

Squeezing the Most Out of Your Decision for Municipal Solids Handling

#### **Dewatering Selection**

Why dewater anyway?

<sup>3</sup>21,594 Publicly Operated Treatment Works (POTW's) provide wastewater collection, treatment and disposal service to 226.4 million people in the U.S.

POTWs generate over 8 million dry tons of sludge annually.

#### -University of Michigan Center for Sustainability





## **Dewatering Selection**

Why dewater anyway?

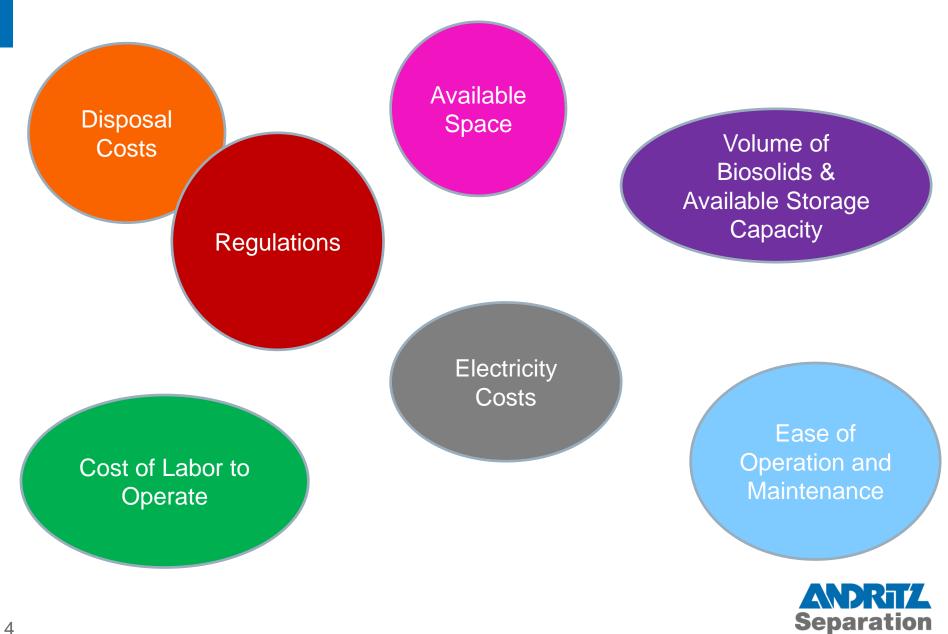


Solids have to go somewhere, And this costs \$!





# **Drivers for Dewatering Equipment Selection**



#### Title of presentation

#### Contents

- Chapter 1: Overview of Some Dewatering Equipment Options
  - **–Belt Filter Press**
  - -Centrifuge
  - -Screw Press
  - -Filter Press
- Chapter 2: Performance of Various Equipment Options
- Chapter 3: Sludge Characteristics
- Chapter 4: Process Defines Dewaterability



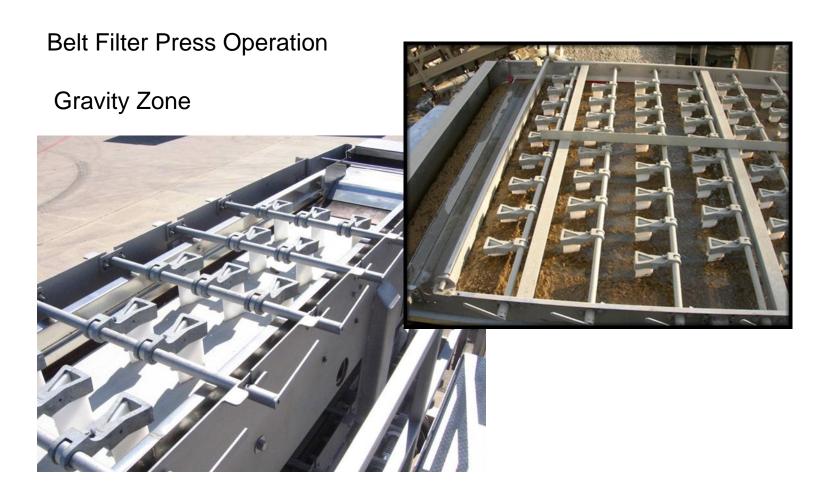
#### Belt Filter Press

- Operates on the theory of incrementally increasing the stability of the sludge by increasing applied pressure
- Flocculation → Gravity drain → Wedge pressure → High pressure rollers





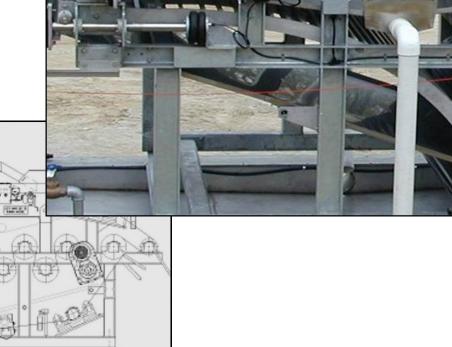
**Belt Filter Press** 





Belt Filter Press

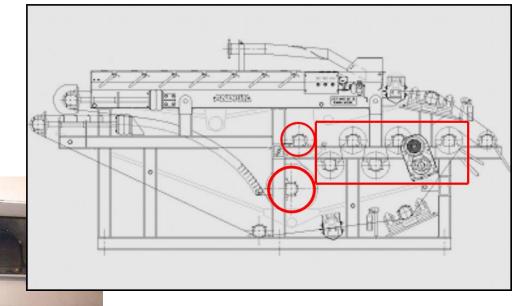
Belt Filter Press Operation Wedge Zone



#### Belt Filter Press

**Belt Filter Press Operation** 

S-Roll Zone





Belt Filter Press

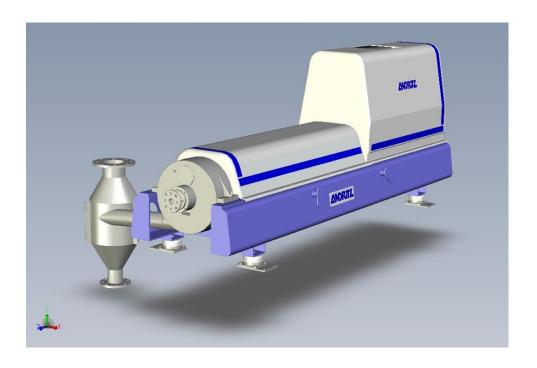
Belt Filter Press Operation Cake Discharge





## Centrifuge

- Operates on the theory of applying centrifugal force to flocculated solids in a bowl, conveyed out by a scroll- operating at slightly different speeds
- Polymer injection → Solids plug formation → 3000 X G + bowl/scroll differential



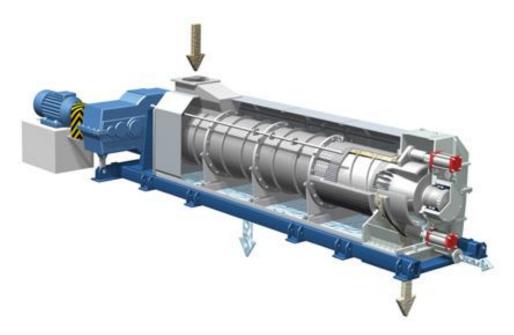


# **Centrifuge Operation**



#### Screw Press

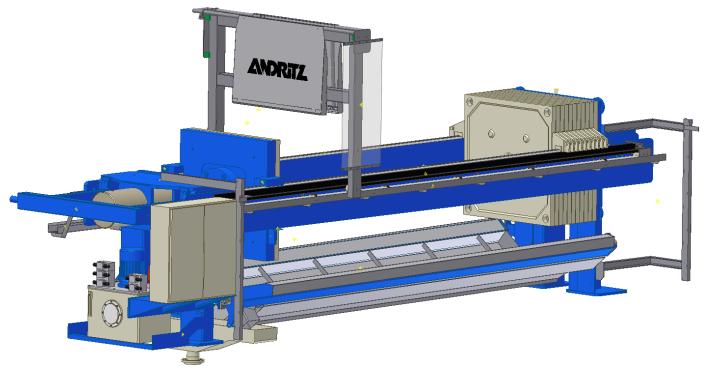
- Operates on the theory of solids conveyance through a cylindrical screen which offers decreasing volume through the use of an increased shaft diameter
- Flocculated sludge → Feed hopper → Cylindrical screen → Compression and back pressure





#### Filter Press

- Operates on the theory of a pump feeding solids into a fixed volume press, which causes an increase in pressure within the press.
- Conditioned feed → Pumped in at 100 to 225 psi → Increase in pressure due to fixed volume → Solids captured on filter cloths



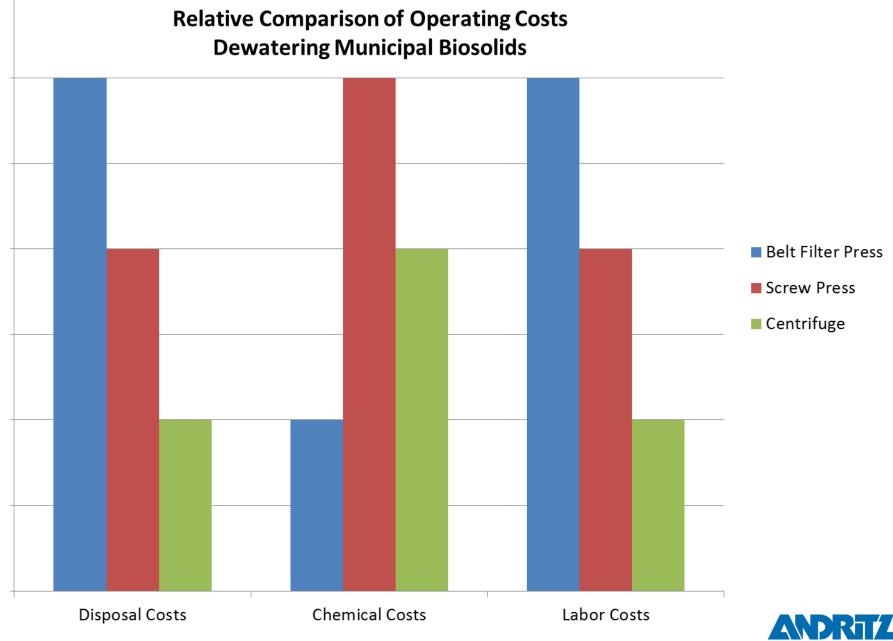
# Belt Filter Press vs. Centrifuge





	Belt Filter Press	Centrifuge		
Footprint	Large space plus clearance	Small space and clearance		
Odor Containment	Open design	Fully enclosed		
Labor Requirement	Requires operator attention	Fully automated, low attention		
Chemical Conditioning	Typically 10 - 30% less polymer	Typically 10 - 30% more polymer		
Cake Dryness	Typically 4 - 8% less on same sludge	Typically 4 - 8% higher on same sludge		
Capture Efficiency	Typically >95% except on dilute sludge	Typically >96%		
Wash Water Requirement	Continuous 40 gpm/meter @ 120 psi	Only at alarm or shut-down		
Power Consumption	Typically lower	Typically higher		
Automation	Partial automation	Fully automated		
Maintenance	See recommended maintenance	See recommended maintenance		
Operator Friendly	Less	More		



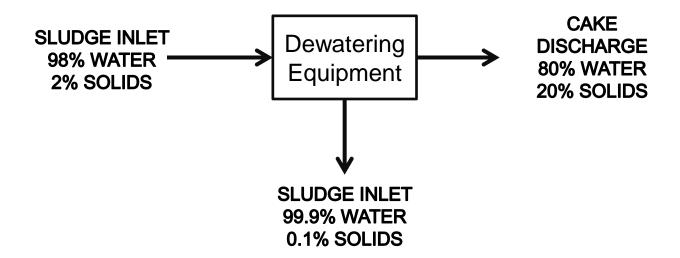


## Sludge Characteristics

Type of sludge and charateristics of each will have impact on decision of type of equipment.

Key Characteristics of Sludge for Dewatering Equipment Suppliers

 Suspended Solids Content – Key for throughput calculations and mass balance





## Sludge Characteristics

Key Characteristics of Sludge for Dewatering Equipment Suppliers

 Ash / Volatile Solids Content – More importantly the amount of biological solids.

Volatile Solids relates with the amount of biomass solids which are 99+% water and can be hydrophillic.

Ash Content relates with the amount of non organic material which is typically easier to dewater. Sand, Silt, etc.



## Sludge Characteristics

Key Characteristics of Sludge for Dewatering Equipment Suppliers

3) Screen Analysis – Used for determination of size and type of solids.

Larger particles including fiber are easier to dewater. They can help form a matrix to apply pressure and even aid in capturing finer solids.

Fiber usually retained on the 30, 50, 100 mesh sieves (600, 300, 150 microns) Also can help determine the amount of sand / grit which can cause abrasion.



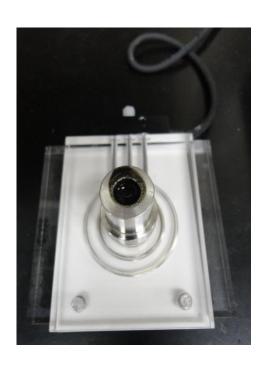


## Sludge Characteristics

Key Characteristics of Sludge for Dewatering Equipment Suppliers

 Capillary Suction Time – An older test Standard Methods 2710 G

A good indicator of how sludge releases water, how much coagulant or flocculant will be required.





**Process Defines Dewaterability** 

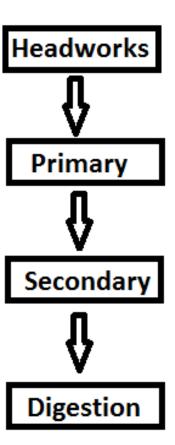
Sources of Solids / Biosolids

Headworks – Screened Solids / Grit Removal

**Primary Clarifiers** 

**Secondary Clarifiers** 

Digestion - Anaerobic, Aerobic, ATAD, etc



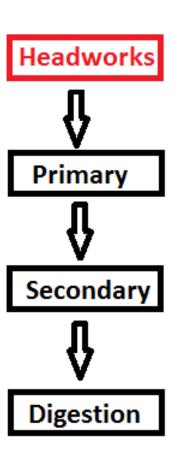


#### **Process Defines Dewaterability**

#### **Headworks**

Screens – Perforated, Wedgewire, Bar, etc Solids are typically disposed in landfill. Compaction sometimes used to dewater / remove organics prior to landfill

Grit Removal – Grit, Sand, Silt, Gravel, etc Solids are typically disposed in landfill





#### **Process Defines Dewaterability**

Primary Sludge - Settleable solids and scum

Solids Concentration – 2 to 4%TS

Volatile Solids Content - 70 to 85%

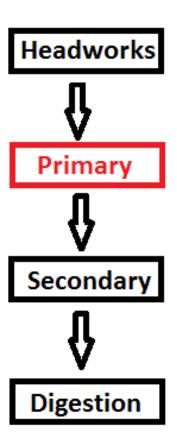
pH - 5-7

Odor – Fecal, Septic

Color – Black to Dark Green or Dark Brown

Solids Description -

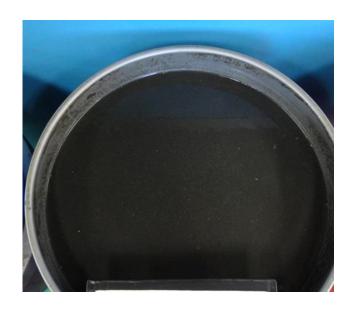
Larger suspended solids that settle out. Typically fibrous (tissue paper), large organic debris not capture in screens. 25-40% of suspended solids larger than 45 microns.





## **Process Defines Dewaterability**

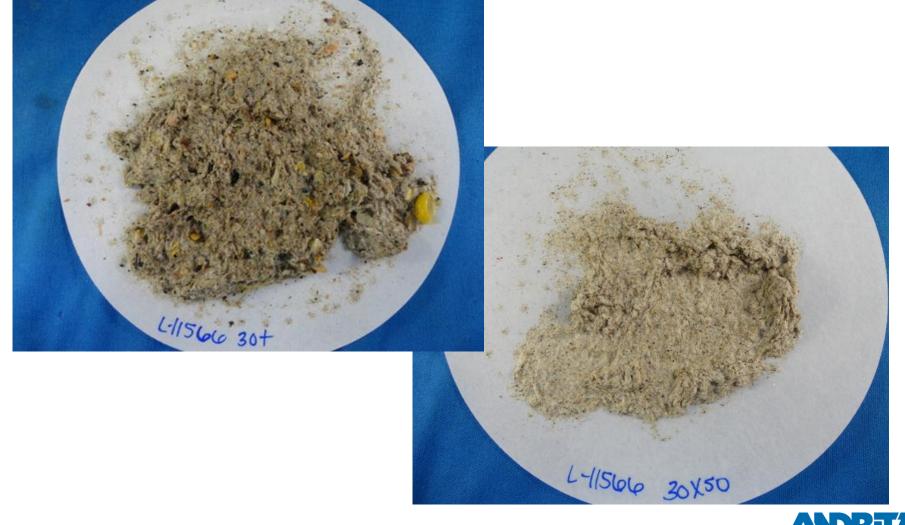
**Primary Sludge** 







**Process Defines Dewaterability** 



#### **Process Defines Dewaterability**

Secondary Sludge – Biological Treatment Sludge Waste Activated Sludge, Sequence Batch Reactor, Oxidation Ditch

Solids Concentration – 0.3 – 2.0%TS

Volatile Solids Content – 65 – 85%

pH - 6 - 8

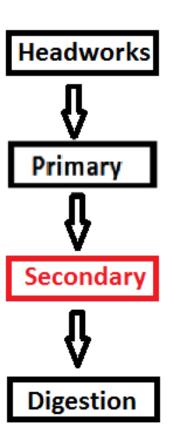
Odor – Faint humic

Color – Light Brown to Tan

Solids Description -

Biological, Smaller Particle size only 10-20% larger than 45 microns

MBR Sludge typically has lower solids and even smaller particle size with 5-10% larger than 45 microns



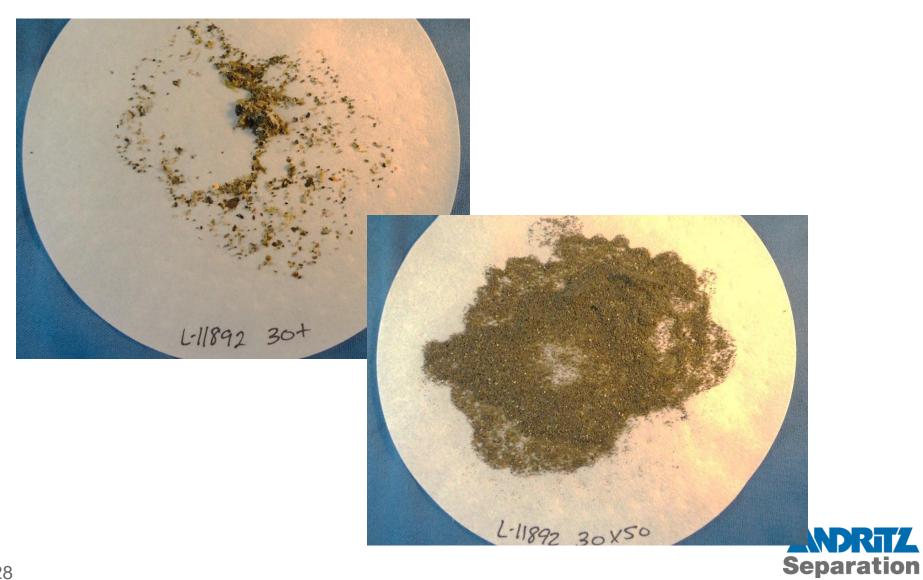


Sludge Characteristics





**Process Defines Dewaterability** 



## **Process Defines Dewaterability**

Digestion

**Anaerobically Digested** 

Solids Concentration – 2 to 4%TS

Volatile Solids Content - 55-65%

pH - 6 - 8

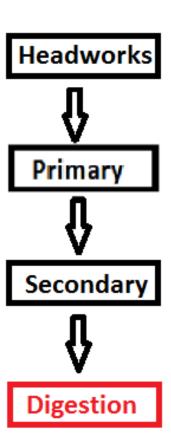
Odor - Humic

Color - Black / Dark Brown

Solids Description -

Biological, Little to No Debris or Fiber, Only solids too large to break down and were not removed

during screening

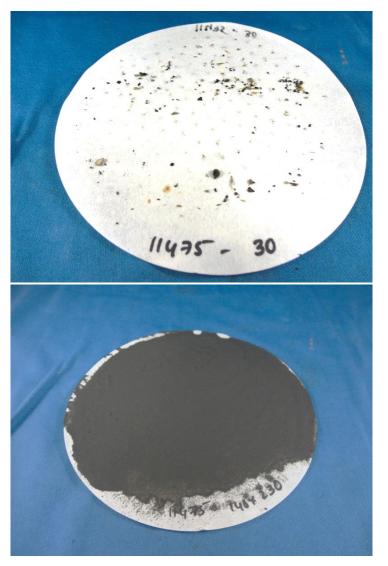




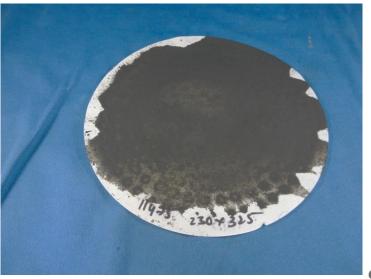
What are you dewatering?



Process Defines Dewaterability









## **Process Defines Dewaterability**

**Aerobically Digested** 

Solids Concentration – 1 to 2%TS

Volatile Solids Content – 60-75%

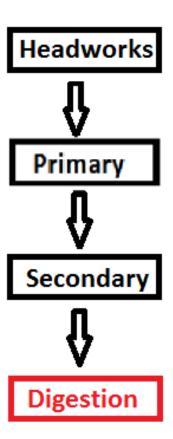
pH - 6 - 8

Odor - Humic

Color - Brown, Tan

Solids Description –

Biological, Little to No Debris or Fiber, Only solids too large to break down and were not removed during screening





Process Defines Dewaterability



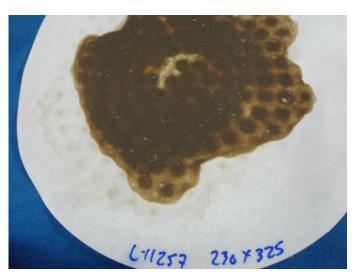


Process Defines Dewaterability











#### Performance

	<b>Belt Press</b>		<b>Screw Press</b>		Centrifuge		Filter Press	
	Cake Solids	Poly	Cake Solids	Poly	Cake Solids	Poly	Cake Solids	Poly
Anaerobic	15-17	21-23	21	32	23-26	20-22		
Aerobic	15-16	14-16	20	25	19-22	20-22		
WAS	15-16	14-16	*	*	17-20	18-20		
Primary	25-29	9-11			20-35	11-12		
Lime (WTP)	30-50	2-5			55-65	0	60-65	0
Alum (WTP)	15-20	5-10			22-26	8-12	20-30	0-5

BFP data from lab simulations (± 0.5%)/ Centrifuge data from full-scale pilot tests Screw press data from Huber's "Predicting Screw Press Performance" presented at 2011 WEFTEC

Units: Cake Solids (%TS), Polymer Dosage (active lbs/ton)



<sup>\*</sup>Similar to Aerobic results, as stated by Huber

#### Summary

- The needs and priorities of each plant will vary
- Every sludge is different
- A holistic approach yields the best dewatering selection
  - Disposal options and limitations
  - Space availability
  - Regulations
  - Electricity costs
  - Labor costs
  - Storage capacity
- Sludge characteristics influence the dewaterability of sludge, so

Bench Testing and/or Pilot Testing are always recommended!

