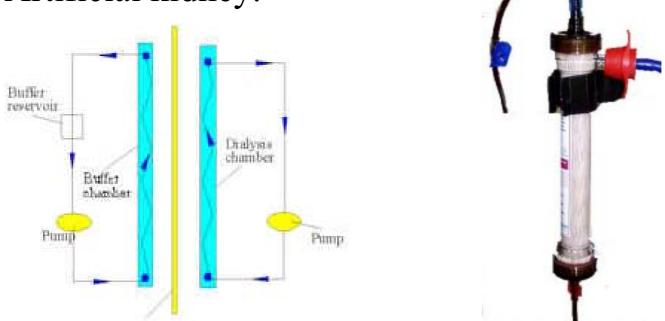
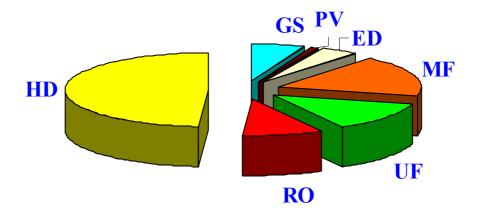
- Dialysis
- Applied since the 70's.
- Low industrial interest.
- Ions & species of low MW (~<100 Da).
- Ionic Membranes (just like ED).
- Driving Force: concentration gradient.
- Slow and low selective.

- Dialysis
- Artificial kidney.



NaOH recovery in textile effluents, alcohol removal from beer, salts removal (pharmaceutical industry).

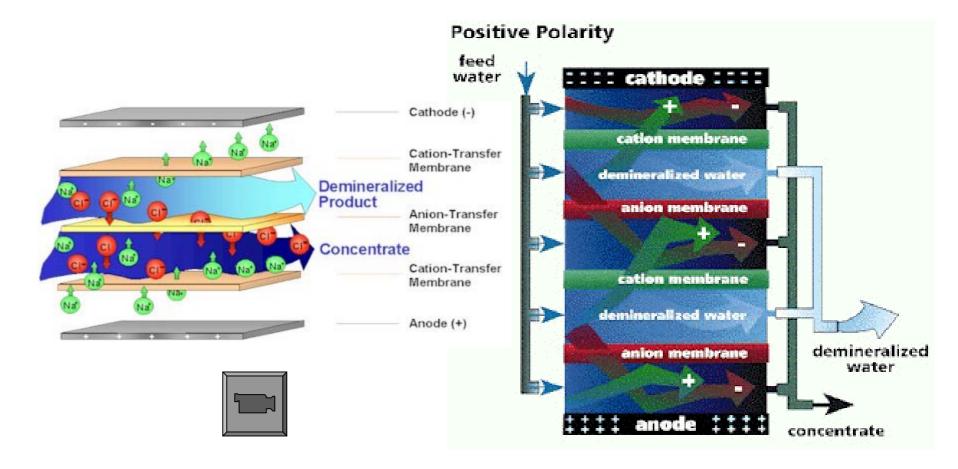
- Dialysis
- Looks not very important...?.

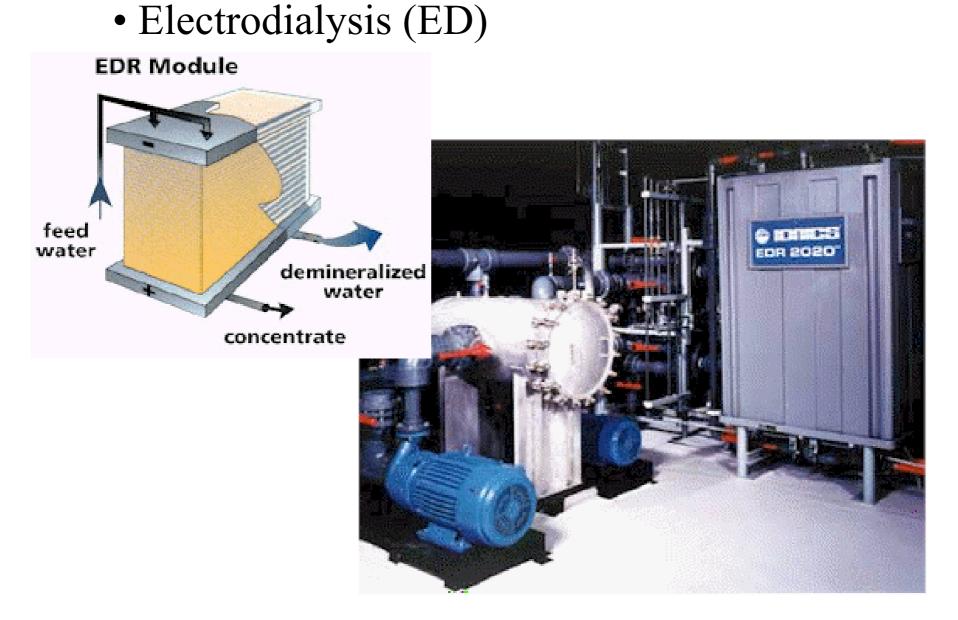


Membrane and module markets

- Electrodialysis (ED)
- First applications back at 30's.
- Ion Separations.
- Ionic Membranes (non porous).
- Driving Force: gradient in electrical potential.
- Potential: 1-2 V.
- Flat configuration.
- Hundreds of anionic and cationic membranes placed alternatively.
- Orthogonal electrical field.

• Electrodialysis (ED)

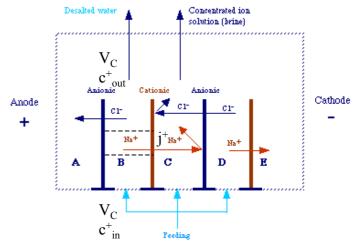




- Electrodialysis (ED)
- Ionic Membranes (non porous).
- Based on polystyrene or polypropylene with sulfonic and quaternary amine groups.
- Thickness: 0.15-0.6 mm.
- ED with reverse polarization (EDR).
- ED at high temperature (60°C).
- ED with electrolysis.

- Electrodialysis (ED)
- Required membrane area
 - Mass balance (in equivalents) $j^{+} \cdot dA_{m}^{+} + V_{C} \cdot z \cdot dc^{+} = 0$
 - Charge flow

 $\frac{\mathbf{j}^+ \cdot \mathbf{F}}{\mathbf{F}} = \mathbf{i}$



```
i: electric current density (A/m<sup>2</sup>)
A<sub>m</sub>: membrane surface (m<sup>2</sup>)
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combining

$$A_{T} = N \cdot A_{m} = \frac{N \cdot V_{C} \cdot (c_{in}^{+} - c_{out}^{+}) \cdot z \cdot F}{\eta \cdot i} = \frac{V \cdot (c_{in}^{+} - c_{out}^{+}) \cdot z \cdot F}{\eta \cdot i}$$

 η : global electrical efficiency (~0.5 commercial equipment) j: cation flow (eq/m² s)

F: Faraday constant (96500 C/eq) N: number cells in the equipment z: cation charge (eq/mol)

- Electrodialysis (ED)
- Then the required energy, E (J), is

 $E = N \cdot U_C \cdot I \cdot t = N \cdot I^2 \cdot R_C \cdot t \qquad U_C: \text{ potential gradient in a cell (V)} \\ R_C: \text{ total resistance in a cell (}\Omega)$

as

$$I = i \cdot A_m = \frac{V_C \cdot (c_{in}^+ - c_{out}^+) \cdot z \cdot F}{\eta}$$

then

$$E = N \cdot \left(\frac{V_C \cdot \Delta c \cdot z \cdot F}{\eta}\right)^2 \cdot R_C \cdot t$$

$$\delta \quad P = N \cdot \left(\frac{V_C \cdot \Delta c \cdot z \cdot F}{\eta}\right)^2 \cdot R_C$$

P: required Power (J/s)

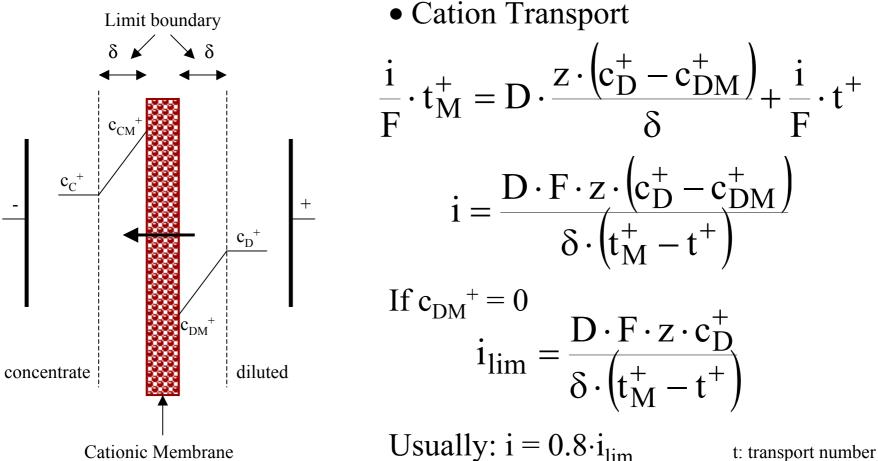
• Electrodialysis (ED)

Where, the required specific energy, (J/m^3) , is

$$\hat{\mathbf{E}} = \frac{\mathbf{E}}{\mathbf{N} \cdot \mathbf{V}_{\mathbf{C}} \cdot \mathbf{t}} = \mathbf{V}_{\mathbf{C}} \cdot \left(\frac{\Delta \mathbf{c} \cdot \mathbf{z} \cdot \mathbf{F}}{\eta}\right)^2 \cdot \mathbf{R}_{\mathbf{C}}$$

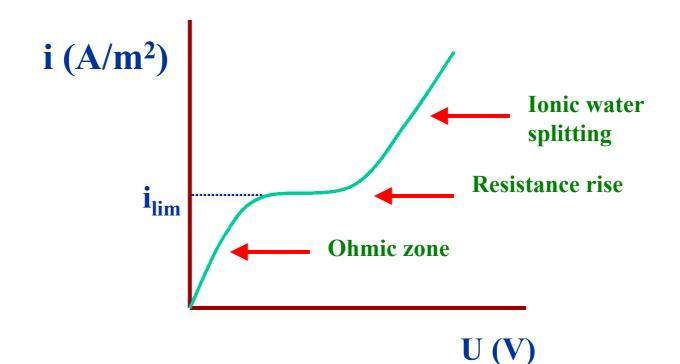
La cell resistance can be estimated from a model based on series of resistances where the resistances to transport are considered through two membranes and the compartments concentrate and diluted.

- Electrodialysis (ED)
- How to determine operational *i*?



D: diffusion coefficient

- Electrodialysis (ED)
- Intensity Evolution versus applied potential



- Electrodialysis (ED)
- Fields of application: Water desalination.
- Competing to RO.
- Economically more interesting at very high or very salt concentrations.
- Other fields of application: Food Industry. Treatment of heavy metal polluted water.

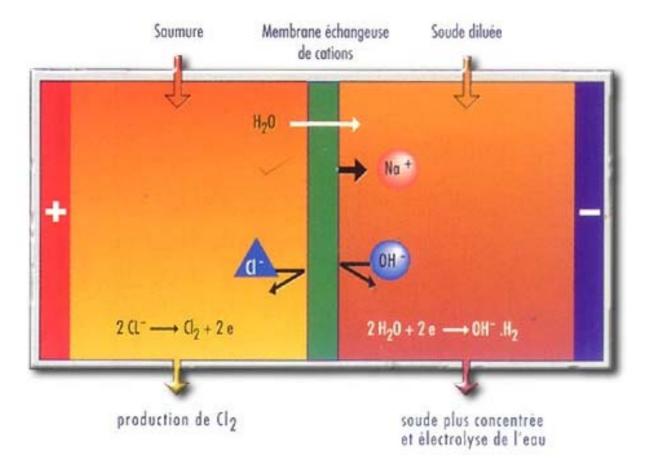
- Electrodialysis (ED)
- Examples:

 $\sqrt{\text{Production of drinking water from salty water.}}$

- $\sqrt{\text{Water softening.}}$
- $\sqrt{\text{Nitrate removal.}}$
- $\sqrt{}$ Lactose demineralization.
- $\sqrt{\text{Acid removal in fruit juice.}}$
- $\sqrt{1}$ Tartrate removal from wines.
- $\sqrt{\text{Heavy metal recovery.}}$

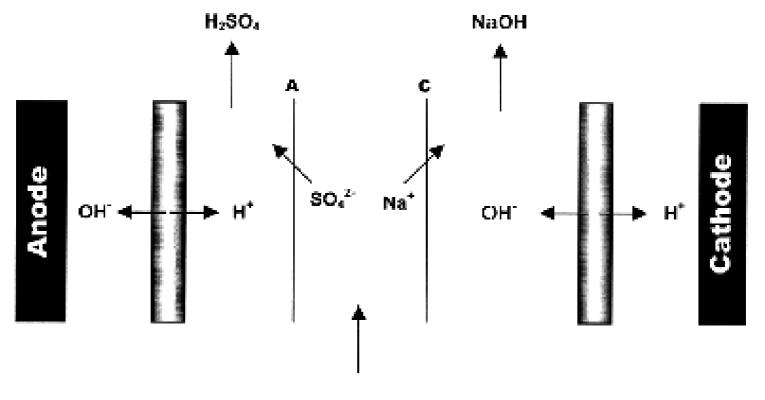
 $\sqrt{\text{Production of chlorine and sodium hydroxide.}}$

• Electrodialysis (ED)



electrolytic Cell for the production of chlorine and sodium hydroxide with cationic membrane.

• Electrodialysis (ED)



 Na_2SO_4

Electrolytic cell for the production of sulfuric acid and sodium hydroxide with bipolar membrane.

