CE 356: Fundamentals of Environmental Engineering

Environmental Microbiology & Engineering Design

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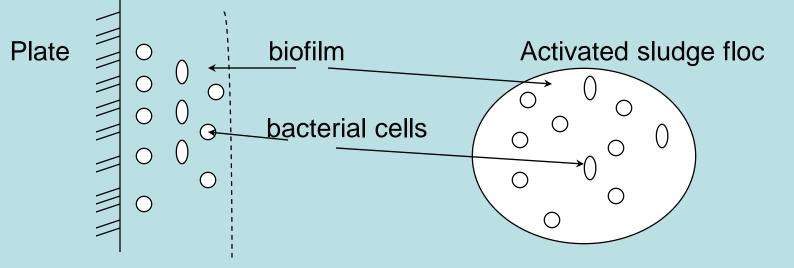
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Learning Objectives

- Comprehend the concepts of:
 - Distribution of energy from BOD under aerobic and anaerobic growth of bacteria,
 - "Nutritional" value of domestic wastewater for bacteria,
 - Batch growth of bacteria,
 - Design equation for continuous growth of bacteria,
 - Sludge age,
 - Food to microorganism (F/M) ratio.

Significant Microorganisms

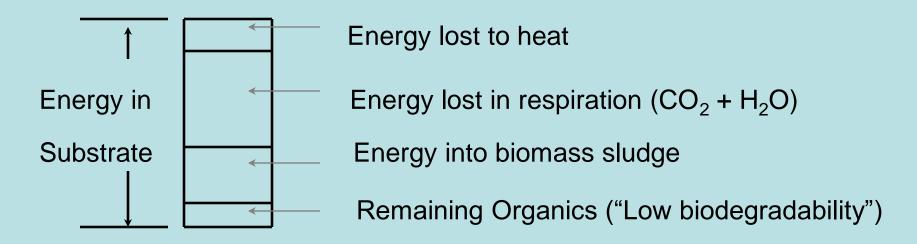
- Bacteria single cell microorganisms that reproduce by binary fission.
- Fungi yeasts and molds.
- Protozoa Single cell animals
 - Bacteria consume soluble (dissolved) BOD (organic substrate) and are aggregated into biofilm and floc to which suspended solids attach.



Aerobic Metabolism

Bio deg radable + Bacteria + $O_2 \rightarrow CO_2 + H_2O$ + Bacteria Organics + remaining organics

• Efficient conversion of energy



 Good for the receiving stream, high biomass yield and low BOD in final effluent

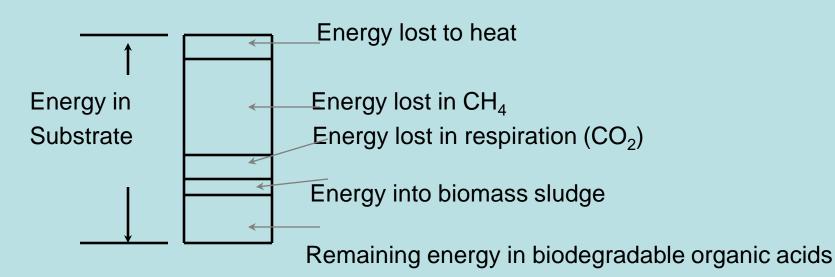
Anaerobic Metabolism

Biodegradable + Bacteria $\rightarrow CH_4 + CO_2 + Bacteria$

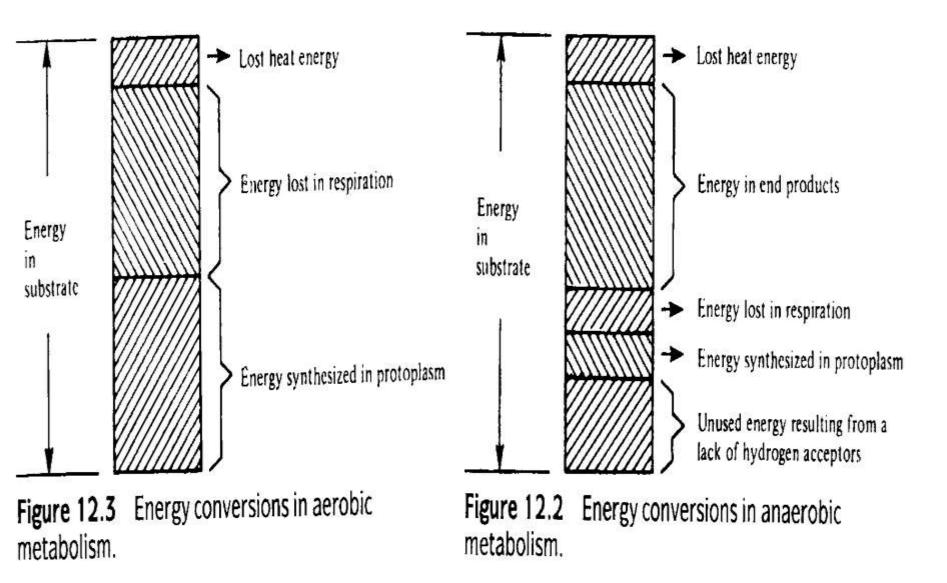
Organics

+ Organic Acids (Biodegradable)

• Inefficient conversion of energy



 Low biomass yield and high BOD in final effluent



(from Viessman, Jr. and Hammer, 1998, pp. 521-522)

Aerobic vs Anaerobic Treatment

- Compare the segments of energy distribution in the waste material for each treatment type.
- Match the segment of each energy bar with the appropriate component of each biochemical equation.
- How does the design engineer decide which form of treatment to use for a given waste source?

Biomass General Formulas

- C₆₀H₈₇O₂₃N₁₂P
- $C_5H_7O_2N_2$
 - C = 50% O = 20% N = 14% H = 8% P = 3%Total = 95%

How does this information relate to the characteristics of wastewater?

Growth of Heterotrophic Cultures

- Cultures:
 - Continuous Growth: substrate (BOD) fed continuously
 - Batch Growth:
 - Single dose of substrate (BOD)
 - Single inoculation of biomass (mixed liquor suspended solids, MLSS)
 - > Growth not limited by O₂, N, or P
 - Monitor change of substrate level (COD or BOD) and MLSS with time

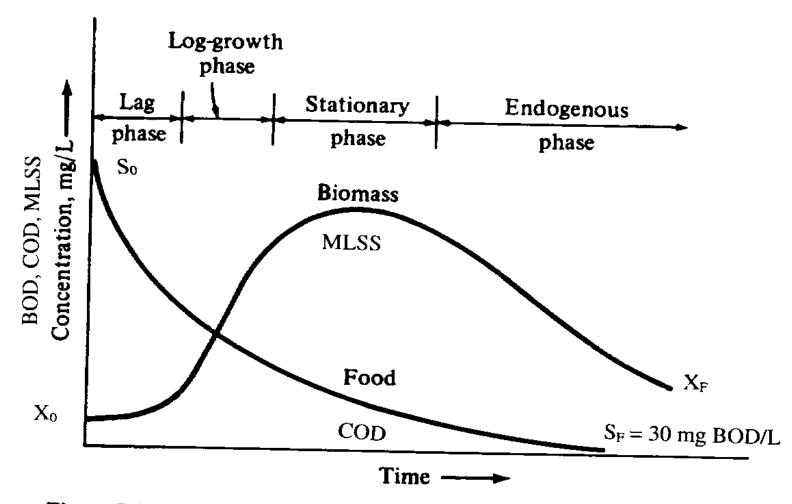


Figure 5-14 Biomass growth and food utilization.

 $X_F - X_O = Sludge \ Production$ $S_0 - S_F = Substrate \ removal \ (BOD \ reduction)$ (from Peavy, Rowe, and Tchobanoglous, 1985, p.231)

Growth of Heterotrophic Cultures

- Lag phase: acclimation to new substrate, could be short lived
- Log Growth: active reproduction by binary fission
- Stationary: Growth = Death
- Endogenous: Death > Growth
- In lag and log growth phases sufficient substrate is available
- In stationary and endogenous phases substrate is limited

$$\frac{X_F - X_0}{S_0 - S_e} = Y = biomass \ yield = \frac{mg \ MLSS \ produced}{mg \ BOD \ or \ COD \ removed}$$

Secondary Treatment Models

- Models for secondary treatment are developed around:
 - BOD (substrate) reduction
 - Sludge (biomass) production
 - Retention time (activated sludge only)
- Log Growth Phase:

 $\frac{dX}{dt} = Y \frac{dS}{dt} \qquad where \ Y = yield \ coefficient$ $\frac{dS}{dt} = substrate \ removal \ rate$

$$\frac{dX}{dt} = biomass growth rate$$

Secondary Treatment Models

Endogenous Phase (starvation/death phase):

$$\frac{dX}{dt} = -k_d X \qquad \text{where } k_d = \text{decay coefficient}$$

• Net Growth:

$$\frac{dX}{dt} = Y \frac{dS}{dt} - k_d X \qquad where \ Y = yield \ coefficient$$
$$\frac{dS}{dt} = substrate \ utilization \ rate$$
$$\frac{dX}{dt} = biomass \ growth \ rate$$

Secondary Treatment Models

Specific Growth Rate & Specific Substrate Utilization Rate

$$\frac{dX}{dt} = Y \frac{dS}{dt} - k_d X$$

$$\frac{dX / dt}{X} = Y \frac{dS / dt}{X} - k_d$$

$$\frac{dX / dt}{X} = \frac{1}{\theta_c} \quad \text{where } Y = \text{yield coefficien } t$$

$$\frac{dS}{dt} = \text{substrate utilization rate}$$

$$\frac{dX}{dt} = \text{biomass growth rate}$$

$$\theta_c = \text{sludge age}$$

Sludge Age

- Sludge age is the length of time (days) the sludge (bacteria) is retained within the secondary treatment process.
 - Activated sludge: 10 days $Y_{net} = 0.4 0.6$
 - Trickling filter: 100 days $Y_{net} = 0.1 0.3$ $Y_{net} = \frac{lb \ sludge \ produced}{lb \ BOD \ removed}$
- Trickling filters also produce a more dense (thicker) sludge:
 - -TF = 1.5% solids
 - -AS=0.8% solids

Quantify in Engineering Design Terms

$$\frac{1}{\theta_c} = Y \frac{dS / dt}{X} - k_d \qquad (1)$$

$$dS = (S_0 - S_e) \qquad (2)$$

$$dt = \frac{V}{Q} \qquad (3)$$

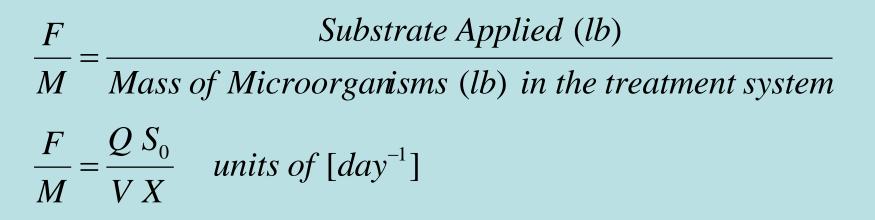
$$Combine \quad Equation \qquad (1), \quad (2), \quad and \quad (3)$$

$$\frac{1}{\theta_c} = Y \frac{(S_0 - S_e)Q}{XV} - k_d$$

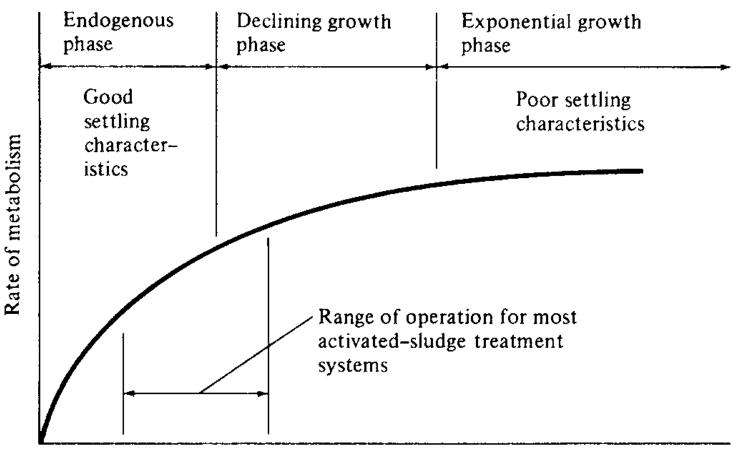
Design Equation: Identify, define (units), and describe the "design parameters" vs "typical known" conditions. Which parameter(s) does the design engineer control?

$$\frac{1}{\theta_c} = Y \frac{(S_0 - S_e)Q}{XV} - k_d$$

Food:Microorganism (F/M) Ratio



- As F/M changes, the phase of growth shifts:
 - High F/M, log growth phase, more sludge
 - Low F/M, endogenous growth phase, less sludge
 - Trickling filter is a low F/M process (less sludge).
 - Activated sludge is a higher F/M process (compared to trickling filter, more sludge)



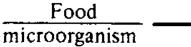


Figure 12.9 Rate of metabolism versus increasing food/ microorganism ratio.

(From Viessman, Jr. and Hammer, 1998, p. 529)

References

- Peavy, Howard S., Rowe, Donald R., and Tchobanoglous, George. (1985).
 Environmental Engineering. New York.
 McGraw-Hill.
- Viessman Jr., Warren and Hammer, Mark J. (1998) Water Supply and Pollution Control. Menlo Park. Addison Wesley Longman.