxidize its organic content. Residual sludge and ash from sludge treatment processes must be disposed of in the ocean or on land. Some of the options for ultimate disposal on land are landfill, land reclamation and crop fertilization.



58

3.9 EMISSIONS, EFFUENTS AND SOLID WASTES GENERATED FROM IWWTP

3.9.1 Emissions

Expected emissions generated from industrial wastewater treatment plants are gaseous and odor emissions. Sources of gaseous emissions from wastewater treatment plants are mainly from H_2S , SO_2 and CO_2 gases which are omitted from specific biological treatment facilities. Odour emissions resulting from these gases also occur as a result of excessive organic loading of industrial wastes or malfunctioning and poor maintenance of trickling filters, primary and secondary clarifiers and sludge thickening tanks.

3.9.2 Effluents

Water effluents generated from IWWTP depend on the type of wastewater treatment applied. If chemical treatment is the case, then the treated water is generally discharged to the public sewer. This mainly depends on the type of industry involved which discharges the wastewater effluent. If, for example, water is treated from a tissue paper mill, then the treated effluent may be reused again in the production. Where biological treatment is the case, the treated effluent after chlorination could be used for irrigation purposes.

Reuse of treated wastewater in various industries is becoming very popular being a cheaper source of water supply where the industrial plant can reuse its own wastewater through recycling or after treatment or it can be used for irrigation. There are many possibilities that some of hazardous and toxic chemicals may pass to the treated effluents. In order to eliminate health hazards, several advanced methods of tertiary treatment for industrial effluents with disinfection are available worldwide to meet the standards for effluent reuse for several purposes.

3.9.3 Solid Waste

The solid waste resulting from wastewater treatment plants include screenings, grit, scum and sludge. The sludge resulting from wastewater treatment operations and processes is usually in the form of a liquid or a semi-solid liquid before dewatering takes place. Problems dealing with sludge are complex because it is composed largely of the substances responsible for the offensive character of untreated wastewater; the portion of sludge produced from biological treatment requiring disposal is produced in a different form (biomass from biological activity) which can also decompose and become offensive ; and only a small part of the sludge is solid matter. Thickening (concentration), conditioning, dewatering, and drying are used primarily to remove moisture from sludge.

Chemical sludge containing hazardous materials (e.g. Heavy Metals) should be dewatered then disposed off in a specially assigned landfill. Dewatered biological sludge and non-hazardous solids from IWWTP are disposed in sanitary solid waste disposal facilities.

3.10 SUMMARY OF INDUSTRIAL WASTE: CHARACTER AND TREATMENT METHODS

Industrial producing wastes	Major characteristics	Major treatment and disposal methods
Textiles	Highly alkaline, colored, COD & temperature, high suspended solids	Neutralization, chemical precipitation, biological treatment, aeration and/or trickling filtration.
Leather goods	High total solids, hardness, salt sulfides, chromium, pH, precipitated lime, and BOD ₅	Equalization, sedimentation, and biological treatment
Laundry trades	High turbidity, alkalinity, and organic solids	Screening, chemical precipitation, flotation, and adsorption
Canned goods	High in suspended solids, colloidal and dissolved organic matter	Screening, lagooning, soil absorption or spray irrigation
Dairy products	High in dissolved organic matter, mainly protein, fat and lactose	Acidification, flotation Biological treatment, aeration trickling filtration, activated sludge
Brewed and distilled beverages	High in dissolved organic solids, containing nitrogen and fermented starches or their products	Recovery, concentration by centrifugation and evaporation, trickling filtration; use in feeds; digestion of slops
Meat and poultry products	High in dissolved and suspended organic matter, blood, other proteins, and fats	Screening, setting and/or flotation, trickling filtration
Beet sugar	High in dissolved and suspended organic matter, containing sugar and protein	Reuse of wastes, coagulation, and lagooning
Pharmaceutical products	High in suspended and dissolved organic matter	Activated sludge
Yeast	High in solids (mainly organic) and BOD ₅	Anaerobic digestion, trickling filtration
Pickles	Variable pH, high suspended solids, color, and organic matter	Good housekeeping, screening, equalization
Coffee	High BOD ₅ & S.S.	Screening, settling, and trickling filtration
Fish	Very high BOD ₅ , total organic solids, O&G and odor	Oil removal, biological treatment
Soft drink	High pH, suspended solids and BOD ₅	Screening, Neutralization
Bakeries	high BOD ₅ , grease, floor washings, sugars, flour, detergents	Amenable to biological oxidation
Water production	Minerals and suspended solids	Screening
Cane Sugar	Variable pH, should organic matter with relatively high BOD ₅ of carbonaceous nature.	Neutralization, recalculation, chemical treatment, some selected aerobic oxidation
Palm oil	High BOD ₅ , COD, Solids and total fats and low pH	Neutralization, coagulation, flotation, filtration
Pulp & Paper	High or low pH, color, high	Settling, lagooning, biological

	suspended, colloidal, and dissolved	treatment earstion recovery of
	solids, inorganic filters	treatment, aeration, recovery of by-products using flotation
	Alkaline, containing various	by-products using notation
Photographic	organic and inorganic reducing agents	Recovery of silver; discharge
Steel	Low pH, acids, cyanogen, phenol, ore, coke, limestone, alkali, oils, mill scale, and fine suspended solids	Neutralization, recovery and reuse, chemical coagulation
Metal-plated	Acid, metals, toxic, low volume, mainly mineral matter	Alkaline chlorination of cyanide, reduction and precipitation of chromium, lime precipitation on other metals
Oil fields and refineries	High dissolved salts from field; high BOD ₅ , odor, phenol, and sulfur compounds from refinery	Recovery of salts; acidification burning of alkaline sludge
Fuel oil use	High in emulsified and dissolved oils	Leak and spill prevention, flotation
Rubber	High BOD ₅ and odor, high suspended solid, variable pH, high chlorides	Aeration chlorination, sulfonation, biological treatment
Glass	Red color, alkaline nonsettleable suspended solids	Calcium-chloride precipitation
Glue manufacturing	High COD, BOD ₅ , pH, chromium, periodic strong mineral acids	Aerobic biological treatment, flotation, chemical precipitation
Candle manufacturing	Organic (fatty) acids.	Anaerobic digestion
Metal container	Metal fines, lub, oils, variable pH, surfactants, dissolved metals.	Oil separation, chemical precipitation, collection and reuse, lagoon storage. Final carbon absorption
Petrochemical	High COD, T.D.S., metals, COD/BOD ₅ ratio.	Recovery and reuse, equalization and neutralization, chemical coagulation, settling or flotation, biological oxidation
Coment	Heated cooling water, suspended solids, some inorganic salts	Segregation of dust-contact streams, neutralization and sedimentation
Asbestos	Suspended asbestos and mineral solids	Detention in ponds, neutralization and land filling
Paint and inks	Contain organic solids from dyes, resins, oils, solvents, etc	Settling ponds for detention of paints, lime coagulation of printing inks.
Acids	Low pH, low organic content	Neutralization, burning when some organic matter is present
Detergents	High in BOD ₅ and saponified soaps	Flotation and skimming, precipitation with CaCl ₂
Cornstarch	High BOD ₅ and dissolved organic matter; mainly starch and related material	Equalization, biological filtration, anaerobic digestion

61

Pesticides	High organic matter, benzenering structure, toxic to bacteria and fish, acid	Activated-carbon adsorption, alkaline chlorination	
Formaldehyde	Normally high BOD ₅ and HCHO, toxic to bacteria in high concentrations	Trickling filtration, adsorption on activated charcoal	
Mortuary	Blood salt, formaldehydes, high BOD ₅	Chlorination	
Hospital-Res.	Bacteria, various chemical radioactive	Holding and biol. Aeration	
Organic	Varied types of organic chemicals	Biological degradation plant control, process modification	
Steam power	Hot, high volume, high inorganic and dissolved solids.	Cooling by aeration, storage of ashes, neutralization of excess acid wastes	
Scrubber power	Particulate, SO ₂ , impure absorbents	Solids removal usually by settling,	
plant wastes	or NH ₃ , NaOH	pH adjustment and reuse	
Coal	High-suspended solids mainly coal, low pH, high H ₂ SO ₄ and FeSO ₄ .	Settling flotation	

4. EGYPTIAN LEGISLATION ON INDUSTRIAL WASTEWATER EMISSIONS AND SLUDGE TREATMENT

4.1 BACKGROUND

Three primary laws regulate the discharge of wastewater according to the government of Egypt environmental regulations. These laws are:

- Law 4 of 1994 regulates discharge in coastal environments.
- Law 93 of 1962 and amended executive decree No. 44 for year 2000 regulates discharge to sewer systems.
- Law 48 of 1982 regulates discharge into underground reservoirs and branches or canals of the Nile, to the main stream of the Nile, and to municipal and industrial drains.

The regulations implementing these laws are independent of each other in terms of regulated streams, inspection, and enforcement entities. However, all these laws, refer to the laboratories of the Ministry of Health and Population (MOHP) as the analytical body for measurements of wastewater parameters, which are shown in table (4-1).

The most important regulatory connection between these laws, as well as other environmental laws, is the environmental register required by law 4/1994. The register includes all information concerning a facility's discharges over a 1-year period. Historical information must be kept for 10 years. EEAA is mandated to do inspection and independent analysis of these registers.

These laws aim to:

- Protect the environment, seashores, and ports of the Arab Republic of Egypt from pollution hazards in all their form and shapes.
- Protect the natural resources in the economic zone.
- Compensate any natural or juridical person for any damage caused due to the pollution of the water.
- Protect the employees who are working to maintain the sewerage system from harmful industrial waste.
- Protect the structures, equipment, and biological treatment operations from harmful industrial waste.

Law	Subject of Law (related to wastewater)	Issues Regulated by the Law and Methods of Regulation	Responsible Entity
4/1994	Discharge of Liquid Wastes to Marine Waters	 Prohibition of untreated (in violation of this law) wastewater discharge to marine waters, either directly or indirectly, intentionally or unintentionally. Banned discharge of wastewater containing non-degradable polluting substances. 	Egyptian General Authority for Shore Protection, in coordination with EEAA.
		• Perform periodic analysis for samples of the treated wastewater, from establishments permitted to discharge to marine waters, and in case of violations, it gives 1 month for compliance. If not completed, disposal will be stopped, license will be revoked without prejudice, and/or penalties as mentioned in this law imposed.	MOHP Laboratories. In case of violation, EEAA is notified and begins administrative procedures.
48/1982	Discharge of Liquid Wastes to the Nile and Waterways	• Prohibition of wastewater discharge to the Nile and waterways, even if in compliance with the specifications of this law, unless a license is acquired.	Ministry of Irrigation. In coordination with the MOHP
		 Perform periodic analysis for samples of the treated wastewater from establishments licensed to discharge into waterways, in case of violations without immediate danger, 3 months to comply are allowed. If renovations are not completed, discharge will be stopped, and/or license will be withdrawn without prejudice to the penalties given in the law. In case of violations with immediate danger, the establishment will be notified to remove the causes of harm immediately. If they are not removed, the license will be withdrawn and discharge stopped <u>OR</u> the Ministry of Irrigation will undertake this at his expense. 	MOHP Laboratories. In case of violation, the Ministry of Irrigation is notified to begin administrative procedures.

Table (4-1) Comparison of Egyptian Laws Related to Wastewater

93/1962 (and amendm ents)	Discharge of Wastewater to the Public Sewer System	• Prohibition of wastewater discharge to the public sewer system, which is in compliance with the specifications of this law, unless a license is acquired. Otherwise, the discharge is stopped by administrative procedures.	Ministry of Housing, in cooperation with the sanitary drainage authorities.
		 Perform periodic analyses for samples of the treated wastewater from establishments licensed to discharge to public sewer systems, and in case of violation, 6-months are give to bring the discharge into compliance. If the work is not completed, license will be withdrawn and/or the grace period may be extended. In case of immediate danger, the discharge is stopped. 	MOHP Laboratories. In case of violation, the Ministry of Housing and the sanitary drainage authorities are to be notified to take administrative procedures.

4.2 CONCERNING WASTEWATER EFFLUENTS TO DIFFERENT RECEIVING BODIES

Limits for pollutants in wastewater vary depending on the type of receiving water body. The parameters that should be monitored and / or inspected are BOD_5 , COD, pH, temperature, residual chlorine, TSS, TDS, oil & grease. Table (4-2) presents the permissible limits for discharges to the different recipients (Sea, Nile, Canals, Agriculture drains, and Public sewer) according to the different relevant laws. Spent lube oil has a negative impact on water and soil and therefore its disposal should be monitored / inspected. A record should be kept for this purpose.

4.3 CONCERNING SOLID WASTE AND SLUDGE

A number of laws address solid waste management. The following laws apply to scrap and sludge from the wastewater treatment plant.

- Law 38/1967 which addresses public cleanliness, regulates the collection and disposal of solid wastes from houses, public places, commercial, and industrial establishments.
- Ministry of Housing, Utilities and Urban Communities (MHUUC) decree No. 134 of 1968, which provides guideline from domestic and industrial sources, including specifications for collection, transportation, composting, incineration and land disposal.
- Law 31/1976, which amended law 38/1967.
- Law 43/1979, the law of local administration, which provided that City councils are responsible for "physical / and social infrastructure", effectively delegating responsibility for infrastructure functions.

Law 4/1994 regulates incineration of solid waste:

- Article 37. It is prohibited to burn, throw away or treat garbage and solid waste except in areas designated for such purpose that are far from housing or industrial or agriculture areas as well as from waterways. The Executive Regulations of this law shall determine the requisites and specifications and the minimal distances between areas designated for such purposes. Local units shall be obliged to designate, in agreement with EEAA, special areas for burning, throwing away or treating garbage and solid wastes according to the provisions of this article.

Articles 38 & 39 of the Executive Regulations.

Parameter	Law 4/94	Law 93/62	Law 48/82 Discharge into			
(mg/l unless otherwise noted)	Discharge in Coastal	Discharge to Sewer System (as modified	Underground Reservoir & Nile	Nile	Non potable s	surface water
,	Environment	by Decree 44/2000)	Branches/Canals	(Main Stream)	Municipal	Industrial
BOD_5 (5 day, $20^{\circ}C$)	60	600	20	30	60	60
COD (Permanganate)	-	-	10	15	40	50
COD (Dichromate)	100	1100	30	40	80	100
pH (units)	6-9	6-9.5	6-9	6-9	6-9	6-9
Oil & Grease	15	100	5	5	10	10
Temperature (deg.)	$10^{\circ}C > avg.$					
	temperature of	43	35	35	35	35
	receiving body					
Total Suspended Solids	60	800	30	30	50	60
Settleable Solids (ml/l)	-	After 10 min: 8 cm After 30 min: 15 cm^3	-	-	-	-
Total Dissolved Solids	2000	-	800	1200	2000	2000
PO ₄	5	25	1	1	-	10
NH ₃ -N (Ammonia)	3	-	-	-	-	-
NO ₃ -N (Nitrate)	40	100	30	30	50	40
TotalRecoverablePhenol	1	0.05	0.001	0.002	-	0.005
Fluoride	1	-	0.5	0.5	-	0.5
Sulfide	1	10	1	1	1	1
Chlorine	-	-	1	1	-	-
Surfactants	-	-	0.05	0.05		-
Probable counting for						
the colon group in 100					-0.55	
cm^3	5000	-	2500	2500	5000	5000

Table (4-2) Egyptian Environmental Requirements

Parameter	Law 4/94 Discharge in	Law 93/62 Discharge to Sewer	Law 48/82 Discharge into					
(mg/l unless otherwise	Coastal	System (as modified	Underground	Nile	Non potable s	surface water		
noted)	Environment	by Decree 44/2000)	Reservoir & Nile Branches/Canals	(Main Stream)	Municipal	Industrial		
Aluminum	3	-	-	-	-	-		
Arsenic	0.05	2	0.05	0.05	-	-		
Barium	2	-	-	-	-	-		
Beryllium	-	-	-	-	-			
Boron	-	1	-	-	-	-		
Cadmium	0.05	0.2	0.01	0.01	-	-		
Chromium	1	-	-	-	Total concentration for these me			
Chromium Hexavalent	-	0.5	0.05	0.05		ould be:		
Copper	1.5	1.5	1	1	1 for all flow streams			
Iron	1.5	-	1	1 1		1 for all flow succins		
Lead	0.5	1	0.05	0.05				
Manganese	1	-	0.5	0.5				
Mercury	0.005	0.2	0.001	0.001	-	-		
Nickel	0.1	1	0.1	0.1		-		
Silver	0.1	0.5	0.05	0.05	-	-		
Tin	-	2	-	-	-	-		
Zinc	5	-	1	1		-		
Cyanide	0.1	0.2	-	-	-	0.1		
Total Metals	-	5	1	1	1	1		
Pesticides	0.2	Should be absent	Should be absent	Should be absent	Should be absent	Should be absent		
Color	Should be absent	-	Should be absent	Should be absent	Should be absent	Should be absent		

4.4 CONCERNING WORK ENVIRONMENT

Violations of work environment could be encountered:

- Near heavy machinery: noise is regulated by article 42 of law 4/1994:
 - Article 42. All agencies and individuals, while performing production, service or other activities, particularly when using tools, equipment, horns or loudspeakers, shall abide by the permissible limits of sound intensity. Authorities issuing licenses shall insure that the total sound produced from fixed sources within one area shall be within the permissible limits, and shall ensure that establishments select appropriate tools and equipment to guarantee this. The Executive Regulations of this law shall define the permissible limits of sound intensity and the permissible time limits for exposure to said noise. *Article 44 of the Executive Regulations and Table 1, Annex 7.*
- ▶ Ventilation is regulated by article 45 of law 4/1994:
 - Article 45. Closed and semi-closed public places must have adequate ventilation facilities relative to their size and capacity as well as the type of activity performed therein, to ensure renewal and purity of the air and a suitable temperature. *Article 47 of the Executive Regulations.*
 - ➢ Work environment conditions are addressed in law 137/1981 for labor, Minister of Housing Decree 380/1983, Minister of Industry Decree 380/1982.

4.5 CONCERNING HAZARDOUS MATERIAL AND WASTE

Law 4/1994 introduced the control of hazardous materials and waste. Articles 29 and 33 of the law make it mandatory for those who produce or handle dangerous materials in gaseous, liquid or solid form, to take precautions to ensure that no environmental damage shall occur. Articles 25, 31 and 32 of the executive regulations (Decree 338/1995) specify the necessary precautions for handling hazardous materials. There is no explicit article in law 4/1994 or in Decree 338/1995 (Executive Regulations), regarding holding a register for the hazardous materials; article 33 is concerned with hazardous wastes, such as sludge resulting from wastewater treatment. However, keeping the register for the hazardous materials is implicit in article 25 of the executive regulations regarding the application for a license.

Articles 29/30/31/32/33 of law 4/1994 regulate hazardous materials and wastes:

Article 29. It is forbidden, without a license from the component administrative authority, to handle hazardous substances and wastes. The Executive Regulations of this law shall determine the procedures and the conditions for granting such a license and the concerned authority.

The Ministers, each in their field of competence, shall issue, in coordination with the Minister of Health and EEAA, a list of the hazardous substances and wastes as aforementioned in paragraph one of this article.

➤ Article 30. Management of hazardous wastes shall be subject to the procedures and regulations stated in the Executive Regulations of this law. The Executive Regulations shall designate the component authority, which, after consulting EEAA, will issue the tables of dangerous wastes to which the provisions of this law shall apply.

➤ Article 31. It is forbidden to construct any establishment for treating dangerous wastes without a permit from the competent administrative authority and before consulting EEAA. Disposal of dangerous wastes shall be according to the norms and conditions that will be stated in the Executive Regulations of this law. The Minister of Housing, Utilities and New Communities shall assign, after consulting with the Ministries of Health, Industry and EEAA, the disposal sites and the required conditions to authorize the disposal of dangerous wastes.

➤ Article 32. It is forbidden to import dangerous waste or to allow its entrance into or passage through Egyptian territories. It is forbidden, without a permit from the competent authority, to allow the passage of ships carrying hazardous wastes through territorial seas or the exclusive economic zone of the ARE.

Article 33. It is mandatory for all those who produce or handle dangerous materials, either in gaseous, liquid or solid form, to take precautions to ensure that no environmental damage shall occur.

The owner of an establishment whose activities may result in hazardous wastes shall, according to the provisions of this law, maintain a register of these wastes and the method of disposing thereof, as well as contracting concerned agencies for receipt of these wastes. The Executive Regulations shall state the data to be recorded in that register and EEAA shall be responsible for following up the register to ensure its conformity with the truth.

Articles 25-32 of the Executive Regulations.

4.6 CONCERNING ENVIRONMENTAL REGISTER

Article 22 of law 4/1994 states that the owner of the establishment shall keep a register showing the impact of the establishment activity on the environment. Article 17 and Annex 3 of the executive regulations specify the type of the data recorded in the register.

The emergency response plan and the hazardous materials register will also be part of the environment register as stated in part 5.4.

Environmental Register is regulated by article 22 of law 4/1994:

Article 22. According to the provisions of this law, owners of establishments shall keep written records of the environmental impact of their establishment's activities. The Executive Regulations will determine the standard form of the required written document as well as its time table to assure the compliance of establishments with such a record. EEAA is designated to review the data of these written records to ensure that they are truthful, to take the required samples, to analyze them, and to measure the environmental impact of the norms established for the protection of the environment. In case of any violation, EEAA will notify the component administrative authority to mandate the owner of the establishment to rapidly correct these violations. If the owner does not comply within 60 days from the date of the required legal and legislative procedures to shut down the activities of the establishment and will request adequate compensation to treat the harm resulting from these violations.

Article 17 of the Executive Regulations and Annex 3.

5. INSPECTION PRINCIPLES AND EXAMPLES

5.1 TARGETS OF INSPECTION

The inspection of industrial wastewater treatment plant (IWWTP) aims to check the compliance of the outputs of the treatment process with respect to liquids, solids and gases with the regulatory limits. This in turn will lead to reduction of the negative environmental impacts.

The effectiveness of inspection will lead to the protection of the environment as well as protection of public health.

The objectives of IWWTP Inspection includes the following:

- Ensuring that the performance parameters are measured and recorded and shows effectiveness.
- Ensuring that treated effluent is in compliance with relevant laws for discharge wastewater to the environment either by direct measurements and/or indirect observations.
- Guiding the industry in case of malfunctioning of the treatment system to utilize technical and/or financial support mechanisms available in EEAA to rehabilitate the system.
- Ensuring the compliance of the establishments with the requirements of the environmental Law 4, 1994 in connection with holding an updated and valid environment register and applying self-monitoring procedures for IWWTP.
- Ensure that air emissions are not violating the law.
- Management of hazardous substances, wastes and non-hazardous solid wastes.

5.2 INSPECTION VISIT

5.2.1 Gathering Information and Auditing

As presented in the general guidelines for inspection team (EPAP 2000), tasks necessary for preparation for field inspection are:-

- Gathering information about the specific facility & review sector specific manuals for each industry in addition to gathering enough information about the treatment plant to be inspected and the generation of hazardous pollutants.
- Preparing of the inspection plan.
- Preparaing the checklist.

a) Gathering and reviewing information

The inspection team should review the general information prepared for the treatment plant type (chapter III) and then checked if possible what units and components are present at this type of treatment plant. It is important at this stage to determine the following:-

- The type of receiving body for the industrial wastewater and relavant Egyptian Laws (Chapter IV).

- The characteristics of the waste effluent which is discharged from the targeted facility and suitable treatment for this type (section 3.8).
- Typical violations, malfunctioning & troubleshooting for the targeted treatment plant.(section 5.2.3)

Note to inspectors:-

Some facilities dilute their polluted wastewater with potable water or groundwater before entering the treatment plant which is prohibited by law.

b) Preparation of the inspection plan

An example of an inspection plan is included in Annex (b) of the Guidelines for Inspection team (EPAP 2000). The plan should take into account the following:-

- At the beginning of the field visit, the inspection team should check the environmental register and the self monitoring system.
- The results of the analysis included in the environmental register should be checked at the end of the field visit and copies of the results should be obtained.

Note to inspectors:-

Make sure that all the production lines are in operation at the time of inspection. Make sure that the treatment plant is operating with a capacity greater than 50% of the design capacity.

c) Preparation of the required checklists

A general checklist for inspection of industrial wastewater plants is designed for this manual and illustrated in Annex (1). It is impossible to fill all the required information in the attached check list, the inspector must prepare a specific checklist case by case. The checklist has been prepared in such a way that it starts with general information about the facility and its operation followed by brief description for treatment plant and cover all relevant environmental aspects.

Note to inspectors:-

Law 4 does not specify standards for effluent from each treatment step but only for final treated effluent. However, effluent quality from each unit is an important indicator for the all efficiency of the treatment plant.

d) Performing the field inspection

The guidelines for Inspection Team (EPAP 2000) describes the procedures involved for entering the industrial facility. The inspector's attitude and behavior are very important from the start and will dictate the factory's personnel response to the inspection tasks.

Information gathered during the facility tour is dependent on interviews of facility personnel and visual observation. The following information should be collected during visiting time:-

General Information

- Establishment name and address.
- Responsible person.
- Industrial sector and subsectors.
- Main products.
- Production capacities.

Wastewater streams

- Sewerage network and wastewater discharge point. (Maps showing the discharge network).
- Quantity of WW discharge m^3/d .
- Discharge outlets.
- Industrial/domestic effluents separate or mixed.
- Points of discharging and receiving bodies (municipal network, the Nile, drainage, sea, reuse).

Treatment Plant

- The location of the plant and surrounding units.
- Units connected to the treatment plant.
- Type and description of the treatment process.

- Description of treatment equipment and its design elements.
- Input / output water loads.
- Input/output water quality.
- Design and actual efficiency.

Sludge Generation

- Sources of sludge generation.
- Sludge treatment.
- Characterization of sludge produced.
- Quantity of sludge.
- Final sludge disposal methods.

Gaseous emissions (if any)

- Characterization of gaseous emission.
- Sources of generation.
- Pollutant concentration and load for each element.
- Odor emissions
- Sources of odor emissions.
- Type of odor.

Chemicals Used

- Type of chemicals used.
- Amounts of chemicals.
- Storage facilities.
- List their main environmental and flammability properties.

Plan for emergency

- Existing a by-pass sewer line.
- Existing an equalizing tank to hold wastewater in case of any process failure.
- Trained maintenance staff.

Monitoring plan

- Indicators to be monitored.
- Sampling timetable.
- Sampling sites.
- Lab conducting analysis (onside or outside).
- Responsible person.
- Analyses protocols.
- Internal reports.
- Maintenance and calibration of self-monitoring instruments.

Note to inspectors:-

It is better at the beginning of the visit not to ask direct questions about quality of the treated effluent & the efficiency of the treatment plant. Interviewing the workers on-site in an indirect manner can give better results.

Check the results of effluent analysis, time and place of sampling. If suspicious make your own analyses.

e) Ending the field visit

When violations are detected a record is prepared stating information pertaining to sampling location and time. Violations of work environment regulations should also state location and time of measurements. Other visual violations as sludge accumulations, hazardous material and waste handling and storage and material spills should be photographed and documented. The facility management should sign these records.

A closing meeting with the facility management can be held to discuss findings and violations.

5.2.2 Collection of Samples for Analysis

The variety of conditions at different sampling locations requires that considerable judgment be exercised regarding the methodologies and procedures for the collection of representative samples of wastewater. There are, basic rules and precautions generally applicable to sample collection. Some important considerations for obtaining a representative wastewater sample include:

- The sample should be collected where the wastewater is well mixed. Therefore, the sample should be collected near the center of the flow channel, at approximately 40 to 60 percent of the water depth, where the turbulence is at a maximum and the possibility of solids settling is minimized. Skimming the water surface or dragging the channel bottom should be avoided. However, allowances should be made for fluctuations in water depth due to flow variations.
- In sampling from wide conduits, cross-sectional sampling should be considered.
- If manual compositing is employed, the individual sample portions must be thoroughly mixed before pouring the individual aliquots into the composite container. For manual composite sampling, the individual sample aliquots should be preserved at the time of sample collection.
- When collecting samples or installing sampling equipment, field investigators should always wear a new pair of the appropriate protective gloves (disposal latex gloves, rubber gloves, etc.) to prevent contamination of the sample and reduce exposure to hazardous substances.

Since law 4/94 does not specify standards for the effluent from production lines but only for the effluent from the final disposal point, therefore, the inspectors are only concerned with the end of pipe discharging points.

Sample Types

Two types of sampling techniques are used: grab and composite.

- **Grab Samples**. Grab samples consist of either a single discreet sample or individual samples collected over a period of time not to exceed 15 minutes. The grab sample should be representative of the wastewater conditions at the time of sample collection. The sample volume depends on the type and number of analyses to be performed.
- **Composite Samples**. Composite samples are collected over time, either by continuos sampling or by mixing discrete samples. A composite sample represents the average wastewater characteristics during the compositing period. Various methods for compositing are available and are based on either time or flow proportioning. The choice of a flow proportional or time composite-sampling scheme depends on the permit requirements, variability of the wastewater flow or concentration of pollutants, equipment availability, and sampling location. The investigator must know each of these criteria before a sampling program can be initiated. If an investigator knows or suspects that there is significant variability in the wastewater flow or if the investigator knows nothing about the facility, a flow proportional sample is preferable. Otherwise, a time composite sample would be acceptable.

A time composite sample consists of equal volume discrete sample aliquots collected at constant time intervals into one container. A time composite sample can be collected either manually or with an automatic sampler.

A flow proportional composite sample can be collected using one of two methods. One method consists of collecting a constant sample volume at varying time intervals proportional to the wastewater flow. For the other method, the sample is collected by varying the volume of each individual aliquot proportional to the flow, while maintaining a constant time interval between the aliquots. Prior to collecting flow proportional samples, the facility's flow measuring system should be examined for proper installation and accuracy. If the facility's primary flow measuring device does not meet standard conditions, or is in an unsafe or inaccessible location, then the investigator may collect time composite samples. If the flow measurement system is acceptable, samples should be collected using the appropriate flow proportioning methods.

Flow proportional samples can be collected with an automatic sampler and a compatible flowmeasuring device, semi-automatically with a flow chart and an automatic sampler capable of collecting discrete samples, or manually.

Use of Automatic Samplers

Automatic samplers may be used to collect composite or grab samples when several aliquots are to be collected at frequent intervals or when a continuous sample is required. For composite sampling applications, the automatic samplers may be used to collect time composite or flow proportional samples. In the flow proportional mode, the samplers are activated by a compatible flow meter. Flow proportional samples can also be collected using an automatic sampler equipped with multiple containers and manually compositing the individual sample portions proportional to the flow.

Automatic samplers must meet the following requirements:

- * Sampling equipment must be properly cleaned to avoid cross-contamination which could result from prior use.
- * No plastic or metal parts of the sampler shall come in contact with the water or wastewater stream when parameters to be analyzed could be impacted by these materials.
- * The automatic sampler must be capable of providing adequate refrigeration during the sampling period. This can be accomplished in the field by using ice.
- * The automatic sampler must be able to collect a large enough sample for all parameter analyses.
- * The individual sample aliquot must be at least 100 ml.
- * The automatic sampler should be capable of providing a lift of at least 20 feet and the sampler should be adjustable since the volume is a function of the pumping head.
- * The pumping velocity must be at least 2 ft/sec to transport solids and not allow solids to settle.
- * The intake line leading to the pump must be purged before each sample is collected.
- * The minimum inside diameter of the intake line should be $\frac{1}{4}$ inch.
- * An adequate power source should be available to operate the sampler for the time required to complete the project. Facility electrical outlets may be used if available.

Manual Sampling

Manual sampling is normally used for collecting grab samples and/or for immediate in-situ field analyses. However, it can also be used in lieu of automatic equipment over extended

waste stream conditions.

The best method to manually collect a sample is to use the actual sample container, which will be used to transport the sample to the laboratory. This eliminates the possibility of contaminating the sample with intermediate collection containers. If the sampling personnel cannot physically reach the wastewater stream or it is not safe to reach for the sample, an intermediate collection container may be used, from which the sample can be redistributed to other containers. If this is done, however, the container used to collect the sample must be properly cleaned and must be made of a material that meets the requirements of the parameter(s) being investigated. Samples for oil and grease, bacteria, phenols, volatile organic compounds, and sulfides analyses must always be collected directly into the sample container.

In some cases it may be best to use a pump, either power or hand operated, to withdraw a sample from the wastewater stream. If a pump is used, it is imperative that all components of the pump that come in contact with the sample are properly cleaned to ensure the integrity of the sample.

In general, samples are manually collected by first selecting a location in the wastewater that is well mixed then dipping the container in the wastewater stream so the mouth of the container faces upstream. The container should not be overfilled if preservatives are present in the container.

Analysis Parameters

The selection of parameters for the analysis depends on the nature and characteristics of the influent which is directly related to the type of industry. The most common parameters requiring analysis for industrial wasteater effluents are:-

pH,	T.S.S,	TDS,
BOD ₅ ,	COD,	O&G,
CL,	$NO_3 - N$,	$PO_4 - P$,
$NH_3 - N$,	Heavy metals,	Phenols,
Cyanide.	•	

5.2.3 Typical Cases of Malfunctioning & Process Failure

The inspector can detect the most significant malfunctioning of the treatment process during his visit by the following observations: -

- Bad odour release and gaseous emissions due to:- a) the septic build up condition especially in sedimentation tanks or b) the accumulation of rags and other debris on the bar screen, c) malfunctioning and poor maintenance of biological filters, clarifiers, sludge thickening and drying beds.
- Black colour of raw wastewater with septic odour indicates that part of the wastewater is being retained because of slow flow due to a build up of sludge or grit.
- Thick, dark, greasy, scummy layers of deep tan to brown foam covering the entire surface of aeration tanks always indicates that the sludge is too old and may be over oxidized.
- Excessive, billowing, white foam in aeration tanks may be due to young sludge. The sludge age should be increased by reducing the sludge waste rate.
- The presence of air bubbles on the surface of the aeration tank is an indication the proper activity of the biomass.

- An extremely dark brown colour with the odour of hydrogen sulphide in aeration tanks of activated sludge treatment indicates poor oxidation. A dark brown colour with an earthy smell of oxidized wastewater in the aeration tank is an indication of proper functioning of the system.
- Surcharging around treatment units due to screens or grit chambers blockage, clogging of under drains biological filters as a result of the growth of algae and development of slime.
- Ponding of filters due to improper grading of the stone media and small size stones filled between larger size media.
- Flies around the biological filters. These may be present due to poor distribution of wastewater along the filter walls and insufficient hydraulic loading.
- High levels of noise due to improper maintenance of mechanical equipment.

The inspectors should check the following points to insure that the operation of industrial process is normal during inspection time: -

- Quality of the influent water to the treatment plant (during peak processing time or during washing time).
- The entry pipeline to the treatment plant and compare with sewerage network map to identify the presence of any by-passing line which goes directly to the sewer line.

The inspectors can detect dubious analysis results provided by the company by checking the relationship between different parameters such as:-

- COD value should be higher than the BOD₅ value.
- High levels of O&G value lead to the high levels of COD value.
- Total solid values should be higher than level of suspended solids.
- Total solids equal the level of suspended solids & dissolved solids.

The inspectors should also check the relationship between the actual production capacity and the performance of wastewater plant at the time of inspection, in order to compare the operation values with design values (i.e. lower capacity means better performance, lower hydraulic load means higher quality of treated water due to the effect of water recycling).

The industrial plant should have a self-monitoring system for the treatment plant. All monitoring should be done and samples be taken, analyzed. Parameters monitoring, sampling locations, and sampling frequencies, analytical procedures and type of sampling also should be reported.

Specific inspection issues for main treatment methods that can be easily used to detect malfunctioning(physical, chemical and biological) are given in table (5-1).

Physical Treatment	Chemical Treatment	Biological Treatment
 Clogging /surcharging 	 Type of chemicals used 	– Bad odor
- Odor emission	 Amounts of Chemical Consumption 	– Black Color
Fouling	Efficient sludge Separation, Turbidity of treated effluent	 Nutrients consumptions
Flies	pH level	 Air bubbling (as measure for Biomass activity)
Noise	Color	– Flies
		 Fouling of biological filters (clogging, flooding)
		Foaming indication of old sludge

Table (5-1) Specific malfunctioning issues for main treatment methods

5.2.4 Examples Cases of Process Failure

• Yeast Production Factory:-

Failure to reach design parameters for treated effluent due to increased levels of introduced pollution influent mainly pH and COD.

• Spinning & Weaving Manufacturing Factory:-

Poor efficiency of activated sludge system due to the increased level of hydraulic loading besides the inefficiency of the Aeration System.

• Food Industry (Chocolate & Confectionery Production Factory):-

Failure of the activateded sludge system to work on full capacity (50 m^3/d) as currently treating only 25 m^3/d . The problem is focussed on the inadequate design of the clarifier (short retention time).

• Spinning & Weaving Manufacturing Factory:-

Physio chemical/Biological treatment failed to fulfill the design parameters as there were problems related to process sequence & chemical additives-e.g chemical are added during biological stage - The plant is out of operation since 13 years ago.

5.3 INSPECTION RESULTS

5.3.1 Observations on operation of IWWTP

• Odour

Odour problem is usually due to the excessive organic loading of industrial wastes or malfunctioning and poor maintenance of trickling filters, primary and secondary clarifiers and sludge thickening tanks.

• Colour

The black colour of raw wastewater with septic odour may indicate that part of wastewater is being retained because of slow flow due to a build up of sludge or grit.

• Surface foam and scum

Thick, dark, greasy, scummy layers of deep tan to brown foam covering the entire surface of aeration tanks always indicates that the sludge is too old and may be over oxidized.

• Dissolved Oxygen

An extremely dark brown colour with the odour of hydrogen sulphide in aeration tanks indicates poor oxidations. In conventional activated systems a DO level in the range of 1-3 mg/l with 2 mg/l is the desired minimum level.

• Water quality testing

Testing the water quality can be further grouped into two groups, the first is testing the performance of individual units and the second group is testing the performance of the total treatment plant. Samples will be taken at the entrance channel and exit point of the treatment plant for testing the integrated effects of the treatment units. The following parameters should be tested for inflow and outflow water; pH, COD, BOD₅, S.S, O&G.

5.3.2 Preparation of Final Inspection Report

The inspection team will be responsible for preparing a technical inspection report for the industrial facility after examining the analysis results. The inspection report should include the name(s) & signature (s) of the inspection team member(s), date & time of visit.

The inspection report will include the following sections: -

Company Description

This part includes general information regarding the industrial facility, brief description of its activity as well as sources & types of industrial wastewater streams.

Treatment Plant

This chapter will include brief description about the type of wastewater treatment plant and its components, treatment capacity, treatment efficiency, etc.

Results of Analysis

This will include the number of samples & the sampling techniques used as well as the results of the samples, which were taken during the visit and should also include the analysis results gathered from the company records during the visit.

Other Emissions

The generation of gaseous emissions (H_2S , SO_2 , CO_2) shall be described as possible, describe all treatment facilities of gaseous emissions,(if any).

Noise & odors in working environment.

Report solid and hazardous wastes and whether it is reside, treated or disposed of.

Conclusions & Recommendations

This chapter will include inspector comments and observations regarding the operation of the treatment plant. In addition, inspection results and the detected violations based on the lab analysis should be pointed out clearly. Further evaluation results may be included for example the efficiency as calculated based on samples obtained during inspection. Finally the inspectors recommendations regarding operation, maintenance, etc. of treatment plant should be stated.

Annexes

This should include samples analysis results, also, which obtained from company & all other correspondence. The inspector's checklist may also be attached in the annex.

The inspection report is to be submitted together with the laboratory report and the facility documents. In case where no violations were detected in the facility, the inspection report is filed at the responsible authority. In cases where violations are detected, the responsible authority informs the concerned administrative authority.

5.3.3 Guidance to the Inspectors

One) Good housekeeping

Good house keeping i.e. regular cleaning, tidying of site, buildings and pump houses, maintenance of green area, gardens and plantations will not only add to the life of the treatment plant but will provided psychological encouragement to the workers to work in an impressive atmosphere.

The site must be well-protected and barricaded and other safety regulations against fire, accidents and storage and handling of chemicals and equipment's should be observed strictly to

avoid any mishaps.

b) Operational records and reports

A full record of the physical plant, performance operation, maintenance equipment and reports drawing should be maintained to calculate the efficiency of the treatment.

Similarly all the operational manuals for each components of the plant and each item of equipment installed must be kept in a safe place for easy references in case of malfunctioning of the plant.

c) Maintenance of wastewater treatment plant

Operation and maintenance should be exercised in parallel and always go hand in hand. It is considered essential that at least the equivalent of one-third of the plant operation time should be spent in maintaining wastewater treatment plant equipment.

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(I)

INTRODUCTION TO INSPECTION OF INDUSTRIAL WWTP

(II)

INTRODUCTION TO INDUSTRIAL WASTEWATER TREATMENT PLANTS

(III)

DESCRIPTION OF MAIN TREATMENT TECHNOLOGIES

(IV)

EGYPTIAN LEGISLATION ON INDUSTRIAL WASTEWATER

(V)

INSPECTION PRINCIPLES AND EXAMPLES

5. INSPECTION PRINCIPLES AND EXAMPLES

5.1 TARGETS OF INSPECTION

The inspection of industrial wastewater treatment plant (IWWTP) aims to check the compliance of the outputs of the treatment process with respect to liquids, solids and gases with the regulatory limits. This in turn will lead to reduction of the negative environmental impacts.

The effectiveness of inspection will lead to the protection of the environment as well as protection of public health.

The objectives of IWWTP Inspection includes the following:

- Ensuring that the performance parameters are measured and recorded and shows effectiveness.
- Ensuring that treated effluent is in compliance with relevant laws for discharge wastewater to the environment either by direct measurements and/or indirect observations.
- Guiding the industry in case of malfunctioning of the treatment system to utilize technical and/or financial support mechanisms available in EEAA to rehabilitate the system.
- Ensuring the compliance of the establishments with the requirements of the environmental Law 4, 1994 in connection with holding an updated and valid environment register and applying self-monitoring procedures for IWWTP.
- Ensure that air emissions are not violating the law.
- Management of hazardous substances, wastes and non-hazardous solid wastes.

5.2 INSPECTION VISIT

5.2.1 Gathering Information and Auditing

As presented in the general guidelines for inspection team (EPAP 2000), tasks necessary for preparation for field inspection are:-

- Gathering information about the specific facility & review sector specific manuals for each industry in addition to gathering enough information about the treatment plant to be inspected and the generation of hazardous pollutants.
- Preparing of the inspection plan.
- Preparaing the checklist.

a) Gathering and reviewing information

The inspection team should review the general information prepared for the treatment plant type (chapter III) and then checked if possible what units and components are present at this type of treatment plant. It is important at this stage to determine the following:-

- The type of receiving body for the industrial wastewater and relavant Egyptian Laws (Chapter IV).

- The characteristics of the waste effluent which is discharged from the targeted facility and suitable treatment for this type (section 3.8).
- Typical violations, malfunctioning & troubleshooting for the targeted treatment plant.(section 5.2.3)

Note to inspectors:-

Some facilities dilute their polluted wastewater with potable water or groundwater before entering the treatment plant which is prohibited by law.

b) Preparation of the inspection plan

An example of an inspection plan is included in Annex (b) of the Guidelines for Inspection team (EPAP 2000). The plan should take into account the following:-

- At the beginning of the field visit, the inspection team should check the environmental register and the self monitoring system.
- The results of the analysis included in the environmental register should be checked at the end of the field visit and copies of the results should be obtained.

Note to inspectors:-

Make sure that all the production lines are in operation at the time of inspection. Make sure that the treatment plant is operating with a capacity greater than 50% of the design capacity.

c) Preparation of the required checklists

A general checklist for inspection of industrial wastewater plants is designed for this manual and illustrated in Annex (1). It is impossible to fill all the required information in the attached check list, the inspector must prepare a specific checklist case by case. The checklist has been prepared in such a way that it starts with general information about the facility and its operation followed by brief description for treatment plant and cover all relevant environmental aspects.

Note to inspectors:-

Law 4 does not specify standards for effluent from each treatment step but only for final treated effluent. However, effluent quality from each unit is an important indicator for the all efficiency of the treatment plant.

d) Performing the field inspection

The guidelines for Inspection Team (EPAP 2000) describes the procedures involved for entering the industrial facility. The inspector's attitude and behavior are very important from the start and will dictate the factory's personnel response to the inspection tasks.

Information gathered during the facility tour is dependent on interviews of facility personnel and visual observation. The following information should be collected during visiting time:-

General Information

- Establishment name and address.
- Responsible person.
- Industrial sector and subsectors.
- Main products.
- Production capacities.

Wastewater streams

- Sewerage network and wastewater discharge point. (Maps showing the discharge network).
- Quantity of WW discharge m^3/d .
- Discharge outlets.
- Industrial/domestic effluents separate or mixed.
- Points of discharging and receiving bodies (municipal network, the Nile, drainage, sea, reuse).

Treatment Plant

- The location of the plant and surrounding units.
- Units connected to the treatment plant.
- Type and description of the treatment process.

- Description of treatment equipment and its design elements.
- Input / output water loads.
- Input/output water quality.
- Design and actual efficiency.

Sludge Generation

- Sources of sludge generation.
- Sludge treatment.
- Characterization of sludge produced.
- Quantity of sludge.
- Final sludge disposal methods.

Gaseous emissions (if any)

- Characterization of gaseous emission.
- Sources of generation.
- Pollutant concentration and load for each element.
- Odor emissions
- Sources of odor emissions.
- Type of odor.

Chemicals Used

- Type of chemicals used.
- Amounts of chemicals.
- Storage facilities.
- List their main environmental and flammability properties.

Plan for emergency

- Existing a by-pass sewer line.
- Existing an equalizing tank to hold wastewater in case of any process failure.
- Trained maintenance staff.

Monitoring plan

- Indicators to be monitored.
- Sampling timetable.
- Sampling sites.
- Lab conducting analysis (onside or outside).
- Responsible person.
- Analyses protocols.
- Internal reports.
- Maintenance and calibration of self-monitoring instruments.

Note to inspectors:-

It is better at the beginning of the visit not to ask direct questions about quality of the treated effluent & the efficiency of the treatment plant. Interviewing the workers on-site in an indirect manner can give better results.

Check the results of effluent analysis, time and place of sampling. If suspicious make your own analyses.

e) Ending the field visit

When violations are detected a record is prepared stating information pertaining to sampling location and time. Violations of work environment regulations should also state location and time of measurements. Other visual violations as sludge accumulations, hazardous material and waste handling and storage and material spills should be photographed and documented. The facility management should sign these records.

A closing meeting with the facility management can be held to discuss findings and violations.

5.2.2 Collection of Samples for Analysis

The variety of conditions at different sampling locations requires that considerable judgment be exercised regarding the methodologies and procedures for the collection of representative samples of wastewater. There are, basic rules and precautions generally applicable to sample collection. Some important considerations for obtaining a representative wastewater sample include:

- The sample should be collected where the wastewater is well mixed. Therefore, the sample should be collected near the center of the flow channel, at approximately 40 to 60 percent of the water depth, where the turbulence is at a maximum and the possibility of solids settling is minimized. Skimming the water surface or dragging the channel bottom should be avoided. However, allowances should be made for fluctuations in water depth due to flow variations.
- In sampling from wide conduits, cross-sectional sampling should be considered.
- If manual compositing is employed, the individual sample portions must be thoroughly mixed before pouring the individual aliquots into the composite container. For manual composite sampling, the individual sample aliquots should be preserved at the time of sample collection.
- When collecting samples or installing sampling equipment, field investigators should always wear a new pair of the appropriate protective gloves (disposal latex gloves, rubber gloves, etc.) to prevent contamination of the sample and reduce exposure to hazardous substances.

Since law 4/94 does not specify standards for the effluent from production lines but only for the effluent from the final disposal point, therefore, the inspectors are only concerned with the end of pipe discharging points.

Sample Types

Two types of sampling techniques are used: grab and composite.

- **Grab Samples**. Grab samples consist of either a single discreet sample or individual samples collected over a period of time not to exceed 15 minutes. The grab sample should be representative of the wastewater conditions at the time of sample collection. The sample volume depends on the type and number of analyses to be performed.
- **Composite Samples**. Composite samples are collected over time, either by continuos sampling or by mixing discrete samples. A composite sample represents the average wastewater characteristics during the compositing period. Various methods for compositing are available and are based on either time or flow proportioning. The choice of a flow proportional or time composite-sampling scheme depends on the permit requirements, variability of the wastewater flow or concentration of pollutants, equipment availability, and sampling location. The investigator must know each of these criteria before a sampling program can be initiated. If an investigator knows or suspects that there is significant variability in the wastewater flow or if the investigator knows nothing about the facility, a flow proportional sample is preferable. Otherwise, a time composite sample would be acceptable.

A time composite sample consists of equal volume discrete sample aliquots collected at constant time intervals into one container. A time composite sample can be collected either manually or with an automatic sampler.

A flow proportional composite sample can be collected using one of two methods. One method consists of collecting a constant sample volume at varying time intervals proportional to the wastewater flow. For the other method, the sample is collected by varying the volume of each individual aliquot proportional to the flow, while maintaining a constant time interval between the aliquots. Prior to collecting flow proportional samples, the facility's flow measuring system should be examined for proper installation and accuracy. If the facility's primary flow measuring device does not meet standard conditions, or is in an unsafe or inaccessible location, then the investigator may collect time composite samples. If the flow measurement system is acceptable, samples should be collected using the appropriate flow proportioning methods.

Flow proportional samples can be collected with an automatic sampler and a compatible flowmeasuring device, semi-automatically with a flow chart and an automatic sampler capable of collecting discrete samples, or manually.

Use of Automatic Samplers

Automatic samplers may be used to collect composite or grab samples when several aliquots are to be collected at frequent intervals or when a continuous sample is required. For composite sampling applications, the automatic samplers may be used to collect time composite or flow proportional samples. In the flow proportional mode, the samplers are activated by a compatible flow meter. Flow proportional samples can also be collected using an automatic sampler equipped with multiple containers and manually compositing the individual sample portions proportional to the flow.

Automatic samplers must meet the following requirements:

- * Sampling equipment must be properly cleaned to avoid cross-contamination which could result from prior use.
- * No plastic or metal parts of the sampler shall come in contact with the water or wastewater stream when parameters to be analyzed could be impacted by these materials.
- * The automatic sampler must be capable of providing adequate refrigeration during the sampling period. This can be accomplished in the field by using ice.
- * The automatic sampler must be able to collect a large enough sample for all parameter analyses.
- * The individual sample aliquot must be at least 100 ml.
- * The automatic sampler should be capable of providing a lift of at least 20 feet and the sampler should be adjustable since the volume is a function of the pumping head.
- * The pumping velocity must be at least 2 ft/sec to transport solids and not allow solids to settle.
- * The intake line leading to the pump must be purged before each sample is collected.
- * The minimum inside diameter of the intake line should be $\frac{1}{4}$ inch.
- * An adequate power source should be available to operate the sampler for the time required to complete the project. Facility electrical outlets may be used if available.

Manual Sampling

Manual sampling is normally used for collecting grab samples and/or for immediate in-situ field analyses. However, it can also be used in lieu of automatic equipment over extended

waste stream conditions.

The best method to manually collect a sample is to use the actual sample container, which will be used to transport the sample to the laboratory. This eliminates the possibility of contaminating the sample with intermediate collection containers. If the sampling personnel cannot physically reach the wastewater stream or it is not safe to reach for the sample, an intermediate collection container may be used, from which the sample can be redistributed to other containers. If this is done, however, the container used to collect the sample must be properly cleaned and must be made of a material that meets the requirements of the parameter(s) being investigated. Samples for oil and grease, bacteria, phenols, volatile organic compounds, and sulfides analyses must always be collected directly into the sample container.

In some cases it may be best to use a pump, either power or hand operated, to withdraw a sample from the wastewater stream. If a pump is used, it is imperative that all components of the pump that come in contact with the sample are properly cleaned to ensure the integrity of the sample.

In general, samples are manually collected by first selecting a location in the wastewater that is well mixed then dipping the container in the wastewater stream so the mouth of the container faces upstream. The container should not be overfilled if preservatives are present in the container.

Analysis Parameters

The selection of parameters for the analysis depends on the nature and characteristics of the influent which is directly related to the type of industry. The most common parameters requiring analysis for industrial wasteater effluents are:-

pH,	T.S.S,	TDS,
BOD ₅ ,	COD,	O&G,
CL,	$NO_3 - N$,	$PO_4 - P$,
$NH_3 - N$,	Heavy metals,	Phenols,
Cyanide.	•	

5.2.3 Typical Cases of Malfunctioning & Process Failure

The inspector can detect the most significant malfunctioning of the treatment process during his visit by the following observations: -

- Bad odour release and gaseous emissions due to:- a) the septic build up condition especially in sedimentation tanks or b) the accumulation of rags and other debris on the bar screen, c) malfunctioning and poor maintenance of biological filters, clarifiers, sludge thickening and drying beds.
- Black colour of raw wastewater with septic odour indicates that part of the wastewater is being retained because of slow flow due to a build up of sludge or grit.
- Thick, dark, greasy, scummy layers of deep tan to brown foam covering the entire surface of aeration tanks always indicates that the sludge is too old and may be over oxidized.
- Excessive, billowing, white foam in aeration tanks may be due to young sludge. The sludge age should be increased by reducing the sludge waste rate.
- The presence of air bubbles on the surface of the aeration tank is an indication the proper activity of the biomass.

- An extremely dark brown colour with the odour of hydrogen sulphide in aeration tanks of activated sludge treatment indicates poor oxidation. A dark brown colour with an earthy smell of oxidized wastewater in the aeration tank is an indication of proper functioning of the system.
- Surcharging around treatment units due to screens or grit chambers blockage, clogging of under drains biological filters as a result of the growth of algae and development of slime.
- Ponding of filters due to improper grading of the stone media and small size stones filled between larger size media.
- Flies around the biological filters. These may be present due to poor distribution of wastewater along the filter walls and insufficient hydraulic loading.
- High levels of noise due to improper maintenance of mechanical equipment.

The inspectors should check the following points to insure that the operation of industrial process is normal during inspection time: -

- Quality of the influent water to the treatment plant (during peak processing time or during washing time).
- The entry pipeline to the treatment plant and compare with sewerage network map to identify the presence of any by-passing line which goes directly to the sewer line.

The inspectors can detect dubious analysis results provided by the company by checking the relationship between different parameters such as:-

- COD value should be higher than the BOD₅ value.
- High levels of O&G value lead to the high levels of COD value.
- Total solid values should be higher than level of suspended solids.
- Total solids equal the level of suspended solids & dissolved solids.

The inspectors should also check the relationship between the actual production capacity and the performance of wastewater plant at the time of inspection, in order to compare the operation values with design values (i.e. lower capacity means better performance, lower hydraulic load means higher quality of treated water due to the effect of water recycling).

The industrial plant should have a self-monitoring system for the treatment plant. All monitoring should be done and samples be taken, analyzed. Parameters monitoring, sampling locations, and sampling frequencies, analytical procedures and type of sampling also should be reported.

Specific inspection issues for main treatment methods that can be easily used to detect malfunctioning(physical, chemical and biological) are given in table (5-1).

Physical Treatment	Chemical Treatment	Biological Treatment
 Clogging /surcharging 	 Type of chemicals used 	– Bad odor
- Odor emission	 Amounts of Chemical Consumption 	– Black Color
Fouling	Efficient sludge Separation, Turbidity of treated effluent	 Nutrients consumptions
Flies	pH level	 Air bubbling (as measure for Biomass activity)
Noise	Color	– Flies
		 Fouling of biological filters (clogging, flooding)
		Foaming indication of old sludge

Table (5-1) Specific malfunctioning issues for main treatment methods

5.2.4 Examples Cases of Process Failure

• Yeast Production Factory:-

Failure to reach design parameters for treated effluent due to increased levels of introduced pollution influent mainly pH and COD.

• Spinning & Weaving Manufacturing Factory:-

Poor efficiency of activated sludge system due to the increased level of hydraulic loading besides the inefficiency of the Aeration System.

• Food Industry (Chocolate & Confectionery Production Factory):-

Failure of the activateded sludge system to work on full capacity (50 m^3/d) as currently treating only 25 m^3/d . The problem is focussed on the inadequate design of the clarifier (short retention time).

• Spinning & Weaving Manufacturing Factory:-

Physio chemical/Biological treatment failed to fulfill the design parameters as there were problems related to process sequence & chemical additives-e.g chemical are added during biological stage - The plant is out of operation since 13 years ago.

5.3 INSPECTION RESULTS

5.3.1 Observations on operation of IWWTP

• Odour

Odour problem is usually due to the excessive organic loading of industrial wastes or malfunctioning and poor maintenance of trickling filters, primary and secondary clarifiers and sludge thickening tanks.

• Colour

The black colour of raw wastewater with septic odour may indicate that part of wastewater is being retained because of slow flow due to a build up of sludge or grit.

• Surface foam and scum

Thick, dark, greasy, scummy layers of deep tan to brown foam covering the entire surface of aeration tanks always indicates that the sludge is too old and may be over oxidized.

• Dissolved Oxygen

An extremely dark brown colour with the odour of hydrogen sulphide in aeration tanks indicates poor oxidations. In conventional activated systems a DO level in the range of 1-3 mg/l with 2 mg/l is the desired minimum level.

• Water quality testing

Testing the water quality can be further grouped into two groups, the first is testing the performance of individual units and the second group is testing the performance of the total treatment plant. Samples will be taken at the entrance channel and exit point of the treatment plant for testing the integrated effects of the treatment units. The following parameters should be tested for inflow and outflow water; pH, COD, BOD₅, S.S, O&G.

5.3.2 Preparation of Final Inspection Report

The inspection team will be responsible for preparing a technical inspection report for the industrial facility after examining the analysis results. The inspection report should include the name(s) & signature (s) of the inspection team member(s), date & time of visit.

The inspection report will include the following sections: -

Company Description

This part includes general information regarding the industrial facility, brief description of its activity as well as sources & types of industrial wastewater streams.

Treatment Plant

This chapter will include brief description about the type of wastewater treatment plant and its components, treatment capacity, treatment efficiency, etc.

Results of Analysis

This will include the number of samples & the sampling techniques used as well as the results of the samples, which were taken during the visit and should also include the analysis results gathered from the company records during the visit.

Other Emissions

The generation of gaseous emissions (H_2S , SO_2 , CO_2) shall be described as possible, describe all treatment facilities of gaseous emissions,(if any).

Noise & odors in working environment.

Report solid and hazardous wastes and whether it is reside, treated or disposed of.

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ANNEX 1

DEFINITIONS AND TERMINOLOGY

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- **Absorption.** The passage of one substance into or through another, e.g. an operation in which one or more soluble components of a gas mixture are dissolved in a liquid.
- Activated Carbon. A highly adsorbent form of carbon used to remove odorous and toxic substances from liquid or gaseous emissions. In waste treatment it is used to remove dissolved organic matter from wastewater.
- Activated Sludge. Sludge that results when primary effluent is mixed with bacterialaden sludge and then agitated and aerated to promote biological treatment. This speeds breakdown of organic matter in raw sewage undergoing secondary waste treatment.
- Adsorption. An advanced method of treating waste in which activated carbon removes organic matter from wastewater.
- Advanced Wastewater Treatment. Any treatment of sewage that goes beyond the secondary or biological water treatment stage and includes the removal of nutrients such as phosphorus and nitrogen and a high percentage of suspended solids.
- Aerobic Treatment. Process by which microbes decompose organic compounds in the presence of oxygen and use liberated energy for reproduction and growth. Types of aerobic processes include extended aeration, trickling filtration, and rotating biological contractors.
- **Agglomeration.** The process by which precipitation particles grow larger by collision or contract with cloud particles or other precipitation particles.
- **Anaerobic.** A process that occurs in, or is not destroyed by, the absence of oxygen.
- **Bar Screen.** In wastewater treatment, a device used to remove large solids.
- **BOD** (**Biochemical Oxygen Demand**). A measure of the amount of oxygen consumed in the biological processes that break down organic matter in water.
- **Biodegradable.** The ability to break down or decompose rapidly under natural conditions and processes.
- **Biological Treatment.** A treatment technology that uses bacteria to consume waste. This treatment breaks down organic materials.
- **COD** (**Chemical Oxygen Demand**). A measure of the oxygen required to oxidize all compounds in water, both organic and inorganic.
- **Chemical Treatment.** Any one of a variety of technologies that use chemicals or a variety of chemicals processes to treat waste.
- **Clarifier.** A tank in which solid is settled to the bottom and is subsequently removed as sludge.
- **Coagulation.** A clumping of particles in wastewater to settle out impurities. It is often induced by chemicals such as lime, alum, and iron salts.
- **Contaminant.** Any physical, chemical, biological, or radiological substance or matter that has an adverse effect on air, water, or soil.
- **Dechlorination.** Removal of chlorine for a substance by chemically replacing it with hydrogen or hydroxide ions in order to detoxify the substances involved.

- **Decomposition.** The breakdown of matter by bacteria and fungi. It changes the chemical makeup and physical appearance of materials.
- **Denitrification.** The anaerobic biological reduction of nitrate nitrogen gas.
- **Diffused Air.** A type of aeration that force oxygen into sewage by pumping air through perforated pipes inside a holding tank and bubbling it through the sewage.
- **Digester.** In wastewater treatment, a unit process for degradation of sludge.
- **Disinfectant.** A chemical or physical process that kills pathogenic organisms in water. Chlorine is often used to disinfect sewage treatment effluent, water supplies, wells, and swimming pools.
- **DO** (**Dissolved Oxygen**). The oxygen freely available in water. Dissolved oxygen is vital to fish and other aquatic life and for the prevention of odors. Secondary and advanced waste treatment are generally designed to protect DO in waste-receiving waters.
- **Dissolved Solids.** Disintegrated organic and inorganic material contained in water. Excessive amounts make water unfit to drink or to use in industrial processes.
- **Evaporation Ponds.** Areas where sewage sludge is dumped and allowed to dry out.
- **Filtration.** A treatment process for removing solid (particulate) matter from water by passing the water through porous media such as sand or a manmade filter. The process is often used to remove particles that contain pathogenic organisms.
- **Flocculation.** The process by which clumps of solids in water or sewage are made to increase in size by biological or chemical action so that they can be separated from the water.
- **Heavy Metals.** Metallic elements with high atomic weights, e.g., mercury, chromium, cadmium, arsenic, and lead. They can damage living things at low concentration and tend to accumulate in the food chain.
- **Ion Exchange Treatment.** A common water softening method often found on a large scale at water purification plants that remove some organisms and radium by adding calcium oxide or calcium hydroxide to increase the pH to a level where the metals will precipitate out.
- **Mechanical Aeration.** Use of mechanical energy to inject air into water to cause a waste stream to absorb oxygen.
- **Nutrient.** Any substance assimilated by living things that promote growth. The term is generally applied to nitrogen and phosphorus in wastewater, but is also applied to other essential and trace elements.
- **Organic Matter.** Carbonaceous waste contained in plant or animal matter and originating from industrial sources.
- **Pathogens.** Microorganism that can cause disease in other organisms or in humans, animals and plants. They may be bacteria, viruses, or parasites and are found in sewage. Fish and shellfish contaminated by pathogens, or the contaminated water itself, can cause serious illnesses.
- **pH**, A measure of the acidity or alkalinity of a liquid or solid material.
- **Physical & Chemical Treatment.** Processes generally used in large-scale wastewater treatment facilities. Physical processes may involve air stripping or filtration. Chemical treatment includes coagulation, chlorination, or ozone addition.

- **Pretreatment.** Processes used to reduce, eliminate, or alter the nature of wastewater pollutants from non-domestic sources before they are discharged into publicly owned treatment works.
- **Primary Waste Treatment.** First steps in wastewater treatment; screens and sedimentation tanks are used to remove most materials that float or will settle. Primary treatment results in the removal of about 30 per cent of carbonaceous biochemical oxygen demand from domestic sewage.
- **Raw Sewage.** Untreated wastewater.
- **Residual.** Amount of pollutant remaining in the environment after a natural or technological process has taken place, e.g., the sludge remaining after initial wastewater treatment.
- **Reverse Osmosis.** A water treatment process used in small water systems by adding pressure to force water through a semi-permeable membrane.
- **Sand Filters.** Devices that remove some suspended solids from sewage. Air and bacteria decompose additional wastes filtering through the sand so that cleaner water drains from the bed.
- Screening. Use of screens to remove coarse floating and suspended solids from sewage.
- Secondary Treatment. The second step in most publicly owned waste treatment systems in which bacteria consume the organic parts of the waste. It is accomplished by bringing together waste, bacteria, and oxygen in trickling filters or in the activated sludge process. This treatment removes floating and settable solids and about 90 per cent of the oxygen-demanding substances and suspended solids. Disinfection is the final stage of secondary treatment.
- **Sedimentation.** Letting solids settle out wastewater by gravity during wastewater treatment.
- **Settlable Solids.** Materials heavy enough to sink to the bottom of a wastewater treatment tank.
- Skimming. Using a machine to remove oil or scum from the surface of the water.
- **Sludge.** A semi-solid residue from any number of air or water treatment processes.
- **Stabilization.** Conversion of the active organic matter in sludge into inert, harmless material.
- **Suspended Solids.** Small particles of solid pollutants that float on the surface of, or are suspended in sewage or other liquids. They resist removal by conventional means.
- **Tertiary Treatment.** Advanced cleaning of wastewater that goes beyond the secondary or biological stage. It removes nutrients such as phosphorus and nitrogen and most BOD and suspended solids.
- **TDS (Total Dissolved Solids).** The total amount of dissolved solid materials present in an aqueous solution.
- **TOC** (**Total Organic Carbon**). TOC is a measure of the amount of carbon in a sample originating from organic matter only. The test is run by burning the sample and measuring the CO₂ produced.

- **TOD** (Total Oxygen Demand). A measure of the oxygen demand of wastewater by injecting a small volume of the sample into oxygen containing carrier gas and passed through a catalyst bed at 900 °C. The carbon, nitrogen, and many minerals are converted to their oxides by consuming oxygen from the carrier gas, this amount of gaseous oxygen consumed is measured and given as the TOD of the sample in mg oxygen/liter of wastewater.
- **TSS** (**Total Suspended Solids**). A measure of the suspended solids in wastewater, effluent, or water bodies.
- **Trickling Filter.** A coarse, biological treatment system in which wastewater is trickled over a bed of stoned or other material covered with bacterial growth, leading to bacterial break down of the waste.
- **Turbidity.** A cloudy condition in water due to suspended silt or organic matter.
- **VSS (Volatile Suspended Solids).** The suspended organic fraction which will oxidize and will driven off as gas at temperature 550 $^{\circ}C \pm 50 ^{\circ}C$.
- **Waste Treatment Plant.** A facility containing a series of tanks, screens, filters, and other processes by which pollutants are removed from water.

ANNEX 2

INSPECTION CHECKLIST FOR INDUSTRIAL WASTEWATER PLANTS

GENERAL CHECKLIST FOR INDUSTRIAL WASTEWATER PLANTS

Information about the Inspection Process					
Data and time of inspection					
Facility Name and address					
Contact person at the facility	Name				
	Title				
	Phone				
Inspection team N	lame		Tit	le	Phone number
Team Leader					
Inspector					
Inspector					
Lab specialist					
Gener	ral Infor	mation al	oout the F	Facility	
Main production units					
Operating times for process					
	Che	ck for the	Presence	of the Follov	wing Service Units
Laboratories					
Workshops					

1

Garage

Storage facilities

Boilers

Information about Wastewater Streams				
Describe the sewerage system and show it on a relevant map				
- Sources of industrial W.W	Washing Boilers Cooling towers Production units (explain) Others (explain)			
- Amount of WW discharge		m ³ /d m ³ /hr		
- Number of final discharge points				
- Final receiving body for industrial wastewater	 * Municipal sewerage * Into the Nile * Brackish * Into sea * On land * Reuse in the factory 			

Visual observations for sewerage network.					
network.					
Quality of raw wastewater	рН				
	COD				mg/l
	BOD ₅				mg/l
	S.S				mg/l
	TDS				mg/l
	0&G				mg/l
	Others -				mg/l
Int	formation	about Tr	eatment	Plant	
1) General information					
- Capacity of treatment plant					m ³ /d m ³ /hr
- Location of the plant and surrounding area					
- Specify the main components in WWTP					
* Equalization tank			Found		Not found
* GOS units			Found		Not found
* Screens			Found		Not found
* Chemical Treatment (Specify t	ype)		Found		Not found
* Biological Treatment (Specify	type)		Found		Not found
* Sludge Treatment (Specify)					
* Others (specify)					
- Process units connected to treatme	ent plant				
- Attach process flow diagram for t	reatment pl	ant (if an	y).		

 <i>Chemicals used</i> List any chemicals & their quant 	ities used for wastewater treatment
- Handling of chemicals	
3) Quality of treated water	pHmg/l S.Smg/l BOD ₅ mg/l CODmg/l O&Gmg/l Othersmg/l Copies for available analysis
Visual observations about quality o	
4) Sludge generation	
 <i>4) Sludge generation</i> Sources of sludge generation 	GOSChemical treatmentBiological treatmentOthers (explain)
	% dewatering Liquid
-Quantity f sludge produce	ton/d

-Determine the sludge disposal method	General municipal	
	Landfill	
	Incineration	
5) Gaseous emission		
- Sources of gaseous emissions		
Types of emission	H_2S	
	Others (specify)	
6) Status of the work environmental		
- Are there any order /noise in work envi	ronmental Yes	No
7) Plain for emergency		
- Existing a by-pass sewer line	Yes	No
- Capacity of the equalizing	m ³	
- Existing of a trained maintenance staff-		
- Others (specify)		
8) Monitoring plan		
- Parameters monitored (specify)		
Emission parameters:		
Operational parameters:		
- Sampling location		
- Sampling frequency		
- Responsible labs for analysis	Inside	outside
The existing of the operation & maintena	nce program Yes	No